Mail Application To:

New Mexico Environment Department Air Quality Bureau Permits Section 525 Camino de los Marquez, Suite 1 Santa Fe, New Mexico, 87505

Phone: (505) 476-4300 Fax: (505) 476-4375 www.env.nm.gov/aqb



For Department use only:

AIRS No.:

Universal Air Quality Permit Application

Use this application for NOI, NSR, or Title V sources.

Use this application for: the initial application, modifications, technical revisions, and renewals. For technical revisions, complete Sections, 1-A, 1-B, 2-E, 3, 9 and any other sections that are relevant to the requested action; coordination with the Air Quality Bureau permit staff prior to submittal is encouraged to clarify submittal requirements and to determine if more or less than these sections of the application are needed. Use this application for streamline permits as well. See Section 1-I for submittal instructions for other permits.

This application is submitted as (cl	theck all that apply):	☐ Request for a No Permit Rec	uired Determination (no fee)
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■ Updating an application currently under NMED review. Include this page and all pages that are being updated (no fee require
Construction Status: \square Not Constructed \square Existing Permitted (or NOI) Facility \square Existing Non-permitted (or NOI) Facility
Minor Source: ☐ a NOI 20.2.73 NMAC ☐ 20.2.72 NMAC application or revision ☐ 20.2.72.300 NMAC Streamline application
$ Title \ V \ Source: \ \Box \ Title \ V \ (new) \ \Box \ Title \ V \ renewal \ \Box \ TV \ minor \ mod. \ \Box \ TV \ significant \ mod. \ TV \ Acid \ Rain: \ \Box \ New \ \Box \ Renewal \ Renewal \ TV \ Acid \ Rain: \ \Box \ New \ \Box \ Renewal \ Renewal \ TV \ Acid \ Rain: \ Description \ Renewal \ Renew$
PSD Major Source: ☐ PSD major source (new) ☐ minor modification to a PSD source ■ a PSD major modification

Acknowledgements:

- I acknowledge that a pre-application meeting is available to me upon request.
 ☐ Title V Operating, Title IV Acid Rain, and NPR applications have no fees.
- \square \$500 NSR application Filing Fee enclosed OR \square The full permit fee associated with 10 fee points (required w/ streamline applications).
- Check No.: 1000397453 in the amount of 500.00 USD.
- I acknowledge the required submittal format for the hard copy application is printed double sided 'head-to-toe', 2-hole punched (except the Sect. 2 landscape tables is printed 'head-to-head'), numbered tab separators. Incl. a copy of the check on a separate page. □ This facility qualifies to receive assistance from the Small Business Environmental Assistance program (SBEAP) and qualifies for 50% of the normal application and permit fees. Enclosed is a check for 50% of the normal application fee which will be verified with the Small Business Certification Form for your company.
- \Box This facility qualifies to receive assistance from the Small Business Environmental Assistance Program (SBEAP) but does not qualify for 50% of the normal application and permit fees. To see if you qualify for SBEAP assistance and for the small business certification form go to https://www.env.nm.gov/aqb/sbap/small_business_criteria.html).

Citation: Please provide the **low level citation** under which this application is being submitted: **20.2.72.219.D NMAC** (e.g. application for a new minor source would be 20.2.72.200.A NMAC, one example for a Technical Permit Revision is 20.2.72.219.B.1.b NMAC, a Title V acid rain application would be: 20.2.70.200.C NMAC)

Section 1 - Facility Information

Sec	tion 1-A: Company Information	to 5 #s of permit IDEA ID No.): 198	Permit/NOI #: PSD-NM-0195-M39R4			
1	Facility Name: Artesia Refinery	Plant primary SIC Code (4 digits): 2911				
1	Thresia termery	Plant NAIC code (6 digits): 324110				
a	Facility Street Address (If no facility street address, provide directions 501 E. Main St., Artesia, NM 88210	from a prominent landmark)	:			
2	Plant Operator Company Name: HollyFrontier Navajo Refining LLC	Phone/Fax: (575) 748-331	1			
a	Plant Operator Address: P.O. Box 159, Artesia, NM 88211-0159					

b	Plant Operator's New Mexico Corporate ID or Tax ID: Tax ID is CRS # 02-488869-00-9								
3	Plant Owner(s) name(s): HollyFrontier Navajo Refining LLC	Phone/Fax: (575) 748-3311							
a	Plant Owner(s) Mailing Address(s): P.O. Box 159, Artesia, NM 88211-0159								
4	Bill To (Company): HollyFrontier Navajo Refining LLC Phone/Fax: (575) 746-5487 / (575) 746-								
a	Mailing Address: P.O. Box 159, Artesia, NM 88211-0159	E-mail: Alena.miro@hollyfrontier.com							
5	□ Preparer: ■ Consultant: RTP Environmental Associates, Inc.	Phone/Fax: (919) 845-1422							
a	Mailing Address: 304-A West Millbrook Road, Raleigh, NC 27609	E-mail: campbell@rtpenv.com							
6	Plant Operator Contact: Alena Miro	Phone/Fax: (713) 865-6825							
a	Address: P.O. Box 159, Artesia, NM 88211-0159	E-mail: Alena.miro@hollyfrontier.com							
7	Air Permit Contact: Alena Miro	Title: Senior Environmental Engineer							
a	E-mail: Alena.Miro@HollyFrontier.com	Phone/Fax: (713) 865-6825							
b	Mailing Address: P.O. Box 159, Artesia, NM 88211-0159								
c	The designated Air permit Contact will receive all official corresponden	nce (i.e. letters, permits) from the Air Quality Bureau.							

Section 1-B: Current Facility Status

	tion 1-B. Current racinty Status						
1.a	Has this facility already been constructed? ■ Yes □ No	1.b If yes to question 1.a, is it currently operating in New Mexico? ■ Yes □ No					
2	If yes to question 1.a, was the existing facility subject to a Notice of Intent (NOI) (20.2.73 NMAC) before submittal of this application?	If yes to question 1.a, was the existing facility subject to a construction permit (20.2.72 NMAC) before submittal of this application? ☐ Yes ☐ No					
3	☐ Yes ■ No	If yes, give month and year of shut down (MM/YY):					
	Is the facility currently shut down? ☐ Yes ■ No	If yes, give month and year of shut down (with 11).					
4	Was this facility constructed before 8/31/1972 and continuously operat	ed since 1972? ■ Yes □ No					
5	If Yes to question 3, has this facility been modified (see 20.2.72.7.P NMAC) or the capacity increased since 8/31/1972? □Yes □No □N/A						
6	Does this facility have a Title V operating permit (20.2.70 NMAC)? ■ Yes □ No	If yes, the permit No. is: P-051R3					
7	Has this facility been issued a No Permit Required (NPR)? ☐ Yes ■ No	If yes, the NPR No. is:					
8	Has this facility been issued a Notice of Intent (NOI)? ☐ Yes ■ No	If yes, the NOI No. is:					
9	Does this facility have a construction permit (20.2.72/20.2.74 NMAC)? ■ Yes □ No	If yes, the permit No. is: PSD-NM-0195-M39R4					
10	Is this facility registered under a General permit (GCP-1, GCP-2, etc.)? ☐ Yes ■ No	If yes, the register No. is:					

Section 1-C: Facility Input Capacity & Production Rate

1	What is the facility's maximum input capacity, specify units (reference here and list capacities in Section 20, if more room is required)								
a	Current	Hourly: N/A	Annually: N/A						
b	Proposed	Hourly: N/A	Daily: N/A	Annually: N/A					
2	What is the facility's maximum production rate, specify units (reference here and list capacities in Section 20, if more room is required)								
a	Current	Hourly: N/A	Daily: N/A	Annually: N/A					
b	Proposed	Hourly: N/A	Daily: N/A	Annually: N/A					

Section 1-D: Facility Location Information

1	Section: 9	Range: 26E	Township: 17S	County: E	Eddy		Elevation (ft): 3,365			
2	UTM Zone: □ 12 or ■ 13				■ NAD 27	□ NAD 8	33 □ WGS 84			
a	UTM E (in meter	s, to nearest 10 meter	s): 557,020	UTM N (i	n meters, to neares	t 10 meters):	3,634,010			
b	AND Latitude ((deg., min., sec.):	32°50'33.6"	Longitude	e (deg., min., se	c.): 104°23	'26.5"			
3	Name and zip c	ode of nearest Ne	ew Mexico town: Artesia 8	8210						
4	Detailed Driving Instructions from nearest NM town (attach a road map if necessary): Refinery is within Artesia city limits									
5	The facility is 0 miles East of Artesia.									
6		• `	<u> </u>				est Service Other (specify)			
7							B.2 NMAC) of the property y, Artesia			
8	on which the facility is proposed to be constructed or operated: Eddy County, Chaves County, Artesia 20.2.72 NMAC applications only: Will the property on which the facility is proposed to be constructed or operated be closer than 50 km (31 miles) to other states, Bernalillo County, or a Class I area (see www.env.nm.gov/aqb/modeling/class1areas.html)? Yes No (20.2.72.206.A.7 NMAC) If yes, list all with corresponding distances in kilometers:									
9	Name nearest C	Class I area: Carls	bad Caverns National Park							
10	Shortest distance	ce (in km) from fa	acility boundary to the bour	ndary of the	nearest Class I	area (to the	nearest 10 meters): 71 km			
11			neter of the Area of Operati den removal areas) to neare							
12	lands, including mining overburden removal areas) to nearest residence, school or occupied structure: 12 m Method(s) used to delineate the Restricted Area: Fencing, walls, and gates "Restricted Area" is an area to which public entry is effectively precluded. Effective barriers include continuous fencing, continuous walls, or other continuous barriers approved by the Department, such as rugged physical terrain with steep grade that would require special equipment to traverse. If a large property is completely enclosed by fencing, a restricted area within the property may be identified with signage only. Public roads cannot be part of a Restricted Area.									
13	Does the owner ☐ Yes ■ No A portable stati	c/operator intend to onary source is n	to operate this source as a poor of a mobile source, such as	oortable stat an automol	ionary source a	s defined in				
14	Will this facility	y operate in conju	unction with other air regulant number (if known) of the	ated parties	on the same pr		■ No ☐ Yes			

Section 1-E: Proposed Operating Schedule (The 1-E.1 & 1-E.2 operating schedules may become conditions in the permit.)

1	Facility maximum operating $(\frac{\text{hours}}{\text{day}})$: 24	(days /week): 7	$(\frac{\text{weeks}}{\text{year}}): 52$	$(\frac{\text{hours}}{\text{year}}): 8,760$				
2	Facility's maximum daily operating schedule (if less	□AM □PM	End:	□AM □PM				
3	Month and year of anticipated start of construction: N/A							
4	Month and year of anticipated construction completion: N/A							
5	Month and year of anticipated startup of new or modified facility: N/A							
6	Will this facility operate at this site for more than or	ne year? ■ Yes □ No						

Section 1-F: Other Facility Information

1	Are there any current Notice of Violations (NOV), complia to this facility? ■ Yes □ No If yes, specify:	nce orders, or any oth	ner compliance or enforcement issues related
a	If yes, NOV date or description of issue: May 1, 2020 (EPA	A Region 6 NOV)	NOV Tracking No:
b	Is this application in response to any issue listed in 1-F, 1 o	r 1a above? □ Yes ▮	No If Yes, provide the 1c & 1d info below:
с	Document Title: N/A	Date:	Requirement # (or page # and paragraph #):
d	Provide the required text to be inserted in this permit: N/A		
2	Is air quality dispersion modeling or modeling waiver being	g submitted with this	application? □ Yes ■ No
3	Does this facility require an "Air Toxics" permit under 20.2	2.72.400 NMAC & 20	0.2.72.502, Tables A and/or B? ■ Yes □ No
4	Will this facility be a source of federal Hazardous Air Pollu	itants (HAP)? Yes	s □ No
a	If Yes, what type of source? Major ($\square \ge 10$ tpy of an OR \square Minor ($\square < 10$ tpy of any		_ :: .
5	Is any unit exempt under 20.2.72.202.B.3 NMAC? • Ye	s □ No	
a	If yes, include the name of company providing commercial Commercial power is purchased from a commercial utility site for the sole purpose of the user.	-	-

Section 1-G: Streamline Application (This section applies to 20.2.72.300 NMAC Streamline applications only)

☐ I have filled out Section 18, "Addendum for Streamline Applications." ■ N/A (This is not a Streamline application.)

Section 1-H: Current Title V Information - Required for all applications from TV Sources (Title V-source required information for all applications submitted pursuant to 20.2.72 NMAC (Minor Construction Permits), or

20.2.74	4/20.2.79 NMAC (Major PSD/NNSR applications), and/or 20.2.70 NMA	C (Title V))	,,						
1	Responsible Official (R.O.) Parrish R. Miller (20.2.70.300.D.2 NMAC):	Phone: (575) 748-3311							
a	R.O. Title: Vice President and Refinery Manager	sh.miller@hollyfrontier.com							
b	R. O. Address: P.O. Box 159, Artesia, NM 88211-0159								
2	Alternate Responsible Official (20.2.70.300.D.2 NMAC):		Phone:						
a	A. R.O. Title:	A. R.O. e-mail:							
b	A. R. O. Address:								
3	Company's Corporate or Partnership Relationship to any other Air Quality Permittee (List the names of any companies that have operating (20.2.70 NMAC) permits and with whom the applicant for this permit has a corporate or partnership relationship): HollyFrontier Navajo Refining LLC								
4	Name of Parent Company ("Parent Company" means the primary repermitted wholly or in part.): HollyFrontier Corporation	name of the organiza	ation that owns the company to be						
a	Address of Parent Company: 2828 N. Harwood, Suite 1300, Dallas, TX 75201								
5	Names of Subsidiary Companies ("Subsidiary Companies" means owned, wholly or in part, by the company to be permitted.): Holly	•	hes, divisions or subsidiaries, which are						
6	Telephone numbers & names of the owners' agents and site contac Kawika Tupou (575) 746-5487	ts familiar with plan	at operations:						
7	Affected Programs to include Other States, local air pollution control Will the property on which the facility is proposed to be constructed states, local pollution control programs, and Indian tribes and puebones and provide the distances in kilometers: Carlsbad Caverns National Park – 71 km, Salt Creek Wilderness A	d or operated be clo los (20.2.70.402.A.2	ser than 80 km (50 miles) from other						

Section 1-I – Submittal Requirements

Each 20.2.73 NMAC (**NOI**), a 20.2.70 NMAC (**Title V**), a 20.2.72 NMAC (**NSR** minor source), or 20.2.74 NMAC (**PSD**) application package shall consist of the following:

Hard Copy Submittal Requirements:

- 1) One hard copy original signed and notarized application package printed double sided 'head-to-toe' 2-hole punched as we bind the document on top, not on the side; except Section 2 (landscape tables), which should be head-to-head. Please use numbered tab separators in the hard copy submittal(s) as this facilitates the review process. For NOI submittals only, hard copies of UA1, Tables 2A, 2D & 2F, Section 3 and the signed Certification Page are required. Please include a copy of the check on a separate page.
- 2) If the application is for a minor NSR, PSD, NNSR, or Title V application, include one working hard **copy** for Department use. This <u>copy</u> should be printed in book form, 3-hole punched, and <u>must be double sided</u>. Note that this is in addition to the head-to-to 2-hole punched copy required in 1) above. Minor NSR Technical Permit revisions (20.2.72.219.B NMAC) only need to fill out Sections 1-A, 1-B, 3, and should fill out those portions of other Section(s) relevant to the technical permit revision. TV Minor Modifications need only fill out Sections 1-A, 1-B, 1-H, 3, and those portions of other Section(s) relevant to the minor modification. NMED may require additional portions of the application to be submitted, as needed.
- 3) The entire NOI or Permit application package, including the full modeling study, should be submitted electronically. Electronic files for applications for NOIs, any type of General Construction Permit (GCP), or technical revisions to NSRs must be submitted with compact disk (CD) or digital versatile disc (DVD). For these permit application submittals, two CD copies are required (in sleeves, not crystal cases, please), with additional CD copies as specified below. NOI applications require only a single CD submittal. Electronic files for other New Source Review (construction) permits/permit modifications or Title V permits/permit modifications can be submitted on CD/DVD or sent through AQB's secure file transfer service.

Electronic files sent by (check one):

☐ CD/DVD attached to paper application

secure electronic transfer. Air Permit Contact Name

James Nellessen

Air Quality Bureau - Air Permit Specialist, Advanced - Major Source Permits Section

New Mexico Environment Department

525 Camino de los Marquez, Suite 1, Santa Fe NM, 87505-1816

Phone number: 505-476-4300|Fx 505476-4375|direct # 476-4347

Email Joseph.kimbrell@state.nm.us

a. If the file transfer service is chosen by the applicant, after receipt of the application, the Bureau will email the applicant with instructions for submitting the electronic files through a secure file transfer service. Submission of the electronic files through the file transfer service needs to be completed within 3 business days after the invitation is received, so the applicant should ensure that the files are ready when sending the hard copy of the application. The applicant will not need a password to complete the transfer. **Do not use the file transfer service for NOIs, any type of GCP, or technical revisions to NSR permits.**

- 4) Optionally, the applicant may submit the files with the application on compact disk (CD) or digital versatile disc (DVD) following the instructions above and the instructions in 5 for applications subject to PSD review.
- 5) If **air dispersion modeling** is required by the application type, include the **NMED Modeling Waiver** and/or electronic air dispersion modeling report, input, and output files. The dispersion modeling <u>summary report only</u> should be submitted as hard copy(ies) unless otherwise indicated by the Bureau.
- 6) If the applicant submits the electronic files on CD and the application is subject to PSD review under 20.2.74 NMAC (PSD) or NNSR under 20.2.79 NMC include,
 - a. one additional CD copy for US EPA,
 - b. one additional CD copy for each federal land manager affected (NPS, USFS, FWS, USDI) and,
 - c. one additional CD copy for each affected regulatory agency other than the Air Quality Bureau.

If the application is submitted electronically through the secure file transfer service, these extra CDs do not need to be submitted.

Electronic Submittal Requirements [in addition to the required hard copy(ies)]:

- 1) All required electronic documents shall be submitted as 2 separate CDs or submitted through the AQB secure file transfer service. Submit a single PDF document of the entire application as submitted and the individual documents comprising the application.
- 2) The documents should also be submitted in Microsoft Office compatible file format (Word, Excel, etc.) allowing us to access the text and formulas in the documents (copy & paste). Any documents that cannot be submitted in a Microsoft Office compatible format shall be saved as a PDF file from within the electronic document that created the file. If you are unable to provide Microsoft office compatible electronic files or internally generated PDF files of files (items that were not created electronically: i.e. brochures, maps, graphics, etc.), submit these items in hard copy format. We must be able to review the formulas and inputs that calculated the emissions.
- 3) It is preferred that this application form be submitted as 4 electronic files (3 MSWord docs: Universal Application section 1 [UA1], Universal Application section 3-19 [UA3], and Universal Application 4, the modeling report [UA4]) and 1 Excel file of the tables (Universal Application section 2 [UA2]). Please include as many of the 3-19 Sections as practical in a single MS Word electronic document. Create separate electronic file(s) if a single file becomes too large or if portions must be saved in a file format other than MS Word.
- 4) The electronic file names shall be a maximum of 25 characters long (including spaces, if any). The format of the electronic Universal Application shall be in the format: "A-3423-FacilityName". The "A" distinguishes the file as an application submittal, as opposed to other documents the Department itself puts into the database. Thus, all electronic application submittals should begin with "A-". Modifications to existing facilities should use the core permit number (i.e. '3423') the Department assigned to the facility as the next 4 digits. Use 'XXXX' for new facility applications. The format of any separate electronic submittals (additional submittals such as non-Word attachments, re-submittals, application updates) and Section document shall be in the format: "A-3423-9-description", where "9" stands for the section # (in this case Section 9-Public Notice). Please refrain, as much as possible, from submitting any scanned documents as this file format is extremely large, which uses up too much storage capacity in our database. Please take the time to fill out the header information throughout all submittals as this will identify any loose pages, including the Application Date (date submitted) & Revision number (0 for original, 1, 2, etc.; which will help keep track of subsequent partial update(s) to the original submittal. Do not use special symbols (#, @, etc.) in file names. The footer information should not be modified by the applicant.

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Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

					Manufact-urer's	urer's Requested	Date of Manufacture ²	Controlled by Unit#	Source Classi-		RICE Ignition	p
Unit Number ¹	Source Description	Make	Model #	Serial #	Rated Capacity ³ (Specify Units)	Permitted Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack #	fication Code (SCC)	For Each Piece of Equipment, Check One		Replacing Unit No.
B-0007	D-:1 7	T- 44/I-b- 7:-1- b	I Indonesia		215 MMBtu/hr	215 MMBtu/hr		N/A	10200701	■ Existing (unchanged) □ To be Removed		
B-0007	Boiler 7	Todd/John Zink burners	Unknown		(LHV Basis)	(LHV Basis)	2001	B-0007	10200701	 □ New/Additional □ To Be Modified □ To be Replaced 		
D 0000	P.11.0	T 11/7 1 77 1 1	** 1		215 MMBtu/hr	215 MMBtu/hr		N/A	10200701	■ Existing (unchanged) □ To be Removed		
B-0008	Boiler 8	Todd/John Zink burners	Unknown		(LHV Basis)	(LHV Basis)	2003	B-0008	10200701	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
D 0000	P. 1. 0	D. 1. 0 W.	** 1		220 MMBtu/hr	220 MMBtu/hr		N/A	10200701	■ Existing (unchanged) □ To be Removed		
B-0009	Boiler 9	Babcock & Wilcox	Unknown		(LHV Basis)	(LHV Basis)	2012	B-0009	10200701	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
D 0010	D 1 10				10 MMBtu/hr	10 MMBtu/hr		N/A	10200701	☐ Existing (unchanged) ■ To be Removed		
B-0010	Boiler 10	-	-		(LHV Basis)	(LHV Basis)		B-0010	10200701	 □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced 		
77.0000	Unit 13 Naphtha Splitter	7 1	GGTW 121		44 MMBtu/hr	44 MMBtu/hr		N/A	20/0010/	■ Existing (unchanged) □ To be Removed		
H-0009	Reboiler	Zeeco burners	GSFW-12 burners		(LHV Basis)	(LHV Basis)	1970	H-0009	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
77.0011					38 MMBtu/hr	38 MMBtu/hr		N/A	20/0010/	■ Existing (unchanged) □ To be Removed		
H-0011	Unit 21 Vacuum Unit Heater	John Zink burners	HEVD-14		(LHV Basis)	(LHV Basis)	est. 1972	H-0011	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
77.0010	V. SAKITBOD I. II	~ ·	garw. o.t		32 MMBtu/hr	32 MMBtu/hr		N/A	20/0010/	■ Existing (unchanged) □ To be Removed		
H-0018	Unit 06 HDS Reboiler	Zeeco burners	GSFW-8 burners		(LHV Basis)	(LHV Basis)	est. 1976	H-0018	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
11 0010		Callidus Technologies,	CUBL-8W		54 MMBtu/hr	54 MMBtu/hr		N/A	20/0010/	■ Existing (unchanged) □ To be Removed		
H-0019	South Crude Charge Heater	LLC burners	burners		(LHV Basis)	(LHV Basis)	2005	H-0019	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
** ***	a 1 a 1 a	Callidus Technologies,	CUBL-12W		90 MMBtu/hr	90 MMBtu/hr		N/A	20/0010/	■ Existing (unchanged) □ To be Removed		
H-0020	South Crude Charge Heater	LLC burners	burners		(LHV Basis)	(LHV Basis)	est. 1972	H-0020	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
77.0000	77 1 01 77		pana 101		12.3 MMBtu/hr	12.3 MMBtu/hr		N/A	20/0010/	■ Existing (unchanged) □ To be Removed		
H-0028	Unit 21 Heater	John Zink burners	PSFG-12 burners		(LHV Basis)	(LHV Basis)	11/1/1993	H-0028	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
77.0020	TI SOCOL II		PSFG-16R		42 MMBtu/hr	42 MMBtu/hr		N/A	20/0010/	■ Existing (unchanged) □ To be Removed		
H-0030	Unit 06 Charge Heater	John Zink burners	burners		(LHV Basis)	(LHV Basis)	12/19/2001	H-0030	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
		- 4 4 4			42 MMBtu/hr	42 MMBtu/hr		N/A		■ Existing (unchanged) □ To be Removed		
H-0040	Unit 13 Charge Heater	John Zink burners	PSFG-16 burners		(LHV Basis)	(LHV Basis)	11/1/1997	H-0040	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
11 0202	H 105 Cl H		HEVD-Q-18		11 MMBtu/hr	11 MMBtu/hr		N/A	20/0010/	☐ Existing (unchanged) ■ To be Removed		
H-0303	Unit 05 Charge Heater	John Zink burners	burners		(LHV Basis)	(LHV Basis)	1982	H-0303	30600106	 □ New/Additional □ To Be Modified □ To be Replaced 		
11.0212	Unit 10 FCC Feed Heater	Inha Zinh hama	VVD 10 h		35 MMBtu/hr	35 MMBtu/hr		N/A	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
H-0312	Unit 10 FCC Feed Heater	John Zink burners	VYD-18 burners		(LHV Basis)	(LHV Basis)	1990	H-0312	30000100	□ New/Additional		
11 0252	Unit 70 CCR Reformer	Callidus Technologies,	CUBL-10W		63 MMBtu/hr	63 MMBtu/hr		N/A	20(0010(■ Existing (unchanged) □ To be Removed		
H-0352	Heaters (previously 70-H1)	LLC burners	burners		(LHV)	(LHV)	est. 1990	H-0352	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
11 0252	Unit 70 CCR Reformer	Callidus Technologies,	CUBL-10W		81 MMBtu/hr	81 MMBtu/hr		N/A	20600106	■ Existing (unchanged) □ To be Removed		
H-0353	Heaters (previously 70-H2)	LLC burners	burners		(LHV)	(LHV)	est. 1990	H-0353	30600106	□ New/Additional		
11.0254	Unit 70 CCR Reformer	Callidus Technologies,	CUBL-10W		56 MMBtu/hr	56 MMBtu/hr		N/A	20600106	■ Existing (unchanged) □ To be Removed		
H-0354	Heaters (previously 70-H3)	LLC burners	burners		(LHV)	(LHV)	est. 1990	H-0354	30600106	□ New/Additional		
11.0255	Unit 70 Stabilizer Reboiler	1.1 7:	TT.1-		28 MMBtu/hr	28 MMBtu/hr		N/A	20/0010/	■ Existing (unchanged) □ To be Removed		
H-0355	Heater (previously 70H-4)	John Zink burners	Unknown		(LHV Basis)	(LHV Basis)	8/28/1990	H-0355	30600106	 □ New/Additional □ To Be Modified □ To be Replaced 		
11.02.62	II. 4.70 CCD II.	Callidus Technologies,	CUBL-8W		40 MMBtu/hr	40 MMBtu/hr		N/A	20/0010/	■ Existing (unchanged) □ To be Removed		
H-0362	Unit 70 CCR Heater	LLC burners	burners		(LHV)	(LHV)	May-2006	H-0362	30600106	 □ New/Additional □ To Be Modified □ To be Replaced 		

					Manufact-urer's	Requested Permitted	Date of Manufacture ²	Controlled by Unit #	Source Classi-		RICE Ignition Type (CI, SI,	Replacing
Unit Number ¹	Source Description Make Model # Serial # Rated Capacity (Specify Units) Capacity (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack#	fication Code (SCC)	For Each Piece of Equipment, Check One		Unit No.					
H-0363	Unit 70 CCR Heater	Callidus Technologies,	CUBL-8W		50 MMBtu/hr	50 MMBtu/hr		N/A	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
	ome / o continue	LLC burners	burners		(LHV)	(LHV)	May-2006	H-0363	20000100	☐ To Be Modified ☐ To be Replaced		
H-0364	Unit 70 CCR Heater	Callidus Technologies, LLC burners	CUBL-6W burners		35 MMBtu/hr (LHV)	35 MMBtu/hr (LHV)	May-2006	N/A H-0364	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
H-0421	Unit 44 Charge Heater	John Zink burners	LNC-PC-18 burners		27 MMBtu/hr (LHV Basis)	27 MMBtu/hr (LHV Basis)	5/23/2001	N/A H-0421	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
H-0464	SRU Hot Oil Heater	Callidus Technologies, LLC burners	LE-CSG-4W burners		9.6 MMBtu/hr (LHV Basis)	9.6 MMBtu/hr (LHV Basis)	11/1/2003	N/A H-0464	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Unit 00 Deprenenizer	Callidus Technologies,	CUBL-12W		84 MMBtu/hr	84 MMBtu/hr	11/1/2003	N/A		■ Existing (unchanged) □ To be Removed		
H-0600	Unit 09 Depropanizer Reboiler Heater	LLC burners	burners		(LHV Basis)	(LHV Basis)	est. 1991	H-0600	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
		Callidus Technologies,	CUB-8P-CW		78 MMBtu/hr	78 MMBtu/hr		N/A		■ Existing (unchanged) □ To be Removed		
H-0601	Unit 33 Charge Heater	LLC burners	burners		(LHV Basis)	(LHV Basis)	2003	H-0601	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
			GLSF-14 Round		27 MMBtu/hr	27 MMBtu/hr		N/A		■ Existing (unchanged) □ To be Removed		
H-2421	Unit 45 Charge Heater	Zeeco, Inc. burners	Flame "Free Jet" burners		(LHV Basis)	(LHV Basis)	2006	H-2421	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Unit 25 ROSE® Unit No. 2	John Zink Company,	COOLstar-18		120 MMBtu/hr	120 MMBtu/hr		N/A		■ Existing (unchanged) □ To be Removed		
H-2501	Hot Oil Heater	LLC burners	burners		(LHV Basis)	(LHV Basis)	2009	H-2501	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
11 2/01	II. '4 26 PDI I P 4 II 4	TDD	TDD		39 MMBtu/hr	39 MMBtu/hr		N/A	20600106	☐ Existing (unchanged) ■ To be Removed		
H-2601	Unit 26 RDU Reactor Heater	TBD	TBD		(LHV Basis)	(LHV Basis)	2021	H-2601	30600106	 □ New/Additional □ To Be Modified □ To be Replaced 		
H-3101	SRU3 Hot Oil Heater	Callidus Technologies,	Unknown		11 MMBtu/hr	11 MMBtu/hr		N/A	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
11-5101	SKC5 Hot On Heater	LLC burners	Chriown		(LHV Basis)	(LHV Basis)	2009	H-3101	30000100	☐ To Be Modified ☐ To be Replaced		
H-3402	Unit 34 Hydrocracker	Callidus Technologies,	LE-CSG-12W		52 MMBtu/hr	52 MMBtu/hr		N/A	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
	Reboiler 1	LLC burners	burners		(LHV Basis)	(LHV Basis)	2009	H-3402	20000100	☐ To Be Modified ☐ To be Replaced		
H-3403	Unit 34 Hydrocracker	Callidus Technologies,	CUBL-10W		32 MMBtu/hr	32 MMBtu/hr		N/A	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
	Reactor Charge Heater	LLC burners	burners		(LHV Basis)	(LHV Basis)	2011	H-3403		☐ To Be Modified ☐ To be Replaced		
H-5401	Unit 54 HDS Reactor Heater	Tulsa Heaters Inc.	TBD		19 MMBtu/hr	19 MMBtu/hr		N/A	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
					(LHV Basis)	(LHV Basis)	2016	H-5401		☐ To Be Modified ☐ To be Replaced		
H-8801	Unit 63 Hydrogen Plant Reformer Furnaces	Callidus Technologies, LLC burners	LE-CSG-12W- PSA burners		76 MMBtu/hr (LHV Basis)	76 MMBtu/hr (LHV Basis)	- / / /	N/A	30600106	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
					<u> </u>		3/1/2006	H-8801		☐ To Be Modified ☐ To be Replaced ■ Existing (unchanged) ☐ To be Removed		
H-8802	Unit 63 Hydrogen Plant Reformer Furnaces	Callidus Technologies, LLC burners	LE-CSG-12W- PSA burners		76 MMBtu/hr (LHV Basis)	76 MMBtu/hr (LHV Basis)	3/1/2006	N/A H-8802	30600106	□ New/Additional □ Replacement Unit		
							3/1/2000	N/A		☐ To Be Modified ☐ To be Replaced ■ Existing (unchanged) ☐ To be Removed		
H-9851	Unit 64 Hydrogen Plant Reformer	Callidus Technologies, LLC burners	CUBL-3WDF burners		337 MMBtu/hr (LHV Basis)	337 MMBtu/hr (LHV Basis)	2009	H-9851	30600106	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
H-0473					35 MMBtu/hr	35 MMBtu/hr	2007	N/A		■ Existing (unchanged) □ To be Removed		
(SRU2 TGI)	SRU2 Tail Gas Incinerator				(LHV Basis)	(LHV Basis)	Dec-2001	H-0473 (SRU2 TGI)	30609904	 □ New/Additional □ To Be Modified □ To be Replaced 		
H-3103	SRU3 Tail Gas Incinerator	Callidus Technologies,			10.2 MMBtu/hr			N/A	30609904	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
(SRU3 TGI)	Sicos ran Gas menerator	LLC burners			(LHV Basis)	(LHV Basis)	5/11/2009	H-3103 (SRH3 TGI)	30007704	☐ To Be Modified ☐ To be Replaced		
FCC Regen	FCC Regenerator Scrubber	Exxon	IV		N/A	N/A		N/A	30600201	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
- 1 cc Rogon	2 S Tregenerator Seraster	Linon	-,			1.771	est. 1979	FCC Regen	50000201	☐ To Be Modified ☐ To be Replaced		
FL-400	North Plant Flare	N/A	N/A	N/A	N/A	N/A		N/A	30600904	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
							est. 1972	FL-400		☐ To Be Modified ☐ To be Replaced		

					Manufact-urer's	Requested Permitted	Date of Manufacture ²	Controlled by Unit#	Source Classi-		RICE Ignition Type (CI, SI,	Doub sine
Unit Number ¹	Source Description	Make	Model #	Serial#	Rated Capacity ³ (Specify Units)	Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack #	fication Code (SCC)	For Each Piece of Equipment, Check One	4SLB, 4SRB, 2SLB) ⁴	Replacing Unit No.
FI 401	Cd. Dlt El	NI/A	21/4	NT/A	NI/A	NI/A		N/A	20/00004	■ Existing (unchanged) □ To be Removed		
FL-401	South Plant Flare	N/A	N/A	N/A	N/A	N/A	est. 1972	FL-401	30600904	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		■ Existing (unchanged) □ To be Removed		
FL-402	FCC Flare	N/A	N/A	N/A	N/A	N/A	est. 1979	FL-402	30600904	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
						/-		N/A		■ Existing (unchanged) □ To be Removed		
FL-403	Alky Flare	N/A	N/A	N/A	N/A	N/A	est. 1991	FL-403	30600904	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		■ Existing (unchanged) ☐ To be Removed		
FL-404	GOHT Flare	N/A	N/A	N/A	N/A	N/A	2003	FL-404	30600904	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		☐ Existing (unchanged) ☐ To be Removed		
FL-HEP-PORT	FL-HEP Portable Flare	N/A	N/A	N/A	N/A	N/A		FL-HEP-PORT	30600904	■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
			080 8 3					N/A		■ Existing (unchanged) □ To be Removed		
MG-0001	Portable Air Compressor	Cummins	QSC 8.3, 44358719		280 HP	280 HP	2012	MG-0001	20200102	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced	CI	
			000.03				2012	N/A		■ Existing (unchanged) □ To be Removed		
MG-0002	Portable Air Compressor	Cummins	QSC 8.3, 46338720		280 HP	280 HP	2012	MG-0002	20200102	□ New/Additional □ Replacement Unit	CI	
							2012			□ To Be Modified □ To be Replaced ■ Existing (unchanged) □ To be Removed		
MG-0003	Portable Air Compressor	Doosan/Cummins	QSB 4.5, 489581UKACF68		138 HP	138 HP	2010	N/A	20200102	□ New/Additional □ Replacement Unit	CI	
			10750101212100				2019	MG-0003		☐ To Be Modified ☐ To be Replaced ☐ Existing (unchanged) ☐ To be Removed		
MG-0004	Portable Fire Water Pump Engine	Caterpillar	C18, WJH07870		700 HP	700 HP		N/A	20200102	■ New/Additional □ Replacement Unit	CI	
	Eligilic						Oct-2010	MG-0004		☐ To Be Modified ☐ To be Replaced		
SG-0100	UPS backup generator	Deutz	F4L912GEN/		52 HP	52 HP	1998	N/A	20200102	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	CI	
	(exempt*)		WDZXL05.7010				2002	SG-0100		☐ To Be Modified ☐ To be Replaced		
SG-0101	UPS backup generator	Deutz	F4L 1011 F/ EI97-		54 HP	54 HP	1999	N/A	20200102	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	CI	
	(exempt*)		68CA00-000-0053				<2006	SG-0101		☐ To Be Modified ☐ To be Replaced		
SG-0102	Server Backup Generator	John Deere	4045HFS80		99 HP	99 HP	2018	N/A	20200102	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	CI	
56 0102	(exempt*)	70.III. 2 00.10	10 10111 500		,, m	// 111		SG-0102	20200102	☐ To Be Modified ☐ To be Replaced		
FWG-0600	Fire Water Pump Engine	Clarke Diesel (John	JW6H-UFAD70/		376 HP	376 HP		N/A	20200102	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	CI	
1 11 3 0000	The water rump Engine	Deere)	RG6090L113548		370111	370111	Nov-2012	FWG-0600	20200102	☐ To Be Modified ☐ To be Replaced	Ci	
FWG-0601	Fire Water Pump Engine	Clarke Diesel (John	JW6H-UFAD70/		376 HP	376 HP		N/A	20200102	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	CI	
1 WG-0001	The water I ump Engine	Deere)	RG6090L113561		370111	3/0111	Nov-2012	FWG-0601	20200102	☐ To Be Modified ☐ To be Replaced	Ci	
FWG-0602	Fire Water Pump Engine	Clarke Diesel (John	JW6H-UFAD70/		376 HP	376 HP		N/A	20200102	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	CI	
F W G-0002	The water Fump Engine	Deere)	RG6090L113574		3/0 HF	3/0 HF	Nov-2012	FWG-0602	20200102	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced	CI	
FW15 0402	Fi 11. B	Clarke Diesel (John	JU6H-UFADX8/		205 110	205 110		N/A	20200102	■ Existing (unchanged) □ To be Removed	er.	
FWG-0603	Fire Water Pump Engine	Deere)	PE6068L228486		305 HP	305 HP	Apr-2013	FWG-0603	20200102	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced	CI	
D.C.			6090HF485/		100	100		N/A	2020222	☐ Existing (unchanged) ■ To be Removed		
E-8010	WWTP Emergency Engine	John Deere	RG6090L101484		400 HP	400 HP	Feb-2011	E-8010	20200102	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced	CI	
								N/A		■ Existing (unchanged) ☐ To be Removed		
Y-0001	TCC Cooling Tower				5,000 gpm	5,000 gpm		Y-0001	30600701	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	S. Alky Cooling Tower							N/A		■ Existing (unchanged) □ To be Removed		
Y-0002	(Marley Cooling Tower)				5,000 gpm	5,000 gpm		Y-0002	30600701	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		■ Existing (unchanged) □ To be Removed		
Y-0008	North Alky Cooling Tower				12,500 gpm	12,500 gpm		Y-0008	30600701	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								1-0000		10 be woulded 10 be keplaced	L	

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Unit Number ¹	Source Description	Make	Model #	Serial#	Rated Capacity ³ (Specify Units)	Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack#	fication Code (SCC)	For Each Piece of Equipment, Check One	4SLB, 4SRB, 2SLB) ⁴	Unit No.
V 0011	ECC % ND Cooling Town				20,000	20 000		N/A	20600701	■ Existing (unchanged) □ To be Removed		
Y-0011	FCC & NP Cooling Tower				30,000 gpm	30,000 gpm		Y-0011	30600701	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Hydrogen Plants Cooling							N/A		■ Existing (unchanged) □ To be Removed		
Y-0012	Tower				10,000 gpm	10,000 gpm		Y-0012	30600701	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Unit 07 Amine W-0745							N/A		■ Existing (unchanged) ☐ To be Removed		
CT TT-0006	Cooling Tower				3,000 gpm	3,000 gpm		CT TT-0006	30600701	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
Y-0026								N/A		☐ Existing (unchanged) ■ To be Removed		
(formerly Y-0014)	RDU Cooling Tower				2,500 gpm	2,500 gpm	2021	Y-0026	30600701	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							2021	N/A		☐ Existing (unchanged) ☐ To be Removed		
Collection Sump	WW System Collection Sump				1,200 gpm	1,200 gpm		Collection Sump	30600503	■ New/Additional □ Replacement Unit		
								D-8000/D-8001		□ To Be Modified □ To be Replaced □ Existing (unchanged) □ To be Removed		
T-0845	Weir Box (WW)				1,200 gpm	1,200 gpm		D-8000/D-8001	30600503	■ New/Additional □ Replacement Unit		
								D-8000/D-8001		□ To Be Modified □ To be Replaced □ Existing (unchanged) □ To be Removed		
T-0844	Stilling Well (WW)				1,200 gpm	1,200 gpm		D-8000/D-8001	30600503	■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Stormwater Lift Station							D-8000/D-8001		☐ Existing (unchanged) ☐ To be Removed		
T-0846	(SWLS)				1,200 gpm	1,200 gpm		D-8000/D-8001	30600503	■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Stormwater Surge Tank							N/A		☐ Existing (unchanged) ☐ To be Removed		
T-0830	(external floater)				109,660 bbl	109,660 bbl	1/1/2011	T-0830	40301150	□ New/Additional □ Replacement Unit ■ To Be Modified □ To be Replaced		
								D-829/D-830		☐ Existing (unchanged) ☐ To be Removed		
S-1/T-1	Barscreen & Junction Box				1,200 gpm	1,200 gpm		D-829/D-830	30600503	■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
1 DI 004/								D-829/D-830		■ Existing (unchanged) □ To be Removed		
API-894/ API-895	API Separators				1,200 gpm	1,200 gpm			30600503	□ New/Additional □ Replacement Unit		
1111035								D-829/D-830		☐ To Be Modified ☐ To be Replaced ☐ Existing (unchanged) ☐ To be Removed		
T-0829	SRO Reject Tank				30,5000 bbl	30,5000 bbl		N/A	30600503	□ New/Additional □ Replacement Unit		
							pre-1971	T-0829		■ To Be Modified □ To be Replaced		
T-801	Enhanced Biodgradation				1,200 gpm	1,200 gpm		N/A	30600503	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
	Tank						1987	T-801		☐ To Be Modified ☐ To be Replaced		
T-836	Enhanced Biodgradation				1,200 gpm	1,200 gpm		N/A	30600503	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
	Tank				-,= v 8r ···	-,= v	1998	T-836		☐ To Be Modified ☐ To be Replaced		
T-805	Flocculator				1,200 gpm	1,200 gpm		N/A	30600503	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1-803	riocculator				1,200 gpiii	1,200 gpiii		T-805	30000303	☐ To Be Modified ☐ To be Replaced		
DAET 004	DAFIL'S T 906				1 200	1 200		N/A	20/00502	■ Existing (unchanged) □ To be Removed		
DAF T-896	DAF Unit T-896				1,200 gpm	1,200 gpm		DAF T-896	30600503	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
B.F- ***	D.D				1.000	1.000		N/A	20/02-03	■ Existing (unchanged) □ To be Removed		
DAF T-806	DAF Unit T-806				1,200 gpm	1,200 gpm		DAF T-806	30600503	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		☐ Existing (unchanged) ☐ To be Removed		
T-897	DAF Surge Open Sump				1,200 gpm	1,200 gpm		T-897	30600503	■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		☐ Existing (unchanged) ☐ To be Removed		
D-810/811	Walnut Hull Filters				1,200 gpm	1,200 gpm		D-810/811	30600503	■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
										☐ Existing (unchanged) ☐ To be Removed		
D-808/809	Mechanical Filters				1,200 gpm	1,200 gpm		N/A	30600503	■ New/Additional □ Replacement Unit		
								D-808/809		☐ To Be Modified ☐ To be Replaced		

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Unit Number ¹	Source Description	Make	Model #	Serial#	Rated Capacity ³ (Specify Units)	Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack#	fication Code (SCC)	For Each Piece of Equipment, Check One	4SLB, 4SRB, 2SLB) ⁴	Unit No.
T 000	DAE Community of				1 200	1 200		N/A	20/00502	☐ Existing (unchanged) ☐ To be Removed		
T-809	DAF Surge Tank				1,200 gpm	1,200 gpm		T-809	30600503	■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Asphalt Truck Loading and							N/A		■ Existing (unchanged) □ To be Removed		
TLO-1	Off-Loading Rack				350 bbl/hr	350 bbl/hr		TLO-1	40400150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Asphalt Truck Loading Rack							N/A		■ Existing (unchanged) □ To be Removed		
TL-2	#2				300 bbl/hr	300 bbl/hr		TL-2	40400150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
TL-4	Fuels Truck Loading Rack				3,571 bbl/hr	3,571 bbl/hr		TL-4 VRU TL-4 VCU	40400150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
	5					- ,		TL-4		☐ To Be Modified ☐ To be Replaced		
	CBO/LCO Truck Loading							N/A		■ Existing (unchanged) □ To be Removed		
TL-7	Rack				681 bbl/hr	681 bbl/hr		TL-7	40400150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Railcar Loading and Off-							N/A		■ Existing (unchanged) □ To be Removed		
RLO-8	Loading Rack				1,500 bbl/hr	1,500 bbl/hr		RLO-8	40400150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	Bailean I and in a and Off							N/A		■ Existing (unchanged) □ To be Removed		
RLO-19	Railcar Loading and Off- Loading Rack				3,950 bbl/hr	3,950 bbl/hr		RLO-19	40400150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	A 1 1/P: 1 T 1 T 1							N/A		■ Existing (unchanged) □ To be Removed		
TLO-20	Asphalt/Pitch Truck Loading Rack				600 bbl/hr	600 bbl/hr		TLO-20	40400150	□ New/Additional □ Replacement Unit		
								N/A		☐ To Be Modified ☐ To be Replaced ☐ Existing (unchanged) ☐ To be Removed		
TRLO-9	Molten Sulfur Truck/Railcar Loading Rack				330 LTPD	330 LTPD			40400150	■ New/Additional □ Replacement Unit		
	Louding Turk							TRLO-9		☐ To Be Modified ☐ To be Replaced ■ Existing (unchanged) ☐ To be Removed		
FUG-02-SP CRUDE	South Division Crude Unit						2000	N/A	40388801	□ New/Additional □ Replacement Unit		
CRODE							2009	N/A		☐ To Be Modified ☐ To be Replaced		
FUG-05-KERO	Kerosene HDS Unit							N/A	40388801	☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit		
								N/A		☐ To Be Modified ☐ To be Replaced		
FUG-06-NHDU	Naphtha HDS Unit 06							N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
								N/A		☐ To Be Modified ☐ To be Replaced		
FUG-07-N	Amine Unit-Treating/Regen.							N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
AMINE	2							N/A		☐ To Be Modified ☐ To be Replaced		
FUG-07-SWS1	Sour Water Stripper							N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1000,000	Sour water stripper							N/A	10500001	☐ To Be Modified ☐ To be Replaced		
FUG-08-TRUCK	Loading Racks							N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
RK	Loading Nacks							N/A	10300001	☐ To Be Modified ☐ To be Replaced		
FUG 00 N ALVV	North Alkylation Unit (New-							N/A	A0380001	■ Existing (unchanged) □ To be Removed		
FUG-09-N ALKY	Inside battery limits)							N/A	40388801	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FLIG 10 PGG	EGG. /GVG							N/A	40200001	■ Existing (unchanged) □ To be Removed		
FUG-10-FCC	FCC w/CVS							N/A	40388801	 □ New/Additional □ To Be Modified □ To be Replaced 		
	v ti mavi i							N/A	4020006	■ Existing (unchanged) □ To be Removed		
FUG-13-NHDU	Naphtha HDS Unit 13							N/A	40388801	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-18-LSR	Merox/Merichem Treating							N/A		■ Existing (unchanged) □ To be Removed		
MEROX TRT	Units							N/A	40388801	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
	I	1			L	<u> </u>				,	1	L

Unit Number ¹	Source Description	Make	Model#	Serial#	Manufact-urer's Rated Capacity ³ (Specify Units)	Requested Permitted Capacity ³ (Specify Units)	Date of Manufacture ² Date of Construction/	Controlled by Unit # Emissions vented to Stack #	Source Classi- fication Code (SCC)	For Each Piece of Equipment, Check One	RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB) ⁴	Replacing Unit No.
FUG-19-							Reconstruction ²	N/A		☐ Existing (unchanged) ☐ To be Removed		
NAPHTHA	Naptha Merox							N/A	40388801	■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-20-ISOM	BenFree Unit							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-21-SP VACUUM	Flasher/Vacuum Unit							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-25-ROSE-2	ROSE Unit							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-26-RDU	Renewable Diesel Unit						2021	N/A N/A	40388801	□ Existing (unchanged) □ New/Additional □ To Be Modified □ To Be Replaced		
FUG-29- BLENDER/TK	Light Oil Tankage							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FARM FUG-30-	SRU2/SWS w/CVS							N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
SRU2/TGTU								N/A		☐ To Be Modified ☐ To be Replaced		
FUG-31- SRU3/TGTU3/TG I3	SRU3 Unit						2007	N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-33-DIST HDU	Diesel HDS Unit w/CVS							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-34- HYDROCRACKE R	WX Hydrocracker						2008	N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-35-SAT GAS	Saturates Gas Plant							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-36-RO	Reverse Osmosis							N/A N/A	40388801	□ Existing (unchanged) □ To be Removed ■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-37-NP-UT	North Plant Utilities							N/A N/A	40388801	□ Existing (unchanged) □ To be Removed ■ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-41-PBC	PBC Unit							N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
FUG-43-S ALKY	South Alky Unit (W-76)							N/A N/A	40388801	□ To Be Modified □ To be Replaced ■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
FUG-44-DIST-	Gas Oil Hydrotreater (incl.							N/A N/A	40388801	□ To Be Modified □ To be Replaced ■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
HDU	CVS)							N/A	1000001	☐ To Be Modified ☐ To be Replaced		
FUG-45-DIST- HDU	Gas Oil Hydrotreater (incl. CVS)							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-54-PRIMEG	Prime G Unit						2016	N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-63-H2 PLANT-1	Hydrogen Plant							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		

					Manufact-urer's	Requested Permitted	Date of Manufacture ²	Controlled by Unit #	Source Classi-		RICE Ignition Type (CI, SI,	Replacing
Unit Number ¹	Source Description	Make	Model #	Serial#	Rated Capacity ³ (Specify Units)	Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack#	fication Code (SCC)	For Each Piece of Equipment, Check One	4SLB, 4SRB, 2SLB) ⁴	Unit No.
FUG-64-H2	Hydrogen Plant							N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
PLANT-2	Trydrogen Franc						2008	N/A	10500001	☐ To Be Modified ☐ To be Replaced		
FUG-70-CCR	CCR Reformer (w/in battery limits)							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-73-SP UTIL	Utilities							N/A N/A	40388801	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-80-WWTP								N/A		■ Existing (unchanged) □ To be Removed		
CVS	Oil/Water Separator							N/A	40388801	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		■ Existing (unchanged) □ To be Removed		
FUG-LPG	LPG Storage System							N/A	40388801	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		☐ Existing (unchanged) ■ To be Removed		
FUG-FUEL GAS	Fuel Gas Distribution System							N/A	40388801	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-ASPHALT								N/A		☐ Existing (unchanged) ■ To be Removed		
STG	Asphalt/Heavy Oil Storage							N/A	40388801	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-RLO-								N/A		☐ Existing (unchanged) ■ To be Removed		
ASPHALT	Asphalt/Pitch Loading Rack							N/A	40388801	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
FUG-								N/A	40200001	☐ Existing (unchanged) ■ To be Removed		
RRTOTRUCK	Crude oil unloading system							N/A	40388801	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
DW C	HED				200 111	200 111		N/A	40201000	☐ Existing (unchanged) ■ To be Removed		
RW-6	HFR				200 bbl	200 bbl	1978	RW-6	40301099	 □ New/Additional □ To Be Modified □ To be Replaced 		
T 0011	DIT				22 120 111	22 120 111		N/A	40201150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
T-0011	INT				32,130 bbl	32,130 bbl	pre-1973	T-0011	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
T-0012	INT				32,130 bbl	32,130 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1-0012	IINI				32,130 001	32,130 001	pre-1973	T-0012	40301130	☐ To Be Modified ☐ To be Replaced		
T-0020	INT				54,380 bbl	54,380 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1-0020	IIVI				34,380 001	34,360 001	10/1/2020	T-0020	40301130	☐ To Be Modified ☐ To be Replaced		
T-0021	INT				54,380 bbl	54,380 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1-0021	1111				34,300 001	34,300 001	10/1/2020	T-0021	40301130	☐ To Be Modified ☐ To be Replaced		
T-0022	INT				37,770 bbl	37,770 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1 0022	1111				37,770 001	37,770 001	10/1/2020	T-0022	10301130	☐ To Be Modified ☐ To be Replaced		
T-0023	INT				37,770 bbl	37,770 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1 0020	11.1				37,770 001	37,770 031	10/1/2020	T-0023	.0201120	☐ To Be Modified ☐ To be Replaced		
T-0040	CR				820 bbl	820 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
- 30.0						227 551	pre-1973	T-0040		☐ To Be Modified ☐ To be Replaced		
T-0041	CR				820 bbl	820 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
- 30.1						227 551	1973	T-0041		☐ To Be Modified ☐ To be Replaced		
T-0049	HFR				610 bbl	610 bbl		Carbon Cannister	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
							pre-1971	T-0049		☐ To Be Modified ☐ To be Replaced		

					Manufact-urer's	Requested Permitted	Date of Manufacture ²	Controlled by Unit#	Source Classi-		RICE Ignition Type (CI, SI,	Replacing
Unit Number ¹	Source Description	Make	Model#	Serial #	Rated Capacity ³ (Specify Units)	Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack#	fication Code (SCC)	For Each Piece of Equipment, Check One	4SLB, 4SRB, 2SLB) ⁴	Unit No.
T-0055	CD				10 200 1-1	10 200 1-1		N/A	40201000	■ Existing (unchanged) □ To be Removed		
1-0055	CR				10,200 bbl	10,200 bbl	1979	T-0055	40301099	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
T 0056	DUT				11 (00 111	11 (00 111		N/A	40201150	■ Existing (unchanged) □ To be Removed		
T-0056	INT				11,600 bbl	11,600 bbl	pre-1971	T-0056	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
T. 0057	EVE				55 520 111	55 500 111		N/A	40201150	☐ Existing (unchanged) ■ To be Removed		
T-0057	EXT				55,520 bbl	55,520 bbl	1981	T-0057	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
T 0050	GP.				5.140.111	5.140.111		N/A	10201000	■ Existing (unchanged) □ To be Removed		
T-0059	CR				5,140 bbl	5,140 bbl	pre-1973	T-0059	40301099	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							•	N/A		■ Existing (unchanged) ☐ To be Removed		
T-0061	CR				10,490 bbl	10,490 bbl	pre-1973	T-0061	40301099	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							1	N/A		■ Existing (unchanged) □ To be Removed		
T-0063	CR				10,910 bbl	10,910 bbl	pre-1973	T-0063	40301099	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							pre 1975	N/A		■ Existing (unchanged) □ To be Removed		
T-0065	CR				10,490 bbl	10,490 bbl	1999	T-0065	40301099	□ New/Additional □ Replacement Unit		
							1999			□ To Be Modified □ To be Replaced ■ Existing (unchanged) □ To be Removed		
T-0075	CR				18,910 bbl	18,910 bbl	2002	N/A	40301099	□ New/Additional □ Replacement Unit		
							2003	T-0075		☐ To Be Modified ☐ To be Replaced		
T-0079	EXT				87,420 bbl	87,420 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
							9/7/2008	T-0079		☐ To Be Modified ☐ To be Replaced		
T-0081	CR				65,870 bbl	65,870 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
							2010	T-0081		☐ To Be Modified ☐ To be Replaced		
T-0082	CR				109,660 bbl	109,660 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
					·		2010	T-0082		☐ To Be Modified ☐ To be Replaced		
T-0106	INT				25,120 bb1	25,120 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
					-, -	-, -	pre-1971	T-0106		☐ To Be Modified ☐ To be Replaced		
T-0107	INT				25,120 bb1	25,120 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1 0107	11,1				25,120 551	25,120 001	pre-1971	T-0107	.0501150	☐ To Be Modified ☐ To be Replaced		
T-0108	INT				25,120 bbl	25,120 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1-0100	1111				23,120 001	25,120 001	pre-1971	T-0108	40301130	☐ To Be Modified ☐ To be Replaced		
T-0109	INT				25,120 bbl	25,120 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1-0109	11/1				23,120 001	23,120 001	pre-1971	T-0109	40301130	☐ To Be Modified ☐ To be Replaced		
T 0110	CP.				57.100.111	57 100 111		N/A	40201000	■ Existing (unchanged) □ To be Removed		
T-0110	CR				57,100 bbl	57,100 bbl	pre-1971	T-0110	40301099	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
T 0111	D. (20)				10.000111	10.000111		N/A	40201150	■ Existing (unchanged) □ To be Removed		
T-0111	INT				10,080 bbl	10,080 bbl	pre-1973	T-0111	40301150	 □ New/Additional □ To Be Modified □ To be Replaced 		
							-	N/A		■ Existing (unchanged) ☐ To be Removed		
T-0112	INT				9,670 bbl	9,670 bbl	pre-1973	T-0112	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							1	N/A		■ Existing (unchanged) □ To be Removed		
T-0117	EXT				15,470 bbl	15,470 bbl	pre-1971	T-0117	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							F 19/1	N/A		■ Existing (unchanged) □ To be Removed		
T-0124	INT				6,710 bbl	6,710 bbl	1981	T-0124	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
						<u> </u>	1901	1-0124		□ 10 be Modified □ 10 be Replaced		

Unit Number ¹ T-0400	Source Description	Make			Manufact-urer's	Requested Permitted	Manufacture ²	Controlled by Unit #	Source Classi-		RICE Ignition Type (CI, SI,	Dl.
T-0400			Model #	Serial#	Rated Capacity ³ (Specify Units)	Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack#	fication Code (SCC)	For Each Piece of Equipment, Check One	4SLB, 4SRB, 2SLB) ⁴	Replacing Unit No.
1-0400	CD				06 690 1-11	06 690 1-1-1		N/A	40201000	■ Existing (unchanged) □ To be Removed		
$\overline{}$	CR				96,680 bbl	96,680 bbl	1983	T-0400	40301099	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
T 0401	EVT				56 650 1-1-1	56 650 1-1-1		N/A	40201150	■ Existing (unchanged) □ To be Removed		
T-0401	EXT				56,650 bbl	56,650 bbl	1982	T-0401	40301150	 □ New/Additional □ To Be Modified □ To be Replaced 		
T 0402	EVT				56 (50 111	56 (50111		N/A	40201150	■ Existing (unchanged) □ To be Removed		
T-0402	EXT				56,650 bbl	56,650 bbl	1983	T-0402	40301150	 □ New/Additional □ To Be Modified □ To be Replaced 		
T 0410	CP				24 020 111	24.020.11.1		N/A	40201000	■ Existing (unchanged) □ To be Removed		
T-0410	CR				34,920 bbl	34,920 bbl	1973	T-0410	40301099	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
T.0444	F.Y.				55.050111	55.050111		N/A	40201150	■ Existing (unchanged) □ To be Removed		
T-0411	EXT				55,950 bbl	55,950 bbl	pre-1971	T-0411	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							-	N/A		■ Existing (unchanged) □ To be Removed		
T-0412	EXT				55,950 bbl	55,950 bbl	pre-1971	T-0412	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							-	N/A		■ Existing (unchanged) □ To be Removed		
T-0413	INT				24,490 bbl	24,490 bbl	pre-1971	T-0413	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							Processia	N/A		■ Existing (unchanged) □ To be Removed		
T-0415	INT				25,120 bbl	25,120 bbl	pre-1971	T-0415	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							pre 17/1	N/A		■ Existing (unchanged) □ To be Removed		
T-0417	INT				10,490 bbl	10,490 bbl	pre-1973	T-0417	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							pre-1773	N/A		☐ Existing (unchanged) ☐ To be Removed		
T-0418	INT				20,720 bbl	20,720 bbl	>2021	T-0418	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							× 2021	N/A		■ Existing (unchanged) □ To be Removed		
T-0419	CR				11,000 bbl	11,000 bbl	1072		40301099	□ New/Additional □ Replacement Unit		
							pre-1973	T-0419 N/A		□ To Be Modified □ To be Replaced ■ Existing (unchanged) □ To be Removed		
T-0420	CR				10,490 bbl	10,490 bbl	1072		40301099	□ New/Additional □ Replacement Unit		
							pre-1973	T-0420		☐ To Be Modified ☐ To be Replaced ■ Existing (unchanged) ☐ To be Removed		
T-0422	CR				10,490 bbl	10,490 bbl	1072	N/A	40301099	□ New/Additional □ Replacement Unit		
							pre-1973	T-0422		□ To Be Modified □ To be Replaced ■ Existing (unchanged) □ To be Removed		
T-0423	CR				10,490 bbl	10,490 bbl	1051	N/A	40301099	□ New/Additional □ Replacement Unit		
							pre-1971	T-0423		☐ To Be Modified ☐ To be Replaced ■ Existing (unchanged) ☐ To be Removed		
T-0431	CR				53,180 bbl	53,180 bbl		N/A	40301099	□ New/Additional □ Replacement Unit		
<u> </u>							pre-1973	T-0431		☐ To Be Modified ☐ To be Replaced		
T-0432	CR				53,180 bbl	53,180 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
							pre-1972	T-0432		☐ To Be Modified ☐ To be Replaced		
T-0433	CR				80,420 bbl	80,420 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
							pre-1973	T-0433		☐ To Be Modified ☐ To be Replaced		
T-0434	CR				80,420 bbl	80,420 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
						· .	1979	T-0434		☐ To Be Modified ☐ To be Replaced		<u> </u>
T-0435	EXT				5,040 bbl	5,040 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
					- ,	- /- *	1/1/1997	T-0435		☐ To Be Modified ☐ To be Replaced		
T-0437	EXT				90,640 bbl	90,640 bbl	D 11 1077	N/A	40301150	■ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit		
1-043/	EAI				90,040 001	90,040 DDI	Built 1976 Relocated 2009	T-0437	40301130	☐ To Be Modified ☐ To be Replaced		

					Manufact-urer's	Requested Permitted	Date of Manufacture ²	Controlled by Unit#	Source Classi-		RICE Ignition Type (CI, SI,	Replacing
Unit Number ¹	Source Description	Make	Model #	Serial#	Rated Capacity ³ (Specify Units)	Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack #	fication Code (SCC)	For Each Piece of Equipment, Check One	4SLB, 4SRB, 2SLB) ⁴	Unit No.
T-0438	CR				54,380 bbl	54,380 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1-0438	CK				34,380 001	34,360 001	6/1/1978	T-0438	40301099	☐ To Be Modified ☐ To be Replaced		
T-0439	INT				108,740 bbl	108,740 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1-0-37	1111				100,740 001	100,740 001	11/1/1978	T-0439	40301130	☐ To Be Modified ☐ To be Replaced		
T-0450	EXT				80,570 bbl	80,570 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
1-0430	EAI				80,570 001	80,370 001	1/1/1997	T-0450	40301130	☐ To Be Modified ☐ To be Replaced		
T 0451	DIT				6.050.111	6.050.111		N/A	40201150	■ Existing (unchanged) □ To be Removed		
T-0451	INT				6,850 bbl	6,850 bbl	1/1/2016	T-0451	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		■ Existing (unchanged) □ To be Removed		
T-0452	INT				6,850 bbl	6,850 bbl	1/1/2016	T-0452	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		■ Existing (unchanged) □ To be Removed		
T-0737	EXT				22,210 bbl	22,210 bbl	1/1/2009	T-0737	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
								N/A		■ Existing (unchanged) □ To be Removed		
T-0802	EXT				11,330 bbl	11,330 bbl	1/1/2002	T-0802	40301150	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							17 17 2002	N/A		■ Existing (unchanged) □ To be Removed		
T-0814	CR				11,190 bbl	11,190 bbl	2005	T-0814	40301099	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							2003	N/A		■ Existing (unchanged) □ To be Removed		
T-0815	CR				80,930 bbl	80,930 bbl	2005	T-0815	40301099	□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced		
							2003	N/A		■ Existing (unchanged) □ To be Removed		
T-0821	EXT				78,580 bbl	78,580 bbl	1/1/2016	T-0821	40301150	□ New/Additional □ Replacement Unit		
							1/1/2016			□ To Be Modified □ To be Replaced ■ Existing (unchanged) □ To be Removed		
T-0834	EXT				40,420 bbl	40,420 bbl	1071	N/A	40301150	□ New/Additional □ Replacement Unit		
							pre-1971	T-0834		□ To Be Modified □ To be Replaced ■ Existing (unchanged) □ To be Removed		
T-0835	EXT				68,940 bbl	68,940 bbl		N/A	40301150	□ New/Additional □ Replacement Unit		
							pre-1973	T-0835		☐ To Be Modified ☐ To be Replaced		
T-0838	CR				30,640 bbl	30,640 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
							4/1/1977	T-0838		☐ To Be Modified ☐ To be Replaced		
T-0914	CR				31,470 bbl	31,470 bbl		N/A	40301099	☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit		
					·	· ·	2021	T-0914		☐ To Be Modified ☐ To be Replaced		
T-1225	EXT				125,890 bbl	125,890 bbl		N/A	40301150	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
					- , , , , , - 3 •	-,	2009	T-1225		☐ To Be Modified ☐ To be Replaced		
T-1227	CR				33,170 bbl	33,170 bbl		N/A	40301099	■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit		
					22,270 001	22,270 002	2009	T-1227		☐ To Be Modified ☐ To be Replaced		
TVCU	Floating Roof Tank Landings Vapor Combustion Unit					52 lb/hr		N/A	30205021	☐ Existing (unchanged) ☐ To be Removed ■ New/Additional ☐ Replacement Unit		
1,00	(VCU)					52 IO/III		N/A	30203021	☐ To Be Modified ☐ To be Replaced		
Pigging	Pigging Operations	N/A	N/A	N/A	N/A	N/A		N/A	2310021801	☐ Existing (unchanged) ☐ To be Removed ■ New/Additional ☐ Replacement Unit		
1 igging	1 1gging Operations	11/17	14/14	14/71	11/71	14/71		Pigging	2310021001	□ To Be Modified □ To be Replaced		

^{*} Standby generator engines satisfy the exempt equipment criteria at 20.2.72.202.B(3) NMAC. According to the application instructions, exempt engines shall be listed in Table 2-B rather than Table 2-A. Based on informal guidance received from NMED AQB, Navajo is listing the engines in Table 2-A.

³ To properly account for power conversion efficiencies, generator set rated capacity shall be reported as the rated capacity of the engine in horsepower, not the kilowatt capacity of the generator set.

^{4&}quot;4SLB" means four stroke lean burn engine, "4SRB" means four stroke rich burn engine, "2SLB" means two stroke lean burn engine, "CI" means compression ignition, and "SI" means spark ignition

Table 2-B: Insignificant Activities (20.2.70 NMAC) **OR** Exempted Equipment (20.2.72 NMAC)

All 20.2.70 NMAC (Title V) applications must list all Insignificant Activities in this table. All 20.2.72 NMAC applications must list Exempted Equipment in this table. If equipment listed on this table is exempt under 20.2.72.202.B.5, include emissions calculations and emissions totals for 202.B.5 "similar functions" units, operations, and activities in Section 6, Calculations. Equipment and activities exempted under 20.2.72.202 NMAC may not necessarily be Insignificant under 20.2.70 NMAC (and vice versa). Unit & stack numbering must be consistent throughout the application package. Per Exemptions Policy 02-012.00 (see http://www.env.nm.gov/apb/permit/apb_pol.html), 20.2.72.202.B NMAC Exemptions do not apply, but 20.2.72.202.A NMAC exemptions do apply to NOI facilities under 20.2.73 NMAC. List 20.2.72.301.D.4 NMAC Auxiliary Equipment for Streamline applications in Table 2-A. The List of Insignificant Activities (for TV) can be found online at https://www.env.nm.gov/wp-content/uploads/sites/2/2017/10/InsignificantListTitleV.pdf. TV sources may elect to enter both TV Insignificant Activities and Part 72 Exemptions on this form.

Unit Number	Source Description	Manufacturer -	Model No.	Max Capacity	List Specific 20.2.72.202 NMAC Exemption (e.g. 20.2.72.202.B.5)	Date of Manufacture /Reconstruction ²	For Each Piece of Equipment, Check Onc
Omt Number	Source Description	Manufacturer	Serial No.	Capacity Units	Insignificant Activity citation (e.g. IA List Item #1.a)	Date of Installation /Construction ²	For Each Fiece of Equipment, Check One
G-2601	Emergency Generator	Caterpillar -	G3512	1468	20.2.72.202.B.3		□ Existing (unchanged) ■ To be Removed □ New/Additional □ Replacement Unit
G-2001	Emergency Generator	Caterpinar		HP	N/A	2021	☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
G 2602	Г С .	G + '11	G3512	1468	20.2.72.202.B.3		☐ Existing (unchanged) ■ To be Removed
G-2602	Emergency Generator	Caterpillar		HP	N/A	2021	☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
DI 0.26	RDU Railcar Loading and			2,250	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed
RLO-26	Off-Loading Rack			bbl/hr	N/A	2021	☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
FUG-26-RDU-	Renewable Diesel Unit - Low				20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed
LOVP	vapor Pressure				N/A	2021	☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
					20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed
T-0001	DAF Waste Talon Tank				N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
					20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed
T-0002	DAF Waste Talon Tank				N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
					20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed
T-0003	DAF Waste Talon Tank				N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
					20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed
T-0004	DAF Waste Talon Tank				N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
T-0026	Daine Income				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1-0026	Brine - Inorganic				N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
	_ ,, _, _,				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed
T-0028	Scrubber Lime - Inorganic	ļ			N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
T-0031	Smoot Covotio Inches				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed
1-0031	Spent Caustic - Inorganic				N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
T-0042	Pressurized - Naphthas				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1-0042	i ressurizeu - ivapitutas				N/A		☐ To Be Modified ☐ To be Replaced
T-0045	Pressurized - Propane/Butane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1-0043	r ressurizeu - r ropane/butane				N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced

Unit Number	Source Description	Manufacturer	Model No.	Max Capacity	List Specific 20.2.72.202 NMAC Exemption (e.g. 20.2.72.202.B.5)	Date of Manufacture /Reconstruction ²	For Each Piece of Equipment, Check Onc
Omt Number	Source Description	Manufacturer	Serial No.	Capacity Units	Insignificant Activity citation (e.g. IA List Item #1.a)	Date of Installation /Construction²	For Each Fleee of Equipment, Check One
T-0046	Pressurized - Isobutane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1-0040	Pressurized - Isobutane				N/A		□ New/Additional □ Replacement Unit □ To Be Modified □ To be Replaced
T-0064	Caustic - Inorganic				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1-0004	Caustic - morganic				N/A		☐ To Be Modified ☐ To be Replaced
T-0071	Pressurized - Propane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1 0071	Tressurized Tropune				N/A		☐ To Be Modified ☐ To be Replaced
T-0072	Pressurized - Propane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
	11000milled 110pune				N/A		☐ To Be Modified ☐ To be Replaced
T-0073	Pressurized - Propane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1 00/5	11000milled 110pune				N/A		☐ To Be Modified ☐ To be Replaced
T-0074	Pressurized - Propane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0076	Pressurized - Propane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0114	Pressurized - n-Butane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0115	Pressurized - n-Butane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0116	Pressurized - Isobutane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0119	Pressurized - Isobutane				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0446	Calcium Chloride - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
	5				N/A		☐ To Be Modified ☐ To be Replaced
T-0447	Sulfuric Acid - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
	-				N/A		☐ To Be Modified ☐ To be Replaced
T-0448	Antiscalant - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0449	Cleaner - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
	8				N/A		☐ To Be Modified ☐ To be Replaced
T-0453	Calcium Chloride - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced

Unit Number	Source Description	Manufacturer	Model No.	Max Capacity	List Specific 20.2.72.202 NMAC Exemption (e.g. 20.2.72.202.B.5)	Date of Manufacture /Reconstruction ²	For Each Piece of Equipment, Check Onc
Chit Number	Source Description	Manufacturer	Serial No.	Capacity Units	Insignificant Activity citation (e.g. IA List Item #1.a)	Date of Installation /Construction²	For Each Fleee of Equipment, Check One
T-0460	Cultum Imanaguia				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1-0400	Sulfur - Inorganic				N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
T-0465	RO Water				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1-0403	KO water				N/A		☐ To Be Modified ☐ To be Replaced
T-0466	RO Water				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1 0 100	No water				N/A		☐ To Be Modified ☐ To be Replaced
T-0467	Sulfuric Acid - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1 0107	Saliane Held Mergame				N/A		☐ To Be Modified ☐ To be Replaced
T-0468	Brine - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1 0 100	Dime mergame				N/A		☐ To Be Modified ☐ To be Replaced
T-0600	Soda Ash - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1 0000	Dodd i Eil Molgamo				N/A		☐ To Be Modified ☐ To be Replaced
T-0803	DAF Waste - Wastewater				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1 0005	DIII Waste Waste Water				N/A		☐ To Be Modified ☐ To be Replaced
T-0804	DAF Waste - Wastewater				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0807	Caustic - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0809	Wastewater				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0816	Amine			940	20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
				GAL	N/A		☐ To Be Modified ☐ To be Replaced
T-0829	RO Reject Tank				20.2.72.202.B.2		☐ Existing (unchanged) ☐ To be Removed ■ New/Additional ☐ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0839	Condensate Water				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0840	Water				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0841	Calcium Chloride - Inorganic				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced
T-0891	Groundwater				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
					N/A		☐ To Be Modified ☐ To be Replaced

Unit Number	Source Description	Manufacturer -	Model No.	Max Capacity	List Specific 20.2.72.202 NMAC Exemption (e.g. 20.2.72.202.B.5)	Date of Manufacture /Reconstruction ²	For Each Piece of Equipment, Check Onc
Unit Number	Source Description	Manufacturer	Serial No.	Capacity Units	Insignificant Activity citation (e.g. IA List Item#1.a)	Date of Installation /Construction ²	For Each Fiece of Equipment, Check One
T 0003	0 1 4				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed
T-0892	Groundwater				N/A		☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
T-0901	RDU Renewable Diesel			89,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed
1-0901	KDO Renewable Diesei			BBL	N/A	2021	☐ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced
T-0902	RDU Renewable Diesel			89,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0902	RDU Reliewable Diesei			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0903	RDU Renewable Diesel			89,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0703	KDO Renewable Dieser			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0904	RDU Charge Tank			29,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0704	KDO Charge Tank			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0905	RDU Charge Tank			29,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0903	KDO Charge Tank			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0906	RDU Feed Tank			63,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0700	RDO recu rank			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0907	RDU Feed Tank			63,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0707	RD0 reed rank			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0908	RDU Feed Tank			17,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0700	RD0 reed rank			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0909	RDU Feed Tank			17,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0707	KDO recu rank			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0910	RDU Feed Tank			19,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0710	KD0 recu rank			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0911	RDU Feed Tank			19,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0711	KDO recu rank			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0912	RDU Feed Tank			109,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0712	ADO FOOT TAIK			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0913	RDU Feed Tank			109,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0713	NDO I CCG Talik			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0929	RDU Rail Unloading			800	20.2.72.202.B.2		□ Existing (unchanged) ■ To be Removed □ New/Additional □ Replacement Unit
1-0727	Acumulation Tank			GAL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0930	RDU Rail Unloading			800	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0730	Acumulation Tank			GAL	N/A	2021	☐ To Be Modified ☐ To be Replaced

Unit Number	Source Description	Manufacturer	Model No.	Max Capacity	List Specific 20.2.72.202 NMAC Exemption (e.g. 20.2.72.202.B.5)	Date of Manufacture /Reconstruction ²	For Each Piece of Equipment, Check Onc
Omt Number	Source Description	Manufacturer	Serial No.	Capacity Units	Insignificant Activity citation (e.g. IA List Item #1.a)	Date of Installation /Construction ²	FOR Each Freee of Equipment, Check One
T-0931	RDU Rail Unloading			800	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0931	Acumulation Tank			GAL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0932	RDU Rail Unloading			800	20.2.72.202.B.2		□ Existing (unchanged) ■ To be Removed □ New/Additional □ Replacement Unit
1-0732	Acumulation Tank			GAL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0933	RDU Rail Containment Tank -			30,000	20.2.72.202.B.2		□ Existing (unchanged) ■ To be Removed □ New/Additional □ Replacement Unit
1-0/33	Feed			GAL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0934	RDU Rail Containment Tank -			30,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0/34	Renewable Diesel			GAL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-0935	RDU Rail Containment Tank -			1,000	20.2.72.202.B.2		☐ Existing (unchanged) ■ To be Removed ☐ New/Additional ☐ Replacement Unit
1-0933	Recovered Oil			BBL	N/A	2021	☐ To Be Modified ☐ To be Replaced
T-1221	RO Water				20.2.72.202.B.2		☐ Existing (unchanged) ☐ To be Removed ■ New/Additional ☐ Replacement Unit
1-1221	KO water				N/A		☐ To Be Modified ☐ To be Replaced
T-1222	RO Water				20.2.72.202.B.2		☐ Existing (unchanged) ☐ To be Removed ■ New/Additional ☐ Replacement Unit
1-1222	KO water				N/A		☐ To Be Modified ☐ To be Replaced
T-1223	Fresh Caustic - Inorganic			84,000	20.2.72.202.B.2		☐ Existing (unchanged) ☐ To be Removed ■ New/Additional ☐ Replacement Unit
1-1223	Presir Caustic - morganic			GAL	N/A		☐ To Be Modified ☐ To be Replaced
T-1224	Filter Backwash - Wastewater				20.2.72.202.B.2		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
1-1224	Filler Backwasii - Wasiewaler				N/A		☐ To Be Modified ☐ To be Replaced
SSM Misc 1	Catalyst Handling				20.2.72.202.B.5		■ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit
SOIVI IVIISC I	Catalyst Handling				N/A		☐ To Be Modified ☐ To be Replaced
	Gas Fueling Tanks			500	20.2.72.202.B.5		☐ Existing (unchanged) ☐ To be Removed ■ New/Additional ☐ Replacement Unit
_	Gas rucinig ranks			GAL	N/A		□ To Be Modified □ To be Replaced
	Diesel Fueling Tanks			500	20.2.72.202.B.5		☐ Existing (unchanged) ☐ To be Removed ■ New/Additional ☐ Replacement Unit
_	Diesei Fueling Tanks			GAL	N/A		☐ To Be Modified ☐ To be Replaced
	Sampling Locations				20.2.72.202.B.5		□ Existing (unchanged) □ To be Removed ■ New/Additional □ Replacement Unit
-	Sampling Locations				N/A		■ New/Additional

Insignificant activities exempted due to size or production rate are defined in 20.2.70.300.D.6, 20.2.70.7.Q NMAC, and the NMED/AQB List of Insignificant Activities, dated September 15, 2008. Emissions from these insignificant activities do not need to be reported, unless specifically requested.

² Specify date(s) required to determine regulatory applicability.

Table 2-C: Emissions Control Equipment

Unit and stack numbering must correspond throughout the application package. Only list control equipment for TAPs if the TAP's maximum uncontrolled emissions rate is over its respective threshold as listed in 20.2.72 NMAC, Subpart V, Tables A and B. In accordance with 20.2.72.203.A(3) and (8) NMAC, 20.2.70.300.D(5)(b) and (e) NMAC, and 20.2.73.200.B(7) NMAC, the permittee shall report all control devices and list each pollutant controlled by the control device regardless if the applicant takes credit for the reduction in emissions.

Control Equipment Unit No.	Control Equipment Description	Date Installed	Controlled Pollutant(s)	Controlling Emissions for Unit Number(s) ¹	Efficiency (% Control by Weight)	Method used to Estimate Efficiency
D-8000/8001	WW Collection System Carbon Canisters	Unknown	VOC	D-8000/8001	0.95	
D-0829/0830	APIs Carbon Canisters	Unknown	VOC	D-0829/0830	0.95	
FCC Scrubber	FCC Regenerator Tertiary Cylcones and Wet Gas Scrubber	Unknown	PM10 and SO ₂	FCC Regerator vent	PM-85% & SO2-99%	
Chlorsorb	CCR Regenerator Vent Control		HAP and PM10	CCR Regenerator Vent	0.99	
FL-0400	North Plant Flare		VOC and H ₂ S	Refinery Process Units	0.98	
FL-0401	South Plant Flare		VOC and H ₂ S	Refinery Process Units	0.98	
FL-0402	FCC Flare		VOC and H ₂ S	Refinery Process Units	0.98	
FL-0403	Alky Flare		VOC	Refinery Process Units	0.98	
FL-0404	GOHT Flare		VOC and H ₂ S	Refinery Process Units	0.98	
H-0473 (SRU2 TGI)	SRU2 Tail Gas Incinerator		H2S	SRU1 and SRU2	0.98	
H-3103 (SRU3 TGI)	SRU3 Tail Gas Incinerator		H2S	SRU3	0.98	
SCR	Selective Catalytic Reduction		NOx	H-9851	0.64	
FL-HEP-PORT	Portable Flare for Holly Energy Partners (HEP) Pipeline Pigging		VOC	Pipeline Pigging Operations	0.98	
TL-4 VRU	John Zink Carbon Adsorption VRU		VOC	TL-4 Gasoline Loading	0.95	
TL-4 VCU	Backup of TL4-VRU		VOC	TL-4 Gasoline Loading	0.95	
T-0049	Tank T-0049 carbon canister		VOC	T-0049 Vent	0.95	
Tanks VCU	VCU for Tank Landings		VOC and H ₂ S	Floating tanks	0.95	
WWTP	Carbon Canisters at WWTP		VOC	WWTP	0.95	
Y-0011, Y-0012	Drift Eliminators on Cooling Towers (BACT)		PM	Y-001, Y-002	0*	
T-0737, T-1225	External Floating Roofs (BACT)		VOC	T-0737, T-1225	0*	
H-2501, H-3402, H-3101	Ultra-low NO _X burners		NO _X	H-2501, H-3402, H-3101	0*	

¹ List each control device on a separate line. For each control device, list all emission units controlled by the control device.

^{*} Navajo interprets the undefined term "emissions control equipment" consistent with the definition of the term "control device" in the federal Compliance Assurance Monitoring rule, 40 CFR § 64.2. Consistent with this interpretation, Navajo generally has listed only active control devices in this table and has not listed passive control measures that act to prevent pollutants from forming (such as the use of seals, lids, or roofs), use of low-polluting fuel or feedstocks, or the use of combustion or other process design features or characteristics (such as low-NOx burners). However, based on informal guidance from NMED AQB, and notwithstanding the application instructions, Navajo has listed in this table certain passive control measures which NMED has relied upon in establishing BACT.

Table 2-D: Maximum Emissions (under normal operating conditions)

■ This Table was intentionally left blank because it would be identical to Table 2-E.

Maximum Emissions are the emissions at maximum capacity and prior to (in the absence of) pollution control, emission-reducing process equipment, or any other emission reduction. Calculate the hourly emissions using the worst case hourly emissions for each pollutant. For each pollutant, calculate the annual emissions as if the facility were operating at maximum plant capacity without pollution controls for 8760 hours per year, unless otherwise approved by the Department. List Hazardous Air Pollutants (HAP) & Toxic Air Pollutants (TAPs) in Table 2-I. Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E-4).

Unit No.		Ox		0	V	OC	S	Ox	P	\mathbf{M}^1	PM	[10 ¹	PM	2.5 ¹	Н	₂ S		ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr								
Totals																		

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ľ	IImia No	N	Ox	(0	V	OC	S	Ox	PI	\mathbf{M}^1	PM	[10 ¹	PM	2.51	Н	$_{2}S$	Le	ead
ı	Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr								

¹Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but PM is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

Table 2-E: Requested Allowable Emissions

Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E⁴).

Unit No.	N	Ox	C	0	V	OC	S	Ox	P	M ¹	PN	/110 ¹	PN	M2.5 ¹	Н	₂ S	Le	ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
B-0007	12.90	56.50	19.67	86.16	1.29	5.64	8.04	13.94	1.78	7.80	1.78	7.80	1.78	7.80	-	-	-	-
B-0008	12.90	56.50	19.67	86.16	1.29	5.64	8.04	13.94	1.78	7.80	1.78	7.80	1.78	7.80	-	-	-	-
B-0009	4.89	21.41	9.04	39.61	0.98	4.28	2.89	12.67	1.82	7.98	1.82	7.98	1.82	7.98	-	-	-	-
H-0009	3.96	17.34	4.03	17.63	0.26	1.20	1.64	2.84	0.36	1.60	0.36	1.60	0.36	1.60	-	-	-	-
H-0011	9.52	31.73	3.48	15.30	0.23	1.00	1.42	2.46	0.31	1.38	0.31	1.38	0.31	1.38	-	-	-	-
H-0018	3.49	15.27	2.93	12.82	0.19	0.84	1.19	2.07	0.26	1.16	0.26	1.16	0.26	1.16	-	-	-	-
H-0019	2.90	12.46	4.94	21.64	0.32	1.42	2.02	3.50	0.45	2.00	0.45	2.00	0.45	2.00	-	-	-	-
H-0020	4.82	21.09	8.23	36.07	0.54	2.36	3.37	5.84	0.75	3.26	0.75	3.26	0.75	3.26	-	-	-	-
H-0028	2.17	9.50	1.13	4.93	0.07	0.32	0.46	0.80	0.10	0.45	0.10	0.45	0.10	0.45	-	-	-	-
H-0030	3.19	13.98	3.84	16.90	0.25	1.10	1.57	2.71	0.40	1.52	0.40	1.52	0.40	1.52	-	-	-	-
H-0040	3.78	16.56	3.84	16.90	0.25	1.10	1.57	2.71	0.40	1.52	0.40	1.52	0.40	1.52	-	-	-	-
H-0312	4.62	20.24	3.20	14.03	0.21	0.92	1.31	2.27	0.29	1.27	0.29	1.27	0.29	1.27	-	-	-	-
H-0352, H-0353, H-0354	9.00	39.42	18.30	80.15	1.20	5.25	8.07	15.56	1.70	7.25	1.70	7.25	1.70	7.25	-	-	-	-
H-0355	2.52	11.04	2.56	11.22	0.17	0.73	1.13	2.18	0.23	1.02	0.23	1.02	0.23	1.02	-	-	-	-
H-0362, H-0363, H-0364	6.88	30.11	11.44	50.09	0.75	3.28	5.04	9.73	1.03	4.53	1.03	4.53	1.03	4.53	-	-	-	-
H-0421	2.43	10.64	2.47	10.82	0.16	0.71	1.01	1.74	0.22	0.98	0.22	0.98	0.22	0.98	-	-	-	-
H-0464	0.52	2.29	0.88	3.85	0.06	0.25	0.36	0.62	0.08	0.40	0.08	0.40	0.08	0.40	-	-	-	-
H-0600	4.70	20.44	7.69	33.66	0.50	2.20	3.14	5.43	0.70	3.05	0.70	3.05	0.70	3.05	-	-	-	-
H-0601	3.51	15.37	7.14	31.26	0.47	2.05	2.91	5.04	0.65	2.83	0.65	2.83	0.65	2.83	-	-	-	-
H-2421	1.22	5.32	2.47	10.82	0.16	0.71	0.98	1.61	0.22	0.98	0.22	0.98	0.22	0.98	-	-	-	-
H-2501	3.60	15.77	7.20	31.54	0.72	3.15	4.35	7.19	0.99	4.35	0.99	4.35	0.99	4.35	-	-	-	-
H-3101	0.33	1.45	0.99	4.34	0.07	0.29	0.41	0.71	0.09	0.40	0.09	0.40	0.09	0.40	-	-	-	-
H-3402	1.56	6.83	4.68	20.50	0.31	1.36	1.89	3.12	0.43	1.89	0.43	1.89	0.43	1.89	-	-	-	-
H-3403	0.96	4.20	2.93	12.82	0.19	0.84	1.16	1.92	0.26	1.16	0.26	1.16	0.26	1.16	-	-	-	-
H-5401	0.77	3.38	0.64	2.82	0.12	0.51	0.72	1.25	0.16	0.70	0.16	0.70	0.16	0.70	-	-	-	-
H-8801/8802	8.66	37.95	13.91	60.91	0.91	3.99	2.85	4.96	1.26	5.51	1.26	5.51	1.26	5.51	-	-	-	-
H-9851	4.21	18.45	20.22	88.56	2.02	8.84	6.32	11.00	2.79	12.30	2.79	12.30	2.79	12.30	-	-	-	-
H-0473 (SRU2 TGI)	6.50	28.50	27.70	121.10	0.10	0.60	30.00	81.80	1.20	2.10	3.50	8.36	3.50	8.36	0.30	1.40	-	-
H-3103 (SRU3-TGI)	6.50	28.50	15.00	65.70	0.10	0.60	30.00	81.80	1.10	2.10	3.40	8.36	3.40	8.36	0.30	1.40	-	-
FCC REGEN	34.92	101.80	121.79	106.69	15.66	68.60	27.85	61.00	25.00	109.50	22.88	95.55	22.88	95.55	-	-	_	-
FL0400	3.47	5.45	14.23	22.35	26.01	32.70	4.48	3.92	-	-	-	-	-	-	0.05	0.04	_	-
FL0401	1.66	1.85	6.82	7.58	19.72	2.51	57.35	5.88	-	-	-	-	-	-	0.61	0.06	-	-
FL0402	8.11	2.21	33.29	9.08	98.18	7.72	98.54	5.58	-	-	-	-	-	-	1.05	0.06	-	-
FL0403	2.74	2.53	11.25	10.38	32.54	13.57	1.10	0.76	-	-	-	-	-	-	0.01	0.01	-	-
FL0404	11.70	23.49	48.01	96.40	160.50	99.85	39.92	11.14	-	-	-	-	-	-	0.42	0.12	-	-
MG-0001	1.84	8.06	1.61	7.06	1.84	8.06	3.48E-03	0.02	0.09	0.40	0.09	0.40	0.09	0.40	-	-	-	-
MG-0002	1.84	8.06	1.61	7.06	1.84	8.06	3.48E-03	0.02	0.09	0.40	0.09	0.40	0.09	0.40	-	-	-	-
MG-0003	0.09	0.40	1.13	4.97	0.04	0.19	1.72E-03	0.01	0.00	0.02	4.54E-03	0.02	#######	0.02	-	-	-	-
MG-0004	4.60	0.23	4.03	0.20	4.60	0.23	8.70E-03	4.35E-04	0.23	0.01	0.23	0.01	0.23	0.01	-	-	-	-

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1124 N	N	Ox	C	O	V	OC	SO	Ox	P	1	PN	M10 ¹	P	M2.5 ¹	Н	₂ S	Le	ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
SG-0100	1.61	0.40	0.35	0.09	0.13	0.03	6.47E-04	1.62E-04	0.11	0.03	0.11	0.03	0.11	0.03	-	-	-	-
SG-0101	1.67	0.42	0.36	0.09	0.14	0.03	6.72E-04	1.68E-04	0.12	0.03	0.12	0.03	0.12	0.03	-	-	-	-
SG-0102	0.07	0.02	0.82	0.20	0.03	0.01	1.23E-03	3.08E-04	3.26E-03	8.16E-04	3.26E-03	8.16E-04	#######	8.16E-04	-	-	-	-
FWG-0600	2.49	0.12	2.16	0.11	2.49	0.12	4.68E-03	2.34E-04	0.12	0.01	0.12	0.01	0.12	0.01	-	-	-	-
FWG-0601	2.49	0.12	2.16	0.11	2.49	0.12	4.68E-03	2.34E-04	0.12	0.01	0.12	0.01	0.12	0.01	-	-	-	-
FWG-0602	2.49	0.12	2.16	0.11	2.49	0.12	4.68E-03	2.34E-04	0.12	0.01	0.12	0.01	0.12	0.01	-	-	-	-
FWG-0603	2.02	0.10	1.75	0.09	2.02	0.10	3.79E-03	1.90E-04	0.10	0.01	0.10	0.01	0.10	0.01	-	-	-	-
Y-0001	-	-	-	-	0.21	0.92	-	-	0.26	1.15	0.158	0.69	0.00059	0.00260	-	-	-	-
Y-0002	-	-	-	-	0.21	0.92	-	-	0.26	1.15	0.16	0.69	0.0006	0.003	-	-	-	-
Y-0008	-	-	-	-	0.53	2.30	-	-	0.61	2.68	0.37	1.62	0.0014	0.0061	-	-	-	-
Y-0011	-	-	-	-	1.26	5.52	-	-	0.53	2.30	0.32	1.38	0.0012	0.005	-	-	-	-
Y-0012	-	-	-	-	0.42	1.84	-	-	0.18	0.77	0.11	0.46	0.0004	0.0017	-	-	-	-
CT TT-0006	-	-	-	-	1.08	4.73	-	-	0.16	0.69	0.09	0.42	0.0004	0.002	-	-	-	-
Collection (collector sump, T-845 Weir Box, T-844 Stilling Well, T-0846 SWKS)					0.02	0.08												
T-0830 Stormwater Surge Tank					5.49E-04	2.40E-03												
S1/T1 API-894/API-895					1.37E-04	6.02E-04												
T-801/T-836					1.34	5.85												
T-805 Flocculator					0.00	0.01												
T-896/T-806 DAF					1.64	7.18												
T-897 DAF Surge Open Sump					0.01	0.02												
D-810/811 & D-808/809 Filters					1.08E-07	4.72E-07												
T-809 DAF Surge Tank					0.004	0.02												
TLO-1	-	-	-	-	14.57	14.46	-	-	-	-	-	-	-	-	0.01	0.01	-	-
TL-2	-	-	-	-	12.49	3.75	-	-	-	-	-	-	-	-	0.01	0.002	-	-
TL-4	-	-	-	-	4.50	4.81	-	-	-	-	-	-	-	-	0.02	0.03	-	
TL-7	-	-	-	-	12.17	1.86	-	-	-	-	-	-	-	-	3.19E-05	4.88E-06	-	-
RLO-8	-	-	-	-	19.93	6.44	-	-	-	-	-	-	-	-	0.01	0.001	-	-
RLO-19	-	-	-	-	65.55	11.72	-	-	-	-	-	-	-	-	0.03	0.003	-	-
TLO-20	-	-	-	-	24.97	3.75	-	-	-	-	-	-	-	-	0.01	0.002	-	-
TRLO-9	-	-	-	-	-	-	-	-	-	-	-	-	-	-	0.005	0.02	-	-
TL4-VCU	1.97	1.23	1.97	1.22	0.050	0.0013	0.51	0.014	0.11	0.066	0.11	0.07	0.11	0.066	-	-	-	-
Fugitives					108.87	476.85									0 =-	0.55		
Tanks						316.21			_						0.72	0.80		
Totals	218.79	728.88	485.70	1,282.09	654.40	1,172.47	363.64	389.75	50.06	208.50	51.74	203.59	50.54	198.35	3.54	3.95	0.00	0.00
1 01413	210.77	/ 20.00	103.70	1,202.07	05-71-70	1,114.7/	JUJ.U7	307.13	20.00	200.30	31./7	200.07	50.57	170.00	J.J7	5.75	0.00	0.00

¹ Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

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Table 2-F: Additional Emissions during Startup, Shutdown, and Routine Maintenance (SSM)

☐ This table is intentionally left blank since all emissions at this facility due to routine or predictable startup, shutdown, or scehduled maintenance are no higher than those listed in Table 2-E and a malfunction emission limit is not already permitted or requested. If you are required to report GHG emissions as described in Section 6a, include any GHG emissions during Startup, Shutdown, and/or Scheduled Maintenance (SSM) in Table 2-P. Provide an explanations of SSM emissions in Section 6 and 6a.

All applications for facilities that have emissions during routine our predictable startup, shutdown or scheduled maintenance (SSM)¹, including NOI applications, must include in this table the Maximum Emissions during routine or predictable startup, shutdown and scheduled maintenance (20.2.7 NMAC, 20.2.73.200.D.2 NMAC). In Section 6 and 6a, provide emissions calculations for all SSM emissions reported in this table. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (https://www.env.nm.gov/aqb/permit/aqb_pol.html) for more detailed instructions. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E-4).

Unit No	N	Ox	C	0	V	OC	SO	Ox	P	M^2	PM	110^2	PM	2.5^{2}	Н	2S	Le	ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
SSM	215.87	21.73	1,483.31	87.83	1,701.98	85.58	1,454.18	17.42	5.16	0.37	19.32	0.41	19.32	0.41	14.74	0.27	-	-
Malfunction Cap	-	10.00	-	10.00	-	10.00	-	10.00	-	-	-	-	-	-	-	1.00		
Totals		31.73		97.83		95.58		27.42		0.37		0.41		0.41		1.27		0.00

¹ For instance, if the short term steady-state Table 2-E emissions are 5 lb/hr and the SSM rate is 12 lb/hr, enter 7 lb/hr in this table. If the annual steady-state Table 2-E emissions are 21.9 TPY, and the number of scheduled SSM events result in annual emissions of 31.9 TPY, enter 10.0 TPY in the table below.

Form Revision: 6/14/2019 Table 2-F: Page 1 Printed 1/24/2022 10:01 AM

² Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

Table 2-G: Stack Exit and Fugitive Emission Rates for Special Stacks

■ I have elected to leave this table blank because this facility does not have any stacks/vents that split emissions from a single source or combine emissions from more than one source listed in table 2-A. Additionally, the emission rates of all stacks match the Requested allowable emission rates stated in Table 2-E.

Use this table to list stack emissions (requested allowable) from split and combined stacks. List Toxic Air Pollutants (TAPs) and Hazardous Air Pollutants (HAPs) in Table 2-I. List all fugitives that are associated with the normal, routine, and non-emergency operation of the facility. Unit and stack numbering must correspond throughout the application package. Refer to Table 2-E for instructions on use of the "-" symbol and on significant figures.

	Serving Unit	N	Ox	C	0	V	OC	SO	Ox	P	M	PM	110	PM	12.5	□ H ₂ S or	r □ Lead
Stack No.	Number(s) from Table 2-A	lb/hr	ton/yr	lb/hr	ton/yr												
						_											
	Totals:																

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Table 2-H: Stack Exit Conditions

Unit and stack numbering must correspond throughout the application package. Include the stack exit conditions for each unit that emits from a stack, including blowdown venting parameters and tank emissions. If the facility has multiple operating scenarios, complete a separate Table 2-H for each scenario and, for each, type scenario name here:

Start Namehou	Serving Unit Number(s)	Orientation	Rain Caps	Height Above	Temp.	Flow	Rate	Moisture by	Velocity	Inside
Stack Number	from Table 2-A	(H-Horizontal V=Vertical)	(Yes or No)	Ground (ft)	(F)	(acfs)	(dscfs)	Volume (%)	(ft/sec)	Diameter (ft)
B0007	B-0007	V	No	75	275	1,036.39	747.33		47.90	5.25
B0008	B-0008	V	No	65	250	998.28	745.20		62.80	4.50
B0009	B-0009	V	No	60	300	936.11	652.82		47.70	5.00
H0009	H-0009	V	No	78	530	284.54	152.33		17.90	4.50
H0011	H-0011	V	No	80	850	326.56	132.12		26.00	4.00
H0018	H-0018	V	No	75	700	244.92	111.90		19.50	4.00
H0019	H-0019	V	No	156	450	321.54	187.27		21.40	4.38
H0020	H-0020	V	No	175	330	404.63	271.46		12.20	6.50
H0028	H-0028	V	No	50	850	105.21	42.57		18.80	2.67
H0030	H-0030	V	No	67	575	282.60	144.71		22.50	4.00
H0040	H-0040	V	No	101	590	286.37	144.55		22.80	4.00
H0312	H-0312	V	No	96	675	256.22	119.65		20.40	4.00
H0352_54	H-0352, H-0353, H-0354	V	No	211	300	991.68	691.56		16.50	8.75
H0355	H-0355	V	No	135	442	140.81	82.74		28.70	2.50
H0362_64	H-0362, H-0363, H-0364	V	No	206	338	650.06	431.74		16.90	7.00
H0421	H-0421	V	No	82	650	196.51	93.83		23.70	3.25
H0464	H-0464	V	No	80	450	56.99	33.19		9.60	2.75
H0600	H-0600	V	No	177	500	548.15	302.62		33.00	4.60
H0601	H-0601	V	No	131	300	384.73	268.30		11.60	6.50
H2421	H-2421	V	No	87	890	238.48	93.63		24.80	3.50
H2501	H-2501	V	No	168	710	914.42	414.23		19.00	7.83
H3101	H-3101	V	No	80	450	57.11	33.26		9.62	2.75
H3402	H-3402	V	No	67	575	350.42	179.44		27.90	4.00
H3403	H-3403	V	No	86	705	243.66	110.85		19.40	4.00
H5401	H-5401	V	No	83	643	62.21	29.89		8.81	3.00
H8801_02	H-8801, H-8802	V	No	130	600	869.60	434.80		75.40	3.83

G. IN	Serving Unit Number(s)	Orientation	Rain Caps	Height Above	Тетр.	Flow	Rate	Moisture by	Velocity	Inside
Stack Number	from Table 2-A	(H-Horizontal V=Vertical)	(Yes or No)	Ground (ft)	(F)	(acfs)	(dscfs)	Volume (%)	(ft/sec)	Diameter (ft)
H9851	H-9851	V	No	176	350	1,868.30	1,222.47		23.80	10.00
H0473	H-0473 (SRU2 TGI)	V	No	150	1,150	555.15	182.75		44.20	4.00
H3103	H-3103 (SRU3 TGI)	V	No	150	1,200	626.74	200.11		49.90	4.00
FCCREGEN	FCC Regen	V	No	153	125	799.76	724.57		28.30	6.00
FL0400	FL-400	V	No	395	1,832	13,363.93	3,090.26		65.60	16.11
FL0401	FL-401	V	No	342	1,832	4,750.21	1,098.43		65.60	9.60
FL0402	FL-402	V	No	305	1,832	4,433.53	1,025.21		65.60	9.28
FL0403	FL-403	V	No	499	1,832	19,475.87	4,503.58		65.60	19.45
FL0404	FL-404	V	No	569	1,832	34,834.89	8,055.19		65.60	26.01
V0543	MG-0001	V	No	6	1,000	21.35	7.75		244.82	0.33
V0545	MG-0002	V	No	6	1,000	21.35	7.75		244.82	0.33
V0546	MG-0003	V	No	6	1,000	19.71	7.16		225.99	0.33
V0511	MG-0004	V	No	8	1,000	25.05	9.09		287.19	0.33
G0100	SG-0100	V	No	10	1,000	5.01	1.82		229.84	0.17
G0101	SG-0101	V	No	12	1,000	5.20	1.89		238.68	0.17
G0102	SG-0102	V	No	10	1,000	30.26	10.99		354.00	0.33
E0600W	FWG-0600	V	No	4	1,000	30.88	11.21		354.04	0.33
E0601M	FWG-0601	V	No	4	1,000	30.88	11.21		354.04	0.33
E0602E	FWG-0602	V	No	4	1,000	30.88	11.21		354.04	0.33
E0603	FWG-0603	V	No	4	1,000	25.05	9.09		287.19	0.33
Y0001	Y-0001	V	No	14	100	1,256.00	1,188.71		25.00	8.00
Y0002	Y-0002	V	No	14	100	1,256.00	1,188.71		25.00	8.00
Y0008	Y-0008	V	No	14	100	1,256.00	1,188.71		25.00	8.00
Y0011	Y-0011	V	No	14	100	1,256.00	1,188.71		25.00	8.00
Y0012	Y-0012	V	No	14	100	1,256.00	1,188.71		25.00	8.00
CTTT0006	CT TT-0006	V	No	14	100	1,256.00	1,188.71		25.00	8.00
TL4VCU	TL4-VCU	V	No	82	1,832	791.70	183.07		65.60	3.92
TVCU	TVCU	V	No	82	1,832	791.70	183.07		65.60	0.20

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

	Т	I abic	2 1.	tack E	ait aiiu	I ugiti	ve Emi	331011 10	ates 10	111/11/	, and 1	1113							
Stack No.	Unit No.(s)	Total	HAPs	Amn			ic Acid or ■TAP		dehyde or TAP		olein or 🗆 TAP		zene or 🗆 TAP	1,3-Bu ■ HAP o	tadiene or TAP		Disulfide or TAP		oenzene or TAP
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
-	B-0007	4.4E-01	1.9E+00					-	-	-	-	4.9E-04	2.2E-03	-	-	-	-	-	-
-	B-0008	4.4E-01	1.9E+00					-	-	-	-	4.9E-04	2.2E-03	-	-	-	-	-	-
-	B-0009	4.5E-01	2.0E+00					-	-	-	-	5.0E-04	2.2E-03	-	-	-	-	-	-
-	H-0009	9.0E-02	3.9E-01					-	-	-	-	1.0E-04	4.4E-04	-	-	-	-	-	-
-	H-0011	7.8E-02	3.4E-01					-	-	-	-	8.7E-05	3.8E-04	-	-	-	-	-	-
-	H-0018	6.6E-02	2.9E-01					-	-	-	-	7.3E-05	3.2E-04	-	-	-	-	-	-
-	H-0019	1.1E-01	4.8E-01					-	-	-	-	1.2E-04	5.4E-04	-	-	-	-	-	-
-	H-0020	1.8E-01	8.1E-01					-	-	-	-	2.1E-04	9.0E-04	-	-	-	-	-	-
-	H-0028	2.5E-02	1.1E-01					-	-	-	-	2.8E-05	1.2E-04	-	-	-	-	-	-
-	H-0030	8.6E-02	3.8E-01					-	-	-	-	9.6E-05	4.2E-04	-	-	-	-	-	-
-	H-0040	8.6E-02	3.8E-01					-	-	-	-	9.6E-05	4.2E-04	-	-	-	-	-	-
-	H-0312	7.2E-02	3.1E-01					-	-	-	-	8.0E-05	3.5E-04	-	-	-	-	-	-
H0352_54	H-0352, H-0353, H-0354	4.1E-01	1.8E+00					-	-	-	-	4.6E-04	2.0E-03	-	-	-	-	-	-
-	H-0355	5.7E-02	2.5E-01					-	-	-	-	6.4E-05	2.8E-04	-	-	-	-	-	-
H0362_64	H-0362, H-0363, H-0364	2.6E-01	1.1E+00					-	-	-	-	2.9E-04	1.3E-03	-	-	-	-	-	-
-	H-0421	5.5E-02	2.4E-01					-	-	-	-	6.2E-05	2.7E-04	-	-	-	-	-	-
-	H-0464	2.0E-02	8.6E-02					-	-	-	-	2.2E-05	9.6E-05	-	-	-	-	-	-
-	H-0600	1.7E-01	7.5E-01					-	-	-	-	1.9E-04	8.4E-04	-	-	-	-	-	-
-	H-0601	1.6E-01	7.0E-01					-	-	-	-	1.8E-04	7.8E-04	-	-	-	-	-	-
-	H-2421	5.5E-02	2.4E-01					-	-	-	-	6.2E-05	2.7E-04	-	-	-	-	-	-
-	H-2501	2.5E-01	1.1E+00					-	-	-	-	2.7E-04	1.2E-03	-	-	-	-	-	-
-	H-3101	2.3E-02	9.9E-02					-	-	-	-	2.5E-05	1.1E-04	-	-	-	-	-	-
-	H-3402	1.1E-01	4.7E-01					-	-	-	-	1.2E-04	5.2E-04	-	-	-	-	-	-
-	H-3403	6.6E-02	2.9E-01					-	-	-	-	7.3E-05	3.2E-04	-	-	-	-	-	-
-	H-5401	4.0E-02	1.7E-01					-	-	-	-	4.4E-05	1.9E-04	-	-	-	-	-	-
H8801_02	H-8801/8802	3.1E-01	1.4E+00					-	-	-	-	3.5E-04	1.5E-03	-	-	-	-	-	-
-	H-9851	6.9E-01	3.0E+00	1.4E+00	6.1E+00			-	-	-	-	7.7E-04	3.4E-03	-	-	-	-	-	-
H0473	H-0473 (SRU2 TGI)	0.0E+00	0.0E+00			2.3E+00	6.3E+00	-	-	-	-	-	-	-	-	-	-	-	-
H3103	H-3103 (SRU3 TGI)	0.0E+00	0.0E+00			2.3E+00	6.3E+00	-	-	-	-	-	-	-	-	-	-	-	-
-	FCC Regen	2.9E+01	1.3E+02	1.6E+01	7.1E+01	2.1E+00	4.7E+00	2.4E-01	1.1E+00	7.7E-01	3.4E+00	7.3E-01	3.2E+00	8.9E-01	3.9E+00	3.0E-01	1.3E+00	1.1E-01	4.8E-01
-	MG-0001	8.3E-03	3.6E-02					1.7E-03	7.5E-03	2.1E-04	9.1E-04	2.1E-03	9.2E-03	8.8E-05	3.8E-04	-	-	0.0E+00	0.0E+00
-	MG-0002	8.3E-03	3.6E-02					1.7E-03	7.5E-03	2.1E-04	9.1E-04	2.1E-03	9.2E-03	8.8E-05	3.8E-04	-	-	0.0E+00	0.0E+00
-	MG-0003	4.1E-03	1.8E-02					8.5E-04	3.7E-03	1.0E-04	4.5E-04	1.0E-03	4.5E-03	4.3E-05	1.9E-04	-	-	0.0E+00	0.0E+00
-	MG-0004	2.1E-02	1.0E-03					4.3E-03	2.1E-04	5.2E-04	2.6E-05	5.2E-03	2.6E-04	2.2E-04	1.1E-05	-	-	0.0E+00	0.0E+00
-	SG-0100	1.5E-03	3.9E-04					3.2E-04	8.0E-05	3.8E-05	9.6E-06	3.9E-04	9.7E-05	1.6E-05	4.1E-06	-	-	0.0E+00	0.0E+00
-	SG-0101	1.6E-03	4.0E-04					3.3E-04	8.3E-05	4.0E-05	1.0E-05	4.0E-04	1.0E-04	1.7E-05	4.2E-06	-	-	0.0E+00	0.0E+00
-	SG-0102	2.9E-03	7.4E-04					6.1E-04	1.5E-04	7.3E-05	1.8E-05	7.4E-04	1.9E-04	3.1E-05	7.8E-06	-	-	0.0E+00	0.0E+00
-	FWG-0600	1.1E-02	5.6E-04					2.3E-03	1.2E-04	2.8E-04	1.4E-05	2.8E-03	1.4E-04	1.2E-04	5.9E-06	-	-	0.0E+00	0.0E+00
-	FWG-0601	1.1E-02	5.6E-04					2.3E-03	1.2E-04	2.8E-04	1.4E-05	2.8E-03	1.4E-04	1.2E-04	5.9E-06	-	-	0.0E+00	0.0E+00

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

		Table 2-1: Stack Exit															
Stack No.	Unit No.(s)	Formal HAP o		Hex HAP of		Hydroger HAP o		Methylen HAP o		Pho HAP o		Tole ■ HAP o	uene or TAP		ethylpentane or TAP	-	enes or TAP
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
- B-	3-0007	1.8E-02	7.7E-02	4.2E-01	1.8E+00	-	-	-	-	-	-	8.0E-04	3.5E-03	-	-	-	-
- B-	3-0008	1.8E-02	7.7E-02	4.2E-01	1.8E+00	-	-	-	-	-	-	8.0E-04	3.5E-03	-	-	-	-
- B-	3-0009	1.8E-02	7.9E-02	4.3E-01	1.9E+00	-	-	-	-	-	-	8.1E-04	3.6E-03	-	-	-	-
- H-	H-0009	3.6E-03	1.6E-02	8.6E-02	3.8E-01	-	-	-	-	-	-	1.6E-04	7.1E-04	-	-	-	-
- H-	H-0011	3.1E-03	1.4E-02	7.5E-02	3.3E-01	-	-	-	-	-	-	1.4E-04	6.2E-04	-	-	-	-
- H-	H-0018	2.6E-03	1.1E-02	6.3E-02	2.7E-01	-	-	-	-	-	-	1.2E-04	5.2E-04	-	-	-	-
- H-	H-0019	4.4E-03	1.9E-02	1.1E-01	4.6E-01	-	-	-	-	-	-	2.0E-04	8.8E-04	-	-	-	-
- H-	H-0020	7.4E-03	3.2E-02	1.8E-01	7.7E-01	-	-	-	-	-	-	3.3E-04	1.5E-03	-	-	-	-
- H-	H-0028	1.0E-03	4.4E-03	2.4E-02	1.1E-01	-	-	-	-	-	-	4.6E-05	2.0E-04	-	-	-	-
- H-	H-0030	3.4E-03	1.5E-02	8.2E-02	3.6E-01	-	-	-	-	-	-	1.6E-04	6.8E-04	-	-	-	-
- H-	H-0040	3.4E-03	1.5E-02	8.2E-02	3.6E-01	-	-	-	-	-	-	1.6E-04	6.8E-04	-	-	-	-
- H-	H-0312	2.9E-03	1.3E-02	6.9E-02	3.0E-01	-	-	-	-	-	-	1.3E-04	5.7E-04	-	-	-	-
	H-0352, H-0353, H-0354	1.6E-02	7.2E-02	3.9E-01	1.7E+00	-	-	-	-	-	-	7.4E-04	3.2E-03	-	-	-	-
- H-	H-0355	2.3E-03	1.0E-02	5.5E-02	2.4E-01	-	-	-	-	-	-	1.0E-04	4.5E-04	-	-	-	-
	H-0362, H-0363, H-0364	1.0E-02	4.5E-02	2.5E-01	1.1E+00	1	-	-	-	-	-	4.6E-04	2.0E-03	-	-	-	-
- H-	I-0421	2.2E-03	9.7E-03	5.3E-02	2.3E-01	-	-	-	-	-	-	1.0E-04	4.4E-04	-	-	-	-
- H-	I-0464	7.8E-04	3.4E-03	1.9E-02	8.2E-02	-	-	-	-	-	-	3.6E-05	1.6E-04	-	-	-	-
- H-	I-0600	6.9E-03	3.0E-02	1.6E-01	7.2E-01	-	-	-	-	-	-	3.1E-04	1.4E-03	-	-	-	-
- H-	I-0601	6.4E-03	2.8E-02	1.5E-01	6.7E-01	-	-	-	-	-	-	2.9E-04	1.3E-03	-	-	-	-
- H-	I-2421	2.2E-03	9.7E-03	5.3E-02	2.3E-01	-	-	-	-	-	-	1.0E-04	4.4E-04	-	-	-	-
- H-	I-2501	9.8E-03	4.3E-02	2.4E-01	1.0E+00	-	-	-	-	-	-	4.4E-04	1.9E-03	-	-	-	-
- H-	I-3101	9.0E-04	3.9E-03	2.2E-02	9.4E-02	-	-	-	-	-	-	4.1E-05	1.8E-04	-	-	-	-
- H-	I-3402	4.2E-03	1.9E-02	1.0E-01	4.5E-01	-	-	-	-	-	-	1.9E-04	8.4E-04	-	-	-	-
- H-	I-3403	2.6E-03	1.1E-02	6.3E-02	2.7E-01	-	-	-	-	-	-	1.2E-04	5.2E-04	-	-	-	-
- H-	I-5401	1.6E-03	6.9E-03	3.8E-02	1.7E-01	-	-	-	-	-	-	7.2E-05	3.1E-04	-	-	-	-
H8801_02 H-	H-8801/8802	1.2E-02	5.4E-02	3.0E-01	1.3E+00	-	-	-	-	-	-	5.6E-04	2.5E-03	-	-	-	-
- H-	I-9851	2.8E-02	1.2E-01	6.6E-01	2.9E+00	-	-	-	-	-	-	1.2E-03	5.5E-03	-	-	-	-
H0473 H-	H-0473 (SRU2 TGI)	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
H3103 H-	I-3103 (SRU3 TGI)	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
- FC	CCC Regen	4.6E-01	2.0E+00	-	-	2.1E+01	9.2E+01	1.9E+00	8.1E+00	1.2E+00	5.3E+00	1.4E+00	6.3E+00	-	-	1.1E-01	4.8E-01
- M	ИG-0001	2.6E-03	1.2E-02	0.0E+00	0.0E+00	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	9.2E-04	4.0E-03	0.0E+00	0.0E+00	6.4E-04	2.8E-03
- M	ИG-0002	2.6E-03	1.2E-02	0.0E+00	0.0E+00	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	9.2E-04	4.0E-03	0.0E+00	0.0E+00	6.4E-04	2.8E-03
- M	ИG-0003	1.3E-03	5.7E-03	0.0E+00	0.0E+00	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	4.5E-04	2.0E-03	0.0E+00	0.0E+00	3.1E-04	1.4E-03
- M	лG-0004	6.6E-03	3.3E-04	0.0E+00	0.0E+00	1	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	2.3E-03	1.1E-04	0.0E+00	0.0E+00	1.6E-03	8.0E-05
- SC	G-0100	4.9E-04	1.2E-04	0.0E+00	0.0E+00	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.7E-04	4.3E-05	0.0E+00	0.0E+00	1.2E-04	3.0E-05
- SC	G-0101	5.1E-04	1.3E-04	0.0E+00	0.0E+00	1	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.8E-04	4.4E-05	0.0E+00	0.0E+00	1.2E-04	3.1E-05
- SC	G-0102	9.4E-04	2.3E-04	0.0E+00	0.0E+00	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	3.2E-04	8.1E-05	0.0E+00	0.0E+00	2.3E-04	5.7E-05
- FV	WG-0600	3.5E-03	1.8E-04	0.0E+00	0.0E+00	1	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.2E-03	6.2E-05	0.0E+00	0.0E+00	8.6E-04	4.3E-05
- FV	WG-0601	3.5E-03	1.8E-04	0.0E+00	0.0E+00	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.2E-03	6.2E-05	0.0E+00	0.0E+00	8.6E-04	4.3E-05

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

	ı	Table 2-1: Stack Exit all			Ait aiiu	Fugitive Emission Rates for HAPs and 1.						1113							
Stack No.	Unit No.(s)	Total HAPs		Ammonia □ HAP or ■TAP			ic Acid or ■TAP		dehyde r 🗆 TAP		olein or 🗆 TAP	Benzene HAP or TAP		1,3-Butadiene ■ HAP or □ TAP		Carbon Disulfide ■ HAP or □ TAP		Ethylbenzene HAP or TAP	
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
-	FWG-0602	1.1E-02	5.6E-04					2.3E-03	1.2E-04	2.8E-04	1.4E-05	2.8E-03	1.4E-04	1.2E-04	5.9E-06	-	-	0.0E+00	0.0E+00
-	FWG-0603	9.0E-03	4.5E-04					1.9E-03	9.4E-05	2.3E-04	1.1E-05	2.3E-03	1.1E-04	9.5E-05	4.8E-06	-	-	0.0E+00	0.0E+00
-	Y-0001	1.2E-02	5.3E-02					-	-	-	-	1.6E-03	7.1E-03	7.6E-04	3.3E-03	-	-	2.2E-04	9.5E-04
-	Y-0002	1.2E-02	5.3E-02					-	-	-	-	1.6E-03	7.1E-03	7.6E-04	3.3E-03	-	-	2.2E-04	9.5E-04
-	Y-0008	3.0E-02	1.3E-01					-	-	-	-	4.0E-03	1.8E-02	1.9E-03	8.4E-03	-	-	5.4E-04	2.4E-03
-	Y-0011	7.3E-02	3.2E-01					-	-	-	-	9.7E-03	4.2E-02	4.6E-03	2.0E-02	-	-	1.3E-03	5.7E-03
-	Y-0012	2.4E-02	1.1E-01					-	-	-	-	3.2E-03	1.4E-02	1.5E-03	6.7E-03	-	-	4.3E-04	1.9E-03
-	CT TT-0006	6.3E-02	2.7E-01					-	-	-	-	8.3E-03	3.6E-02	3.9E-03	1.7E-02	-	-	1.1E-03	4.9E-03
-	Wastewater	2.4E+00	1.1E+01					-	-	-	-	3.2E-01	1.4E+00	-	-	6.2E-01	2.7E+00	2.6E-01	1.1E+00
-	TLO-1	5.7E-01	5.7E-01					-	-	-	-	4.8E-02	4.8E-02	-	-	-	-	3.8E-03	3.7E-03
-	TL-2	4.9E-01	1.5E-01					-	-	-	-	4.1E-02	1.2E-02	-	-	-	-	3.2E-03	9.7E-04
-	TL-4	4.8E-02	5.1E-02					-	-	-	-	5.7E-03	6.0E-03	-	-	-	-	4.3E-04	4.6E-04
-	TL-7	2.3E-03	3.7E-05					-	-	-	-	2.5E-04	5.0E-06	-	-	-	-	1.5E-04	2.6E-06
-	RLO-8	4.9E-01	1.2E-01					-	-	-	-	4.1E-02	9.8E-03	-	-	-	-	3.3E-03	8.0E-04
-	RLO-19	2.6E+00	2.2E-01					-	-	-	-	2.3E-01	2.4E-02	-	-	-	-	1.7E-02	1.5E-03
-	TLO-20	9.8E-01	1.5E-01					-	-	-	-	8.2E-02	1.2E-02	-	-	-	-	6.5E-03	9.7E-04
-	FUG-02-SP CRUDE	1.8E-01	7.7E-01					-	-	-	-	1.3E-02	5.5E-02	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.3E-02	5.7E-02
-	FUG-06-NHDU	5.0E-01	2.2E+00					-	-	-	-	4.9E-02	2.2E-01	0.0E+00	0.0E+00	5.2E-05	2.3E-04	2.4E-02	1.1E-01
-	FUG-07-N AMINE	0.0E+00	0.0E+00					-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-07-SWS1	0.0E+00	0.0E+00					-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-08-TRUCK RK	3.3E-01	1.4E+00					-	-	-	-	1.2E-02	5.1E-02	0.0E+00	0.0E+00	0.0E+00	0.0E+00	8.1E-03	3.5E-02
-	FUG-09-N ALKY	1.8E+00	7.9E+00					-	-	-	-	1.5E-02	6.7E-02	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.7E-03	7.6E-03
-	FUG-10-FCC	1.3E+00	5.8E+00					-	-	-	-	4.7E-02	2.1E-01	0.0E+00	0.0E+00	0.0E+00	0.0E+00	3.3E-02	1.4E-01
-	FUG-13-NHDU	6.7E-01	2.9E+00					-	-	-	-	6.6E-02	2.9E-01	0.0E+00	0.0E+00	7.0E-05	3.1E-04	3.2E-02	1.4E-01
-	FUG-18-LSR MEROX TRT	2.9E-02	1.3E-01					-	-	-	-	1.0E-03	4.5E-03	0.0E+00	0.0E+00	0.0E+00	0.0E+00	7.2E-04	3.2E-03
-	FUG-19-NAPHTHA	2.6E-02	1.1E-01					-	-	-	-	2.5E-03	1.1E-02	0.0E+00	0.0E+00	2.7E-06	1.2E-05	1.2E-03	5.4E-03
-	FUG-20-ISOM	1.6E-01	7.2E-01					-	-	-	-	1.1E-02	4.9E-02	0.0E+00	0.0E+00	0.0E+00	0.0E+00	8.5E-03	3.7E-02
-	FUG-21-SP VACUUM	2.2E-02	9.5E-02					-	-	-	-	2.2E-02	9.5E-02	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-25-ROSE-2	4.4E-04	1.9E-03					-	-	-	-	1.2E-05	5.1E-05	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.3E-05	5.9E-05
-	FUG-29-BLENDER/TK FARM	1.5E+00	6.5E+00					-	-	-	-	5.2E-02	2.3E-01	0.0E+00	0.0E+00	0.0E+00	0.0E+00	3.7E-02	1.6E-01
-	FUG-30-SRU2/TGTU	0.0E+00	0.0E+00					-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-31-SRU3/TGTU3/TGI3	0.0E+00	0.0E+00					-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-33-DIST HDU	1.1E+00	4.9E+00					-	-	-	-	2.2E-01	9.5E-01	0.0E+00	0.0E+00	0.0E+00	0.0E+00	2.7E-02	1.2E-01
-	FUG-34-HYDROCRACKER	4.7E-01	2.1E+00					-	-	-	-		2.0E-01						
-	FUG-35-SAT GAS		2.4E+00					-	-	-	-								
-	FUG-36-RO		3.7E-02					-	-	-	-		3.7E-03					4.1E-04	
-	FUG-37-NP-UT		7.1E-01					-	-	-	-		7.0E-02					7.9E-03	
-	FUG-41-PBC	4.2E-02						-	-	-	-	2.1E-03						7.0E-03	
	FUG-43-S ALKY							-	-	_	-	3.7E-03							
-	FUG-44-DIST-HDU		2.2E+00					-		-	_								
	FUG-35-SAT GAS FUG-36-RO FUG-37-NP-UT FUG-41-PBC FUG-43-S ALKY	5.5E-01 8.5E-03 1.6E-01 4.2E-02 1.1E-01	2.4E+00 3.7E-02 7.1E-01 1.8E-01 4.6E-01					-	-	-	-	5.4E-02 8.5E-04 1.6E-02 2.1E-03 3.7E-03	2.4E-01 3.7E-03 7.0E-02 9.2E-03 1.6E-02	0.0E+00 0.0E+00 0.0E+00 9.7E-04 0.0E+00	0.0E+00 0.0E+00 0.0E+00 4.2E-03 0.0E+00	5.7E-05 9.0E-07 1.7E-05 0.0E+00 0.0E+00	2 3 7 0.0	.5E-04 .9E-06 .5E-05 .0E+00 .0E+00	.5E-04 2.6E-02 9E-06 4.1E-04 .5E-05 7.9E-03

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

	i		-1: Stat											l			
Stack No.	Unit No.(s)		ldehyde or TAP	Hexane HAP or TAP			n Cyanide or TAP	Methylen HAP o	e Chloride r 🗆 TAP	Phenol HAP or TAP		Toluene ■ HAP or □ TAP		2,2,4-Trime HAP o	thylpentane r TAP	Xylenes ■ HAP or □ TAP	
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
-	FWG-0602	3.5E-03	1.8E-04	0.0E+00	0.0E+00	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.2E-03	6.2E-05	0.0E+00	0.0E+00	8.6E-04	4.3E-05
-	FWG-0603	2.9E-03	1.4E-04	0.0E+00	0.0E+00	1	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.0E-03	5.0E-05	0.0E+00	0.0E+00	7.0E-04	3.5E-05
-	Y-0001	-	-	8.8E-03	3.9E-02	-	-	-	-	-	-	6.0E-04	2.6E-03	1.1E-04	4.9E-04	3.5E-05	1.5E-04
-	Y-0002	-	-	8.8E-03	3.9E-02	-	-	-	-	-	-	6.0E-04	2.6E-03	1.1E-04	4.9E-04	3.5E-05	1.5E-04
-	Y-0008	-	-	2.2E-02	9.7E-02	-	-	-	-	-	-	1.5E-03	6.6E-03	2.8E-04	1.2E-03	8.8E-05	3.9E-04
-	Y-0011	-	-	5.3E-02	2.3E-01	-	-	-	-	-	-	3.6E-03	1.6E-02	6.7E-04	2.9E-03	2.1E-04	9.3E-04
-	Y-0012	-	-	1.8E-02	7.7E-02	-	-	-	-	-	-	1.2E-03	5.2E-03	2.2E-04	9.8E-04	7.1E-05	3.1E-04
-	CT TT-0006	-	-	4.5E-02	2.0E-01	-	-	-	-	-	-	3.1E-03	1.3E-02	5.7E-04	2.5E-03	1.8E-04	7.9E-04
-	Wastewater	1.2E-01	5.1E-01	-	-	-	-	2.6E-02	1.1E-01	-	-	5.0E-01	2.2E+00	-	-	5.6E-01	2.4E+00
-	TLO-1	-	-	4.7E-01	4.7E-01	-	-	-	-	-	-	3.1E-02	3.1E-02	6.0E-03	5.9E-03	9.4E-03	9.3E-03
-	TL-2	-	-	4.1E-01	1.2E-01	-	-	-	-	-	-	2.7E-02	8.1E-03	5.1E-03	1.5E-03	8.1E-03	2.4E-03
-	TL-4	-	-	6.4E-03	6.7E-03	-	-	-	-	-	-	5.6E-03	5.9E-03	2.4E-02	2.5E-02	6.6E-03	7.0E-03
-	TL-7	-	-	2.3E-04	3.4E-07	-	-	-	-	-	-	5.3E-04	1.4E-05	4.9E-04	7.2E-07	6.7E-04	1.4E-05
-	RLO-8	-	-	4.1E-01	9.7E-02	-	-	-	-	-	-	2.7E-02	6.5E-03	5.1E-03	1.2E-03	8.6E-03	2.3E-03
-	RLO-19	-	-	2.1E+00	1.8E-01	-	-	-	-	-	-	1.4E-01	1.2E-02	2.7E-02	2.4E-03	4.3E-02	3.8E-03
-	TLO-20	-	-	8.1E-01	1.2E-01	-	-	-	-	-	-	5.4E-02	8.1E-03	1.0E-02	1.5E-03	1.6E-02	2.4E-03
-	FUG-02-SP CRUDE	-	-	7.5E-02	3.3E-01	-	-	-	-	-	-	3.4E-02	1.5E-01	4.3E-03	1.9E-02	3.7E-02	1.6E-01
-	FUG-06-NHDU	-	-	2.4E-01	1.0E+00	-	-	-	-	-	-	1.2E-01	5.4E-01	1.9E-03	8.1E-03	6.2E-02	2.7E-01
-	FUG-07-N AMINE	-	-	0.0E+00	0.0E+00	-	-	-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-07-SWS1	-	-	0.0E+00	0.0E+00	-	-	-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-08-TRUCK RK	-	-	8.3E-03	3.6E-02	-	-	-	-	-	-	3.8E-02	1.7E-01	1.2E-01	5.4E-01	1.4E-01	6.1E-01
-	FUG-09-N ALKY	-	-	5.3E-03	2.3E-02	-	-	-	-	-	-	3.3E-02	1.5E-01	1.7E+00	7.7E+00	9.1E-03	4.0E-02
-	FUG-10-FCC	-	-	3.4E-02	1.5E-01	-	-	-	-	-	-	1.6E-01	6.8E-01	5.0E-01	2.2E+00	5.6E-01	2.5E+00
-	FUG-13-NHDU	-	-	3.2E-01	1.4E+00	-	-	-	-	-	-	1.7E-01	7.3E-01	2.5E-03	1.1E-02	8.4E-02	3.7E-01
-	FUG-18-LSR MEROX TRT	-	-	7.4E-04	3.2E-03	-	-	-	-	-	-	3.4E-03	1.5E-02	1.1E-02	4.8E-02	1.2E-02	5.4E-02
-	FUG-19-NAPHTHA	-	-	1.2E-02	5.3E-02	-	-	-	-	-	-	6.4E-03	2.8E-02	9.6E-05	4.2E-04	3.2E-03	1.4E-02
-	FUG-20-ISOM	-	-	1.3E-01	5.6E-01	-	-	-	-	-	-	1.3E-02	5.5E-02	3.2E-03	1.4E-02	4.8E-04	2.1E-03
-	FUG-21-SP VACUUM	-	-	0.0E+00	0.0E+00	-	-	-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-25-ROSE-2	-	-	3.3E-04	1.4E-03	-	-	-	-	-	-	4.3E-05	1.9E-04	0.0E+00	0.0E+00	5.1E-05	2.2E-04
-	FUG-29-BLENDER/TK FARM	-	-	3.8E-02	1.7E-01	-	-	-	-	-	-	1.7E-01	7.6E-01	5.6E-01	2.5E+00	6.3E-01	2.8E+00
-	FUG-30-SRU2/TGTU	-	-	0.0E+00	0.0E+00	-	-	-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-31-SRU3/TGTU3/TGI3	-	-	0.0E+00	0.0E+00	-	-	-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	FUG-33-DIST HDU	-	-	7.2E-01	3.1E+00	-	-	-	-	-	-	1.0E-01	4.6E-01	1.2E-02	5.2E-02	3.9E-02	1.7E-01
-	FUG-34-HYDROCRACKER	-	-	2.2E-01	9.7E-01	-	-	-	-	-	-	1.2E-01	5.1E-01	1.8E-03	7.7E-03	5.9E-02	2.6E-01
	FUG-35-SAT GAS	-	-	2.6E-01	1.1E+00	-	-	-	-	-	-	1.4E-01	6.0E-01	2.0E-03	9.0E-03	6.8E-02	3.0E-01
-	FUG-36-RO	-	-	4.0E-03	1.8E-02	-	-	-	-	-	-	2.1E-03	9.3E-03	3.2E-05	1.4E-04	1.1E-03	4.7E-03
-	FUG-37-NP-UT	-	-	7.7E-02	3.4E-01	-	-	-	-	-	-	4.0E-02	1.8E-01	6.1E-04	2.7E-03	2.0E-02	8.9E-02
	FUG-41-PBC	-	-	1.6E-02	7.0E-02	-	-	-	-	-	-	1.6E-02	6.8E-02	0.0E+00	0.0E+00	0.0E+00	0.0E+00
	FUG-43-S ALKY	-	-	2.7E-03	1.2E-02	-	-	_	-	-	-	1.2E-02	5.4E-02	4.0E-02	1.7E-01	4.4E-02	1.9E-01
	FUG-44-DIST-HDU	_	_	3.2E-01	1.4E+00	_	-	_	-	-	_	4.7E-02	2.1E-01	5.3E-03	2.3E-02	1.8E-02	7.7E-02
	5.51 1.50	_	_	J.210-01	1.12.00	-					_	1.72-02	2.12-01	J.JL-0J	2.51-02	1.01-02	7.7L-02

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

		Table	2-1. K	T I I I I I I I I I I I I I I I I I I I			ugitive Emission Rates for				anu i	115							
Stack No.	Unit No.(s)	Total HAPs		Ammonia □ HAP or ■TAP		Sulfuric Acid ☐ HAP or ■TAP		Acetaldehyde HAP or TAP		Acrolein HAP or TAP		Benzene HAP or TAP		1,3-Butadiene ■ HAP or □ TAP		Carbon Disulfide ■ HAP or □ TAP		Ethylbenzene HAP or TA	
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
-	FUG-45-DIST-HDU	1.9E-01	8.5E-01					-	-	-	-	3.8E-02	1.7E-01	0.0E+00	0.0E+00	0.0E+00	0.0E+00	4.7E-03	2.0E-02
-	FUG-54-PRIMEG	7.5E-01	3.3E+00					-	-	-	-	2.6E-02	1.2E-01	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.9E-02	8.1E-02
-	FUG-70-CCR	1.4E+00	6.3E+00					-	-	-	-	5.0E-02	2.2E-01	0.0E+00	0.0E+00	0.0E+00	0.0E+00	3.5E-02	1.5E-01
-	FUG-80-WWTP CVS	6.0E-02	2.6E-01						-	-	-	1.1E-02	4.6E-02	0.0E+00	0.0E+00	0.0E+00	0.0E+00	6.1E-03	2.7E-02
-	T-0011	4.7E-02	1.3E-01					-	-	-	-	4.4E-03	1.2E-02	4.1E-03	1.2E-02	0.0E+00	0.0E+00	7.1E-04	2.0E-03
-	T-0012	4.6E-02	1.1E-01					-	-	-	-	4.3E-03	1.1E-02	4.0E-03	1.0E-02	0.0E+00	0.0E+00	7.0E-04	1.7E-03
-	T-0020	1.5E-02	3.4E-02					-	-	-	-	1.4E-03	3.2E-03	1.3E-03	3.0E-03	0.0E+00	0.0E+00	2.3E-04	5.2E-04
-	T-0021	1.5E-02	3.4E-02					-	-	-	-	1.4E-03	3.2E-03	1.3E-03	3.0E-03	0.0E+00	0.0E+00	2.3E-04	5.2E-04
-	T-0022	1.3E-02	3.0E-02					-	-	-	-	1.2E-03	2.8E-03	1.2E-03	2.6E-03	0.0E+00	0.0E+00	2.0E-04	4.5E-04
-	T-0023	1.3E-02	3.0E-02					-	-	-	-	1.2E-03	2.8E-03	1.2E-03	2.6E-03	0.0E+00	0.0E+00	2.0E-04	4.5E-04
-	T-0040	5.5E-06	3.2E-07					9.5E-07	5.6E-08	-	-	2.0E-07	1.2E-08	-	-	-	-	2.1E-09	1.2E-10
-	T-0041	5.5E-06	3.2E-07					9.5E-07	5.6E-08	-	-	2.0E-07	1.2E-08	-	-	-	-	2.1E-09	1.2E-10
-	T-0049	1.1E-02	1.5E-03					0.0E+00	0.0E+00	-	-	2.9E-03	4.0E-04	-	-	-	-	1.8E-04	2.5E-05
-	T-0055	1.3E-03	2.1E-05					2.3E-04	3.7E-06	-	-	4.9E-05	8.0E-07	-	-	-	-	5.0E-07	8.2E-09
-	T-0056	6.9E-03	6.3E-03					-	-	-	-	9.0E-04	8.3E-04	0.0E+00	0.0E+00	0.0E+00	0.0E+00	3.2E-04	2.9E-04
-	T-0059	5.3E-05	2.0E-05					0.0E+00	0.0E+00	-	-	5.6E-06	2.1E-06	-	-	-	-	3.3E-06	1.2E-06
-	T-0061	8.0E-05	9.7E-05					0.0E+00	0.0E+00	-	-	8.5E-06	1.0E-05	-	-	-	-	5.0E-06	6.1E-06
-	T-0063	2.3E-05	7.5E-06					0.0E+00	0.0E+00	-	-	3.3E-06	1.0E-06	-	-	-	-	1.7E-06	5.3E-07
-	T-0065	1.0E-03	7.5E-06					0.0E+00	0.0E+00	-	-	1.4E-04	1.0E-06	-	-	-	-	7.3E-05	5.3E-07
-	T-0075	1.0E-03	9.0E-06					0.0E+00	0.0E+00	-	-	1.4E-04	1.3E-06	-	-	-	-	7.3E-05	6.4E-07
-	T-0079	5.9E-02	1.6E-01					-	-	-	-	5.4E-03	1.4E-02	5.1E-03	1.4E-02	0.0E+00	0.0E+00	8.9E-04	2.4E-03
-	T-0081	4.7E+00	1.2E-02					0.0E+00	0.0E+00	-	-	3.9E-01	1.0E-03	-	-	-	-	3.1E-02	8.1E-05
-	T-0082	4.9E+00	5.8E-03					0.0E+00	0.0E+00	-	-	4.1E-01	4.8E-04	-	-	-	-	3.2E-02	3.8E-05
-	T-0106	5.2E-03	5.2E-03					-	-	-	-	1.4E-03	1.4E-03	0.0E+00	0.0E+00	0.0E+00	0.0E+00	8.4E-05	8.4E-05
-	T-0107	1.1E-01	2.9E-01					-	-	-	-	8.9E-03	2.4E-02	8.8E-03	2.4E-02	0.0E+00	0.0E+00	2.3E-04	6.3E-04
-	T-0108	3.0E-02	1.1E-01					-	-	-	-	2.8E-03	1.0E-02	2.6E-03	9.5E-03	0.0E+00	0.0E+00	4.5E-04	1.7E-03
-	T-0109	4.4E-02	1.5E-01					-	-	-	-	4.1E-03	1.4E-02	3.8E-03	1.3E-02	0.0E+00	0.0E+00	6.7E-04	2.2E-03
-	T-0110	1.2E-01	1.3E-01					0.0E+00	0.0E+00	-	-	1.0E-02	1.1E-02	-	-	-	-	8.1E-04	8.3E-04
-	T-0111	2.6E-02	8.5E-02					-	-	-	-	2.4E-03	7.9E-03	2.3E-03	7.4E-03	0.0E+00	0.0E+00	3.9E-04	1.3E-03
-	T-0112	7.0E-03	2.5E-03					-	-	-	-	9.2E-04	3.3E-04	0.0E+00	0.0E+00	0.0E+00	0.0E+00	3.2E-04	1.2E-04

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

Stack No.	Unit No.(s)	Forma	ldehyde or TAP	Hexane P ■ HAP or □ TAP		Hydroge	n Cyanide or TAP	Methylene Chloride ■ HAP or □ TAP		Phenol HAP or TAP		Toluene HAP or TAP		2,2,4-Trimethylpentane ■ HAP or □ TAP		Xylenes ■ HAP or □ TAP	
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
-	FUG-45-DIST-HDU	-	-	1.2E-01	5.5E-01	-	-	-	-	-	-	1.8E-02	8.0E-02	2.1E-03	9.0E-03	6.9E-03	3.0E-02
-	FUG-54-PRIMEG	-	-	1.9E-02	8.3E-02	-	-	-	-	-	-	8.8E-02	3.8E-01	2.8E-01	1.2E+00	3.2E-01	1.4E+00
-	FUG-70-CCR	-	-	3.6E-02	1.6E-01	-	-	-	-	-	-	1.7E-01	7.3E-01	5.4E-01	2.4E+00	6.0E-01	2.6E+00
-	FUG-80-WWTP CVS	-	-	1.5E-02	6.5E-02	-	-	-	-	-	-	1.5E-02	6.5E-02	1.2E-03	5.4E-03	1.2E-02	5.4E-02
-	T-0011	-	-	6.9E-03	2.0E-02	-	-	-	-	-	-	1.1E-02	3.2E-02	1.5E-02	4.4E-02	4.4E-03	1.3E-02
-	T-0012	-	-	6.8E-03	1.7E-02	-	-	-	-	-	-	1.1E-02	2.7E-02	1.5E-02	3.8E-02	4.4E-03	1.1E-02
-	T-0020	-	-	2.2E-03	5.0E-03	-	-	-	-	-	-	3.6E-03	8.1E-03	4.9E-03	1.1E-02	1.4E-03	3.2E-03
-	T-0021	-	-	2.2E-03	5.0E-03	-	-	-	-	-	-	3.6E-03	8.1E-03	4.9E-03	1.1E-02	1.4E-03	3.2E-03
-	T-0022	-	-	1.9E-03	4.4E-03	1	-	-	-	-	-	3.1E-03	7.1E-03	4.3E-03	9.8E-03	1.2E-03	2.8E-03
-	T-0023	-	-	1.9E-03	4.4E-03	1	-	-	-	-	-	3.1E-03	7.1E-03	4.3E-03	9.8E-03	1.2E-03	2.8E-03
-	T-0040	-	-	0.0E+00	0.0E+00	1	-	-	-	4.3E-06	2.5E-07	4.2E-08	2.4E-09	0.0E+00	0.0E+00	6.8E-09	4.0E-10
-	T-0041	-	-	0.0E+00	0.0E+00	1	-	-	-	4.3E-06	2.5E-07	4.2E-08	2.4E-09	0.0E+00	0.0E+00	6.8E-09	4.0E-10
-	T-0049	-	-	6.3E-03	8.7E-04	1	-	-	-	0.0E+00	0.0E+00	1.2E-03	1.7E-04	1.3E-04	1.8E-05	3.3E-04	4.6E-05
-	T-0055	-	-	0.0E+00	0.0E+00	1	-	-	-	1.0E-03	1.7E-05	9.9E-06	1.6E-07	0.0E+00	0.0E+00	1.6E-06	2.7E-08
-	T-0056	-	-	8.5E-04	7.8E-04	-	-	-	-	-	-	4.2E-03	3.8E-03	9.7E-06	8.9E-06	6.2E-04	5.6E-04
-	T-0059	-	-	5.6E-06	2.1E-06	1	-	-	-	0.0E+00	0.0E+00	1.1E-05	4.3E-06	1.2E-05	4.5E-06	1.5E-05	5.7E-06
-	T-0061	-	-	8.6E-06	1.0E-05	1	-	-	-	0.0E+00	0.0E+00	1.7E-05	2.1E-05	1.8E-05	2.2E-05	2.3E-05	2.8E-05
-	T-0063	-	-	0.0E+00	0.0E+00	-	-	-	-	0.0E+00	0.0E+00	9.5E-06	3.0E-06	0.0E+00	0.0E+00	9.1E-06	2.9E-06
-	T-0065	-	-	0.0E+00	0.0E+00	-	-	-	-	0.0E+00	0.0E+00	4.2E-04	3.0E-06	0.0E+00	0.0E+00	4.0E-04	2.9E-06
-	T-0075	-	-	0.0E+00	0.0E+00	-	-	-	-	0.0E+00	0.0E+00	4.2E-04	3.6E-06	0.0E+00	0.0E+00	4.0E-04	3.5E-06
-	T-0079	-	-	8.6E-03	2.3E-02	-	-	-	-	-	-	1.4E-02	3.7E-02	1.9E-02	5.1E-02	5.5E-03	1.5E-02
-	T-0081	-	-	3.9E+00	1.0E-02	-	-	-	-	0.0E+00	0.0E+00	2.5E-01	6.7E-04	4.9E-02	1.3E-04	7.7E-02	2.0E-04
-	T-0082	-	-	4.1E+00	4.8E-03	-	-	-	-	0.0E+00	0.0E+00	2.7E-01	3.2E-04	5.1E-02	6.0E-05	8.1E-02	9.5E-05
-	T-0106	-	-	3.0E-03	3.0E-03	1	-	-	-	-	-	5.7E-04	5.7E-04	6.2E-05	6.2E-05	1.6E-04	1.6E-04
-	T-0107	-	-	8.7E-02	2.3E-01	-	-	-	-	-	-	3.3E-03	9.0E-03	1.3E-04	3.5E-04	0.0E+00	0.0E+00
-	T-0108	-	-	4.4E-03	1.6E-02	-	-	-	-	-	-	7.1E-03	2.6E-02	9.8E-03	3.6E-02	2.8E-03	1.0E-02
-	T-0109	-	-	6.5E-03	2.2E-02	-	-	-	-	-	-	1.0E-02	3.5E-02	1.4E-02	4.8E-02	4.1E-03	1.4E-02
-	T-0110	-	-	1.0E-01	1.0E-01	-	-	-	-	0.0E+00	0.0E+00	6.7E-03	6.9E-03	1.3E-03	1.3E-03	2.0E-03	2.1E-03
-	T-0111	-	-	3.8E-03	1.2E-02	-	-	-	-	-	-	6.1E-03	2.0E-02	8.5E-03	2.8E-02	2.4E-03	8.0E-03
-	T-0112	-	-	8.7E-04	3.1E-04	-	-	-	-	-	-	4.3E-03	1.5E-03	9.9E-06	3.6E-06	6.3E-04	2.3E-04

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

Stack No.	Unit No.(s)	Total	HAPs	Amn	nonia or TAP	Sulfuri	ic Acid	Acetal	dehyde	Acr	olein	Ben	zene or TAP		tadiene r 🗆 TAP		Disulfide or TAP	Ethylb HAP o	oenzene or TAP
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
-	T-0117	1.7E-02	6.5E-03					-	-	-	-	2.3E-03	8.5E-04	0.0E+00	0.0E+00	0.0E+00	0.0E+00	7.9E-04	3.0E-04
-	T-0124	3.0E-02	6.9E-02					-	-	-	-	2.8E-03	6.4E-03	2.6E-03	6.0E-03	0.0E+00	0.0E+00	4.6E-04	1.0E-03
-	T-0400	8.7E-01	5.2E-02					0.0E+00	0.0E+00	-	-	8.7E-01	5.2E-02	-	-	-	-	0.0E+00	0.0E+00
-	T-0401	8.9E-03	2.6E-02					-	-	-	-	8.2E-04	2.4E-03	7.7E-04	2.2E-03	0.0E+00	0.0E+00	1.3E-04	3.9E-04
-	T-0402	2.1E-02	3.6E-02					-	-	-	-	4.1E-03	6.9E-03	1.7E-03	2.9E-03	0.0E+00	0.0E+00	4.9E-04	8.3E-04
-	T-0410	2.1E+00	7.1E-02					0.0E+00	0.0E+00	-	-	1.8E-01	5.9E-03	-	-	-	-	1.4E-02	4.7E-04
-	T-0411	1.4E-01	3.5E-01					-	-	-	-	1.2E-02	2.9E-02	1.2E-02	2.9E-02	0.0E+00	0.0E+00	3.1E-04	7.6E-04
-	T-0412	2.0E-02	7.9E-03					-	-	-	-	2.7E-03	1.0E-03	0.0E+00	0.0E+00	0.0E+00	0.0E+00	9.3E-04	3.6E-04
-	T-0413	2.2E-03	3.4E-04					-	-	-	-	2.1E-04	3.3E-05	0.0E+00	0.0E+00	0.0E+00	0.0E+00	1.7E-04	2.6E-05
-	T-0415	3.2E-02	7.0E-02					-	-	-	-	3.0E-03	6.5E-03	2.8E-03	6.1E-03	0.0E+00	0.0E+00	4.8E-04	1.1E-03
-	T-0417	4.1E-02	1.0E-01					-	-	-	-	3.8E-03	9.7E-03	3.5E-03	9.1E-03	0.0E+00	0.0E+00	6.2E-04	1.6E-03
-	T-0418	2.6E-03	3.7E-04					-	-	-	-	2.6E-04	3.7E-05	0.0E+00	0.0E+00	0.0E+00	0.0E+00	2.0E-04	2.9E-05
-	T-0419	2.6E-03	1.2E-04					0.0E+00	0.0E+00	-	-	7.5E-04	3.4E-05	-	-	-	-	1.7E-04	7.5E-06
-	T-0420	2.7E-01	2.7E-05					0.0E+00	0.0E+00	-	-	2.3E-02	2.2E-06	-	-	-	-	1.8E-03	1.8E-07
-	T-0422	4.6E-04	1.7E-04					0.0E+00	0.0E+00	-	-	4.9E-05	1.8E-05	-	-	-	-	2.9E-05	1.1E-05
-	T-0423	5.5E-04	2.1E-04					0.0E+00	0.0E+00	-	-	5.8E-05	2.2E-05	-	-	-	-	3.4E-05	1.3E-05
-	T-0431	3.0E-02	6.8E-04					0.0E+00	0.0E+00	-	-	3.2E-03	7.2E-05	-	-	-	-	1.9E-03	4.2E-05
-	T-0432	2.6E-02	9.4E-04					0.0E+00	0.0E+00	-	-	2.8E-03	1.0E-04	-	-	-	-	1.6E-03	5.9E-05
-	T-0433	1.1E-02	2.8E-02					0.0E+00	0.0E+00	-	-	1.1E-02	2.8E-02	-	-	-	-	0.0E+00	0.0E+00
-	T-0434	4.0E-02	1.6E-02					0.0E+00	0.0E+00	-	-	1.1E-02	4.5E-03	-	-	-	-	2.5E-03	1.0E-03
-	T-0435	2.5E-03	6.8E-03					-	-	-	-	6.6E-04	1.8E-03	0.0E+00	0.0E+00	0.0E+00	0.0E+00	4.1E-05	1.1E-04
-	T-0437	2.7E-02	5.2E-02					-	-	-	-	2.4E-03	4.5E-03	0.0E+00	0.0E+00	0.0E+00	0.0E+00	2.6E-04	5.0E-04
-	T-0438	2.2E-01	1.2E-02					0.0E+00	0.0E+00	-	-	2.2E-01	1.2E-02	-	-	-	-	0.0E+00	0.0E+00
-	T-0439	7.6E-02	1.6E-01					-	-	-	-	8.1E-03	1.7E-02	0.0E+00	0.0E+00	0.0E+00	0.0E+00	4.3E-04	8.9E-04
-	T-0450	1.1E-01	2.0E-01					-	-	-	-	1.2E-02	2.1E-02	0.0E+00	0.0E+00	0.0E+00	0.0E+00	6.1E-04	1.1E-03
-	T-0451	3.4E-04	5.2E-05					-	-	-	-	9.7E-05	1.5E-05	0.0E+00	0.0E+00	0.0E+00	0.0E+00	2.1E-05	3.3E-06
-	T-0452	0.0E+00	0.0E+00					-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	T-0737	2.2E-03	6.0E-03					-	-	-	-	5.7E-04	1.6E-03	0.0E+00	0.0E+00	0.0E+00	0.0E+00	3.5E-05	9.7E-05
-	T-0802	2.1E-03	6.7E-03					-	-	-	-	5.5E-04	1.8E-03	0.0E+00	0.0E+00	0.0E+00	0.0E+00	3.4E-05	1.1E-04
-	T-0814	9.4E-01	2.8E-01					0.0E+00	0.0E+00	-	-	7.9E-02	2.3E-02	-	-	-	-	6.2E-03	1.8E-03
-	T-0815	4.0E-02	6.4E-04					0.0E+00	0.0E+00	-	-	1.1E-02	1.8E-04	-	-	-	-	2.5E-03	4.0E-05
-	T-0821	2.6E-02	4.1E-02					-	-	-	-	5.0E-03	7.8E-03	2.1E-03	3.3E-03	0.0E+00	0.0E+00	6.0E-04	9.4E-04
-	T-0834	4.0E-04	5.1E-04					-	-	-	-	1.1E-04	1.4E-04	0.0E+00	0.0E+00	0.0E+00	0.0E+00	2.5E-05	3.2E-05
-	T-0835	1.4E-03	2.3E-04					-	-	-	-	3.9E-04	6.6E-05	0.0E+00	0.0E+00	0.0E+00	0.0E+00	8.7E-05	1.5E-05
-	T-0838	1.1E-02	4.8E-04					0.0E+00	0.0E+00	-	-	3.1E-03	1.4E-04	-	-	-	-	6.8E-04	3.0E-05
-	T-1225	2.1E-02	8.3E-02					-	-	-	-	1.9E-03	7.2E-03	0.0E+00	0.0E+00	0.0E+00	0.0E+00	2.1E-04	8.0E-04
-	T-1227	1.8E+00	3.8E-01					0.0E+00	0.0E+00	-	-	1.5E-01	3.1E-02	-	-	-	-	1.2E-02	2.5E-03
Tot	als:	70.92	217.11	17.63	77.23	6.73	17.19	0.26	1.08	0.77	3.38	4.90	9.01	0.96	4.10	0.92	4.05	0.85	3.11

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

Stack No.	Unit No.(s)		ldehyde or TAP	Her HAP o			n Cyanide or TAP	Methylene HAP o	e Chloride r 🗆 TAP		enol or TAP	Tol		2,2,4-Trime HAP o			enes or TAP
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
-	T-0117	-	-	2.1E-03	8.0E-04	-	-	-	-	-	-	1.0E-02	3.9E-03	2.4E-05	9.2E-06	1.5E-03	5.8E-04
-	T-0124	-	-	4.4E-03	1.0E-02	-	-	1	1	-	-	7.2E-03	1.6E-02	9.9E-03	2.2E-02	2.9E-03	6.5E-03
-	T-0400	-	-	0.0E+00	0.0E+00	-	-	-	1	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	T-0401	-	-	1.3E-03	3.8E-03	-	-	1	1	-	-	2.1E-03	6.1E-03	2.9E-03	8.4E-03	8.4E-04	2.4E-03
-	T-0402	-	-	1.3E-02	2.2E-02	-	-	-	1	-	-	0.0E+00	0.0E+00	2.3E-04	3.9E-04	1.9E-03	3.2E-03
-	T-0410	-	-	1.7E+00	5.9E-02	-	-	-	1	0.0E+00	0.0E+00	1.2E-01	3.9E-03	2.2E-02	7.4E-04	3.5E-02	1.2E-03
-	T-0411	-	-	1.2E-01	2.8E-01	-	-	-	1	-	-	4.4E-03	1.1E-02	1.7E-04	4.2E-04	0.0E+00	0.0E+00
-	T-0412	-	-	2.5E-03	9.7E-04	-	-	1	1	-	-	1.2E-02	4.8E-03	2.9E-05	1.1E-05	1.8E-03	7.1E-04
-	T-0413	-	-	8.1E-04	1.3E-04	-	-	1	1	-	-	3.5E-04	5.4E-05	2.5E-04	3.8E-05	3.9E-04	6.0E-05
-	T-0415	-	-	4.7E-03	1.0E-02	-	-	1	1	-	-	7.5E-03	1.7E-02	1.0E-02	2.3E-02	3.0E-03	6.6E-03
-	T-0417	-	-	6.0E-03	1.5E-02	-	-	1	1	-	-	9.6E-03	2.5E-02	1.3E-02	3.4E-02	3.8E-03	9.8E-03
-	T-0418	-	-	9.7E-04	1.4E-04	-	-	1	1	-	-	4.2E-04	6.0E-05	2.9E-04	4.2E-05	4.6E-04	6.6E-05
-	T-0419	-	-	2.7E-04	1.2E-05	-	-	1	1	0.0E+00	0.0E+00	6.6E-04	3.0E-05	0.0E+00	0.0E+00	7.9E-04	3.6E-05
-	T-0420	-	-	2.2E-01	2.2E-05	-	-	1	1	0.0E+00	0.0E+00	1.5E-02	1.5E-06	2.8E-03	2.8E-07	4.4E-03	4.4E-07
-	T-0422	-	-	4.9E-05	1.9E-05	-	-	1	1	0.0E+00	0.0E+00	9.8E-05	3.7E-05	1.0E-04	3.9E-05	1.3E-04	4.9E-05
-	T-0423	-	-	5.9E-05	2.2E-05	-	-	-	-	0.0E+00	0.0E+00	1.2E-04	4.4E-05	1.2E-04	4.6E-05	1.5E-04	5.9E-05
-	T-0431	-	-	3.2E-03	7.2E-05	-	-	1	1	0.0E+00	0.0E+00	6.5E-03	1.5E-04	6.8E-03	1.5E-04	8.5E-03	1.9E-04
-	T-0432	-	-	2.8E-03	1.0E-04	-	-	1	1	0.0E+00	0.0E+00	5.6E-03	2.0E-04	5.9E-03	2.1E-04	7.4E-03	2.7E-04
-	T-0433	-	-	0.0E+00	0.0E+00	-	-	1	1	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	T-0434	-	-	4.2E-03	1.7E-03	-	-	-	-	0.0E+00	0.0E+00	1.0E-02	4.0E-03	0.0E+00	0.0E+00	1.2E-02	4.8E-03
-	T-0435	-	-	1.5E-03	3.9E-03	-	-	-	-	-	-	2.8E-04	7.5E-04	3.0E-05	8.1E-05	7.6E-05	2.0E-04
-	T-0437	-	-	2.2E-02	4.2E-02	-	-	-	-	-	-	1.9E-03	3.6E-03	3.1E-04	6.0E-04	6.7E-04	1.3E-03
-	T-0438	-	-	0.0E+00	0.0E+00	-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	T-0439	-	-	6.0E-02	1.3E-01	-	-	-	-	-	-	6.1E-03	1.3E-02	1.2E-04	2.5E-04	9.9E-04	2.1E-03
-	T-0450	-	-	8.6E-02	1.6E-01	-	-	-	-	-	-	8.7E-03	1.6E-02	1.7E-04	3.1E-04	1.4E-03	2.6E-03
-	T-0451	-	-	3.5E-05	5.4E-06	-	-	-	-	-	-	8.6E-05	1.3E-05	0.0E+00	0.0E+00	1.0E-04	1.5E-05
-	T-0452	-	-	0.0E+00	0.0E+00	-	-	-	-	-	-	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00
-	T-0737	-	-	1.2E-03	3.4E-03	-	-	-	-	-	-	2.4E-04	6.6E-04	2.6E-05	7.1E-05	6.5E-05	1.8E-04
-	T-0802	-	-	1.2E-03	3.8E-03	-	-	-	-	-	-	2.3E-04	7.4E-04	2.5E-05	8.0E-05	6.4E-05	2.0E-04
-	T-0814	-	-	7.8E-01	2.3E-01	-	-	-	-	0.0E+00	0.0E+00	5.1E-02	1.5E-02	9.8E-03	2.9E-03	1.5E-02	4.6E-03
-	T-0815	-	-	4.2E-03	6.7E-05	-	-	-	-	0.0E+00	0.0E+00	1.0E-02	1.6E-04	0.0E+00	0.0E+00	1.2E-02	1.9E-04
-	T-0821	-	-	1.6E-02	2.5E-02	-	-	-	-	-	-	0.0E+00	0.0E+00	2.8E-04	4.4E-04	2.3E-03	3.6E-03
-	T-0834	-	-	4.2E-05	5.3E-05	-	-	-	-	-	-	1.0E-04	1.3E-04	0.0E+00	0.0E+00	1.2E-04	1.5E-04
-	T-0835	-	-	1.4E-04	2.4E-05	-	-	-	-	-	-	3.5E-04	5.9E-05	0.0E+00	0.0E+00	4.1E-04	7.0E-05
-	T-0838	-	-	1.1E-03	5.0E-05	-	-	-	-	0.0E+00	0.0E+00	2.7E-03	1.2E-04	0.0E+00	0.0E+00	3.3E-03	1.4E-04
-	T-1225	-	-	1.7E-02	6.6E-02	-	-	-	-	-	-	1.5E-03	5.7E-03	2.5E-04	9.6E-04	5.3E-04	2.1E-03
-	T-1227	-	-	1.5E+00	3.1E-01	-	-	-	-	0.0E+00	0.0E+00	1.0E-01	2.1E-02	1.9E-02	3.9E-03	3.0E-02	6.2E-03
Tot	als:	0.79	3.38	24.48	35.32	21.02	92.06	1.88	8.25	1.22	5.32	4.78	15.72	4.23	17.28	3.84	15.06

Table 2-J: Fuel

Specify fuel characteristics and usage. Unit and stack numbering must correspond throughout the application package.

	Fuel Type (low sulfur	Fuel Source: purchased commercial,		S	pecify Units		
Unit No.	Diesel, ultra low sulfur diesel, Natural Gas, Coal,)	pipeline quality natural gas, residue gas, raw/field natural gas, process gas (e.g. SRU tail gas) or other	Lower Heating Value	Hourly Usage	Annual Usage	% Sulfur	% Ash
B-0007	Refinery Fuel Gas	Process gas	749 Btu/scf	238.9 MMBtu/hr (HHV)	2,092,457 MMBtu/yr (HHV)	0.02	0
B-0008	Refinery Fuel Gas	Process gas	749 Btu/scf	238.9 MMBtu/hr (HHV)	2,092,457 MMBtu/yr (HHV)	0.02	0
B-0009	Refinery Fuel Gas	Process gas	845 Btu/scf	244.4 MMBtu/hr (HHV)	2,141,119 MMBtu/yr (HHV)	0.01	0
H-0009	Refinery Fuel Gas	Process gas	749 Btu/scf	48.9 MMBtu/hr (HHV)	428,224 MMBtu/yr (HHV)	0.02	0
H-0011	Refinery Fuel Gas	Process gas	749 Btu/scf	42.2 MMBtu/hr (HHV)	369,830 MMBtu/yr (HHV)	0.02	0
H-0018	Refinery Fuel Gas	Process gas	749 Btu/scf	35.6 MMBtu/hr (HHV)	311,436 MMBtu/yr (HHV)	0.02	0
H-0019	Refinery Fuel Gas	Process gas	749 Btu/scf	60.0 MMBtu/hr (HHV)	525,547 MMBtu/yr (HHV)	0.02	0
H-0020	Refinery Fuel Gas	Process gas	749 Btu/scf	100.0 MMBtu/hr (HHV)	875,912 MMBtu/yr (HHV)	0.02	0
H-0028	Refinery Fuel Gas	Process gas	749 Btu/scf	13.7 MMBtu/hr (HHV)	119,708 MMBtu/yr (HHV)	0.02	0
H-0030	Refinery Fuel Gas	Process gas	749 Btu/scf	46.7 MMBtu/hr (HHV)	408,759 MMBtu/yr (HHV)	0.02	0
H-0040	Refinery Fuel Gas	Process gas	749 Btu/scf	46.7 MMBtu/hr (HHV)	408,759 MMBtu/yr (HHV)	0.02	0
H-0312	Refinery Fuel Gas	Process gas	749 Btu/scf	38.9 MMBtu/hr (HHV)	340,633 MMBtu/yr (HHV)	0.02	0
H-0352, H-0353, H-0354	Refinery Fuel Gas	Process gas	749 Btu/scf	222.2 MMBtu/hr (HHV)	1,946,472 MMBtu/yr (HHV)	0.02	0
H-0355	Refinery Fuel Gas	Process gas	749 Btu/scf	31.1 MMBtu/hr (HHV)	272,506 MMBtu/yr (HHV)	0.02	0
H-0362, H-0363, H-0364	Refinery Fuel Gas	Process gas	749 Btu/scf	138.9 MMBtu/hr (HHV)	1,216,545 MMBtu/yr (HHV)	0.02	0
H-0421	Refinery Fuel Gas	Process gas	749 Btu/scf	30.0 MMBtu/hr (HHV)	262,774 MMBtu/yr (HHV)	0.02	0
H-0464	Refinery Fuel Gas	Process gas	749 Btu/scf	10.7 MMBtu/hr (HHV)	93,431 MMBtu/yr (HHV)	0.02	0
H-0600	Refinery Fuel Gas	Process gas	749 Btu/scf	93.3 MMBtu/hr (HHV)	817,518 MMBtu/yr (HHV)	0.02	0
H-0601	Refinery Fuel Gas	Process gas	749 Btu/scf	86.7 MMBtu/hr (HHV)	759,124 MMBtu/yr (HHV)	0.02	0
H-2421	Refinery Fuel Gas	Process gas	749 Btu/scf	30.0 MMBtu/hr (HHV)	262,774 MMBtu/yr (HHV)	0.02	0

	Fuel Type (low sulfur Diesel, ultra low sulfur diesel, Natural Gas, Coal raw/field natural gas, process gas			Sı	pecify Units		
Unit No.	diesel, Natural Gas, Coal,)	pipeline quality natural gas, residue gas, raw/field natural gas, process gas (e.g. SRU tail gas) or other	Lower Heating Value	Hourly Usage	Annual Usage	% Sulfur	% Ash
H-2501	Refinery Fuel Gas	Process gas	749 Btu/scf	133.3 MMBtu/hr (HHV)	1,167,883 MMBtu/yr (HHV)	0.02	0
H-3101	Refinery Fuel Gas	Process gas	749 Btu/scf	12.2 MMBtu/hr (HHV)	107,056 MMBtu/yr (HHV)	0.02	0
H-3402	Refinery Fuel Gas	Process gas	749 Btu/scf	57.8 MMBtu/hr (HHV)	506,083 MMBtu/yr (HHV)	0.02	0
H-3403	Refinery Fuel Gas	Process gas	749 Btu/scf	35.6 MMBtu/hr (HHV)	311,436 MMBtu/yr (HHV)	0.02	0
H-5401	Refinery Fuel Gas	Process gas	749 Btu/scf	21.5 MMBtu/hr (HHV)	188,029 MMBtu/yr (HHV)	0.02	0
H-8801/8802	PSA OffGas & Refinery Fuel Gas	Process gas	PSA Offgas: 975 Btu/sef RFG: 749 Btu/sef	168.9 MMBtu/hr (HHV)	1,479,319 MMBtu/yr (HHV)	PSA Offgas: 0.0001 Btu/scf RFG: 0.02 Btu/scf	0
H-9851	PSA OffGas & Refinery Fuel Gas	Process gas	PSA Offgas: 975 Btu/scf RFG: 749 Btu/scf	374.4 MMBtu/hr (HHV)	3,279,805 MMBtu/yr (HHV)	PSA Offgas: 0.0001 Btu/scf RFG: 0.02 Btu/scf	0
MG-0001	Diesel	Refinery Product	137,000 Btu/scf	4.5 MMBtu/hr (HHV)	39,245 MMBtu/yr (HHV)	0.0015	0
MG-0002	Diesel	Refinery Product	137,000 Btu/gal	4.48 MMBtu/hr	39,245 MMBtu/yr	0.0015	0
MG-0003	Diesel	Refinery Product	137,000 Btu/scf	2.2 MMBtu/hr (HHV)	19,342 MMBtu/yr (HHV)	0.0015	0
MG-0004	Diesel	Refinery Product	137,000 Btu/gal	11.20 MMBtu/hr	98,112 MMBtu/yr	0.0015	0
SG-0100	Diesel	Refinery Product	137,000 Btu/scf	0.8 MMBtu/hr (HHV)	7,288 MMBtu/yr (HHV)	0.0015	0
SG-0101	Diesel	Refinery Product	137,000 Btu/gal	0.86 MMBtu/hr	7,569 MMBtu/yr	0.0015	0
SG-0102	Diesel	Refinery Product	137,000 Btu/scf	1.6 MMBtu/hr (HHV)	13,908 MMBtu/yr (HHV)	0.0015	0
FWG-0600	Diesel	Refinery Product	137,000 Btu/gal	6.02 MMBtu/hr	52,700 MMBtu/yr	0.0015	0
FWG-0601	Diesel	Refinery Product	137,000 Btu/scf	6.0 MMBtu/hr (HHV)	52,700 MMBtu/yr (HHV)	0.0015	0
FWG-0602	Diesel	Refinery Product	137,000 Btu/gal	6.02 MMBtu/hr	52,700 MMBtu/yr	0.0015	0
FWG-0603	Diesel	Refinery Product	137,000 Btu/scf	4.9 MMBtu/hr (HHV)	42,749 MMBtu/yr (HHV)	0.0015	0

Table 2-K: Liquid Data for Tanks Listed in Table 2-L

For each tank, list the liquid(s) to be stored in each tank. If it is expected that a tank may store a variety of hydrocarbon liquids, enter "mixed hydrocarbons" in the Composition column for that tank and enter the corresponding data of the most volatile liquid to be stored in the tank. If tank is to be used for storage of different materials, list all the materials in the "All Calculations" attachment, run the newest version of TANKS on each, and use the material with the highest emission rate to determine maximum uncontrolled and requested allowable emissions rate. The permit will specify the most volatile category of liquids that may be stored in each tank. Include appropriate tank-flashing modeling input data. Use additional sheets if necessary. Unit and stack numbering must correspond throughout the application package.

					Vapor	Average Stor	age Conditions	Max Storag	ge Conditions
Tank No.	SCC Code	Material Name	Composition	Liquid Density (lb/gal)	Molecular Weight (lb/lb*mol)	Temperature (°F)	True Vapor Pressure (psia)	Temperature (°F)	True Vapor Pressure (psia)
T-0011	40301150	High Vapor Pressure	Varies	5.60	62	72.5	9.1	100	11.1
T-0012	40301150	High Vapor Pressure	Varies	5.60	62	68.0	8.4	100	11.1
T-0020	40301150	High Vapor Pressure	Varies	5.60	62	65.7	8.1	100	11.1
T-0021	40301150	High Vapor Pressure	Varies	5.60	62	65.7	8.1	100	11.1
T-0022	40301150	High Vapor Pressure	Varies	5.60	62	65.7	8.0	100	11.1
T-0023	40301150	High Vapor Pressure	Varies	5.60	62	65.7	8.0	100	11.1
T-0040	40301099	Low Vapor Pressure	Varies	7.10	130	66.7	0.01	75	0.01
T-0041	40301099	Low Vapor Pressure	Varies	7.10	130	66.7	0.01	75	0.01
T-0049	40301099	Moderate Vapor Pressure	Varies	7.10	130	66.9	1.6	75	1.9
T-0055	40301099	Low Vapor Pressure	Varies	7.10	130	118.6	0.04	126	1.5
T-0056	40301150	Moderate Vapor Pressure	Varies	6.40	80	67.6	1.9	100	11.1
T-0059	40301099	Low Vapor Pressure	Varies	7.00	130	74.6	0.01	87	0.02
T-0061	40301099	Low Vapor Pressure	Varies	7.00	130	75.0	0.01	88	0.02
T-0063	40301099	Low Vapor Pressure	Varies	7.10	130	78.4	0.01	91	0.02
T-0065	40301099	Low Vapor Pressure	Varies	7.10	130	79.4	0.01	92	0.75
T-0075	40301099	Low Vapor Pressure	Varies	7.10	130	74.7	0.01	87	0.75
T-0079	40301150	High Vapor Pressure	Varies	5.60	62	72.8	9.1	100	11.1
T-0081	40301099	Low Vapor Pressure	Varies	Varies	84	208.3	0.004	330	0.75
T-0082	40301099	Low Vapor Pressure	Varies	Varies	84	173.7	0.001	321	0.75
T-0106	40301150	Moderate Vapor Pressure	Varies	5.60	66	70.7	7.0	100	11.1
T-0107	40301150	High Vapor Pressure	Varies	5.60	62	71.6	9.0	100	11.1
T-0108	40301150	High Vapor Pressure	Varies	5.60	62	79.4	10.3	100	11.1
T-0109	40301150	High Vapor Pressure	Varies	5.60	62	78.3	10.1	100	11.1
T-0110	40301099	Low Vapor Pressure	Varies	Varies	84	289.3	0.04	317	0.1
T-0111	40301150	High Vapor Pressure	Varies	5.60	62	77.9	10.0	100	11.1
T-0112	40301150	Moderate Vapor Pressure	Varies	6.40	80	67.2	1.9	100	11.1
T-0117	40301150	Moderate Vapor Pressure	Varies	6.40	80	67.7	1.9	100	11.1
T-0124	40301150	High Vapor Pressure	Varies	5.60	62	68.0	8.4	100	11.1
T-0400	40301099	Low Vapor Pressure	Varies	7.10	130	131.2	0.1	144	1.5

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				Liquid Density (lb/gal)	Vapor	Average Stor	age Conditions	Max Storag	ge Conditions
Tank No.	SCC Code	Material Name	Composition	Density	Wapor Molecular Weight (lb/lb*mol)	Temperature (°F)	True Vapor Pressure (psia)	Temperature (°F)	True Vapor Pressure (psia)
T-0401	40301150	High Vapor Pressure	Varies	5.60	62	70.8	8.8	100	11.1
T-0402	40301150	Moderate Vapor Pressure	Varies	5.60	66	70.7	6.3	100	11.1
T-0410	40301099	Low Vapor Pressure	Varies	Varies	84	278.5	0.03	312	1.5
T-0411	40301150	High Vapor Pressure	Varies	5.60	62	68.3	8.4	100	11.1
T-0412	40301150	Moderate Vapor Pressure	Varies	6.40	80	68.3	1.9	100	11.1
T-0413	40301150	Moderate Vapor Pressure	Varies	7.00	130	72.9	0.5	100	11.1
T-0415	40301150	High Vapor Pressure	Varies	5.60	62	67.4	8.3	100	11.1
T-0417	40301150	High Vapor Pressure	Varies	5.60	62	71.3	8.9	100	11.1
T-0418	40301150	High Vapor Pressure	Varies	7.00	130	75.7	0.5	100	11.1
T-0419	40301099	Low Vapor Pressure	Varies	7.10	130	75.7	0.01	83	0.5
T-0420	40301099	Low Vapor Pressure	Varies	Varies	84	131.4	0.0002	339	0.2
T-0422	40301099	Low Vapor Pressure	Varies	7.00	130	99.8	0.03	106	0.03
T-0423	40301099	Low Vapor Pressure	Varies	7.00	130	106.4	0.03	113	0.04
T-0431	40301099	Low Vapor Pressure	Varies	7.10	130	177.8	0.2	266	0.8
T-0432	40301099	Low Vapor Pressure	Varies	7.10	130	186.5	0.2	259	0.7
T-0433	40301099	Low Vapor Pressure	Varies	7.10	130	120.7	0.1	130	0.1
T-0434	40301099	Moderate Vapor Pressure	Varies	7.10	130	65.9	0.3	72	0.75
T-0435	40301150	Moderate Vapor Pressure	Varies	5.60	66	66.7	6.6	100	11.1
T-0437	40301150	High Vapor Pressure	Varies	7.10	58	69.2	6.9	100	11.1
T-0438	40301099	Low Vapor Pressure	Varies	7.10	130	99.0	0.03	112	1.5
T-0439	40301150	Moderate Vapor Pressure	Varies	5.60	66	71.3	7.5	100	11.1
T-0450	40301150	Moderate Vapor Pressure	Varies	5.60	66	68.6	7.1	100	11.1
T-0451	40301150	Moderate Vapor Pressure	Varies	7.10	130	74.5	0.4	100	11.1
T-0452	40301150	Moderate Vapor Pressure	Varies	6.59	46.07	66.3	0.8	100	11.1
T-0737	40301150	Moderate Vapor Pressure	Varies	5.60	66	66.8	6.6	100	11.1
T-0802	40301150	Moderate Vapor Pressure	Varies	5.60	66	66.7	6.6	100	11.1
T-0814	40301099	Low Vapor Pressure	Varies	Varies	84	370.3	0.3	407	0.75
T-0815	40301099	Low Vapor Pressure	Varies	7.10	130	65.9	0.01	72	0.5
T-0821	40301150	Moderate Vapor Pressure	Varies	5.60	66	68.2	6.0	100	11.1
T-0834	40301150	Moderate Vapor Pressure	Varies	7.10	130	72.8	0.4	100	1.9
T-0835	40301150	Moderate Vapor Pressure	Varies	7.10	130	72.9	0.4	100	11.1
T-0838	40301099	Low Vapor Pressure	Varies	7.10	130	78.6	0.01	85	0.75
T-1225	40301150	High Vapor Pressure	Varies	7.10	58	69.3	6.9	100	11.1
T-1227	40301099	Low Vapor Pressure	Varies	Varies	84	385.3	0.4	450	0.75

Table 2-L: Tank Data

Include appropriate tank-flashing modeling input data. Use an addendum to this table for unlisted data categories. Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary. See reference Table 2-L2.

Note: 1.00 bbl = 10.159 M3 = 42.0 gal

Tank No.	Date Installed	Materials Stored	Seal Type (refer to Table 2-LR below)	Roof Type (refer to Table 2-	Capa	city ⁽¹⁾	Diameter (M)	Vapor Space		olor ble VI-C)	Paint Condition (from Table VI-	Annual Throughput	Turn- overs
	Instancu		(Telef to Table 2-ER below)	LR below)	(bbl)	(M ³)	(141)	(M)	Roof	Shell	(from Table VI-	(gal/yr)	(per year)
T-0011	<1973	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	32,130	5,100	27.1	N/A	White	White	New	84,000,000	N/A
T-0012	<1973	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	32,130	5,100	27.1	N/A	White	White	New	84,000,000	N/A
T-0020	2020	High Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Shoe-mounted	IF	54,380	8,632	27.4	N/A	White	White	New	75,600,000	N/A
T-0021	2020	High Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Shoe-mounted	IF	54,380	8,632	27.4	N/A	White	White	New	75,600,000	N/A
T-0022	2020	High Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Shoe-mounted	IF	37,770	5,995	22.9	N/A	White	White	New	75,600,000	N/A
T-0023	2020	High Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Shoe-mounted	IF	37,770	5,995	22.9	N/A	White	White	New	75,600,000	N/A
T-0040	<1973	Low Vapor Pressure	N/A	FX	820	130	2.7	11.0	White	White	Aged	1,176,000	1,483
T-0041	1973	Low Vapor Pressure	N/A	FX	820	130	2.7	11.0	White	White	Aged	1,176,000	1,483
T-0049	1965	Moderate Vapor Pressure	N/A	FX	610	97	3.4	1.3	White	White	Aged	18,882,799	30,986
T-0055	1979	Low Vapor Pressure	N/A	FX	10,200	1,619	13.7	5.6	White	White	Average	45,728,406	4,747
T-0056	<1973	Moderate Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	11,600	1,841	14.6	N/A	White	White	Average	413,910,000	N/A
T-0059	<1973	Low Vapor Pressure	N/A	FX	5,140	816	10.7	4.7	Black	Black	Average	1,998,288	416
T-0061	<1973	Low Vapor Pressure	N/A	FX	10,490	1,665	15.2	4.7	Black	Black	Average	42,490,997	4,339
T-0063	<1973	Low Vapor Pressure	N/A	FX	10,910	1,732	15.5	4.7	Black	Black	Average	18,082,540	1,775
T-0065	1999	Low Vapor Pressure	N/A	FX	10,490	1,665	15.2	4.7	Black	Black	Average	18,082,540	1,846
T-0075	2003	Low Vapor Pressure	N/A	FX	18,910	3,002	19.8	5.1	Black	Black	Aged	18,082,540	1,020
T-0079	2008	High Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	87,420	13,876	38.1	N/A	White	White	New	242,760,000	N/A
T-0081	2010	Low Vapor Pressure	N/A	FX	65,870	10,456	33.1	6.4	Aluminum - Specular	Aluminum - Specular	Average	210,000,000	3,356
T-0082	2010	Low Vapor Pressure	N/A	FX	109,660	17,406	42.7	6.5	Aluminum - Specular	Aluminum - Specular	Average	252,000,000	2,418
T-0106	<1971	Moderate Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	25,120	3,987	20.4	N/A	White	White	New	100,380,000	N/A
T-0107	<1971	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	25,120	3,987	20.4	N/A	White	White	New	134,290,800	N/A
T-0108	<1951	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	25,120	3,987	20.4	N/A	White	White	Average	117,466,188	N/A
T-0109	<1971	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	25,120	3,987	20.4	N/A	White	White	Aged	144,984,000	N/A
T-0110	1929	Low Vapor Pressure	N/A	FX	57,100	9,063	32.9	5.7	Aluminum - Specular	Aluminum - Specular	Average	220,752,000	4,099
T-0111	<1973	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	10,080	1,600	14.9	N/A	White	White	Aged	59,430,000	N/A

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Tank No.	Date	Materials Stored	Seal Type (refer to Table 2-LR below)	Roof Type (refer to Table 2-	Capa	ncity ⁽¹⁾	Diameter	Vapor Space		olor ible VI-C)	Paint Condition	Annual Throughput	Turn- overs
	Installed		(refer to Table 2-LK below)	LR below)	(bbl)	(M ³)	(M)	(M)	Roof	Shell	(from Table VI- C)	(gal/yr)	(per year)
T-0112	<1973	Moderate Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	9,670	1,535	14.6	N/A	White	White	Average	1,260,000	N/A
T-0117	1960	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	15,470	2,456	14.6	N/A	White	White	New	54,264,000	N/A
T-0124	1981	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	6,710	1,065	12.2	N/A	White	White	New	96,936,000	N/A
T-0400	1983	Low Vapor Pressure	N/A	FX	96,680	15,346	36.6	7.7	Black	Black	Aged	306,600,000	3,309
T-0401	1982	High Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	FALSE	56,650	8,992	27.4	N/A	White	White	New	214,620,000	N/A
T-0402	1983	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	56,650	8,992	27.4	N/A	White	White	New	260,610,000	N/A
T-0410	1973	Low Vapor Pressure	N/A	FX	34,920	5,543	24.1	6.3	Aluminum - Specular	Aluminum - Specular	Average	220,752,000	6,653
T-0411	1951	High Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	55,950	8,881	30.5	N/A	White	White	Average	134,290,800	N/A
T-0412	1951	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	55,950	8,881	30.5	N/A	White	White	Average	54,264,000	N/A
T-0413	1960	Moderate Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	24,490	3,887	20.4	N/A	White	White	New	206,955,000	N/A
T-0415	1953	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	25,120	3,987	20.4	N/A	White	White	New	144,984,000	N/A
T-0417	<1973	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	10,490	1,665	15.2	N/A	White	White	Aged	59,430,000	N/A
T-0418	>2021	High Vapor Pressure	Primary Seal: Vapor-mounted Secondary Seal: Rim-mounted	IF	20,720	3,289	20.4	N/A	White	White	New	176,400,000	N/A
T-0419	<1973	Low Vapor Pressure	N/A	FX	11,000	1,746	16.2	4.4	White	White	Average	153,300,000	15,004
T-0420	<1973	Low Vapor Pressure	N/A	FX	10,490	1,665	15.2	4.7	Aluminum - Specular	Aluminum - Specular	Average	4,074,939	416
T-0422	<1973	Low Vapor Pressure	N/A	FX	10,490	1,665	15.2	4.7	White	White	New	42,086,320	4,298
T-0423	1970	Low Vapor Pressure	N/A	FX	10,490	1,665	15.2	4.7	White	White	New	42,490,997	4,339
T-0431	<1973	Low Vapor Pressure	N/A	FX	53,180	8,441	33.2	5.2	Aluminum - Specular	Aluminum - Specular	Average	16,556,400	332
T-0432	<1972	Low Vapor Pressure	N/A	FX	53,180	8,441	33.2	5.2	Aluminum - Specular Rust - Red	Aluminum - Specular Rust - Red	Average	19,370,988	388
T-0433	<1973	Low Vapor Pressure	N/A	FX	80,420	12,765	35.7	6.8	Iron Oxide	Iron Oxide	Aged	173,250,000	2,262
T-0434	1979	Moderate Vapor Pressure	N/A Primary Seal: Mechanical Shoe	FX	80,420	12,765	35.7	6.8	White	White	New	315,000,000	4,112
T-0435	1997 Tank was built	Moderate Vapor Pressure	Secondary Seal: Rim-mounted	EF	5,040	800	9.1	N/A	White	White	New	110,376,000	N/A
T-0437	in 1976 and relocated in 2009	High Vapor Pressure	Primary Seal: Liquid-mounted Secondary Seal: Rim-mounted	EF	90,640	14,387	36.6	N/A	White	White	New	703,668,000	N/A
T-0438	1978	Low Vapor Pressure	N/A	FX	54,380	8,632	27.4	7.6	Black	Black	Aged	173,250,000	3,324
T-0439	1978	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	IF	108,740	17,260	39.6	N/A	White	White	Average	758,835,000	N/A
T-0450	1997	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	80,570	12,789	36.6	N/A	White	White	New	413,910,000	N/A
T-0451	2016	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	IF	6,850	1,087	10.7	N/A	Aluminum - Specular	Aluminum - Specular	Average	39,858,000	N/A
T-0452	2016	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	IF	6,850	1,087	10.7	N/A	White	White	Average	5,978,700	N/A

Tank No.	Date Installed	Materials Stored	Seal Type (refer to Table 2-LR below)	Roof Type (refer to Table 2-	Сара	city ⁽¹⁾	Diameter (M)	Vapor Space		lor ble VI-C)	Paint Condition (from Table VI	Annual Throughput	Turn- overs
	Instanca		(refer to ruble 2 Ert below)	LR below)	(bbl)	(M ³)	(111)	(M)	Roof	Shell	C)	(gal/yr)	(per year)
T-0737	2009	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	22,210	3,525	19.2	N/A	White	White	New	210,252,000	N/A
T-0802	2002	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	11,330	1,798	13.7	N/A	White	White	New	210,252,000	N/A
T-0814	2005	Low Vapor Pressure	N/A	FX	11,190	1,776	15.2	5.0	Aluminum - Specular	Aluminum - Specular	Average	141,120,000	13,450
T-0815	2005	Low Vapor Pressure	N/A	FX	80,930	12,846	35.4	6.9	White	White	New	1,096,095,000	14,201
T-0821	2016	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	78,580	12,473	32.3	N/A	White	White	Average	268,581,600	N/A
T-0834	1967	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: None	EF	40,420	6,416	25.9	N/A	White	White	Average	659,190,000	N/A
T-0835	<1973	Moderate Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	68,940	10,943	33.8	N/A	White	White	Average	659,190,000	N/A
T-0838	1977	Low Vapor Pressure	N/A	FX	30,640	4,863	22.6	6.3	White	White	New	659,190,000	22,644
T-1225	2009	High Vapor Pressure	Primary Seal: Mechanical Shoe Secondary Seal: Rim-mounted	EF	125,890	19,983	45.7	N/A	White	White	Average	1,600,452,000	N/A
T-1227	2009	Low Vapor Pressure	N/A	FX	33,170	5,265	23.5	6.3	Aluminum - Specular	Aluminum - Specular	Average	36,792,000	1,167

Notes:
(1) Tank shell capacity
(2) Vapor Space Outage (Hvo), per AP-42, Ch. 7.1 (6/20), Eq. 1-16

Table 2-L2: Liquid Storage Tank Data Codes Reference Table

Seal Type, Welded Tank Seal Type Mechanical Shoe Seal Liquid-mounted resilient		Seal Type, Rivet	ted Tank Seal Type	Roof, Shell Color	Paint Condition
Mechanical Shoe Seal	Liquid-mounted resilient seal	Vapor-mounted resilient seal	Seal Type	WH: White	Good
A: Primary only	A: Primary only	A: Primary only	A: Mechanical shoe, primary only	AS: Aluminum (specular)	Poor
B: Shoe-mounted secondary	B: Weather shield	B: Weather shield	B: Shoe-mounted secondary	AD: Aluminum (diffuse)	
C: Rim-mounted secondary	C: Rim-mounted secondary	C: Rim-mounted secondary	C: Rim-mounted secondary	LG: Light Gray	ĺ
l	Mechanical Shoe Seal A: Primary only 3: Shoe-mounted secondary	Mechanical Shoe Seal Liquid-mounted resilient seal A: Primary only A: Primary only B: Weather shield	Mechanical Shoe Seal Liquid-mounted resilient seal Vapor-mounted resilient seal A: Primary only A: Primary only A: Primary only B: Weather shield B: Weather shield	Mechanical Shoe Seal Liquid-mounted resilient seal Vapor-mounted resilient seal Seal Type A: Primary only A: Primary only A: Mechanical shoe, primary only B: Weather shield B: Weather shield B: Shoe-mounted secondary	Mechanical Shoe Seal Liquid-mounted resilient seal Vapor-mounted resilient seal Seal Type WH: White A: Primary only A: Primary only A: Primary only A: Primary only A: Mechanical shoe, primary only AS: Aluminum (specular) B: Weather shield B: Shoe-mounted secondary AD: Aluminum (diffuse)

Note: $1.00 \text{ bbl} = 0.159 \text{ M}^3 = 42.0 \text{ gal}$

MG: Medium Gray

BL: Black

OT: Other (specify)

Table 2-M: Materials Processed and Produced (Use additional sheets as necessary.)

	Materi	al Processed		M	Iaterial Produced		
Description	Chemical Composition	Phase (Gas, Liquid, or Solid)	Quantity (specify units)	Description	Chemical Composition	Phase	Quantity (specify units)
Crude Oil	Mixed Hydrocarbons	Liquid	N/A-Varies	Butanes	Butanes	Gas	N/A-Varies
Casinghead Gas	Mixed Hydrocarbons	Liquid	N/A-Varies	Propanes	Propanes	Gas	N/A-Varies
Transmix	Mixed Hydrocarbons	Liquid	N/A-Varies	Liquified Petroleum Gas	Butanes, Propanes	Gas	N/A-Varies
Isobutane	Isobutane	Gas	N/A-Varies	Refinery Gas	Mixed Hydrocarbons	Gas	N/A-Varies
Raw Kerosenes	Mixed Hydrocarbons	Liquid	N/A-Varies	Kerosenes	Mixed Hydrocarbons	Liquid	N/A-Varies
Raw Jet Fuels	Mixed Hydrocarbons	Liquid	N/A-Varies	Jet Fuels	Mixed Hydrocarbons	Liquid	N/A-Varies
Naphthas	Mixed Hydrocarbons	Liquid	N/A-Varies	Naphthas	Mixed Hydrocarbons	Liquid	N/A-Varies
Raw Gasolines	Mixed Hydrocarbons	Liquid	N/A-Varies	Gasolines	Mixed Hydrocarbons	Liquid	N/A-Varies
Gas Oils	Mixed Hydrocarbons	Liquid	N/A-Varies	Diesel Fuels	Mixed Hydrocarbons	Liquid	N/A-Varies
Asphalts	Mixed Hydrocarbons	Liquid	N/A-Varies	Gas Oils	Mixed Hydrocarbons	Liquid	N/A-Varies
				Fuel Oils	Mixed Hydrocarbons	Liquid	N/A-Varies
				Asphalts	Mixed Hydrocarbons	Liquid	N/A-Varies
				Carbon Black Oil	Mixed Hydrocarbons	Liquid	N/A-Varies
				Pitch	Mixed Hydrocarbons	Liquid	N/A-Varies
				Sulfur	Sulfur	Liquid	N/A-Varies

Table 2-N: CEM Equipment

Enter Continuous Emissions Measurement (CEM) Data in this table. If CEM data will be used as part of a federally enforceable permit condition, or used to satisfy the requirements of a state or federal regulation, include a copy of the CEM's manufacturer specification sheet in the Information Used to Determine Emissions attachment. Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary.

Stack No.	Pollutant(s)	Manufacturer	Model No.	Serial No.	Sample Frequency	Averaging Time	Range	Sensitivity	Accuracy
FCC Regen	O2	Servomex	X 4902C1	04902C1-3747	< 15 sec		0-10%	0.0001	< 0.05%
FCC Regen	SO2	California Analytical	ZRF1AGY2-2EJYY	A2P0815T	0.25 sec		0-2,000 ppm	20 ppm	10 ppm
FCC Regen	CO/CO2	Servomex	Xentra 4904C1	04904C1-3746	< 30 sec		0-1000 ppm	2 ppm	2 ppm
FCC Regen	NOx	California Analytical	600-CLD Digital	PO2056	< 2 sec		0-300 ppm	3 ppm	1.5 ppm
H-2501	NOx/O2	Thermo Scientific	42ILS-ASSSSPCB	901534190	NOx < 2 sec $O2 < 30 sec$		NOx 0-50 ppm O2 0-10%	O2 0.5 ppm zero	O2 0.5 ppm zero
H-2501	СО	Thermo Scientific	48i-ANPCB	809828981	< 15 sec		0-2000 ppm	0.0001	< 0.05%
H-0473 (SRU2 TGI)	SO2	California Analytical	ZPA2	N8A0263	<=60 sec		0-2,500 ppm	25 ppm	17.5 ppm
H-0473 (SRU2 TGI)	O2	Servomex	04900C1	653036	< 15 sec		0-25%	0.0001	< 0.05%
H-3103 (SRU3 TGI)	SO2	California Analytical	ZRE-NDIR	A8K9291T	<=60 sec		0-2,500 ppm	25 ppm	17.5 ppm
H-3103 (SRU3 TGI)	O2	Servomex	04900C1	652878	< 15 sec		0-25%	0.0001	< 0.05%
H-0601	O2	Servomex	Xendos 2700	1362	< 15 sec		0-25%	0.0001	< 0.05%
H-3402	O2	Servomex	2700 PN 02710734	276	< 15 sec		0-25%	0.0001	< 0.05%
B-0009	O2/CO	Servomex	ServoPro-4900	04900C1-653783					
B-0009	CO2	Servomex	ServoPro-4900	04900C1-653788					
B-0009	NOx	California Analytical	600-CLD	A10011			0-300 ppm	3 ppm	1.5 ppm
B-0008	NOx	California Analytical	600-CLD	E05005	< 2 sec		0-300 ppm	3 ppm	1.5 ppm
B-0008	O2	Servomex	Xentra 4902C1	04900C1-3658	< 15 sec		0-10%	0.0001	< 0.05%
B-0007	NOx	California Analytical	600-CLD	E05004	< 2 sec		0-300 ppm	3 ppm	1.5 ppm
B-0007	O2	Servomex	Xentra 4902C1	04900C1-3657	< 15 sec		0-10%	0.0001	< 0.05%
H-8801/8802	O2	California Analytical	ZRE-NDIR	N4K1912	< 15 sec		0-10%	0.0001	< 0.05%
H-8801/8802	СО	same analyzer as above	"	"	< 30 sec		0-2000 ppm	0.5-2 ppm	0.5-2 ppm

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Table 2-N: CEM Equipment

Enter Continuous Emissions Measurement (CEM) Data in this table. If CEM data will be used as part of a federally enforceable permit condition, or used to satisfy the requirements of a state or federal regulation, include a copy of the CEM's manufacturer specification sheet in the Information Used to Determine Emissions attachment. Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary.

Stack No.	Pollutant(s)	Manufacturer	Model No.	Serial No.	Sample Frequency	Averaging Time	Range	Sensitivity	Accuracy
H-8801/8802	NOx	same analyzer as above	"	"					
H-9851	O2	Servomex dual range	04900C1	653166	< 15 sec		0-10%	0.0001	< 0.05%
H-9851	СО	same analyzer as above	"	"	< 2 sec		0-2000 ppm	0.5-2 ppm	0.5-2 ppm
H-9851	NOx	California Analytical	600-CLD	W01040	< 2 sec		0-50 ppm	3 ppm	1.5 ppm
TL-4	VOC	Infrared Industries	IR8400D	4814	20 Seconds		0-2%		0.0706

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Unit No.	Parameter/Pollutant Measured	Location of Measurement	Unit of Measure	Acceptable Range	Frequency of Maintenance	Nature of Maintenance	Method of Recording	Averaging Time
HP Fuel Gas	$ m H_2S$	In the CCR division near D-0359 and near D-0770	ppmvd	0-300 ppm	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	3 hr rolling avg for regulatory requirement
LP Fuel Gas	$ m H_2S$	In the North division near D-0019	ppmvd	0-300 ppm	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	3 hr rolling avg for regulatory requirement
FL-0400	Vent Gas H2S Concentration	In the North Plant Flare header, downstream of the knockout drum	ppmvd	5-300	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	3 hr rolling avg for regulatory requirement
FL-0400	Vent Gas Total Sulfur Concentration	In the North Plant Flare header, downstream of the knockout drum	% v/v	0-50	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0400	Vent Gas Flow Velocity	In the North Plant Flare header, upstream of the flare stack, in a position that is representative of the total gas	ft/sec	0.1 - 328	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0400	Vent Gas Composition (Gas Chromatograph)	At the existing sample site ~200 ft from sampling cabinet in the flare line.	%	0-100%	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0400	Vent Gas Heating Value (Calorimeter)	At the existing sample site ~200 ft from sampling cabinet in the flare line.	BTU/scf	0-2,000	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0400	Pilot Flame Presence	On pig pen building ~530 ft SW of flare	%	0-100%	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0400	Assist Steam Flow Velocity	upstream of the control valves	lb/hr	0-37,000 lb/hr	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0400	Supplemental Gas Flow Velocity	upstream of the control valves	scfh	0-245,000 scfh	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0400	Visible Emissions Camera	On pig pen building ~530 ft SW of flare	visual	n/a	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	

Unit and stac		orrespond throughout the applic	ation package. Use	additional sheets if nec	essary.			
Unit No.	Parameter/Pollutant Measured	Location of Measurement	Unit of Measure	Acceptable Range	Frequency of Maintenance	Nature of Maintenance	Method of Recording	Averaging Time
FL-0401	Vent Gas H2S Concentration	In the South Plant Flare header, downstream of the knockout drum	ppmvd	5-300	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	3 hr rolling avg for regulatory requirement
FL-0401	Vent Gas Total Sulfur Concentration	In the South Plant Flare header, downstream of the knockout drum	% v/v	0-25	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0401	Vent Gas Flow Velocity	In the South Plant Flare header, upstream of the flare stack, in a position that is representative of the total gas flow rate	ft/sec	0.1 - 328	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0401	Vent Gas Composition (Gas Chromatograph)	At the existing sample site ~200 ft from sampling cabinet in the flare line.	BTU/scf	0-2,000	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0401	Vent Gas Heating Value (Calorimeter)	At the existing sample site ~200 ft from sampling cabinet in the flare line.	%	0-100%	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0401	Pilot Flame Presence	On South control room ~370 ft SE of flare	%	0-100%	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0401	Assist Steam Flow Velocity	upstream of the control valves	lb/hr	0-37,000 lb/hr	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0401	Supplemental Gas Flow Velocity	upstream of the control valves	scfh	0-245,000 scfh	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0401	Visible Emissions Camera	On South control room ~370 ft SE of flare	visual	n/a	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0402	Vent Gas H2S Concentration	In the FCCU Flare header, downstream of the knockout drum	ppmvd	5-300	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	3 hr rolling avg for regulatory requirement
FL-0402	Vent Gas Total Sulfur Concentration	In the FCCU Flare header, downstream of the knockout drum	% v/v	0-50	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	

Unit No.	Parameter/Pollutant Measured	Location of Measurement	Unit of Measure	Acceptable Range	Frequency of Maintenance	Nature of Maintenance	Method of Recording	Averaging Time
FL-0402	Vent Gas Flow Velocity	In the FCCU Flare header, upstream of the flare stack, in a position that is representative of the total gas	ft/sec	0.1 - 328	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0402	Vent Gas Composition (Mass Spectrometer)	At the existing sample site ~200 ft from sampling cabinet in the flare line.	%	0-100%	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0402	Vent Gas Heating Value (Mass Spectrometer)	At the existing sample site ~200 ft from sampling cabinet in the flare line.	BTU/scf	0-5,000	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0402	Pilot Flame Presence	On pig pen building ~340 ft SW of flare	%	0-100%	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0402	Assist Steam Flow Velocity	upstream of the control valves	lb/hr	0-37,000 lb/hr	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0402	Supplemental Gas Flow Velocity	upstream of the control valves	scfh	0-245,000 scfh	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0402	Visible Emissions Camera	on pig per building ~340 ft SW of building	visual	n/a	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0403	Vent Gas Flow Velocity	In the FCCU Flare header, upstream of the flare stack, in a position that is representative of the total gas	ft/sec	0.1 - 328	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0403	Vent Gas Heating Value (Mass Spectrometer)	At the existing sample site ~200 ft from sampling cabinet in the flare line.	BTU/scf	0-5,000	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0403	Pilot Flame Presence	On pig pen building ~530 ft SW of flare	%	0-100%	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0403	Assist Steam Flow Velocity	maximum total steam rate 24,000 lbs-hr	lbs-hr	0-37,000 lb/hr	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	

	Parameter/Pollutant	orrespond throughout the application					Method of	
Unit No.	Measured	Location of Measurement	Unit of Measure	Acceptable Range	Frequency of Maintenance	Nature of Maintenance	Recording	Averaging Time
FL-0403	Supplemental Gas Flow Velocity	maximum supplemental gas flow rate 245,000 scfh	scfh	0-245,000 scfh	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0403	Visible Emissions Camera	On pig pen building ~530 ft SW of flare	visual	n/a	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0404	Vent Gas H2S Concentration	In the GOHT Flare header, downstream of the knockout drum	ppmvd	5-300	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0404	Vent Gas Total Sulfur Concentration	In the GOHT Flare header, downstream of the knockout drum	% v/v	0-50	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0404	Vent Gas Flow Velocity	In the GOHT Flare header, upstream of the flare stack, in a position that is representative of the total gas	ft/sec	0.1 - 328	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0404	Vent Gas Composition (Gas Chromatograph)	At the existing sample site ~200 ft from sampling cabinet in the flare line.	%	0-100%	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	3 hr rolling avg for regulatory requirement
FL-0404	Vent Gas Heating Value (Calorimeter)	At the existing sample site ~200 ft from sampling cabinet in the flare line.	BTU/scf	0-5,000	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0404	Pilot Flame Presence	On GOHT CMS shelter ~460 ft SE of flare	%	0-100%	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0404	Assist Steam Flow Velocity	upstream of the control valves	lb/hr	0-37,000 lb/hr	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0404	Supplemental Gas Flow Velocity	upstream of the control valves	scfh	0-245,000 scfh	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	
FL-0404	Visible Emissions Camera	On GOHT CMS shelter ~460 ft SE of flare	visual	n/a	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	per manufacturer's recommendation, industry practice and Navajo Refinery maintenance experience.	Datastream	

Table 2-P: Greenhouse Gas Emissions

Applications submitted under 20.2.70, 20.2.72, & 20.2.74 NMAC are required to complete this Table. Power plants, Title V major sources, and PSD major sources must report and calculate all GHG emissions for each unit. Applicants must report potential emission rates in short tons per year (see Section 6.a for assistance). Include GHG emissions during Startup, Shutdown, and Scheduled Maintenance in this table. For minor source facilities that are not power plants, are not Title V, or are not PSD, there are three options for reporting GHGs 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of the report all combustion source GHGs as a single unit and all venting GHG as a second separate unit; OR 3) check the following box \Box By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

		CO ₂ ton/yr	N ₂ O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ton/yr²					Total GHG Mass Basis ton/yr ⁴	Total CO ₂ e ton/yr ⁵
Unit No.	GWPs 1	1	298	25	22,800	footnote 3						
B-0007	mass GHG	136,084	1.4	6.9							136,092	
B 0007	CO ₂ e	136,084	412.4	173.0								136,669
B-0008	mass GHG	136,084	1.4	6.9							136,092	
	CO ₂ e	136,084	412.4	173.0								136,669
B-0009	mass GHG	139,248	1.4	7.1							139,257	
	CO ₂ e	139,248	422.0	177.0								139,847
H-0009	mass GHG	27,850	0.3	1.4							27,851	
	CO ₂ e	27,850	84.4	35.4								27,969
H-0011	mass GHG	24,052	0.2	1.2							24,053	
	CO ₂ e	24,052	72.9	30.6								24,155
H-0018	mass GHG	20,254	0.2	1.0							20,256	
	CO ₂ e	20,254	61.4	25.7								20,341
H-0019	mass GHG	34,179	0.3	1.7							34,181	
	CO ₂ e	34,179	103.6	43.4								34,326
H-0020	mass GHG	56,965	0.6	2.9							56,969	
	CO ₂ e	56,965	172.6	72.4								57,210
H-0028	mass GHG	7,785	0.1	0.4							7,786	
	CO ₂ e	7,785	23.6	9.9								7,819
H-0030	mass GHG	26,584	0.3	1.4							26,585	
	CO ₂ e	26,584	80.6	33.8								26,698
H-0040	mass GHG	26,584	0.3	1.4							26,585	
11 00 10	CO ₂ e	26,584	80.6	33.8								26,698
H-0312	mass GHG	22,153	0.2	1.1							22,154	
11 0312	CO ₂ e	22,153	67.1	28.2								22,248
H-0352,	mass GHG	126,589	1.3	6.4							126,597	
H-0353, H-0354	CO2e	126,589	383.6	160.9								127,134
H-0355	mass GHG	17,723	0.2	0.9							17,724	
11-0333	CO ₂ e	17,723	53.7	22.5								17,799
H-0362,	mass GHG	79,118	0.8	4.0							79,123	
H-0363, H-0364	CO ₂ e	79,118	239.8	100.6								79,459
H-0421	mass GHG	17,090	0.2	0.9							17,091	
11-0421	CO ₂ e	17,090	51.8	21.7								17,163
H-0464	mass GHG	6,076	0.1	0.3							6,077	
11-0404	CO ₂ e	6,076	18.4	7.7								6,102
H-0600	mass GHG	53,168	0.5	2.7							53,171	
H-0000	CO ₂ e	53,168	161.1	67.6								53,396
II 0/01	mass GHG	49,370	0.5	2.5							49,373	
H-0601	CO ₂ e	49,370	149.6	62.8								49,582
II 2421	mass GHG	17,090	0.2	0.9							17,091	
H-2421	CO ₂ e	17,090	51.8	21.7								17,163

Table 2-P: Greenhouse Gas Emissions

Applications submitted under 20.2.70, 20.2.72, & 20.2.74 NMAC are required to complete this Table. Power plants, Title V major sources, and PSD major sources must report and calculate all GHG emissions for each unit. Applicants must report potential emission rates in short tons per year (see Section 6.a for assistance). Include GHG emissions during Startup, Shutdown, and Scheduled Maintenance in this table. For minor source facilities that are not power plants, are not Title V, or are not PSD, there are three options for reporting GHGs i) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHG as a second separate unit; OR 3) check the following box \Box By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

		CO ₂ ton/yr	N ₂ O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ton/yr²					To GHG Basis	Mass	Total CO ₂ e ton/yr ⁵
Unit No.	GWPs 1	1	298	25	22,800	footnote 3							
H-2501	mass GHG	75,954	0.8	3.9							75,	958	
11 2301	CO ₂ e	75,954	230.2	96.6									76,280
H-3101	mass GHG	6,962	0.1	0.4							6,9	63	
113101	CO2e	6,962	21.1	8.9									6,992
H-3402	mass GHG	32,913	0.3	1.7							32,	915	
	CO ₂ e	32,913	99.7	41.8									33,055
H-3403	mass GHG	20,254	0.2	1.0							20,	256	
	CO ₂ e	20,254	61.4	25.7									20,341
H-5401	mass GHG	12,229	0.1	0.6							12,	229	
	CO ₂ e	12,229	37.1	15.5									12,281
H-8801/8802	mass GHG	96,208	1.0	4.9							96,	214	
	CO ₂ e	96,208	291.6	122.3									96,622
H-9851	mass GHG	213,303	2.2	10.8							213	316	24 4 224
	CO ₂ e	213,303	646.4	271.1							- 10		214,221
H-0473	mass GHG	13,914									13,)14	12.011
(SRU2 TGI)	CO ₂ e	13,914									16	22	13,914
H-3103 (SRU3 TGI)	mass GHG	16,233									16,	233	16.000
(SKUS TGI)	CO ₂ e	16,233 430,013	2.5	12.6							430	020	16,233
FCC Regen	mass GHG CO ₂ e	430,013	749.0	314.7							430	028	431,077
	mass GHG	10,384	0.02	314.7							10,	115	431,077
FL-400	CO ₂ e	10,384	5.2	774.9							10,	113	11,164
	mass GHG	3,523	0.01	10.5							3,5	3/1	11,104
FL-401	CO ₂ e	3,523	1.7	262.9							3,0	54	3,788
	mass GHG	4,220	0.01	12.6							4,2	33	3,766
FL-402	CO ₂ e	4,220	2.1	314.9							7,2	33	4,537
	mass GHG	4,824	0.01	14.4							4,8	39	1,557
FL-403	CO ₂ e	4,824	2.4	360.0							.,,	-	5,187
	mass GHG	44,784	0.1	133.7							44,	917	5,107
FL-404	CO ₂ e	44,784	22.2	3,342.1						 	1.,		48,148
	mass GHG	1,600	0.01	0.06							1,6	00	,
MG-0001	CO ₂ e	1,600	3.9	1.6							-,,		1,605
	mass GHG	1,600	0.01	0.06							1,6	00	-,
MG-0002	CO2e	1,600	3.9	1.6							-,,		1,605
	mass GHG	788	0.01	0.03							78	8	,
MG-0003	CO ₂ e	788	1.9	0.8									791
	mass GHG	46	0.0004	0.002							4	5	
MG-0004	CO ₂ e	46	0.1	0.05							<u> </u>		46

Table 2-P: Greenhouse Gas Emissions

Applications submitted under 20.2.70, 20.2.72, & 20.2.74 NMAC are required to complete this Table. Power plants, Title V major sources, and PSD major sources must report and calculate all GHG emissions for each unit. Applicants must report potential emission rates in short tons per year (see Section 6.a for assistance). Include GHG emissions during Startup, Shutdown, and Scheduled Maintenance in this table. For minor source facilities that are not power plants, are not Title V, or are not PSD, there are three options for reporting GHGs i) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHG as a second separate unit; OR 3) check the following box \Box By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

		CO ₂ ton/yr	N ₂ O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ton/yr²					Total GHG Mass Basis ton/yr ⁴	Total CO ₂ e ton/yr ⁵
Unit No.	GWPs 1	1	298	25	22,800	footnote 3						
SG-0100	mass GHG	17	0.0001	0.001							17	
30-0100	CO ₂ e	17	0.04	0.02								17
SG-0101	mass GHG	18	0.0001	0.001							18	
50-0101	CO ₂ e	18	0.04	0.02								18
SG-0102	mass GHG	32	0.0003	0.001							32	
56 0102	CO ₂ e	32	0.1	0.03								32
FWG-0600	mass GHG	25	0.0002	0.001							25	
1 11 3 0000	CO ₂ e	25	0.1	0.02								25
FWG-0601	mass GHG	25	0.0002	0.001							25	
1 11 3 0001	CO ₂ e	25	0.1	0.02								25
FWG-0602	mass GHG	25	0.0002	0.001							25	
1 11 0 0002	CO ₂ e	25	0.1	0.02								25
FWG-0603	mass GHG	20	0.0002	0.001							20	
1 11 0 0000	CO ₂ e	20	0.05	0.02								20
TL-4 VCU	mass GHG	1,359	0.01	0.06							1,359	
12	CO ₂ e	1,359	3.4	1.4								1,363
Fugitives	mass GHG	817	0.005	26.26							843	
- T ugilives	CO ₂ e	817	1.4	656.5								1,474
Tanks	mass GHG			6.05							6.0	
	CO ₂ e			151								151
FL-HEP-PORT	mass GHG	165	0.0003	0.54							166	
	CO2e	165	0.1	13.6								179
Tanks VCU	mass GHG	43	0.0002	0.001							43	
	CO ₂ e	43	0.1	0.03								43
Total	mass GHG	2,016,340	17.75	323.21							2,016,681	
	CO ₂ e	2,016,340	5,288.5	8,080.36		A Lof 40 CEP part						2,029,709

TGWP (Global Warming Potential): Applicants must use the most current GWPs codified in Table A-1 of 40 CFR part 98. GWPs are subject to change, therefore, applicants need to check 40 CFR 98 to confirm GWP values.

² For HFCs or PFCs describe the specific HFC or PFC compound and use a separate column for each individual compound.

³ For each new compound, enter the appropriate GWP for each HFC or PFC compound from Table A-1 in 40 CFR 98.

⁴ Green house gas emissions on a **mass basis** is the ton per year green house gas emission before adjustment with its GWP.

⁵ CO₂e means Carbon Dioxide Equivalent and is calculated by multiplying the TPY mass emissions of the green house gas by its GWP.

Application Summary

The <u>Application Summary</u> shall include a brief description of the facility and its process, the type of permit application, the applicable regulation (i.e. 20.2.72.200.A.X, or 20.2.73 NMAC) under which the application is being submitted, and any air quality permit numbers associated with this site. If this facility is to be collocated with another facility, provide details of the other facility including permit number(s). In case of a revision or modification to a facility, provide the lowest level regulatory citation (i.e. 20.2.72.219.B.1.d NMAC) under which the revision or modification is being requested. Also describe the proposed changes from the original permit, how the proposed modification will affect the facility's operations and emissions, debottlenecking impacts, and changes to the facility's major/minor status (both PSD & Title V).

The **Process Summary** shall include a brief description of the facility and its processes.

<u>Startup, Shutdown, and Maintenance (SSM)</u> routine or predictable emissions: Provide an overview of how SSM emissions are accounted for in this application. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on SSM emissions.

Facility Description / Process Summary

HollyFrontier Navajo Refining LLC ("Navajo") owns and operates the Artesia Refinery, located along Highway 82, partially within and partially outside of the city limits of Artesia, in Eddy County, New Mexico (see Section 8 Maps). The Artesia Refinery has a crude oil capacity of 100,000 barrel per day. The facility process units include atmospheric and vacuum distillation, fluid catalytic cracking ("FCC"), alkylation, isomerization, saturates gas plants, amine units, sulfur recovery units ("SRU"), and various hydrodesulphurization units ("HDS"). Products from the refining processes include, but are not limited to, gasoline of various grades, kerosene, diesel, liquefied petroleum gas ("LPG"), jet fuel (primarily JP-8), carbon black oil, and asphalt products.

The emissions from the refining processes include nitrogen oxides ("NO_X"), carbon monoxide ("CO"), volatile organic compounds ("VOCs"), sulfur dioxide ("SO₂"), particulate matter (i.e., PM, PM₁₀, and PM_{2.5}), hydrogen sulfide ("H₂S"), sulfuric acid mist ("SAM"), hazardous air pollutants ("HAPs,") and greenhouse gases ("GHG.")

Permit Application Summary

Navajo is submitting this application for a Significant Permit Revision of Permit No. PSD-NM-0195M39R4, in accordance with 20.2.72.219.D and 20.2.72.402 New Mexico Administrative Code ("NMAC"). This revision is necessary to adequately represent the operational conditions at the refinery, to update the calculations' methodology where appropriate and according to latest guidance published, and to update representations from previous submittals.

Specifically, with this application Navajo is seeking a number of separate and independent revisions as follows. Additional details regarding these changes are provided in Sections 6, 7, and 20 of this permit application.

- 1. Authorize changes in fuel composition for three process heaters.
- 2. Revise design heat inputs of, and make corresponding revisions to emission limits for, certain existing combustion units.
- 3. Revise emission limits for flares.
- 4. Reconcile emission calculations for the SRU tail gas incinerators ("TGI"), the fluidized catalytic cracking ("FCC") regenerator, and the cooling towers.
- 5. Reconcile emission calculations for truck and railcar loading.
- 6. Revise emission limits and representations of true vapor pressure for storage tanks and loading racks
- 7. Reflect retrofit of T-0418 with an internal floating roof consistent with the requirements of 40 CFR § 63.660.
- 8. Reduce emission limits for fugitive emissions from equipment leaks by 562 tons per year, as a result of more accurate component counts, and the use of appropriate control efficiencies required for compliance with 40 CFR 60, subpart GGGa.
- 9. Revise emission limits for wastewater treatment operations.
- 10. Revise the emission cap for malfunction events such that it applies both to flares and to other emissions units.
- 11. Remove from the permit emissions units that have been dismantled and emissions units associated with the Renewable Diesel Unit ("RDU"), as that unit is part of a separate stationary source covered by NSR Permit No. 9213.
- 12. Add startup, shutdown, and maintenance ("SSM") cap for all SSM activities.

Change to Facility's Operations and Emissions

The Artesia Refinery is and will continue to be a major source subject to the Prevention of Significant Deterioration ("PSD") regulations codified in NMAC 20.2.74 and in the federally approved State Implementation Plan for New Mexico.¹ Under the preconstruction permitting provisions of the PSD program, a PSD permit is required if a project at an existing major source is a "major modification" as defined in NMAC 20.2.74.7.AE.

All of the requested permit revisions other than the four separate proposed projects discussed below (involving storage tanks and loading racks, flares, hydrogen reformer furnaces, and the dissolved air flotation units) are reconciliations involving no physical changes in or changes in method of operation of the stationary source. These requested reconciliations do not constitute a "modification," a "project," or a "major modification," as these terms are defined in 20.2.72.7.P and 20.2.74.7.AQ and AE of NMAC respectively.

Storage tanks and loading racks. The first of the four projects covered by this permit application involves requested revisions to permit terms to allow increases in maximum vapor pressure of some petroleum liquids stored in fixed-roof and floating-roof storage vessels and loaded at loading racks. Navajo is conservatively treating these requested revisions to permit terms for tanks and loading racks as changes in method of operation constituting a single project for PSD purposes because these changes could be construed as being substantially related to one another.

This project will not cause a significant increase in emissions of any regulated NSR pollutant, as shown in Section 12.A; therefore, this project is not a major modification subject to PSD review.

Flares. The second of the four projects covered by this permit application involves requested increases in permitted emission rates for the refinery's five flares terms to allow for higher gas flow rates to the flares. Navajo is conservatively treating these higher flow rates and increased emission rates as being not unrelated to physical changes made to each of the flares. Specifically, in 2018, to facilitate continuous compliance with the minimum combustion efficiency requirements of MACT CC that took effect on January 30, 2019, Navajo installed new piping for supplemental gas to each flare, and in 2020, in order to improve control of supplemental gas flow to the flares, Navajo replaced the supplemental gas control valves. Navajo is conservatively treating the physical changes at all five flares as a single project for PSD purposes because these changes could be construed as being substantially related to one another. This project is not in any way technically or economically related to the requested changes at the storage tanks and loading racks and, therefore, each of these two independent projects is evaluated separately for purposes of determining applicability of the preconstruction PSD permitting program.²

The changes at the flares will cause significant increases in emissions of VOC, as shown in Section 12.A; therefore, this project constitutes a major modification subject to PSD review for VOC.

<u>Hydrogen reformer furnaces</u>. The third of the four projects covered by this permit application involves changes to the hydrogen reformer furnaces, H-8801/8802 and H-9851, to accommodate combustion of amine-treated refinery fuel gas. Navajo is conservatively treating the physical and operational changes at both furnaces as a single project for PSD purposes because these changes could be construed as being substantially related to one another. This project is not in any way technically or economically related to the requested changes at the storage tanks, loading racks, and flares. This independent project is, therefore, evaluated separately for purposes of determining applicability of the preconstruction PSD permitting program.

This project will not cause a significant increase in emissions of any regulated NSR pollutant, as shown in Section 12.A; therefore, this project is not a major modification subject to PSD review.

<u>Dissolved air flotation units.</u> The last of the four projects covered by this permit application involves requested revisions to permit terms to allow increased VOC emissions from the dissolved air flotation units. This project is not in any way technically or economically related to the requested changes at the storage tanks, loading racks, flares, and hydrogen reformer furnaces. This independent project is, therefore, evaluated separately for purposes of determining applicability of the preconstruction PSD permitting program.

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¹ 40 CFR § 52.1620(c). The nonattainment New Source Review ("NSR") program codified at NMAC 20.2.79 and approved at 40 CFR § 52.1620(c) is not applicable because the Artesia Refinery is located in Eddy County, an area that is designated as unclassifiable or attainment with respect to all National Ambient Air Quality Standards. See, 40 CFR § 81.332.

² See, 20.2.74.7.AE and .AQ NMAC, establishing that PSD applicability is determined separately for each "project," where that term is defined as a single "physical change" or "change in method of operation." See, also, U.S. EPA's final rule regarding project aggregation, 83 *Fed. Reg.* 57324 at p. 57332, clarifying that projects are evaluated separately unless they are substantially related.

This project will not cause a significant increase in emissions of any regulated NSR pollutant, as shown in Section 12.A; therefore, this project is not a major modification subject to PSD review.

<u>Retrospective PSD review.</u> Several of the permit terms that are the subject of requested revisions in this permit application were imposed historically in conjunction with impact analyses performed with permitting actions for major modifications under the PSD program or in conjunction with PSD non-applicability determinations. Where applicable, these historical applicability analyses and impact analyses are updated in Section 20 of this permit application.

Startup, Shutdown, and Maintenance ("SSM") Routine or Predictable Emissions

SSM emissions are fully accounted for in this application consistent with NMED's *Implementation Guidance for Permitting SSM Emissions and Excess Emissions*, version 7, June 2012.³ This application does not include any material changes to the manner in which SSM emissions are addressed, but it has been updated to include crude oil pigging activities. Details of SSM emissions calculations are discussed in Section 7.

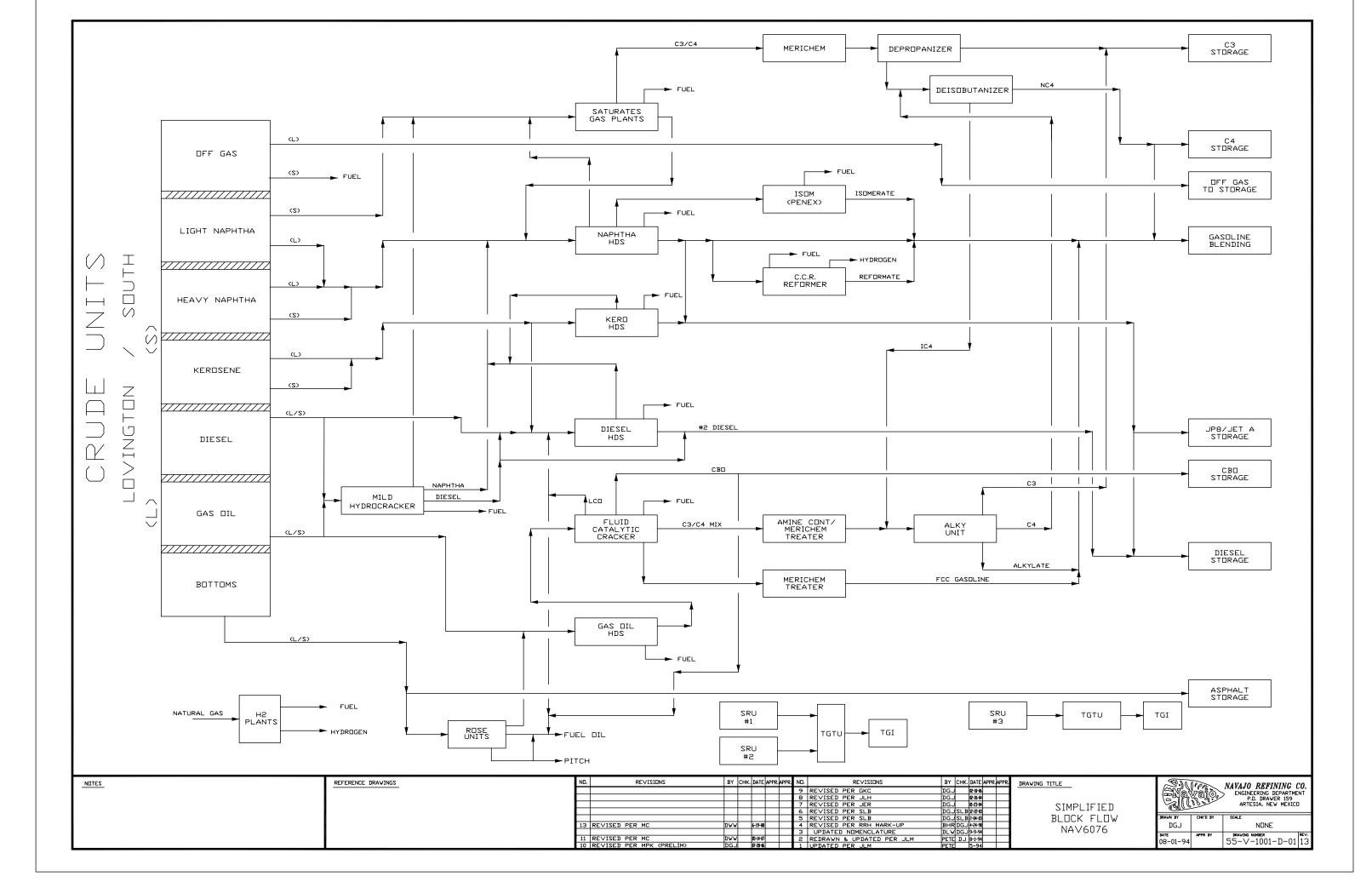
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³ Available at www.env.nm.gov/wp-content/uploads/sites/2/2017/06/AQBP_SSM_PERMITTING_IMPLEMENTATION_GUIDANCE_07Jun12.doc

Process Flow Sheet

A <u>process flow sheet</u> and/or block diagram indicating the individual equipment, all emission points and types of control applied to those points. The unit numbering system should be consistent throughout this application.

A process flow diagram for the refinery is included in this section.

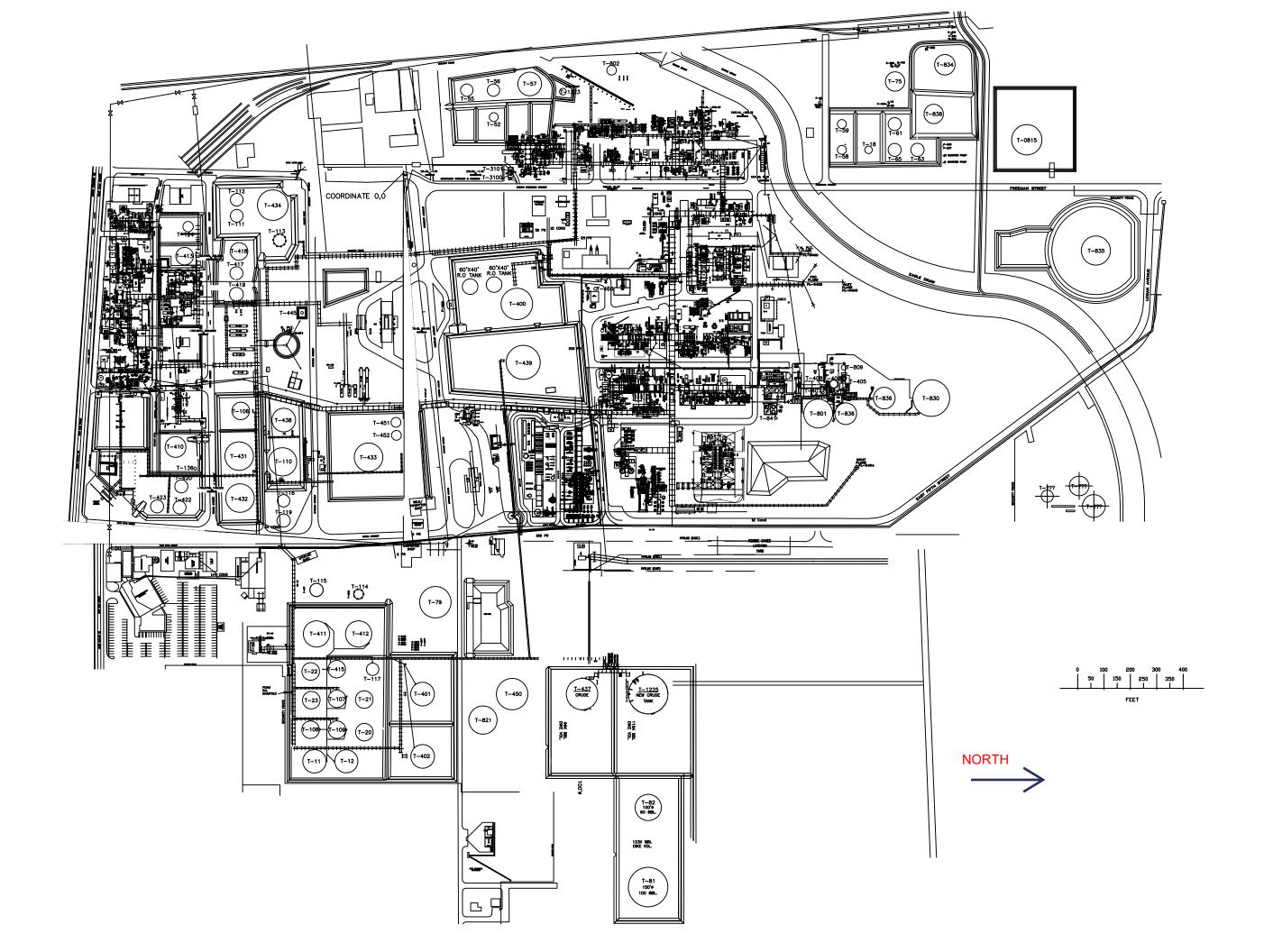


Plot Plan Drawn To Scale

A <u>plot plan drawn to scale</u> showing emissions points, roads, structures, tanks, and fences of property owned, leased, or under direct control of the applicant. This plot plan must clearly designate the restricted area as defined in UA1, Section 1-D.12. The unit numbering system should be consistent throughout this application.

A plot plan is included in this section.

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All Calculations

Show all calculations used to determine both the hourly and annual controlled and uncontrolled emission rates. All calculations shall be performed keeping a minimum of three significant figures. Document the source of each emission factor used (if an emission rate is carried forward and not revised, then a statement to that effect is required). If identical units are being permitted and will be subject to the same operating conditions, submit calculations for only one unit and a note specifying what other units to which the calculations apply. All formulas and calculations used to calculate emissions must be submitted. The "Calculations" tab in the UA2 has been provided to allow calculations to be linked to the emissions tables. Add additional "Calc" tabs as needed. If the UA2 or other spread sheets are used, all calculation spread sheet(s) shall be submitted electronically in Microsoft Excel compatible format so that formulas and input values can be checked. Format all spread sheets and calculations such that the reviewer can follow the logic and verify the input values. Define all variables. If calculation spread sheets are not used, provide the original formulas with defined variables. Additionally, provide subsequent formulas showing the input values for each variable in the formula. All calculations, including those calculations are imbedded in the Calc tab of the UA2 portion of the application, the printed Calc tab(s), should be submitted under this section.

Tank Flashing Calculations: The information provided to the AQB shall include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., NOI, permit, or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis. If Hysis is used, all relevant input parameters shall be reported, including separator pressure, gas throughput, and all other relevant parameters necessary for flashing calculation.

SSM Calculations: It is the applicant's responsibility to provide an estimate of SSM emissions or to provide justification for not doing so. In this Section, provide emissions calculations for Startup, Shutdown, and Routine Maintenance (SSM) emissions listed in the Section 2 SSM and/or Section 22 GHG Tables and the rational for why the others are reported as zero (or left blank in the SSM/GHG Tables). Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on calculating SSM emissions. If SSM emissions are greater than those reported in the Section 2, Requested Allowables Table, modeling may be required to ensure compliance with the standards whether the application is NSR or Title V. Refer to the Modeling Section of this application for more guidance on modeling requirements.

Glycol Dehydrator Calculations: The information provided to the AQB shall include the manufacturer's maximum design recirculation rate for the glycol pump. If GRI-Glycalc is used, the full input summary report shall be included as well as a copy of the gas analysis that was used.

Road Calculations: Calculate fugitive particulate emissions and enter haul road fugitives in Tables 2-A, 2-D and 2-E for:

- 1. If you transport raw material, process material and/or product into or out of or within the facility and have PER emissions greater than 0.5 tpy.
- 2. If you transport raw material, process material and/or product into or out of the facility more frequently than one round trip per day.

Significant Figures:

A. All emissions standards are deemed to have at least two significant figures, but not more than three significant figures.

- **B.** At least 5 significant figures shall be retained in all intermediate calculations.
- C. In calculating emissions to determine compliance with an emission standard, the following rounding off procedures shall be used:
 - (1) If the first digit to be discarded is less than the number 5, the last digit retained shall not be changed;
 - (2) If the first digit discarded is greater than the number 5, or if it is the number 5 followed by at least one digit other than the number zero, the last figure retained shall be increased by one unit; and
 - (3) If the first digit discarded is exactly the number 5, followed only by zeros, the last digit retained shall be rounded upward if it is an odd number, but no adjustment shall be made if it is an even number.
 - (4) The final result of the calculation shall be expressed in the units of the standard.

Control Devices: In accordance with 20.2.72.203.A(3) and (8) NMAC, 20.2.70.300.D(5)(b) and (e) NMAC, and 20.2.73.200.B(7) NMAC, the permittee shall report all control devices and list each pollutant controlled by the control device regardless if the applicant takes credit for the reduction in emissions. The applicant can indicate in this section of the

application if they chose to not take credit for the reduction in emission rates. For notices of intent submitted under 20.2.73 NMAC, only uncontrolled emission rates can be considered to determine applicability unless the state or federal Acts require the control. This information is necessary to determine if federally enforceable conditions are necessary for the control device, and/or if the control device produces its own regulated pollutants or increases emission rates of other pollutants.

Attached are the emission calculations that were revised as part of this permit revision. Files containing emission calculations for all sources are included with the submitted electronic files.

Section 6.a

Green House Gas Emissions

(Submitting under 20.2.70, 20.2.72 20.2.74 NMAC)

Title V (20.2.70 NMAC), Minor NSR (20.2.72 NMAC), and PSD (20.2.74 NMAC) applicants must estimate and report greenhouse gas (GHG) emissions to verify the emission rates reported in the public notice, determine applicability to 40 CFR 60 Subparts, and to evaluate Prevention of Significant Deterioration (PSD) applicability. GHG emissions that are subject to air permit regulations consist of the sum of an aggregate group of these six greenhouse gases: carbon dioxide (CO_2), nitrous oxide (CO_2), methane (CO_3), methane (CO_3), methane (CO_3), perfluorocarbons (CO_3), and sulfur hexafluoride (CO_3).

Calculating GHG Emissions:

- 1. Calculate the ton per year (tpy) GHG mass emissions and GHG CO₂e emissions from your facility.
- **2.** GHG mass emissions are the sum of the total annual tons of greenhouse gases without adjusting with the global warming potentials (GWPs). GHG CO₂e emissions are the sum of the mass emissions of each individual GHG multiplied by its GWP found in Table A-1 in 40 CFR 98 Mandatory Greenhouse Gas Reporting.
- 3. Emissions from routine or predictable start up, shut down, and maintenance must be included.
- **4.** Report GHG mass and GHG CO₂e emissions in Table 2-P of this application. Emissions are reported in **short** tons per year and represent each emission unit's Potential to Emit (PTE).
- **5.** All Title V major sources, PSD major sources, and all power plants, whether major or not, must calculate and report GHG mass and CO2e emissions for each unit in Table 2-P.
- **6.** For minor source facilities that are not power plants, are not Title V, and are not PSD there are three options for reporting GHGs in Table 2-P: 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHGs as a second separate unit; 3) or check the following \Box By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

Sources for Calculating GHG Emissions:

- Manufacturer's Data
- AP-42 Compilation of Air Pollutant Emission Factors at http://www.epa.gov/ttn/chief/ap42/index.html
- EPA's Internet emission factor database WebFIRE at http://cfpub.epa.gov/webfire/
- 40 CFR 98 <u>Mandatory Green House Gas Reporting</u> except that tons should be reported in short tons rather than in metric tons for the purpose of PSD applicability.
- API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Natural Gas Industry. August 2009 or most recent version.
- Sources listed on EPA's NSR Resources for Estimating GHG Emissions at http://www.epa.gov/nsr/clean-air-act-permitting-greenhouse-gases:

Global Warming Potentials (GWP):

Applicants must use the Global Warming Potentials codified in Table A-1 of the most recent version of 40 CFR 98 Mandatory Greenhouse Gas Reporting. The GWP for a particular GHG is the ratio of heat trapped by one unit mass of the GHG to that of one unit mass of CO₂ over a specified time period.

"Greenhouse gas" for the purpose of air permit regulations is defined as the aggregate group of the following six gases: carbon dioxide, nitrous oxide, methane, hydrofluorocarbons, perfluorocarbons, and sulfur hexafluoride. (20.2.70.7 NMAC, 20.2.74.7 NMAC). You may also find GHGs defined in 40 CFR 86.1818-12(a).

Metric to Short Ton Conversion:

Short tons for GHGs and other regulated pollutants are the standard unit of measure for PSD and title V permitting programs. 40 CFR 98 Mandatory Greenhouse Reporting requires metric tons.

1 metric ton = 1.10231 short tons (per Table A-2 to Subpart A of Part 98 – Units of Measure Conversions)

		Design	Design	Food	Heat		Emission Factors a												Potentia	l to Emit				
		Capacity (LHV)	Capacity (HHV)		tent	со	NO _x	PM/PM ₁₀ / PM _{2.5}			SO ₂			voc	С	0	N	O _x	PM/PM	₁₀ / PM _{2.5}	S	O ₂	V	ос
ID	Description	MMBtu/hi	MMBtu/hr	Btu/scf @ 60 °F	Basis	lb/MMBtu	lb/MMBtu	lb/MMBtu	H2S max grH2S/dsc f	non-H2S Sulfur Species max grS/dscf	H2S avg grH2S/dscf	non-H2S Sulfur Species avg. grS/dscf		lb/MMBtu	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
B-0007	Boiler 7	215.0	238.9	749	LHV	0.082	0.06 c	0.0075	0.10	0.00391	0.037	0.00391	f	0.0054	19.67	86.16	12.90	56.50	1.78	7.80	8.04	13.94	1.29	5.64
B-0008	Boiler 8	215.0	238.9	749	LHV	0.082	0.06 c	0.0075	0.10	0.00391	0.037	0.00391	f	0.0054	19.67	86.16	12.90	56.50	1.78	7.80	8.04	13.94	1.29	5.64
B-0009	Boiler 9	220.0	244.4	845	HHV	0.037 b	0.02 b		0.03	5 grS/dscf	0.035	grS/dscf	g	0.0040 b	9.04	39.61	4.89	21.41	1.82	7.98	2.89	12.67	0.98	4.28
H-0009	Unit 13 Naphtha Splitter Reboiler	44.0	48.9	749	LHV	0.082	0.09 c	0.0075	0.10	0.00375	0.037	0.00375	f	0.0054	4.03	17.63	3.96	17.34	0.36	1.60	1.64	2.84	0.26	1.20
H-0011	Unit 21 Vacuum Unit Heater	38.0	42.2	749	LHV	0.082	- e	0.0075	0.10	0.00391	0.037	0.00391	f	0.0054	3.48	15.30	9.52	31.73	0.31	1.38	1.42	2.46	0.23	1.00
H-0018	Unit 06 HDS Reboiler	32.0	35.6	749	LHV	0.082	0.098	0.0075	0.10	0.00375	0.037	0.00375	f	0.0054	2.93	12.82	3.49	15.27	0.26	1.16	1.19	2.07	0.19	0.84
H-0019	South Crude Charge Heater	54.0	60.0	749	LHV	0.082	0.0527 d	0.0075	0.10	0.00391	0.037	0.00391	f	0.0054	4.94	21.64	2.90	12.46	0.45	2.00	2.02	3.50	0.32	1.42
H-0020	South Crude Charge Heater	90.0	100.0	749	LHV	0.082	0.0535 d	0.0075	0.10	0.00391	0.037	0.00391	f	0.0054	8.23	36.07	4.82	21.09	0.75	3.26	3.37	5.84	0.54	2.36
H-0028	Unit 21 Heater	12.3	13.7	749	LHV	0.082	0.176 d	0.0075	0.10	0.00391	0.037	0.00391	f	0.0054	1.13	4.93	2.17	9.50	0.10	0.45	0.46	0.80	0.07	0.32
H-0030	Unit 06 Charge Heater	42.0	46.7	749	LHV	0.082	0.076 c	0.0075	0.10	0.00375	0.037	0.00375	f	0.0054	3.84	16.90	3.19	13.98	0.40	1.52	1.57	2.71	0.25	1.10
H-0040	Unit 13 Charge Heater	42.0	46.7	749	LHV	0.082	0.09 c	0.0075	0.10	0.00375	0.037	0.00375	f	0.0054	3.84	16.90	3.78	16.56	0.40	1.52	1.57	2.71	0.25	1.10
H-0312	Unit 10 FCC Feed Heater	35.0	38.9	749	LHV	0.082	0.132 c	0.0075	0.10	0.00391	0.037	0.00391	f	0.0054	3.20	14.03	4.62	20.24	0.29	1.27	1.31	2.27	0.21	0.92
H-0352, H-0353, H-0354	Unit 70 CCR Reformer Heaters	200.0	222.2	749	LHV	0.082	0.045 d	0.0075	0.10	0.01166	0.037	0.01166	f	0.0054	18.30	80.15	9.00	39.42	1.70	7.25	8.07	15.56	1.20	5.25
H-0355	Unit 70 Stabilizer Reboiler Heater	28.0	31.1	749	LHV	0.082	0.09 c	0.0075	0.10	0.01166	0.037	0.01166	f	0.0054	2.56	11.22	2.52	11.04	0.23	1.02	1.13	2.18	0.17	0.73
H-0362, H-0363, H-0364	Unit 70 CCR Heaters	125.0	138.9	749	LHV	0.082	0.055 d	0.0075	0.10	0.01166	0.037	0.01166	f	0.0054	11.44	50.09	6.88	30.11	1.03	4.53	5.04	9.73	0.75	3.28
H-0421	Unit 44 Charge Heater	27.0	30.0	749	LHV	0.082	0.09 c	0.0075	0.10	0.00375	0.037	0.00375	f	0.0054	2.47	10.82	2.43	10.64	0.22	0.98	1.01	1.74	0.16	0.71
H-0464	SRU Hot Oil Heater	9.6	10.7	749	LHV	0.082	0.049	0.0075	0.10	0.00375	0.037	0.00375	f	0.0054	0.88	3.85	0.52	2.29	0.08	0.40	0.36	0.62	0.06	0.25
H-0600	Unit 09 Depropanizer Reboiler Heater	84.0	93.3	749	LHV	0.082	0.05 b	0.0075	0.10	0.00375	0.037	0.00375	f	0.0054	7.69	33.66	4.70	20.44	0.70	3.05	3.14	5.43	0.50	2.20
H-0601	Unit 33 Charge Heater	78.0	86.7	749	LHV	0.082	0.045 c	0.0075	0.10	0.00375	0.037	0.00375	f	0.0054	7.14	31.26	3.51	15.37	0.65	2.83	2.91	5.04	0.47	2.05
H-2421	Unit 45 Charge Heater	27.0	30.0	749	LHV	0.082	0.045 c	0.0075	0.10	0.00079	0.037	0.00079	f	0.0054	2.47	10.82	1.22	5.32	0.22	0.98	0.98	1.61	0.16	0.71
H-2501	Unit 25 ROSE [®] Unit No. 2 Hot Oil Heater	120.0	133.3	749	LHV	0.06 c	0.03 c	0.0075	0.10	0.00095	0.037	0.00095	f	0.0054	7.20	31.54	3.60	15.77	0.99	4.35	4.35	7.19	0.72	3.15
H-3101	SRU3 Hot Oil Heater	11.0	12.2	749	LHV	0.09 c	0.03 c	0.0075	0.10	0.00375	0.037	0.00375	f	0.0054	0.99	4.34	0.33	1.45	0.09	0.40	0.41	0.71	0.07	0.29
H-3402	Unit 34 Hydrocracker Reboiler 1	52.0	57.8	749	LHV	0.09 c	0.03 c	0.0075	0.10	0.00095	0.037	0.00095	f	0.0054	4.68	20.50	1.56	6.83	0.43	1.89	1.89	3.12	0.31	1.36
H-3403	Unit 34 Hydrocracker Reactor Charge Heater	32.0	35.6	749	LHV	0.082	0.03 c	0.0075	0.10	0.00095	0.037	0.00095	f	0.0054	2.93	12.82	0.96	4.20	0.26	1.16	1.16	1.92	0.19	0.84
H-5401	Unit 54 HDS Reactor Heater	19.3	21.5	749	LHV	0.03 b	0.04 d	0.0075	0.10	0.00391	0.037	0.00391	f	0.0054	0.64	2.82	0.77	3.38	0.16	0.70	0.72	1.25	0.12	0.51
H-8801/8802	Unit 63 Hydrogen Plant Reformer Furnaces	152.0	168.9	975	LHV	0.082	0.057 c	0.0075	-	0.00032	-	0.00032	h	0.0054	13.91	60.91	8.66	37.95	1.26	5.51	2.85	4.96	0.91	3.99
	neronner rumaces			749	LHV				0.10	0.00391	0.037	0.00391												
H-9851	Unit 64 Hydrogen Plant Reformer	337	374	975	LHV	0.060 c	0.0125 c	0.0075	-	0.00032	-	0.00032	h	0.0054	20.2	88.6	4.2	18.5	2.8	12.3	6.3	11.0	2.0	8.8
	Kerorinei			749	LHV				0.10	0.00391	0.037	0.00391												

Notes

- a. Unless otherwise noted, the emission factors are from AP-42 Tables 1.4-1 and 1.4-2, dated 7/98. Factors are converted to lb/MMBtu by dividing by 1020 Btu/scf as specified in AP-42 and are based on HHV.
- b. Based on manufacturer guarantee on HHV basis.
- c. Based on manufacturer guarantee on LHV basis.
- d. Factor based on performance testing and LHV basis
- e. Permitted NO_X emission factor based on AP-42 Section 1.4 dated 5/74: Hourly factor = 230 lb/MMscf and Annual = 175 lb/MMscf
- f. Except as indicated, the hourly SO₂ emissions are calculated based on the NSPS Subpart J limit of 0.1 gr H2S/dscf (162 ppm H2S) on 3-hr rolling NSPS Ja limit and the
- annual SO2 emissions are calculated based on the NSPS Subpart Ja, 365-day calendar rolling average limit of 0.037 gr H2S/dscf (60 ppmv H2S), plus non-H2S species present in fuel gas as determined based on sampling data
- g. Permitted emission factor of 0.035 gr S/scf fuel and a HHV of 845 Btu/scf.
- h. H-8801, H-8802, and H-9851 will combust a mixture of PSA Offgas and amine-treated refinery fuel gas (RFG). It has been conservatively assumed 50/50 mix for SO2 emissions calculation.

Sample calculation for SO₂ emissions:

 $SO2 (lb/hr) = [gr_{H22}/dscf* 1lb_{H22}/7000 gr_{H22}* 1lbmole_{H22}/34 lb_{H25} + gr_2/dscf* 1 lb_3/7000 gr_5* 1 lbmole_3/32 lb_5]* 64 lb_{502}/lbmoleSO2 * Heat Rate (MMBtu/hr)* 1000000 Btu/MMBtu / Fuel Heat Content (Btu/scf)* 8760 hr/yr* 1 ton_{502}/2000 lb_{502}* 1lbmole_{H22}/34 lb_{H25} + gr_2/dscf* 1 lb_3/7000 gr_5* 1 lbmole_3/32 lb_5]* 64 lb_{502}/lbmoleSO2 * Heat Rate (MMBtu/hr)* 1000000 Btu/MMBtu / Fuel Heat Content (Btu/scf)* 8760 hr/yr* 1 ton_{502}/2000 lb_{502}* 1 lbmole_3/32 lb_5]* 64 lb_{502}/lbmoleSO2 * 11 bmole_3/32 lb_5]* 64 lb_{502}/lb$

H-9851 SO2 Emissions = [0.00032 grS/dscf * 1 lbS/7000 grS * 1 lbmoleS/32 lbS / 975 Btu/scf * 337 MMBtu/hr * 0.5 + <math>[0.04 grH2S/dscf * 1 lbH2S/7000 grH2S * 1 lbmoleH2S/34 lbH2S + 0.004 grS/dscf * 1 lbS/7000 grS * 1 lbmoleS/32 lbS) * 749 Btu/scf * 337 MMBtu/hr * 0.5] * 64 lbSO2/ lbmoleSO2 * 1,000,000 Btu/ MMBtu * 8760 hr/yr * 1 tonSO2/2000 lbSO2 = 11.0 tpy

H-9851 SCR Ammonia Slip Emissions:

		NH ₃	Exhaust		
		Exhaust	Flow		
		Conc.	Rate	NH ₃ Emissio	n Rate
		ppmv, wet	scfm @		
ID	Description	basis	60°F	lb/hr	ton/yr
H-9851	Unit 64 Hydrogen Plant Reformer	7	73,500	1.38	6.06

Sample calculation for NH₃ emissions:

NH3 Emissions H-9851 = 7 lbmol NH3 / 10^6 lbmol exhaust * 73,500 scf exhaust/min * 60 min/hr / 379 scf exhaust / lbmol * 17 lb NH3 / lbmol = 1.38 lb/hr NH3 Emissions H-9851 = 1.38 lb/hr * 8760 hr/yr * 1 ton/2,000 lb = 6.06 ton/yr

H-2501

H-3101

H-3402

H-3403

H-5401

H-9851

H-8801/8802

Heater

Heater

Furnaces

SRU3 Hot Oil Heater

Unit 34 Hydrocracker Reboiler 1

Unit 63 Hydrogen Plant Reformer

Unit 64 Hydrogen Plant Reformer

Unit 54 HDS Reactor Heater

Unit 34 Hydrocracker Reactor Charge

				CO ₂	CH ₄	N ₂ O	GHG
Table.	s C-1 and C-2 to 40 CFR 98, subpart C,	Fuel Gas Emission I	Factor lb/mmBtu	130.07	0.007	0.001	(as CO ₂ e
	Table A-1 TO 40 CFR 98, su	bpart A, Global Wa	rming Potentials	1	25	298	(as CO ₂ C)
		Design Capacity	Design Capacity				
		(LHV)	(HHV)	ton/yr	ton/yr	ton/yr	ton/yr
ID	Description	MMBtu/hr	MMBtu/hr				
B-0007	Boiler 7	215	239	136,084	6.9	1.4	136,669
B-0008	Boiler 8	215	239	136,084	6.9	1.4	136,669
B-0009	Boiler 9	220	244	139,248	7.1	1.4	139,847
H-0009	Unit 13 Naphtha Splitter Reboiler	44	49	27,850	1.4	0.3	27,969
H-0011	Unit 21 Vacuum Unit Heater	38	42	24,052	1.2	0.2	24,155
H-0018	Unit 06 HDS Reboiler	32	36	20,254	1.0	0.2	20,341
H-0019	South Crude Charge Heater	54	60	34,179	1.7	0.3	34,326
H-0020	South Crude Charge Heater	90	100	56,965	2.9	0.6	57,210
H-0028	Unit 21 Heater	12	14	7,785	0.4	0.1	7,819
H-0030	Unit 06 Charge Heater	42	47	26,584	1.4	0.3	26,698
H-0040	Unit 13 Charge Heater	42	47	26,584	1.4	0.3	26,698
H-0312	Unit 10 FCC Feed Heater	35	39	22,153	1.1	0.2	22,248
H-0352, H-0353, H-0354	Unit 70 CCR Reformer Heaters	200	222	126,589	6.4	1.3	127,134
H-0355	Unit 70 Stabilizer Reboiler Heater	28	31	17,723	0.9	0.2	17,799
H-0362, H-0363, H-0364	Unit 70 CCR Heaters	125	139	79,118	4.0	0.8	79,459
H-0421	Unit 44 Charge Heater	27	30	17,090	0.9	0.2	17,163
H-0464	SRU Hot Oil Heater	10	11	6,076	0.3	0.1	6,102
H-0600	Unit 09 Depropanizer Reboiler Heater	84	93	53,168	2.7	0.5	53,396
H-0601	Unit 33 Charge Heater	78	87	49,370	2.5	0.5	49,582
H-2421	Unit 45 Charge Heater	27	30	17,090	0.9	0.2	17,163
H-2501	Unit 25 ROSE® Unit No. 2 Hot Oil	120	133	75 954	3.9	0.8	76 280

120

11

52

32

19

152

337

133

12

58

36

21

169

374

75,954

6,962

32,913

20,254

12,229

96,208

213,303

TOTAL 1,481,867

3.9

0.4

1.7

1.0

0.6

4.9

10.8

75.3

0.8

0.1

0.3

0.2

0.1

1.0

2.2

15.1

76,280

6,992

33,055

20,341

12,281

96,622

214,221

1,488,242

					aphthalene	Methylch	3- olanthrene	Dimethy nthr	12- rlbenz(a)a acene	<u> </u>	hthene	•	nthylene	Anthr			nthracene
			CAS No.	91-	57-6	56-	-49-5	57-	97-6	83-	32-9	208-	96-8	120-	12-7	56-!	55-3
AP-	42, Ch. 1.4 (7/98) Table 1.4-3 HAPs for Natural Gas Combustion Units	Emission I	actor lb/mmBtu	2.41	E-08	1.8	BE-09	1.6	E-08	1.8	E-09	1.8	E-09	2.41	E-09	1.81	E-09
			Design Capacity														
		(LHV)	(HHV)	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
ID	Description	MMBtu/hr	MMBtu/hr														
B-0007	Boiler 7	215	239	5.6E-06	2.46E-05	4.2E-07	1.85E-06		1.64E-05		1.85E-06		1.85E-06	5.6E-07	2.46E-06		1.85E-06
B-0008	Boiler 8	215	239	5.6E-06	2.46E-05	4.2E-07	1.85E-06		1.64E-05		1.85E-06	4.2E-07	1.85E-06		2.46E-06		1.85E-06
B-0009	Boiler 9	220	244	5.8E-06	2.52E-05	4.3E-07	1.89E-06		1.68E-05		1.89E-06						
H-0009	Unit 13 Naphtha Splitter Reboiler	44	49	1.2E-06	5.04E-06	8.6E-08	3.78E-07		3.36E-06		3.78E-07		3.78E-07		5.04E-07		3.78E-07
H-0011	Unit 21 Vacuum Unit Heater	38	42	9.9E-07	4.35E-06	7.5E-08	3.26E-07		2.90E-06			7.5E-08			4.35E-07		
H-0018	Unit 06 HDS Reboiler	32	36	8.4E-07	3.66E-06	6.3E-08	2.75E-07		2.44E-06		2.75E-07		2.75E-07		3.66E-07		2.75E-07
H-0019	South Crude Charge Heater	54	60	1.4E-06	6.18E-06	1.1E-07	4.64E-07		4.12E-06		4.64E-07		4.64E-07	1.4E-07	6.18E-07		
H-0020	South Crude Charge Heater	90	100	2.4E-06	1.03E-05	1.8E-07	7.73E-07		6.87E-06	1.8E-07	7.73E-07		7.73E-07		1.03E-06		
H-0028	Unit 21 Heater	12	14	3.2E-07	1.41E-06	2.4E-08	1.06E-07		9.39E-07		1.06E-07		1.06E-07	3.2E-08	1.41E-07	2.4E-08	
H-0030	Unit 06 Charge Heater	42	47	1.1E-06	4.81E-06	8.2E-08	3.61E-07	7.3E-07	3.21E-06	8.2E-08	3.61E-07	8.2E-08	3.61E-07	1.1E-07	4.81E-07	8.2E-08	3.61E-07
H-0040	Unit 13 Charge Heater	42	47	1.1E-06	4.81E-06	8.2E-08	3.61E-07	7.3E-07	3.21E-06	8.2E-08	3.61E-07	8.2E-08	3.61E-07	1.1E-07	4.81E-07	8.2E-08	3.61E-07
H-0312	Unit 10 FCC Feed Heater	35	39	9.1E-07	4.01E-06	6.9E-08	3.01E-07	6.1E-07	2.67E-06	6.9E-08	3.01E-07	6.9E-08	3.01E-07	9.1E-08	4.01E-07	6.9E-08	3.01E-07
H-0352, H-0353, H-0354	Unit 70 CCR Reformer Heaters	200	222	5.2E-06	2.29E-05	3.9E-07	1.72E-06	3.5E-06	1.53E-05	3.9E-07	1.72E-06	3.9E-07	1.72E-06	5.2E-07	2.29E-06	3.9E-07	1.72E-06
H-0355	Unit 70 Stabilizer Reboiler Heater	28	31	7.3E-07	3.21E-06	5.5E-08	2.40E-07	4.9E-07	2.14E-06	5.5E-08	2.40E-07	5.5E-08	2.40E-07	7.3E-08	3.21E-07	5.5E-08	2.40E-07
H-0362, H-0363, H-0364	Unit 70 CCR Heaters	125	139	3.3E-06	1.43E-05	2.5E-07	1.07E-06	2.2E-06	9.54E-06	2.5E-07	1.07E-06	2.5E-07	1.07E-06	3.3E-07	1.43E-06	2.5E-07	1.07E-06
H-0421	Unit 44 Charge Heater	27	30	7.1E-07	3.09E-06	5.3E-08	2.32E-07	4.7E-07	2.06E-06	5.3E-08	2.32E-07	5.3E-08	2.32E-07	7.1E-08	3.09E-07	5.3E-08	2.32E-07
H-0464	SRU Hot Oil Heater	10	11	2.5E-07	1.10E-06	1.9E-08	8.24E-08	1.7E-07	7.33E-07	1.9E-08	8.24E-08	1.9E-08	8.24E-08	2.5E-08	1.10E-07	1.9E-08	8.24E-08
H-0600	Unit 09 Depropanizer Reboiler Heater	84	93	2.2E-06	9.62E-06	1.6E-07	7.21E-07	1.5E-06	6.41E-06	1.6E-07	7.21E-07	1.6E-07	7.21E-07	2.2E-07	9.62E-07	1.6E-07	7.21E-07
H-0601	Unit 33 Charge Heater	78	87	2.0E-06	8.93E-06	1.5E-07	6.70E-07	1.4E-06	5.95E-06	1.5E-07	6.70E-07	1.5E-07	6.70E-07	2.0E-07	8.93E-07	1.5E-07	6.70E-07
H-2421	Unit 45 Charge Heater	27	30	7.1E-07	3.09E-06	5.3E-08	2.32E-07	4.7E-07	2.06E-06	5.3E-08	2.32E-07	5.3E-08	2.32E-07	7.1E-08	3.09E-07	5.3E-08	2.32E-07
H-2501	Unit 25 ROSE® Unit No. 2 Hot Oil Heater	120	133	3.1E-06	1.37E-05	2.4E-07	1.03E-06	2.1E-06	9.16E-06	2.4E-07	1.03E-06	2.4E-07	1.03E-06	3.1E-07	1.37E-06	2.4E-07	1.03E-06
H-3101	SRU3 Hot Oil Heater	11	12	2.9E-07	1.26E-06	2.2E-08	9.45E-08	1.9E-07	8.40E-07	2.2E-08	9.45E-08	2.2E-08	9.45E-08	2.9E-08	1.26E-07	2.2E-08	9.45E-08
H-3402	Unit 34 Hydrocracker Reboiler 1	52	58	1.4E-06	5.95E-06	1.0E-07	4.47E-07		3.97E-06				4.47E-07		5.95E-07		4.47E-07
H-3403	Unit 34 Hydrocracker Reactor Charge Heater	-	36	8.4E-07	3.66E-06	6.3E-08	2.75E-07		2.44E-06		2.75E-07		2.75E-07		3.66E-07		
H-5401	Unit 54 HDS Reactor Heater	19	21	5.1E-07	2.21E-06	3.8E-08	1.66E-07	3.4E-07	1.47E-06	3.8E-08	1.66E-07	3.8E-08	1.66E-07	5.1E-08	2.21E-07	3.8E-08	1.66E-07
H-8801/8802	Unit 63 Hydrogen Plant Reformer Furnaces	152	169	4.0E-06	1.74E-05	3.0E-07	1.31E-06	2.6E-06	1.16E-05		1.31E-06		1.31E-06		1.74E-06		
H-9851	Unit 64 Hydrogen Plant Reformer	337	374	8.8E-06	3.86E-05	6.6E-07	2.89E-06	5.9E-06	2.57E-05	6.6E-07	2.89E-06	6.6E-07	2.89E-06	8.8E-07	3.86E-06	6.6E-07	2.89E-06
TOTAL (AP-	42, Ch. 1.4 (7/98) Table 1.4-3 HAPs for	Natural Gas Com	bustion Units)		2.68E-04		2.01E-05		1.79E-04		2.01E-05		2.01E-05		2.68E-05		2.01E-05

				Benzene Ben		Benzo(a	Benzo(a)pyrene		Benzo(b)fluoranth ene		Benzo(g,h,i)peryle ne		Benzo(k)fluoranth ene		Chrysene		Dibenzo(a,h)anthr acene		Dichlorobenzene		Fluoranthene	
			CAS No.	71-	43-2	50-	32-8	205	-99-2	191	-24-2	207-	-08-9	218-	01-9	53-	70-3	2532	1-22-6	206-	44-0	
AP-	AP-42, Ch. 1.4 (7/98) Table 1.4-3 HAPs for Natural Gas Combustion Units Emission Factor lb/mi		actor lb/mmBtu	2.1E-06		1.2E-09		1.8E-09		1.2E-09		1.8E-09		1.8E-09		1.2E-09		1.2E-06		2.9E-09		
		Design Capacity (LHV)	(HHV)	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	
ID	Description	MMBtu/hr	MMBtu/hr																			
B-0007	Boiler 7	215	239		2.15E-03				_		1.23E-06				1.85E-06							
B-0008	Boiler 8	215	239		2.15E-03						1.23E-06								1.23E-03			
B-0009	Boiler 9	220	244		2.20E-03						1.26E-06								1.26E-03			
H-0009	Unit 13 Naphtha Splitter Reboiler	44	49		4.41E-04						2.52E-07								2.52E-04			
H-0011	Unit 21 Vacuum Unit Heater	38	42		3.81E-04														2.18E-04		$\overline{}$	
H-0018	Unit 06 HDS Reboiler	32	36		3.21E-04						1.83E-07				2.75E-07				1.83E-04		4.58E-07	
H-0019	South Crude Charge Heater	54	60		5.41E-04						3.09E-07								3.09E-04			
H-0020	South Crude Charge Heater	90	100		9.02E-04		5.15E-07		_										5.15E-04		1.29E-06	
H-0028	Unit 21 Heater	12	14		1.23E-04						7.04E-08								7.04E-05		1.76E-07	
H-0030	Unit 06 Charge Heater	42	47																2.40E-04			
H-0040	Unit 13 Charge Heater	42	47	9.6E-05	4.21E-04	5.5E-08	2.40E-07	8.2E-08	3.61E-07	5.5E-08	2.40E-07	8.2E-08	3.61E-07	8.2E-08	3.61E-07	5.5E-08	2.40E-07	5.5E-05	2.40E-04	1.4E-07	6.01E-07	
H-0312	Unit 10 FCC Feed Heater	35	39	8.0E-05	3.51E-04	4.6E-08	2.00E-07	6.9E-08	3.01E-07	4.6E-08	2.00E-07	6.9E-08	3.01E-07	6.9E-08	3.01E-07	4.6E-08	2.00E-07	4.6E-05	2.00E-04	1.1E-07	5.01E-07	
H-0352, H-0353, H-0354	Unit 70 CCR Reformer Heaters	200	222	4.6E-04	2.00E-03	2.6E-07	1.14E-06	3.9E-07	1.72E-06	2.6E-07	1.14E-06	3.9E-07	1.72E-06	3.9E-07	1.72E-06	2.6E-07	1.14E-06	2.6E-04	1.14E-03	6.5E-07	2.86E-06	
H-0355	Unit 70 Stabilizer Reboiler Heater	28	31	6.4E-05	2.81E-04	3.7E-08	1.60E-07	5.5E-08	2.40E-07	3.7E-08	1.60E-07	5.5E-08	2.40E-07	5.5E-08	2.40E-07	3.7E-08	1.60E-07	3.7E-05	1.60E-04	9.1E-08	4.01E-07	
H-0362, H-0363, H-0364	Unit 70 CCR Heaters	125	139	2.9E-04	1.25E-03	1.6E-07	7.16E-07	2.5E-07	1.07E-06	1.6E-07	7.16E-07	2.5E-07	1.07E-06	2.5E-07	1.07E-06	1.6E-07	7.16E-07	1.6E-04	7.16E-04	4.1E-07	1.79E-06	
H-0421	Unit 44 Charge Heater	27	30	6.2E-05	2.71E-04	3.5E-08	1.55E-07	5.3E-08	2.32E-07	3.5E-08	1.55E-07	5.3E-08	2.32E-07	5.3E-08	2.32E-07	3.5E-08	1.55E-07	3.5E-05	1.55E-04	8.8E-08	3.86E-07	
H-0464	SRU Hot Oil Heater	10	11	2.2E-05	9.62E-05	1.3E-08	5.50E-08	1.9E-08	8.24E-08	1.3E-08	5.50E-08	1.9E-08	8.24E-08	1.9E-08	8.24E-08	1.3E-08	5.50E-08	1.3E-05	5.50E-05	3.1E-08	1.37E-07	
H-0600	Unit 09 Depropanizer Reboiler Heater	84	93	1.9E-04	8.42E-04	1.1E-07	4.81E-07	1.6E-07	7.21E-07	1.1E-07	4.81E-07	1.6E-07	7.21E-07	1.6E-07	7.21E-07	1.1E-07	4.81E-07	1.1E-04	4.81E-04	2.7E-07	1.20E-06	
H-0601	Unit 33 Charge Heater	78	87	1.8E-04	7.81E-04	1.0E-07	4.47E-07	1.5E-07	6.70E-07	1.0E-07	4.47E-07	1.5E-07	6.70E-07	1.5E-07	6.70E-07	1.0E-07	4.47E-07	1.0E-04	4.47E-04	2.5E-07	1.12E-06	
H-2421	Unit 45 Charge Heater	27	30	6.2E-05	2.71E-04	3.5E-08	1.55E-07	5.3E-08	2.32E-07	3.5E-08	1.55E-07	5.3E-08	2.32E-07	5.3E-08	2.32E-07	3.5E-08	1.55E-07	3.5E-05	1.55E-04	8.8E-08	3.86E-07	
H-2501	Unit 25 ROSE® Unit No. 2 Hot Oil Heater	120	133	2.7E-04	1.20E-03	1.6E-07	6.87E-07	2.4E-07	1.03E-06	1.6E-07	6.87E-07	2.4E-07	1.03E-06	2.4E-07	1.03E-06	1.6E-07	6.87E-07	1.6E-04	6.87E-04	3.9E-07	1.72E-06	
H-3101	SRU3 Hot Oil Heater	11	12	2.5E-05	1.10E-04	1.4E-08	6.30E-08	2.2E-08	9.45E-08	1.4E-08	6.30E-08	2.2E-08	9.45E-08	2.2E-08	9.45E-08	1.4E-08	6.30E-08	1.4E-05	6.30E-05	3.6E-08	1.57E-07	
H-3402	Unit 34 Hydrocracker Reboiler 1	52	58	1.2E-04	5.21E-04	6.8E-08	2.98E-07	1.0E-07	4.47E-07	6.8E-08	2.98E-07	1.0E-07	4.47E-07	1.0E-07	4.47E-07	6.8E-08	2.98E-07	6.8E-05	2.98E-04	1.7E-07	7.44E-07	
H-3403	Unit 34 Hydrocracker Reactor Charge Heater	32	36	7.3E-05	3.21E-04	4.2E-08	1.83E-07	6.3E-08	2.75E-07	4.2E-08	1.83E-07	6.3E-08	2.75E-07	6.3E-08	2.75E-07	4.2E-08	1.83E-07	4.2E-05	1.83E-04	1.0E-07	4.58E-07	
H-5401	Unit 54 HDS Reactor Heater	19	21	4 4F-05	1.94E-04	2.5E-08	1.11E-07	3 8F-08	1 66F-07	2 5F-08	1.11E-07	3 8F-08	1 66F-07	3.8E-08	1.66E-07	2 5F-08	1 11F-07	2 5F-05	1.11E-04	6 3F-08	2.77E-07	
H-8801/8802	Unit 63 Hydrogen Plant Reformer Furnaces	152	169		1.52E-03						8.70E-07		1.31E-06		1.31E-06				8.70E-04			
H-9851	Unit 64 Hydrogen Plant Reformer	337	374	7.7E-04	3.38E-03	4.4E-07	1.93E-06	6.6E-07	2.89E-06	4.4E-07	1.93E-06	6.6E-07	2.89E-06	6.6E-07	2.89E-06	4.4E-07	1.93E-06	4.4E-04	1.93E-03	1.1E-06	4.82E-06	
TOTAL (AP-42, Ch. 1.4 (7/98) Table 1.4-3 HAPs for Natural Gas Combustion Units)					0.02		1.34E-05		2.01E-05		1.34E-05		2.01E-05		2.01E-05		1.34E-05		0.01		3.35E-05	

				Fluo	rene	Formal	dehyde	He	exane		o(1,2,3- yrene	Napht	halene	Phenan	athrene	Руг	ene	Toli	uene	Ars	senic
			CAS No.	86-	73-7	50-0	00-0	110	0-54-3	193	-39-5	91-2	20-3	85-	01-8	129	-00-0	108-	-88-3	7440	0-38-2
	AP-42, Ch. 1.4 (7/98) Table 1.4-3 HAPs for Natural Gas Combustion Units		Emission Factor lb/mmBtu		2.7E-09		7.4E-05		1.8E-03		1.8E-09		6.0E-07		1.7E-08		E-09	3.3E-06		2.0E-07	
		Design Capacity (LHV)	Design Capacity (HHV)	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
ID	Description	MMBtu/hr	MMBtu/hr																		
B-0007	Boiler 7	215	239	6.6E-07	2.87E-06	1.8E-02	7.69E-02	4.2E-01	1.85E+00	4.2E-07	1.85E-06	1.4E-04	6.26E-04	4.0E-06	1.74E-05	1.2E-06	5.13E-06	8.0E-04	3.49E-03	4.7E-05	2.05E-04
B-0008	Boiler 8	215	239	6.6E-07	2.87E-06	1.8E-02	7.69E-02	4.2E-01	1.85E+00	4.2E-07	1.85E-06	1.4E-04	6.26E-04	4.0E-06	1.74E-05	1.2E-06	5.13E-06	8.0E-04	3.49E-03	4.7E-05	2.05E-04
B-0009	Boiler 9	220	244	6.7E-07	2.94E-06	1.8E-02	7.87E-02	4.3E-01	1.89E+00	4.3E-07	1.89E-06	1.5E-04	6.40E-04	4.1E-06	1.78E-05	1.2E-06	5.25E-06	8.1E-04	3.57E-03	4.8E-05	2.10E-04
H-0009	Unit 13 Naphtha Splitter Reboiler	44	49	1.3E-07	5.88E-07	3.6E-03	1.57E-02	8.6E-02	3.78E-01	8.6E-08	3.78E-07	2.9E-05	1.28E-04	8.1E-07	3.57E-06	2.4E-07	1.05E-06	1.6E-04	7.14E-04	9.6E-06	4.20E-05
H-0011	Unit 21 Vacuum Unit Heater	38	42	1.2E-07	5.08E-07	3.1E-03	1.36E-02	7.5E-02	3.26E-01	7.5E-08	3.26E-07	2.5E-05	1.11E-04	7.0E-07	3.08E-06	2.1E-07	9.06E-07	1.4E-04	6.16E-04	8.3E-06	3.63E-05
H-0018	Unit 06 HDS Reboiler	32	36	9.8E-08	4.27E-07	2.6E-03	1.14E-02	6.3E-02	2.75E-01	6.3E-08	2.75E-07	2.1E-05	9.31E-05	5.9E-07	2.60E-06	1.7E-07	7.63E-07	1.2E-04	5.19E-04	7.0E-06	3.05E-05
H-0019	South Crude Charge Heater	54	60	1.6E-07	7.21E-07	4.4E-03	1.93E-02	1.1E-01	4.64E-01	1.1E-07	4.64E-07	3.6E-05	1.57E-04	1.0E-06	4.38E-06	2.9E-07	1.29E-06	2.0E-04	8.76E-04	1.2E-05	5.15E-05
H-0020	South Crude Charge Heater	90	100	2.7E-07	1.20E-06	7.4E-03	3.22E-02	1.8E-01	7.73E-01	1.8E-07	7.73E-07	6.0E-05	2.62E-04	1.7E-06	7.30E-06	4.9E-07	2.15E-06	3.3E-04	1.46E-03	2.0E-05	8.59E-05
H-0028	Unit 21 Heater	12	14	3.8E-08	1.64E-07	1.0E-03	4.40E-03	2.4E-02	1.06E-01	2.4E-08	1.06E-07	8.2E-06	3.58E-05	2.3E-07	9.98E-07	6.7E-08	2.93E-07	4.6E-05	2.00E-04	2.7E-06	1.17E-05
H-0030	Unit 06 Charge Heater	42	47	1.3E-07	5.61E-07	3.4E-03	1.50E-02	8.2E-02	3.61E-01	8.2E-08	3.61E-07	2.8E-05	1.22E-04	7.8E-07	3.41E-06	2.3E-07	1.00E-06	1.6E-04	6.81E-04	9.1E-06	4.01E-05
H-0040	Unit 13 Charge Heater	42	47	1.3E-07	5.61E-07	3.4E-03	1.50E-02	8.2E-02	3.61E-01	8.2E-08	3.61E-07	2.8E-05	1.22E-04	7.8E-07	3.41E-06	2.3E-07	1.00E-06	1.6E-04		9.1E-06	
H-0312	Unit 10 FCC Feed Heater	35	39	1.1E-07	4.68E-07	2.9E-03	1.25E-02	6.9E-02	3.01E-01	6.9E-08	3.01E-07	2.3E-05	1.02E-04	6.5E-07	2.84E-06	1.9E-07	8.35E-07	1.3E-04	5.68E-04	7.6E-06	3.34E-05
H-0352, H-0353, H-035	Unit 70 CCR Reformer Heaters	200	222	6.1E-07	2.67E-06	1.6E-02	7.16E-02	3.9E-01	1.72E+00	3.9E-07	1.72E-06	1.3E-04	5.82E-04	3.7E-06	1.62E-05	1.1E-06	4.77E-06	7.4E-04	3.24E-03	4.4E-05	1.91E-04
H-0355	Unit 70 Stabilizer Reboiler Heater	28	31	8.5E-08	3.74E-07	2.3E-03	1.00E-02	5.5E-02	2.40E-01	5.5E-08	2.40E-07	1.9E-05	8.15E-05	5.2E-07	2.27E-06	1.5E-07	6.68E-07	1.0E-04	4.54E-04	6.1E-06	2.67E-05
H-0362, H-0363, H-036	Unit 70 CCR Heaters	125	139	3.8E-07	1.67E-06	1.0E-02	4.47E-02	2.5E-01	1.07E+00	2.5E-07	1.07E-06	8.3E-05	3.64E-04	2.3E-06	1.01E-05	6.8E-07	2.98E-06	4.6E-04	2.03E-03	2.7E-05	1.19E-04
H-0421	Unit 44 Charge Heater	27	30	8.2E-08	3.61E-07	2.2E-03	9.66E-03	5.3E-02	2.32E-01	5.3E-08	2.32E-07	1.8E-05	7.86E-05	5.0E-07	2.19E-06	1.5E-07	6.44E-07	1.0E-04	4.38E-04	5.9E-06	2.58E-05
H-0464	SRU Hot Oil Heater	10	11	2.9E-08	1.28E-07	7.8E-04	3.43E-03	1.9E-02	8.24E-02	1.9E-08	8.24E-08	6.4E-06	2.79E-05	1.8E-07	7.79E-07	5.2E-08	2.29E-07	3.6E-05	1.56E-04	2.1E-06	9.16E-06
H-0600	Unit 09 Depropanizer Reboiler Heater	84	93	2.6E-07	1.12E-06	6.9E-03	3.01E-02	1.6E-01	7.21E-01	1.6E-07	7.21E-07	5.6E-05	2.44E-04	1.6E-06	6.81E-06	4.6E-07	2.00E-06	3.1E-04	1.36E-03	1.8E-05	8.01E-05
H-0601	Unit 33 Charge Heater	78	87	2.4E-07	1.04E-06	6.4E-03	2.79E-02	1.5E-01	6.70E-01	1.5E-07	6.70E-07	5.2E-05	2.27E-04	1.4E-06	6.33E-06	4.2E-07	1.86E-06	2.9E-04	1.27E-03	1.7E-05	7.44E-05
H-2421	Unit 45 Charge Heater	27	30	8.2E-08	3.61E-07	2.2E-03	9.66E-03	5.3E-02	2.32E-01	5.3E-08	2.32E-07	1.8E-05	7.86E-05	5.0E-07	2.19E-06	1.5E-07	6.44E-07	1.0E-04	4.38E-04	5.9E-06	2.58E-05
H-2501	Unit 25 ROSE® Unit No. 2 Hot Oil Heater	120	133	3.7E-07	1.60E-06	9.8E-03	4.29E-02	2.4E-01	1.03E+00	2.4E-07	1.03E-06	8.0E-05	3.49E-04	2.2E-06	9.73E-06	6.5E-07	2.86E-06	4.4E-04	1.95E-03	2.6E-05	1.14E-04
H-3101	SRU3 Hot Oil Heater	11	12	3.4E-08	1.47E-07	9.0E-04	3.94E-03	2.2E-02	9.45E-02	2.2E-08	9.45E-08	7.3E-06	3.20E-05	2.0E-07	8.92E-07	6.0E-08	2.62E-07	4.1E-05	1.78E-04	2.4E-06	1.05E-05
H-3402	Unit 34 Hydrocracker Reboiler 1	52	58	1.6E-07	6.95E-07	4.2E-03	1.86E-02	1.0E-01	4.47E-01	1.0E-07	4.47E-07	3.5E-05	1.51E-04	9.6E-07	4.22E-06	2.8E-07	1.24E-06	1.9E-04	8.43E-04	1.1E-05	4.96E-05
H-3403	Unit 34 Hydrocracker Reactor Charge Heater	32	36	9.8E-08	4.27E-07	2.6E-03	1.14E-02	6.3E-02	2.75E-01	6.3E-08	2.75E-07	2.1E-05	9.31E-05	5.9E-07	2.60E-06	1.7E-07	7.63E-07	1.2E-04	5.19E-04	7.0E-06	3.05E-05
H-5401	Unit 54 HDS Reactor Heater	19	21	5.9E-08	2.58E-07	1.6E-03	6.91E-03	3.8E-02	1.66E-01	3.8E-08	1.66E-07	1.3E-05	5.62E-05	3.6E-07	1.57E-06	1.1E-07	4.61E-07	7.2E-05	3.13E-04	4.2E-06	1.84E-05
H-8801/8802	Unit 63 Hydrogen Plant Reformer Furnaces	152	169	4.6E-07	2.03E-06	1.2E-02	5.44E-02	3.0E-01	1.31E+00	3.0E-07	1.31E-06	1.0E-04	4.42E-04	2.8E-06	1.23E-05	8.3E-07	3.63E-06	5.6E-04	2.47E-03	3.3E-05	1.45E-04
H-9851	Unit 64 Hydrogen Plant Reformer	337	374	1.0E-06	4.50E-06	2.8E-02	1.21E-01	6.6E-01	2.89E+00	6.6E-07	2.89E-06	2.2E-04	9.81E-04	6.2E-06	2.73E-05	1.8E-06	8.04E-06	1.2E-03	5.47E-03	7.3E-05	3.22E-04
TOTAL (AP-42, Ch. 1.4 (7/98) Table 1.4-3 HAPs for Natural Gas Combustion Units)					3.13E-05		0.84		20.10		2.01E-05		0.01		1.90E-04		5.58E-05		0.04		0.002

	CAS No.					Cadmium		Chromium		Cobalt		Manganese			cury		
4.0	7440	-41-7	7440-43-9		7440-47-3		7440-48-4		7439-96-5		7439-97-6		7782-49-2				
AP-42, Ch. 1.4 (7/98) Table 1.4-3 HAPs for Natural Gas Combustion Units Emission Factor lb/mmBtu					E-08 1.1E		1E-06 1		E-06	8.2E-08		3.7E-07		2.5E-07		2.41	E-08
	Design Capacity Design Capa										l						
ID	Description	(LHV)	(HHV)	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
B-0007	Boiler 7	MMBtu/hr 215	MMBtu/hr 239	2.8E-06	1.23E-05	2.6E-04	1.13E-03	2 2E 04	1.44E-03	2 05 05	8.62E-05	9 DE DE	3.90E-04	6 1E 0E	2.67E-04	E 6E 06	2.46E-05
B-0007	Boiler 8	215	239	2.8E-06	1.23E-05		1.13E-03		1.44E-03		8.62E-05				2.67E-04		2.46E-05
B-0008	Boiler 9	220	244				1.15E-03								2.73E-04		
H-0009	Unit 13 Naphtha Splitter Reboiler	44	49	5.8E-07	2.52E-06		2.31E-04		2.94E-04						5.46E-05		5.04E-06
H-0011	Unit 21 Vacuum Unit Heater	38	42	5.0E-07	2.32L-06		1.99E-04		2.54E-04			1.6E-05			4.71E-05		4.35E-06
H-0011	Unit 06 HDS Reboiler	32	36				1.68E-04		2.14E-04						3.97E-05		3.66E-06
H-0019	South Crude Charge Heater	54	60	7.1E-07	3.09E-06		2.83E-04		3.61E-04		2.16E-05		9.79E-05		6.70E-05		6.18E-06
H-0020	South Crude Charge Heater	90	100	1.2E-06			4.72E-04		6.01E-04			3.7E-05			1.12E-04		
H-0028	Unit 21 Heater	12	14	1.6E-07	7.04E-07		6.45E-05		8.22E-05						1.53E-05		1.41E-06
H-0030	Unit 06 Charge Heater	42	47	5.5E-07	2.40E-06		2.20E-04		2.81E-04						5.21E-05		4.81E-06
H-0040	Unit 13 Charge Heater	42	47	5.5E-07	2.40E-06		2.20E-04		2.81E-04			1.7E-05			5.21E-05		
H-0312	Unit 10 FCC Feed Heater	35	39	4.6E-07	2.00E-06		1.84E-04		2.34E-04				6.35E-05		4.34E-05		
H-0352,	Unit 70 CCR Reformer Heaters	200	222	2.6E-06	1.14E-05	2.4E-04	1.05E-03		1.34E-03		8.01E-05		3.63E-04		2.48E-04	5.2E-06	
H-0353, H-0354					4 505 05	2 45 25	== 0.		4 075 04	2 55 25		4 25 25		7.05.00	0.475.05	7.05.07	2245.00
H-0355	Unit 70 Stabilizer Reboiler Heater	28	31	3.7E-07	1.60E-06	3.4E-05	1.47E-04	4.3E-05	1.87E-04	2.6E-06	1.12E-05	1.2E-05	5.08E-05	7.9E-06	3.47E-05	7.3E-07	3.21E-06
H-0362, H-0363, H-0364	Unit 70 CCR Heaters	125	139	1.6E-06	7.16E-06	1.5E-04	6.56E-04	1.9E-04	8.35E-04	1.1E-05	5.01E-05	5.2E-05	2.27E-04	3.5E-05	1.55E-04	3.3E-06	1.43E-05
H-0421	Unit 44 Charge Heater	27	30	3.5E-07	1.55E-06	3.2E-05	1.42E-04	4.1E-05	1.80E-04	2.5E-06	1.08E-05	1.1E-05	4.89E-05	7.6E-06	3.35E-05	7.1E-07	3.09E-06
H-0464	SRU Hot Oil Heater	10	11	1.3E-07	5.50E-07	1.2E-05	5.04E-05	1.5E-05	6.41E-05	8.8E-07	3.85E-06	4.0E-06	1.74E-05	2.7E-06	1.19E-05	2.5E-07	1.10E-06
H-0600	Unit 09 Depropanizer Reboiler Heater	84	93	1.1E-06	4.81E-06	1.0E-04	4.41E-04	1.3E-04	5.61E-04	7.7E-06	3.37E-05	3.5E-05	1.52E-04	2.4E-05	1.04E-04	2.2E-06	9.62E-06
H-0601	Unit 33 Charge Heater	78	87	1.0E-06	4.47E-06	9.3E-05	4.09E-04	1.2E-04	5.21E-04	7.1E-06	3.13E-05	3.2E-05	1.41E-04	2.2E-05	9.68E-05	2.0E-06	8.93E-06
H-2421	Unit 45 Charge Heater	27	30	3.5E-07	1.55E-06	3.2E-05	1.42E-04	4.1E-05	1.80E-04	2.5E-06	1.08E-05	1.1E-05	4.89E-05	7.6E-06	3.35E-05	7.1E-07	3.09E-06
H-2501	Unit 25 ROSE® Unit No. 2 Hot Oil Heater	120	133	1.6E-06	6.87E-06	1.4E-04	6.30E-04	1.8E-04	8.01E-04	1.1E-05	4.81E-05	5.0E-05	2.18E-04	3.4E-05	1.49E-04	3.1E-06	1.37E-05
H-3101	SRU3 Hot Oil Heater	11	12	1.4E-07	6.30E-07	1.3E-05	5.77E-05	1.7E-05	7.35E-05	1.0E-06	4.41E-06	4.6E-06	1.99E-05	3.1E-06	1.36E-05	2.9E-07	1.26E-06
H-3402	Unit 34 Hydrocracker Reboiler 1	52	58	6.8E-07	2.98E-06	6.2E-05	2.73E-04	7.9E-05	3.47E-04	4.8E-06	2.08E-05	2.2E-05	9.43E-05	1.5E-05	6.45E-05	1.4E-06	5.95E-06
11.2402	Unit 34 Hydrocracker Reactor Charge			4 25 07	4 025 65	2.05.05	4 605 61	4.05.05	2 4 4 5 6 4	2.05.05	4 205 65	4 25 65	5 005 CT	0.45.65	2.075.65	0.45.07	2.555.65
H-3403	Heater	32	36	4.2E-07	1.83E-06	3.8E-05	1.68E-04	4.9E-05	2.14E-04	2.9E-06	1.28E-05	1.3E-05	5.80E-05	9.1E-06	3.97E-05	8.4E-07	3.66E-06
H-5401	Unit 54 HDS Reactor Heater	19	21	2.5E-07	1.11E-06	2.3E-05	1.01E-04	2.9E-05	1.29E-04	1.8E-06	7.74E-06	8.0E-06	3.50E-05	5.5E-06	2.40E-05	5.1E-07	2.21E-06
H-8801/8802	Unit 63 Hydrogen Plant Reformer Furnaces	152	169	2.0E-06	8.70E-06	1.8E-04	7.98E-04	2.3E-04	1.02E-03	1.4E-05	6.09E-05	6.3E-05	2.76E-04	4.3E-05	1.89E-04	4.0E-06	1.74E-05
H-9851	Unit 64 Hydrogen Plant Reformer	337	374	4.4E-06	1.93E-05	4.0E-04	1.77E-03	5.1E-04	2.25E-03	3.1E-05	1.35E-04	1.4E-04	6.11E-04	9.5E-05	4.18E-04	8.8E-06	3.86E-05
TOTAL (AP-42, Ch. 1.4 (7/98) Table 1.4-3 HAPs for Natural Gas Combustion Units)					1.34E-04		0.01		0.02		9.38E-04		0.004		0.003		2.68E-04

SRUs POTENTIAL TO EMIT

			RU2 lust Flow Rate ⁽¹⁾	H-0473 (SRU2 TGI)						
Pollutant	MW	Maximum	Average	Concentration at max flow ⁽²⁾	Concentration at average flow ⁽²⁾	Potential to Emit				
		dscfm	dscfm	ppmvd	ppmvd	lb/hr	ton/yr			
NOx	46			36	93	6.50	28.50			
CO	28			250	650	27.70	121.10			
VOC	44			0.4	2.0	0.10	0.60			
SO2	64	35,000		118.1	192	30.00	81.80			
H2S	34	25,000	9,600	1.9	5.8	0.30	1.40			
SAM	98]		-	-	2.30	6.26			
PM	-	1		0.006 gr/dscf	0.006 gr/dscf	1.20	2.10			
PM ₁₀ /PM _{2.5}	-			-	-	3.50	8.36			

		_	RU 3 lust Flow Rate ⁽¹⁾	H-3103 (SRU3 TGI)						
Pollutant	MW	Maximum Average		Concentration at max flow ⁽²⁾	Concentration at average flow ⁽²⁾	Potential to Emit				
		dscfm	dscfm	ppmvd	ppmvd	lb/hr	ton/yr			
NOx	46			42	93	6.50	28.50			
СО	28			161	352	15.00	65.70			
VOC	44			0.1	2.0	0.10	0.60			
SO2	64	24 000		140.8	192	30.00	81.80			
H2S	34	21,000	9,600	2.1	5.8	0.30	1.40			
SAM	98			-	-	2.30	6.26			
PM	-]		0.006 gr/dscf	0.006 gr/dscf	1.10	2.10			
PM ₁₀ /PM _{2.5}	-			-	-	3.40	8.36			

Notes

- (1) TGI stack exhaust flow rate per operations (60°F and 1 atm)
- (2) NO_x, CO, and VOC per site data. SO₂, and H₂S concentration per CEMS data. SAM assumed 5% conversion SO₂ to SO₃ and 100% SO₃ to H₂SO₄. PM per AP-42, Ch. 8.13 (4/15), Chevron Texaco Pascagoula Refinery Emissions Test Data, 2007. PM ₁₀/PM_{2.5} assumed to be PM + SAM
- (3) Standard molar volume at 60F

379.51 scf/lbmol

Sample Calculation H-0473 (SRU 2 TGI)

 $NOx = 25,000 \text{ scf/min} * 60 \text{ min/hr} * 1 \text{ lbmol/380 scf} * 35.7/10^6 * 46 \text{ lb/lbmole} = 6.5 \text{ lb/hr}$

 $NOx = 9,600 \ scf/min * 60 \ min/hr * 1 \ lbmol/380 \ scf * 93.0/10^6 * 46 \ lb/lbmole * 8760 \ hr/yr * 1 \ ton/2,000 \ lb = 28.5 \ lb/hr =$

SRU POTENTIAL TO EMIT GHG

	Sour Gas Volumetric Flow Rate ⁽¹⁾	Molar Volume Conversion (MVC) ⁽²⁾	Mole Fraction of Carbon (MFc) ⁽³⁾	СС	2 ⁽⁴⁾
Unit	scf/yr	scf/kgmole	kgmolC/kgmolgas	metric tons/yr	ton/yr
H-0473 (SRU2 TGI)	1,200	836.6	0.20	12,623	13,914
H-3103 (SRU3 TGI)	1,400	836.6	0.20	14,726	16,233

Notes:

- (1) Sour volumetric flow rate (amine acid gas and sour water gas) per Operation, Maintenance and Instruction Manuals, 2001
- (2) Molar volume conversion factor (849.5 scf/kg-mole at 68 $^{\circ}$ F and 14.7 psia or 836.6 scf/kg-mole at 60 $^{\circ}$ F and 14.7 psia).
- (3) Mole fraction of carbon in the sour gas fed to the sulfur recovery plant or the sour gas feed sent off-site for sulfur recovery (kg-mole C/kg-mole gas); default = 0.20.
- (4) CO2 metric tons, per Eq. Y-12, subpart Y of Part 98. 1 metric ton = 1.10231 tons

FCC REGEN POTENTIAL TO EMIT

Calculation Basis:		Units
FCC Capacity	30,000	bbl/day
FCC Stack Exhaust Flow Rate	55,000	dscfm
Maximum Coke Burn Rate	25,000	lb/hr
Conversion Factor	379	scf/lbmol
Annual Hours of Operation	8,760	hr/yr

	Units	NO _x (1)	CO (2)	VOC (3)	SO ₂ (4)	SAM (5)	PM ⁽⁶⁾	PM ₁₀ ⁽⁷⁾	PM _{2.5} ⁽⁷⁾
Molecular Weight	lb/lb-mol	46	28	-	64	98	-	-	-
Concentration for Maximum Hourly Emission Rate	ppmvd	87.3	500	-	50	-	-	-	-
Concentration for Annual Average Emission Rate	ppmvd	58.1	100	-	25	-	-	-	-
Maximum PM emission rate	lb/toncoke	-	-	-	-	-	2		
Maximum Hourly Emission Rate	lb/hr	34.92	121.79	15.66	27.85	2.13	25.00	22.88	22.88
Annual Average Emission Rate	ton/yr	101.80	106.69	68.60	61.00	4.67	109.50	95.55	68.81

Notes:

- (1) Per Consent Decree NO_x max. hourly emissions based on 87.3 ppmvd at 0% O₂ on a 7-day rolling avg. basis, and annual avg. emissions based on 58.1 ppmvd at 0% O₂ on a 365-day rolling avg. basis
- (2) Per NSPS Subpart J CO max. hourly emissions based on 500 ppvd at 0% O2 on a 1-hr avg. basis, and annual avg. emissions based on 100 ppmvd at 0% O2 on a 365-day rolling avg. basis
- (3) VOC assumed to be 2 * sum of volatile and semi-volatile HAPs
- (4) Per Consent Decree SO₂ max. hourly emissions based on 50 ppmvd at 0% O₂ on a 7-day rolling avg. basis, and annual avg. emissions based on 25 ppmvd at 0% O₂ on a 365-day rolling avg. basis
- (5) SAM based on 5% oxidation SO₂ to SAM
- (6) Per NSPS Subpart J PM 2.0 lb/ton of coke burn-off in the catalyst regenerator
- (7) PM_{10 is} 83% of PM plus 100% SAM; PM2.5 is 83% of PM plus 100% SAM for maximum hourly calculation and 58.6% of PM plus 100% SAM for annual average

Sample Calculation:

 $NOx = 55,000 \ dscf/min*60 \ min/hr*1/379 \ scf/lbmol*87.3/10^6*46lb/lbmol=34.9 \ lb/hr$ $NOx = 55,000 \ dscf/min*60 \ min/hr*1/379 \ scf/lbmol*58.1/10^6*46lb/lbmol*8,760 \ hr/yr*1 \ ton/2,000 \ lb=101.8 \ ton/yr$

FCC REGEN POTENTIAL TO EMIT GHG

GHG emissions associated with FCC are based on the maximum reported rate between 2011 and 2015 increased by 100% to estimate the potential to emit.

	Fugi	GHG (as CO₂e)		
	CO ₂	CH ₄	N ₂ O	(ton/yr)
ls	1	25	298	
CC	430,013	12.6	2.5	431,077

Table A-1 to 40 CFR 98, subpart A, Global Warming Potentials

FCC REGEN POTENTIAL TO EMIT HAPS

Maximum Individual HAPs (Hydrogen cyanide) 92.1 ton/yr
Total HAPs 127.7 ton/yr

		Emissions Factor	Emissions	Emissions	Emissions	Emissions
CAS No.	Compound	(lb/klb coke burn	Factor	Factor	(lb/hr)	(ton/yr)
		off) ⁽¹⁾	(lb/MMbbl) ⁽¹⁾	(lb/MMbbl) ⁽²⁾	(ID/Nr)	(ton/yr)
Volatile Org	anics				,	
75-07-0	Acetaldehyde	0.0013	20	194.3	0.2	1.1
67-64-1	Acetone	1.60E-04	2.4	468.6	0.6	2.6
107-02-8	Acrolein	6.60E-05	1	617.1	0.8	3.4
71-43-2	Benzene	1.10E-03	18	582.9	0.7	3.2
74-83-9	Bromomethane	1.40E-04	2.1	0	0.004	0.02
106-99-0	1,3-Butadiene	2.00E-06	0.033	708.6	0.9	3.9
100-41-4	Ethylbenzene	1.60E-05	0.24	86.9	0.1	0.5
50-00-0	Formaldehyde	0.016	260	365.5	0.5	2.0
75-09-2	Methylene chloride	4.40E-04	6.7	1,485.7	1.9	8.1
108-95-2	Phenol	5.70E-04	8.7	971.2	1.2	5.3
108-88-3	Toluene	2.10E-04	3.5	1,156.0	1.4	6.3
75-69-4	Trichlorofluoromethane	1.60E-04	2.4	0.0	0.0	0.0
1330-20-7	Xylene	2.10E-04	3.2	86.9	0.1	0.5
Semivolatile	and Nonvolatile Organics(excl	uding dioxin/furan	s)			
83-32-9	Acenaphthene	2.20E-07	0.0033	0.04	4.6E-05	2.0E-04
208-96-8	Acenaphthylene	7.80E-06	0.13	0	2.0E-04	8.5E-04
120-12-7	Anthracene	6.70E-06	0.1	0.1	1.7E-04	7.3E-04
56-55-3	Benzo(a)anthracene	3.80E-08	0.00052	0.2	1.9E-04	8.2E-04
50-32-8	Benzo(a)pyrene	7.10E-07	0.011	0.02	2.2E-05	9.8E-05
205-99-2	Benzo(b)fluoranthene	2.40E-07	0.0035	0.02	2.2E-05	9.8E-05
192-97-2	Benzo(e)pyrene	3.30E-08	0.00045	0.02	2.2E-05	9.8E-05
191-24-2	Benzo(g,h,i)perylene	3.10E-07	0.0046	0.02	2.2E-05	9.8E-05
207-08-9	Benzo(k)fluoranthene	1.80E-07	0.0026	0.02	2.2E-05	9.8E-05
218-01-9	Chrysene	2.30E-07	0.0033	0.1	1.8E-04	7.7E-04
53-70-3	Dibenz(a,h)anthracene	2.80E-07	0.0042	0.02	2.2E-05	9.8E-05
206-44-0	Fluoranthene	6.10E-06	0.093	0.3	3.2E-04	1.4E-03
86-73-7	Fluorene	2.40E-06	0.037	0.02	6.0E-05	2.6E-04
193-39-5	Indeno(1,2,3-cd)pyrene	3.00E-07	0.0044	0.02	2.2E-05	9.8E-05
91-57-6	2-Methylnaphthalene	1.80E-06	0.026	0.02	4.5E-05	2.0E-04
91-20-3	Naphthalene	7.00E-05	1	0.2	1.8E-03	7.7E-03
85-01-8	Phenanthrene	1.60E-05	0.24	0.4	4.7E-04	2.0E-03
129-00-0	Pyrene	2.20E-07	0.0031	0.8	9.7E-04	4.3E-03
Dioxins/Fur	· ·	2.202 07	0.0001	0.0	31,72 0 1	
57117-31-4	Pentachlorodibenzofurans	3.20E-11	5.50E-07	9.03E-07	1.1E-09	4.9E-09
57117-31-4	Hexachlorodibenzofuran	6.30E-11	1.10E-06	9.03E-07	1.6E-09	6.9E-09
35822-46-9	Heptachlorodibenzo-p-dioxin	5.60E-11	9.40E-07	4.91E-07	1.4E-09	6.1E-09
Inorganics	i reptacino ouibenzo-p-uloxiii	J.00L-11	J. T UL ⁻ U/	4.J1L-0/	1.76-03	U.1L-UJ
7664-41-7	Ammonia	0.57	13,000	1,576	16.3	71.2
75-15-0	Carbon disulfide			243	0.3	1.3
7647-01-0		3.70E-05	0.56	243	2.8	1.3
	Hydrogen chloride	0.11	1,800	-	-	
74-90-8	Hydrogen cyanide	0.43	7,000	16,814	21.0	92.1
7439-97-6	Mercury ⁽³⁾	6.00E-06	0.094	0.2	0.0002	0.001

Notes

(1) Emissions factors for CCU controlled for organics in pounds per thousand pounds of coke burn-off. April 2015 Emissions Estimation Protocol for Petroleum Refineries, Version 3

(2) Emissions factors based on ICR reported FCCU data and NPRA capacities

(3) Total mercury emissions factor. Elemental mercury emissions are approximately 80 percent of total mercury emissions and divalent (oxidized plus particulate) mercury emissions are approximately 20 percent of total mercury emissions.

FLARES POTENTIAL TO EMIT

Molar Volume: 385.3 scf/lbmol (STP 68°F and 14.7 psia)

NOx Factor: 0.068 lb/MMBtu (HHV) per EPA AP-42, Table 13.5-1, dated Feb. 2018

0.076 lb/MMBtu (LHV) HHV/LHV ratio of 1.111

CO Factor: 0.31 lb/MMBtu (LHV) per EPA AP-42, Table 13.5-2, dated Feb. 2018

Flare VOC Eff: 98.0%

Emission Calculations for Proposed Permit 0195-M40 Emission Limits - Normal Operations ^a

	FLOW	voc	S	NO _x	со	VOC	SO ₂	H ₂ S	
	MMBtu/hr	lb/hr	lbmol/hr			lb/hr			
Flare ID	(LHV)	,				,			
FL-400	45.91	1,301	0.06989	3.47	14.23	26.01	4.48	0.05	
FL-401	22.01	986	0.89514	1.66	6.82	19.72	57.35	0.61	
FL-402	107.39	4,909	1.53806	8.11	33.29	98.18	98.54	1.05	
FL-403	36.30	1,627	0.01717	2.74	11.25	32.54	1.10	0.01	
FL-404	154.87	8,025	0.62308	11.70	48.01	160.50	39.92	0.42	
	SUM	OF PROPOSED EM	27.69	113.61	336.95	201.38	2.14		
	SUI	M OF CURRENT EN	IISSION LIMITS:	18.25	83.17	97.00	101.34	0	
P	ROPOSED INCREA	ASE IN SUM OF EM	ISSION LIMITS:	9.44	30.44	239.95	100.04	2.14	
				tpy					
FL-400	16.46	373.3	0.01397	5.45	22.35	32.70	3.92	0.04	
FL-401	5.59	28.7	0.02096	1.85	7.58	2.51	5.88	0.06	
FL-402	6.69	88.1	0.01990	2.21	9.08	7.72	5.58	0.06	
FL-403	7.65	154.9	0.00270	2.53	10.38	13.57	0.76	0.01	
FL-404	70.99	1139.9	0.03969	23.49	96.40	99.85	11.14	0.12	
	SUM	OF PROPOSED EM	35.53	145.80	156.35	27.28	0.29		
	SUI	M OF CURRENT EN	IISSION LIMITS:	27.74	126.46	99.26	22.27	0	
P	ROPOSED INCREA	ASE IN SUM OF EM	ISSION LIMITS:	7.79	19.34	57.09	5.01	0.29	

Notes:

FLARES POTENTIAL TO EMIT GHG ^a

CO ₂ Emission Factor	60	kg/MMBtu (HHV)	40 CFR §98.253(b)(1), default flare gas
CH ₄ Emission Factor	1.00E-03	kg/MMBtu (HHV)	Table C-2 to Subpart C to Part 98, Natural Gas
N ₂ O Emission Factor	1.00E-04	kg/MMBtu (HHV)	Table C-2 to Subpart C to Part 98, Natural Gas
Metric tons to short tons	1.10231	short ton/metric ton	Table A-2 to Subpart C of Part 98
Weight Fraction of Carbon			

Weight Fraction of Carbon in Flare Gas (f_{CH4}) 0.40 kg/kg 40 CFR §98.253(b)(1), default flare gas

HHV/LHV Ratio 1.111

GHG GWP									
CO ₂ CH ₄ N ₂ O									
1	25	298							

Potential to Emit:

	FLOW (MMBtu/hr)	CO2	CH₄	N ₂ O	CO₂e						
Flare ID	(LHV)		TP								
FL-400	16.461	10,384	31.0	0.02	11,164						
FL-401	5.585	3,523	10.5	0.01	3,788						
FL-402	6.690	4,220	12.6	0.01	4,537						
FL-403	7.648	4,824	14.4	0.01	5,187						
FL-404	70.994	44,784	133.7	0.1	48,148						
	PROPOSED TOTAL:										

Notes:

(1) GHG emissions conservatively calculated using 40 CFR Part 98, Subpart Y, Equation Y-2:

Eq. Y-2

$$CO_2 = 0.98 \times 0.001 \times \sum_{p=1}^{n} Flare_p \times HHV_p \times EF_{CO2}$$

Eq. Y-4

$$CH_4 = \left(CO_2 \times \frac{EF_{CH_4}}{EF_{CO_2}}\right) + \left(CO_2 \times \frac{0.02}{0.98} \times \frac{16}{44} \times f_{CH_4}\right)$$

Eq. Y-5 $N_2O = CO_2 \times \frac{EF_{N_2O}}{EF_{CO_2}}$

Where

Flare_p: volume of flare gas combusted (scf)

HHVp: Higher heating value for the flare gas combusted during measurement period (Btu/scf)

EF_{CO2}: default CO2 emissionf actor for flare gas:

 EF_CH4 : default emission factor for fuel gas for CH4, per Table C-2 to Part 98:

 EF_N2O : default emission factor for fuel gas for N2O, per Table C-2 to Part 98:

 $f_{\text{CH4}}\text{: weight fraction of carbon in the flare gas, monitored or default 0.4 } kg_{\text{CCH4}}/kg_{\text{Cflaregas}}$

a. Emission limits are based on flare monitoring data for October 2020 through March 2021. Inputs used in calculations above (e.g., MMBtu/hr, uncontrolled VOC, sulfur input) are for representation purposes only. They are not proposed limits.

						F!!		-/						Potentia	l to Emit					
Fastas	Danasistias	НР	Operating	BSFC		Emissi	on Factors	, g/np-nr		N	O _x	С	ю.	V	oc	S	02	PM/PM	₁₀ /PM _{2.5}	Emission
Engine	Description	ни	Hours	(Btu/hp-hr)	NO _x	со	voc	SO ₂	PM/PM ₁₀ / PM _{2.5}	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	Factors
MG-0001	Portable Air Compressor	280	8760	8,000	3.0	2.6	3.0	15 ppm	0.15	1.84	8.06	1.61	7.06	1.84	8.06	0.003	0.015	0.09	0.40	Note 1
MG-0002	Portable Air Compressor	280	8760	8,000	3.0	2.6	3.0	15 ppm	0.15	1.84	8.06	1.61	7.06	1.84	8.06	0.003	0.015	0.09	0.40	Note 1
MG-0003	Portable Air Compressor	138	8760	8,000	0.3	3.7	0.14	15 ppm	0.015	0.09	0.40	1.13	4.97	0.04	0.19	0.002	0.008	4.5E-03	0.02	Note 2
MG-0004	Portable Fire Water Pump Engine	700	100	8,000	3.0	2.6	3.0	15 ppm	0.15	4.60	0.23	4.03	0.20	4.60	0.23	0.009	0.000	0.23	0.01	Note 1
SG-0100	UPS backup generator (exempt*)	52	500	8,000	14.1	3.0	1.1	15 ppm	1.0	1.61	0.40	0.35	0.09	0.13	0.03	0.001	0.0002	0.11	0.03	Note 4
SG-0101	UPS backup generator (exempt*)	54	500	8,000	14.1	3.0	1.1	15 ppm	1.0	1.67	0.42	0.36	0.09	0.14	0.03	0.001	0.0002	0.12	0.03	Note 4
SG-0102	Server Backup Generator (exempt*)	99.23	500	8,000	0.3	3.7	0.14	15 ppm	0.015	0.07	0.02	0.82	0.20	0.03	0.01	0.001	0.0003	0.003	0.001	Note 2
FWG-0600	Fire Water Pump Engine	376	100	8,000	3.0	2.6	3.0	15 ppm	0.15	2.49	0.12	2.16	0.11	2.49	0.12	0.005	0.0002	0.12	0.01	Note 3
FWG-0601	Fire Water Pump Engine	376	100	8,000	3.0	2.6	3.0	15 ppm	0.15	2.49	0.12	2.16	0.11	2.49	0.12	0.005	0.0002	0.12	0.01	Note 3
FWG-0602	Fire Water Pump Engine	376	100	8,000	3.0	2.6	3.0	15 ppm	0.15	2.49	0.12	2.16	0.11	2.49	0.12	0.005	0.0002	0.12	0.01	Note 3
FWG-0603	Fire Water Pump Engine	305	100	8,000	3.0	2.6	3.0	15 ppm	0.15	2.02	0.10	1.75	0.09	2.02	0.10	0.004	0.0002	0.10	0.01	Note 3

Notes:

- 1. NSPS IIII, 40 CFR §89.112, Table 1
- 2. NSPS IIII, 40 CFR §1039.101 Table 1
- 3. NSPS IIII Table 4
- 4. AP-42 Table 3.3-1
- 5. SO2 based on fuel sulfur content
- * Standby generator engines satisfy the exempt equipment criteria at 20.2.72.202.B(3) NMAC. According to the application instructions, exempt engines shall be listed in Table 2-B rather than Table 2-A.

 Based on informal guidance received from NMED AQB, Navajo is listing the engines in Table 2-A.

Sample calculation for MG-0001:

NOx (lb/hr) = Emissions Factor (g/hp-hr) * Engine Rating (hp) * 1 lb/453.6 g = 3.0 g/hp-hr * 280 hp * 1 lb/453.6 g = 1.84 lb/hr NOx (ton/yr) = NOx (lb/hr) * Operating Hours (hr/yr) * 1 ton/2,000 lb = 1.841 lb/hr * 8,760 hr/yr * 1 ton/2,000 lb = 8.06 ton/yr + 1 ton/2,000 lb = 1.841 lb/hr * 8,760 hr/yr * 1 ton/2,000 lb = 8.06 ton/yr

					CO2	CH₄	N ₂ O	
Tables	s C-1 and C-2 to 40 CFR 98	′ ′	,	Fuel Oil No. 2 or lb/mmBtu	163.05	0.007	0.001	GHG
Tabl	es C-1 and C-2 to 40 CFR	98, subpa	•	Gas Emission or lb/mmBtu	116.98	0.002	0.0002	(as CO ₂ e)
Tal	ble A-1 to 40 CFR 98, subp	art A, Glo	bal Warming	g Potentials	1	25	298	
Engine	Description	НР	Operating Hours	BSFC (Btu/hp-hr)	ton/yr	ton/yr	ton/yr	ton/yr
MG-0001	Portable Air Compressor	280	8760	8,000	1,600	0.06	0.01	1,605
MG-0002	Portable Air Compressor	280	8760	8,000	1,600	0.06	0.01	1,605
MG-0003	Portable Air Compressor	138	8760	8,000	788	0.03	0.01	791
SG-0100	UPS backup generator (exempt*)	52	500	8,000	17	0.001	0.0001	17.0
SG-0101	UPS backup generator (exempt*)	54	500	8,000	18	0.001	0.0001	17.7
SG-0102	Server Backup Generator (exempt*)	99.23	500	8,000	32	0.001	0.0003	32.5
FWG-0600	Fire Water Pump Engine	376	100	8,000	25	0.001	0.0002	24.6
FWG-0601	Fire Water Pump Engine	376	100	8,000	25	0.001	0.0002	24.6
FWG-0602	Fire Water Pump Engine	376	100	8,000	25	0.001	0.0002	24.6
FWG-0603	Fire Water Pump Engine	305	100	8,000	20	0.001	0.0002	20.0
MG-0004	Portable Fire Water Pump Engine	700	100	8,000	46	0.002	0.0004	45.8
				TOTAL:	4,194	0.2	0.03	4,208

Maximum Individual HAPs (Formaldehyde) 0.03 ton/yr

Total HAPs 0.10 ton/yr

					Ben	zene	Tolu	iene	Xyle	enes	Acenap	hthene	Acenapl	nthylene	Acetal	dehyde	Acro	olein
				CAS No.	71-4	13-2	108-	88-3	1330	-20-7	83-3	32-9	208-	96-8	75-0	07-0	107-	-02-8
AP-42, Ch. 3.	3 (10/96), Table 3.3-2 HAPs for	Diesel Engin	es Emission Fa	ctor lb/mmBtu	9.33	E-04	4.09	E-04	2.85	E-04	<1.4	2E-06	<5.0	5E-06	7.67	E-04	<9.2	5E-05
AP-42, Ch	n. 3.2 (7/00), Table 3.2-2. Unco	ntrolled Emis	ssion Factors fo	r 4SLB Engines Ib/mmBtu	4.40	E-04	4.08	E-04	1.84	E-04		-		-	8.36	E-03	5.14	IE-03
Engine	Description	НР	BSFC (Btu/hp-hr)	Operating Hours	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
MG-0001	Portable Air Compressor	280	8,000	8760	2.1E-03	9.2E-03	9.2E-04	4.0E-03	6.4E-04	2.8E-03	3.2E-06	1.4E-05	1.1E-05	5.0E-05	1.7E-03	7.5E-03	2.1E-04	9.1E-04
MG-0002	Portable Air Compressor	280	8,000	8760	2.1E-03	9.2E-03	9.2E-04	4.0E-03	6.4E-04	2.8E-03	3.2E-06	1.4E-05	1.1E-05	5.0E-05	1.7E-03	7.5E-03	2.1E-04	9.1E-04
MG-0003	Portable Air Compressor	138	8,000	8760	1.0E-03	4.5E-03	4.5E-04	2.0E-03	3.1E-04	1.4E-03	1.6E-06	6.9E-06	5.6E-06	2.4E-05	8.5E-04	3.7E-03	1.0E-04	4.5E-04
MG-0004	Portable Fire Water Pump E	700	8,000	100	5.2E-03	2.6E-04	2.3E-03	1.1E-04	1.6E-03	8.0E-05	8.0E-06	4.0E-07	2.8E-05	1.4E-06	4.3E-03	2.1E-04	5.2E-04	2.6E-05
SG-0100	UPS backup generator (exer	52	8,000	500	3.9E-04	9.7E-05	1.7E-04	4.3E-05	1.2E-04	3.0E-05	5.9E-07	1.5E-07	2.1E-06	5.3E-07	3.2E-04	8.0E-05	3.8E-05	9.6E-06
SG-0101	UPS backup generator (exer	54	8,000	500	4.0E-04	1.0E-04	1.8E-04	4.4E-05	1.2E-04	3.1E-05	6.1E-07	1.5E-07	2.2E-06	5.5E-07	3.3E-04	8.3E-05	4.0E-05	1.0E-05
SG-0102	Server Backup Generator (e	99.23	8,000	500	7.4E-04	1.9E-04	3.2E-04	8.1E-05	2.3E-04	5.7E-05	1.1E-06	2.8E-07	4.0E-06	1.0E-06	6.1E-04	1.5E-04	7.3E-05	1.8E-05
FWG-0600	Fire Water Pump Engine	376	8,000	100	2.8E-03	1.4E-04	1.2E-03	6.2E-05	8.6E-04	4.3E-05	4.3E-06	2.1E-07	1.5E-05	7.6E-07	2.3E-03	1.2E-04	2.8E-04	1.4E-05
FWG-0601	Fire Water Pump Engine	376	8,000	100	2.8E-03	1.4E-04	1.2E-03	6.2E-05	8.6E-04	4.3E-05	4.3E-06	2.1E-07	1.5E-05	7.6E-07	2.3E-03	1.2E-04	2.8E-04	1.4E-05
FWG-0602	Fire Water Pump Engine	376	8,000	100	2.8E-03	1.4E-04	1.2E-03	6.2E-05	8.6E-04	4.3E-05	4.3E-06	2.1E-07	1.5E-05	7.6E-07	2.3E-03	1.2E-04	2.8E-04	1.4E-05
FWG-0603	Fire Water Pump Engine	305	8,000	100	2.3E-03	1.1E-04	1.0E-03	5.0E-05	7.0E-04	3.5E-05	3.5E-06	1.7E-07	1.2E-05	6.2E-07	1.9E-03	9.4E-05	2.3E-04	1.1E-05
				TOTAL:		0.02		0.01		0.01		3.65E-05		1.30E-04		0.02		0.002

Sample calculation for MG-0001:

Benzene (lb/hr) = Emissions Factor (lb/mmBtu) * Engine Rating (hp) * 8,000 Btu/hp-hr * 1mmBtu/10^6 Btu = 0.002 lb/hr Benzene (ton/yr) = Benzene (lb/hr) * Operating Hours (hr/yr) * 1 ton/2,000 lb = 0.002 lb/hr * 8,760 hr/yr * 1 ton/2,000 lb = 0.002 ton/yr

Maximum Individual HAPs (Formaldehyde) 0.03 ton/yr

Total HAPs 0.10 ton/yr

					Anthr	acene	· , ,	anthrace e	,)fluorant ne	Benzo(k)		Benzo(a)pyrene		,h,i)peryl ne	1,3-Bu	tadiene
				CAS No.	120-	-12-7	56-5	55-3	205-	99-2	207-	08-9	50-3	32-8	191-	24-2	106-	-99-0
AP-42, Ch. 3.	3 (10/96), Table 3.3-2 HAPs for	Diesel Engir	nes Emission Fac	ctor lb/mmBtu	1.87	'E-06	1.68	E-06	<9.9	1E-08	<1.55	5E-07	<1.88	BE-07	<4.89	9E-07	<3.9	1E-05
AP-42, Ch	n. 3.2 (7/00), Table 3.2-2. Unco	ntrolled Emis	ssion Factors fo	r 4SLB Engines		_			1 66	E-07					4 14	E-07	2 67	7E-04
				lb/mmBtu		_			1.00						4.14	.L-07	2.07	L-04
Engine	Description	HP	BSFC	Operating	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
	·		(Btu/hp-hr)	Hours	•								-				•	
MG-0001	Portable Air Compressor	280	8,000	8760	4.2E-06	1.8E-05	3.8E-06	1.6E-05	2.2E-07	9.7E-07	3.5E-07	1.5E-06	4.2E-07	1.8E-06	1.1E-06	4.8E-06	8.8E-05	3.8E-04
MG-0002	Portable Air Compressor	280	8,000	8760	4.2E-06	1.8E-05	3.8E-06	1.6E-05	2.2E-07	9.7E-07	3.5E-07	1.5E-06	4.2E-07	1.8E-06	1.1E-06	4.8E-06	8.8E-05	3.8E-04
MG-0003	Portable Air Compressor	138	8,000	8760	2.1E-06	9.0E-06	1.9E-06	8.1E-06	1.1E-07	4.8E-07	1.7E-07	7.5E-07	2.1E-07	9.1E-07	5.4E-07	2.4E-06	4.3E-05	1.9E-04
MG-0004	Portable Fire Water Pump E	700	8,000	100	1.0E-05	5.2E-07	9.4E-06	4.7E-07	5.5E-07	2.8E-08	8.7E-07	4.3E-08	1.1E-06	5.3E-08	2.7E-06	1.4E-07	2.2E-04	1.1E-05
SG-0100	UPS backup generator (exer	52	8,000	500	7.8E-07	1.9E-07	7.0E-07	1.7E-07	4.1E-08	1.0E-08	6.4E-08	1.6E-08	7.8E-08	2.0E-08	2.0E-07	5.1E-08	1.6E-05	4.1E-06
SG-0101	UPS backup generator (exer	54	8,000	500	8.1E-07	2.0E-07	7.3E-07	1.8E-07	4.3E-08	1.1E-08	6.7E-08	1.7E-08	8.1E-08	2.0E-08	2.1E-07	5.3E-08	1.7E-05	4.2E-06
SG-0102	Server Backup Generator (e	99.23	8,000	500	1.5E-06	3.7E-07	1.3E-06	3.3E-07	7.9E-08	2.0E-08	1.2E-07	3.1E-08	1.5E-07	3.7E-08	3.9E-07	9.7E-08	3.1E-05	7.8E-06
FWG-0600	Fire Water Pump Engine	376	8,000	100	5.6E-06	2.8E-07	5.1E-06	2.5E-07	3.0E-07	1.5E-08	4.7E-07	2.3E-08	5.7E-07	2.8E-08	1.5E-06	7.4E-08	1.2E-04	5.9E-06
FWG-0601	Fire Water Pump Engine	376	8,000	100	5.6E-06	2.8E-07	5.1E-06	2.5E-07	3.0E-07	1.5E-08	4.7E-07	2.3E-08	5.7E-07	2.8E-08	1.5E-06	7.4E-08	1.2E-04	5.9E-06
FWG-0602	Fire Water Pump Engine	376	8,000	100	5.6E-06	2.8E-07	5.1E-06	2.5E-07	3.0E-07	1.5E-08	4.7E-07	2.3E-08	5.7E-07	2.8E-08	1.5E-06	7.4E-08	1.2E-04	5.9E-06
FWG-0603	Fire Water Pump Engine	305	8,000	100	4.6E-06	2.3E-07	4.1E-06	2.0E-07	2.4E-07	1.2E-08	3.8E-07	1.9E-08	4.6E-07	2.3E-08	1.2E-06	6.0E-08	9.5E-05	4.8E-06
				TOTAL:		4.81E-05		4.32E-05		2.55E-06		3.99E-06		4.84E-06		1.26E-05		1.01E-03

Sample calculation for MG-0001:

Benzene (lb/hr) = Emissions Factor (lb/mmBtu) * Engine Rating (hp) * 8,000 Btu/hp-hr Benzene (ton/yr) = Benzene (lb/hr) * Operating Hours (hr/yr) * 1 ton/2,000 lb = 0.002 \parallel

Maximum Individual HAPs (Formaldehyde) 0.03 ton/yr

Total HAPs 0.10 ton/yr

					Chry	sene	Dibenz(a		Fluora	nthene	Fluo	rene	Formal	dehyde)(1,2,3- yrene	Napht	halene
				CAS No.	218-	01-9	53-7	70-3	206-	44-0	86-7	73-7	50-0	00-0	193-	39-5	91-2	20-3
AP-42, Ch. 3	3 (10/96), Table 3.3-2 HAPs for	Diesel Engin	nes Emission Fa	ctor lb/mmBtu	3.53	E-07	<5.83	BE-07	7.61	E-06	2.92	E-05	1.18	BE-03	<3.75	5E-07	8.48	BE-05
AP-42, Cł	n. 3.2 (7/00), Table 3.2-2. Unco	ntrolled Emis	ssion Factors fo	r 4SLB Engines Ib/mmBtu	6.93	E-07	-	-	1.11	E-06	5.67	E-06	5.28	BE-02		-	7.44	IE-05
Engine	Description	НР	BSFC (Btu/hp-hr)	Operating Hours	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
MG-0001	Portable Air Compressor	280	8,000	8760	7.9E-07	3.5E-06	1.3E-06	5.7E-06	1.7E-05	7.5E-05	6.5E-05	2.9E-04	2.6E-03	1.2E-02	8.4E-07	3.7E-06	1.9E-04	8.3E-04
MG-0002	Portable Air Compressor	280	8,000	8760	7.9E-07	3.5E-06	1.3E-06	5.7E-06	1.7E-05	7.5E-05	6.5E-05	2.9E-04	2.6E-03	1.2E-02	8.4E-07	3.7E-06	1.9E-04	8.3E-04
MG-0003	Portable Air Compressor	138	8,000	8760	3.9E-07	1.7E-06	6.4E-07	2.8E-06	8.4E-06	3.7E-05	3.2E-05	1.4E-04	1.3E-03	5.7E-03	4.1E-07	1.8E-06	9.4E-05	4.1E-04
MG-0004	Portable Fire Water Pump E	700	8,000	100	2.0E-06	9.9E-08	3.3E-06	1.6E-07	4.3E-05	2.1E-06	1.6E-04	8.2E-06	6.6E-03	3.3E-04	2.1E-06	1.1E-07	4.7E-04	2.4E-05
SG-0100	UPS backup generator (exer	52	8,000	500	1.5E-07	3.7E-08	2.4E-07	6.1E-08	3.2E-06	7.9E-07	1.2E-05	3.0E-06	4.9E-04	1.2E-04	1.6E-07	3.9E-08	3.5E-05	8.8E-06
SG-0101	UPS backup generator (exer	54	8,000	500	1.5E-07	3.8E-08	2.5E-07	6.3E-08	3.3E-06	8.2E-07	1.3E-05	3.2E-06	5.1E-04	1.3E-04	1.6E-07	4.1E-08	3.7E-05	9.2E-06
SG-0102	Server Backup Generator (e	99.23	8,000	500	2.8E-07	7.0E-08	4.6E-07	1.2E-07	6.0E-06	1.5E-06	2.3E-05	5.8E-06	9.4E-04	2.3E-04	3.0E-07	7.4E-08	6.7E-05	1.7E-05
FWG-0600	Fire Water Pump Engine	376	8,000	100	1.1E-06	5.3E-08	1.8E-06	8.8E-08	2.3E-05	1.1E-06	8.8E-05	4.4E-06	3.5E-03	1.8E-04	1.1E-06	5.6E-08	2.6E-04	1.3E-05
FWG-0601	Fire Water Pump Engine	376	8,000	100	1.1E-06	5.3E-08	1.8E-06	8.8E-08	2.3E-05	1.1E-06	8.8E-05	4.4E-06	3.5E-03	1.8E-04	1.1E-06	5.6E-08	2.6E-04	1.3E-05
FWG-0602	Fire Water Pump Engine	376	8,000	100	1.1E-06	5.3E-08	1.8E-06	8.8E-08	2.3E-05	1.1E-06	8.8E-05	4.4E-06	3.5E-03	1.8E-04	1.1E-06	5.6E-08	2.6E-04	1.3E-05
FWG-0603	Fire Water Pump Engine	305	8,000	100	8.6E-07	4.3E-08	1.4E-06	7.1E-08	1.9E-05	9.3E-07	7.1E-05	3.6E-06	2.9E-03	1.4E-04	9.2E-07	4.6E-08	2.1E-04	1.0E-05
				TOTAL:		9.08E-06		1.50E-05		1.96E-04		0.001		0.03		9.65E-06		0.002

Sample calculation for MG-0001:

Benzene (lb/hr) = Emissions Factor (lb/mmBtu) * Engine Rating (hp) * 8,000 Btu/hp-hr Benzene (ton/yr) = Benzene (lb/hr) * Operating Hours (hr/yr) * 1 ton/2,000 lb = 0.002 \parallel

Maximum Individual HAPs (Formaldehyde) 0.03 ton/yr

Total HAPs 0.10 ton/yr

					Phenar	nthrene	Pyr	ene	тота	L PAH
				CAS No.	85-0	01-8	129-	00-0	P.A	AΗ
AP-42, Ch. 3	3 (10/96), Table 3.3-2 HAPs for	Diesel Engir	es Emission Fa	ctor lb/mmBtu	2.94	E-05	4.78	E-06	1.68	E-04
AP-42, Cł	n. 3.2 (7/00), Table 3.2-2. Unco	ntrolled Emis	ssion Factors fo	r 4SLB Engines Ib/mmBtu	1.04	E-05		-	2.69	E-05
Engine	Description	НР	BSFC (Btu/hp-hr)	Operating Hours	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
MG-0001	Portable Air Compressor	280	8,000	8760	6.6E-05	2.9E-04	1.1E-05	4.7E-05	3.8E-04	1.6E-03
MG-0002	Portable Air Compressor	280	8,000	8760	6.6E-05	2.9E-04	1.1E-05	4.7E-05	3.8E-04	1.6E-03
MG-0003	Portable Air Compressor	138	8,000	8760	3.2E-05	1.4E-04	5.3E-06	2.3E-05	1.9E-04	8.1E-04
MG-0004	Portable Fire Water Pump E	700	8,000	100	1.6E-04	8.2E-06	2.7E-05	1.3E-06	9.4E-04	4.7E-05
SG-0100	UPS backup generator (exer	52	8,000	500	1.2E-05	3.1E-06	2.0E-06	5.0E-07	7.0E-05	1.7E-05
SG-0101	UPS backup generator (exer	54	8,000	500	1.3E-05	3.2E-06	2.1E-06	5.2E-07	7.3E-05	1.8E-05
SG-0102	Server Backup Generator (e	99.23	8,000	500	2.3E-05	5.8E-06	3.8E-06	9.5E-07	1.3E-04	3.3E-05
FWG-0600	Fire Water Pump Engine	376	8,000	100	8.8E-05	4.4E-06	1.4E-05	7.2E-07	5.1E-04	2.5E-05
FWG-0601	Fire Water Pump Engine	376	8,000	100	8.8E-05	4.4E-06	1.4E-05	7.2E-07	5.1E-04	2.5E-05
FWG-0602	Fire Water Pump Engine	376	8,000	100	8.8E-05	4.4E-06	1.4E-05	7.2E-07	5.1E-04	2.5E-05
FWG-0603	Fire Water Pump Engine	305	8,000	100	7.2E-05	3.6E-06	1.2E-05	5.8E-07	4.1E-04	2.0E-05
				TOTAL:		7.56E-04		1.23E-04		0.004

Sample calculation for MG-0001:

Benzene (lb/hr) = Emissions Factor (lb/mmBtu) * Engine Rating (hp) * 8,000 Btu/hp-hr Benzene (ton/yr) = Benzene (lb/hr) * Operating Hours (hr/yr) * 1 ton/2,000 lb = 0.002 \parallel

COOLING TOWERS POTENTIAL TO EMIT

Cooling Tower	Description	Water	Annual Circulation	Annual Hours of	TDS	Drift Eliminator	VOC Controlled	VOC Emission Factor	D.	л ⁽⁴⁾	DM	Potentia	l to Emit	(5)	voc	voc
cooming router	2000	Circulation	Rate	Operation	(ppmw) ⁽¹⁾	(% drift)	(LDAR)?	(lb/MMgal) (3)	PI	VI	PIVI	10	PIVI	2.5	VOC	VOC
		Rate (gpm)	gpm) (MMgal/yr) (hr/yr)			(,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	(==:::-,:	(12,1111821)	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
Y-0001	TCC Cooling Tower	5,000	2,628	8760	3,500	0.003	Yes	0.7	0.26	1.15	0.158	0.69	0.0006	0.00260	0.21	0.92
Y-0002	S. Alky Cooling Tower (Marley Cooling Tower)	5,000	2,628	8760	3,500	0.003	Yes	0.7	0.26	1.15	0.16	0.69	0.001	0.00	0.21	0.92
Y-0008	North Alky Cooling Tower	12,500	6,570	8760	3,500	0.003	Yes	0.7	0.61	2.68	0.37	1.62	0.0014	0.006	0.53	2.30
Y-0011	FCC & NP Cooling Tower	30,000	15,768	8760	3,500	0.001	Yes	0.7	0.53	2.30	0.32	1.38	0.0012	0.005	1.26	5.52
Y-0012	Hydrogen Plants Cooling Tower	10,000	5,256	8760	3,500	0.001	Yes	0.7	0.18	0.77	0.11	0.46	0.0004	0.0017	0.42	1.84
CT TT-0006	Unit 07 Amine W-0745 Cooling Tower	3,000	1,576.8	8760	3,500	0.003	No	6	0.16	0.69	0.095	0.42	0.00036	0.0016	1.08	4.73
									2.00	8.75	1.20	5.26	0.005	0.02	3.71	16.23

Notes:

- (1) Total dissolved solids (TDS) is based on cooling water sampling data.
- (2) VOC emission factors are from AP-42 Table 5.1-3 (dated 4/15).
- (3) PM emissions are calculated per AP-42 Section 13.4, dated January 1995.
- (4) PM_{2.5} and PM₁₀ emissions are calculated in accordance with NMED's Technical Memorandum "Calculating TSP, PM-10 and PM-2.5 from Cooling Towers" dated 9/9/2013.

For a TDS of 3,5000 ppmw and per the size distribution table in the memorandum (average between 3,000 ppmw and 4,000 ppmw), the percents mass of total particulate emissions represented by PM2.5 and PM10 are as follows:

% Mass PM₁₀ = 60.161 % Mass PM_{2.5} = 0.226

Sample Calculations (CT Y-0001):

 $VOC = 5,000 \ gal/min * 60 \ min/hr * 1 \ lb/MMgal * 1 \ MMgal/10^6 \ gal = 0.21 \ lb/hr \\ PM = 5,000 \ galH2O/min * 60 \ min/hr * 8.34 \ lbH2O/galH2O * 3,500 \ lbTDS/ 10^6 \ lbH2O * 0.003 /100 = 0.26 \ lb/hr \\ PM10 = 0.26 \ lb/hr * 60.161 /100 = 0.16 \ lb/hr \\ PM2.5 = 0.26 \ lb/hr * 0.226 /100 = 0.0006 \ lb/hr$

COOLING TOWERS POTENTIAL TO EMIT HAPS

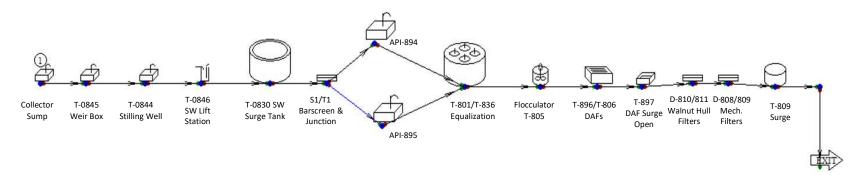
Maximum Individual HAPs (n-Hexane) 0.68 ton/yr
Total HAPs 1.04 ton/yr

		1,3-Bı	ıtadiene	2,2,4-Trimet	hylpentane	Arser	nic	Benzer	ie	Cadn	nium	Chro	mium	Cum	iene	Ethylbe	enzene
		106	5-99-0	540-8	84-1	7440-3	8-2	71-43-	2	7440	-43-9	7440	-47-3	98-8	32-8	100-	41-4
API 4723A wt%	Hydrodesulfurization - Naphtha	C	0.36	0.0)5	4.87E-	-06	0.77		2.4E	-07	3.01	E-07	0.0	05	0.:	10
Cooling Tower	Description	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
Y-0001	TCC Cooling Tower	7.6E-04	3.3E-03	1.1E-04	4.9E-04	1.0E-08	4.5E-08	1.6E-03	7.1E-03	5.0E-10	2.2E-09	6.3E-10	2.8E-09	1.0E-04	4.5E-04	2.2E-04	9.5E-04
Y-0002	S. Alky Cooling Tower (Marley Cooling Tower)	7.6E-04	3.3E-03	1.1E-04	4.9E-04	1.0E-08	4.5E-08	1.6E-03	7.1E-03	5.0E-10	2.2E-09	6.3E-10	2.8E-09	1.0E-04	4.5E-04	2.2E-04	9.5E-04
Y-0008	North Alky Cooling Tower	1.9E-03	8.4E-03	2.8E-04	1.2E-03	2.6E-08	1.1E-07	4.0E-03	1.8E-02	1.2E-09	5.4E-09	1.6E-09	6.9E-09	2.6E-04	1.1E-03	5.4E-04	2.4E-03
Y-0011	FCC & NP Cooling Tower	4.6E-03	2.0E-02	6.7E-04	2.9E-03	6.1E-08	2.7E-07	9.7E-03	4.2E-02	3.0E-09	1.3E-08	3.8E-09	1.7E-08	6.2E-04	2.7E-03	1.3E-03	5.7E-03
Y-0012	Hydrogen Plants Cooling Tower	1.5E-03	6.7E-03	2.2E-04	9.8E-04	2.0E-08	9.0E-08	3.2E-03	1.4E-02	9.9E-10	4.3E-09	1.3E-09	5.6E-09	2.1E-04	9.1E-04	4.3E-04	1.9E-03
CT TT-0006	Unit 07 Amine W-0745 Cooling Tower	3.9E-03	1.7E-02	5.7E-04	2.5E-03	5.3E-08	2.3E-07	8.3E-03	3.6E-02	2.5E-09	1.1E-08	3.3E-09	1.4E-08	5.3E-04	2.3E-03	1.1E-03	4.9E-03
	TOTAL		0.06		0.01		7.9E-07		0.12		3.8E-08		4.9E-08		0.01		0.02

COOLING TOWERS POTENTIAL TO EMIT HAPS

		Lead cor	npounds	m-Xy	/lene	Napht	halene	n-He	xane	Nic	:kel	о-Ху	lene	р-Ху	lene	Tolu	ene	Xylene isom	(mixed ners)
		7439	-92-1	108-	38-3	91-2	20-3	110-	54-3	7440	-02-0	95-4	47-6	106-	42-3	108-	88-3	1330	-20-7
API 4723A wt%	Hydrodesulfurization - Naphtha	4.31	E-07	0.	33	0.	02	4.	21	2.01	E-06	0.	12	0.	13	0.	29	0.0	02
Cooling Tower	Description	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
Y-0001	TCC Cooling Tower	9.1E-10	4.0E-09	6.9E-04	3.0E-03	3.2E-05	1.4E-04	8.8E-03	3.9E-02	4.2E-09	1.9E-08	2.4E-04	1.1E-03	2.8E-04	1.2E-03	6.0E-04	2.6E-03	3.5E-05	1.5E-04
Y-0002	S. Alky Cooling Tower (Marley Cooling Tower)	9.1E-10	4.0E-09	6.9E-04	3.0E-03	3.2E-05	1.4E-04	8.8E-03	3.9E-02	4.2E-09	1.9E-08	2.4E-04	1.1E-03	2.8E-04	1.2E-03	6.0E-04	2.6E-03	3.5E-05	1.5E-04
Y-0008	North Alky Cooling Tower	2.3E-09	1.0E-08	1.7E-03	7.5E-03	8.0E-05	3.5E-04	2.2E-02	9.7E-02	1.1E-08	4.6E-08	6.1E-04	2.7E-03	6.9E-04	3.0E-03	1.5E-03	6.6E-03	8.8E-05	3.9E-04
Y-0011	FCC & NP Cooling Tower	5.5E-09	2.4E-08	4.1E-03	1.8E-02	1.9E-04	8.4E-04	5.3E-02	2.3E-01	2.5E-08	1.1E-07	1.5E-03	6.4E-03	1.7E-03	7.3E-03	3.6E-03	1.6E-02	2.1E-04	9.3E-04
Y-0012	Hydrogen Plants Cooling Tower	1.8E-09	8.0E-09	1.4E-03	6.0E-03	6.4E-05	2.8E-04	1.8E-02	7.7E-02	8.5E-09	3.7E-08	4.9E-04	2.1E-03	5.5E-04	2.4E-03	1.2E-03	5.2E-03	7.1E-05	3.1E-04
CT TT-0006	Unit 07 Amine W-0745 Cooling Tower	4.7E-09	2.1E-08	3.5E-03	1.5E-02	1.6E-04	7.2E-04	4.5E-02	2.0E-01	2.2E-08	9.6E-08	1.3E-03	5.5E-03	1.4E-03	6.2E-03	3.1E-03	1.3E-02	1.8E-04	7.9E-04
	TOTAL		7.0E-08		0.05		0.002		0.68		3.3E-07		0.02		0.02		0.05		0.003

WASTEWATER SYSTEM POTENTIAL TO EMIT



NAVAJO REFINERY WASTEWATER PLANT LAYOUT

Wastewater System Characteristics		
Design Flow (gpm)	1,200	
Wastewater composition (ppm)		
Benzene	5.00	ToxChem Model
Ethylbenzene	3.10	ToxChem Model
Toluene	8.50	ToxChem Model
Xylene	7.10	ToxChem Model
Acetone	7.50	Sampling Data * 3
Carbon Disulfide	3.03	Sampling Data * 3
Methylene chloride	0.321	Sampling Data * 3
Naphthalene	1.341	Sampling Data * 3
1,3,5-Trimethylbenzene	2.913	Sampling Data * 3
n-Butylbenzene	1.143	Sampling Data * 3
Isopropylbenzene (Cumene)	0.15	Sampling Data * 3
1,2-Dichloroethene	0.423	Sampling Data * 3
Formaldehyde	100.5	Sampling Data * 3
n-Propylbenzene	0.6	Sampling Data * 3
sec-Butylbenzene	0.132	Sampling Data * 3

^{*} Formaldehyde reacts in basic environments (in the presence of NaOH) to create equal molar amounts of sodium formate and methanol. pH is expected to be basic, thus Water9 modeled methanol at 100.5 ppmw

Water9 Output Summary Results by Unit

waters output summary results by o		V	OC Emission	s
Units	Control	g/s	(lb/hr)	(ton/yr)
Collector Sump				
T-0845 Weir Box	95%	2.31E-03	1.84E-02	8.05E-02
T-0844 Stilling Well	95%	2.31E-03	1.64E-02	6.U3E-U2
T-0846 Stormwater Lift Station (SWLS)				
T-0830 SW Surge Tank	-	6.91E-05	5.49E-04	2.40E-03
S1/T1 Barscreen & Junction Box				
API T-894	95%	1.73E-05	1.37E-04	6.02E-04
API T-895				
T-801/T-836 Equalization	-	1.68E-01	1.34	5.85
T-805 Flocculator	-	2.65E-04	2.11E-03	9.23E-03
T-896/T-806 DAF	-	2.06E-01	1.64	7.18
T-897 DAF Surge Open Sump	-	6.75E-04	5.36E-03	2.35E-02
D-810/811 Walnut Hull Filters	-	0.00E+00	0.00E+00	0.00E+00
D-808/809 Mechanical Filters	-	1.36E-08	1.08E-07	4.72E-07
T-809 Surge Tank	-	4.67E-04	3.70E-03	1.62E-02
TOTAL WASTEWATER SYSTEM		0.38	3.00	13.16

Notes:

(1) T-0845, T-0844, and T-0846 are controlled with carbon cannister D-8000/D-8001.

S1/T1 routes through the APIs and API-894 and API-895 are controlled with carbon cannister D-0829/D-0830. A 95% control efficiency applied per 2015 Emissions Estimation Protocol for Petroleum Refineries, Table 3-2 - Carbon adsorption.

Water9 Output Summary Results by Pollutant

Pollutant	CAS No.	112(b)		Emissions	
Pollutant	CAS NO.	HAP?	g/s	lb/hr	ton/yr
Benzene	71-43-2	Yes	0.04	0.32	1.39
Ethylbenzene	100-41-4	Yes	0.03	0.26	1.13
Toluene	108-88-3	Yes	0.06	0.50	2.20
Xylenes	1330-20-7	Yes	0.07	0.56	2.45
Propanone (acetone)	67-64-1	No	0.00	0.01	0.04
Carbon Disulfide	75-15-0	Yes	0.08	0.62	2.72
Methylene Chloride, dichlorom	75-09-2	Yes	0.00	0.03	0.11
Naphthalene	91-20-3	Yes	0.00	0.03	0.11
Trimethylbenzene (1,3,5)	108-67-8	No	0.02	0.16	0.72
Butyl Benzene	104-51-8	No	0.01	0.05	0.21
Cumene (isopropylbenzene)	98-82-8	Yes	0.00	0.01	0.06
Dichloroethylene(1,2) cis	156-59-2	No	0.03	0.23	0.99
Methanol	50-00-0	Yes	0.01	0.12	0.51
Propyle(-n) Benzene	103-65-1	No	0.01	0.08	0.33
sec Butylbenzene	135-98-8	No	0.01	0.08	0.33
TOTAL WASTEWATER SYSTEM			0.38	3.04	13.31

TRUCK AND RAILCAR LOADING POTENTIAL TO EMIT ^a

Petroleum Products Loading Racks

			Vapor Molecular	Liquid Molecular	Saturation Factor	Loading Te	mperature	Vapor Pr Loading Te		H2S in Liquid ^c	H2S in Vapor ^c	Capture Ef. d	Control Ef. °	Loading T	hroughputs		itrolled ng Loss	Uncon		Contr VOC En per Con	nissions	Contr VOC En per Loadii	nissions	Contr H2S Em per Com	nissions	H2S Er	trolled missions ling Rack ^{f,g}
Loading Rack	Loading Rack Description	Material Loaded	Weight	Weight	ractor	Maximum Hourly	Annual Average	Maximum Hourly	Annual Average	Liquid	Tupo.	E1.	E1.	Maximum Hourly	Annual Average	Maximum Hourly	Annual Average	Maximum Hourly	Annual Average	Maximum Hourly	Annual Average	Maximum Hourly	Annual Average	Maximum Hourly	Annual Average	Maximum Hourly	Annual Average
			M _v	ML	S	T _{max}	Tavg	P _{max}	Pavg	H2S _{liq}	H2S _{vap}																
			lb/lbmol	lb/lbmol		°F	°F	psia	psia	ppmw	lb _{H2S} /lb _{vap}	%	%	bbl/hr	bbl/yr	lb/Mgal	lb/Mgal	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
	phalt Truck Loading nd Off-Loading Rack	Asphalt/Pitch	84	1000	1.45	400	320	0.56	0.10					350	3,662,756	0.99	0.19	14.57	14.46	14.57	14.46	14.57	14.46	0.01	0.01	0.01	0.01
	sphalt Truck Loading ack #2	Asphalt/Pitch	84	1000	1.45	400	320	0.56	0.10					300	950,000	0.99	0.19	12.49	3.75	12.49	3.75	12.49	3.75	0.01	0.002	0.01	0.002
		Gasoline - MACT				Emissions	based on 1	0 mg/L as requ	ired by MAC	T CC.				1,214	2,555,000					4.25	4.48			-	-		
TL-4 Fu	iels Truck Loading	Gasoline	62	92	0.6	100	64	14.45	7.80			98.7%	95%	1,214	2,555,000	11.97	6.90	610.16	370.25			4.50	4.81			0.02	0.03
Ra	ick e, i	Diesel	130	188	0.6	100	64	0.02	0.01	3.54	0.09	98.7%	95%	2,000	17,520,000	0.04	0.01	3.22	5.04	0.20	0.31			0.02	0.03		
		Jet Fuel	130	162	0.6	100	64	0.03	0.01			98.7%	95%	357	1,021,718	0.05	0.02	0.73	0.37	0.05	0.02			-	-		
TL-7 CB	3O/LCO Truck Loading	Carbon Black Oil	130	188	1.45	180	125	0.16	0.04	8.50	2.6E-06			300	500,808	0.59	0.18	7.48	1.84	7.48	1.84	12.17	1.86	1.96E-05	4.83E-06	3 10F-05	4.88E-06
Ra	ick	Light Cycle Oil	130	162	1.45	180	64	0.21	0.01	2.19	2.6E-06			381	20,119	0.76	0.04	12.17	0.02	12.17	0.02	12.17	1.00	3.19E-05	4.66E-08	3.132-03	4.001-00
		Carbon Black Oil	130	188	1.45	180	125	0.16	0.04	8.50	2.6E-06			800	455,488	0.59	0.18	19.93	1.68	19.93	1.68			5.23E-05	4.39E-06		
RIO-X			130	188	1.45	100	64	0.02	0.01	3.54	2.6E-06			200	1,144,000	0.09	0.03	0.78	0.80	0.78	0.80	19.93	6.44	2.04E-06	2.09E-06	0.01	0.001
Loa	ading Rack	Jet Fuel	130	162	1.45	100	64	0.03	0.01					200	1,144,000	0.12	0.04	0.99	1.01	0.99	1.01			-	-		
		Asphalt	84	1000	1.45	400	320	0.56	0.10					300	750,000	0.99	0.19	12.49	2.96	12.49	2.96			0.01	0.001		
Rai	ilcar Loading and Off-	Asphalt/Pitch	84	1000	1.45	400	320	0.56	0.10					1,575	1,394,250	0.99	0.19	65.55	5.50	65.55	5.50			0.03	0.003		
RLO-19 Loa	ading Rack ^f	Gas Oil	130	188	1.45	100	64	0.03	0.01	1.34	2.6E-06			1,575	3,057,600	0.13	0.04	8.82	2.76	8.82	2.76	65.55	11.72	2.31E-05	7.24E-06	0.03	0.003
		Fuel Oil	130	188	1.45	100	64	0.02	0.01	2.19	2.6E-06			800	4,968,600	0.09	0.03	3.11	3.45	3.11	3.45			8.16E-06	9.06E-06		+
	phalt/Pitch Truck ading Rack	Asphalt/Pitch	84	1000	1.45	400	320	0.56	0.10					600	950,000	0.99	0.19	24.97	3.75	24.97	3.75	24.97	3.75	0.01	0.002	0.01	0.002
																					TOTAL	154.18	46.80	0.08	0.04	0.08	0.04

Notes:

- a. Loading emissions are calculated using AP-42, Ch. 5.2 (6/2008)
- b. Vapor pressure calculated using Antoine Coefficients (Ch. 7.1 (6/2020) and maximum and annual average tempeatures during loading activities.
- c. H2S in liquid per API 4723A. For asphalts, 500 ppm is used per David C. Trumbore, 1999 (asphalts/pitch).
- H2S is limited at the loading racks for distillate products to no more than

 d. TL-4 vapors are captured and routed to a Vapor Recovery Unit (VRU) with a carbon adsorption system. A Vapor Combustion Unit (VCU) is used as an alternate control device. Captured efficiency is 98.7% per annual seal certification. Control efficiency per carbon adsorption and VCU manufacturer.
- e. The gasoline loading controlled emissions are calculated based on MACT R (§63.422(b)) emission standard of 10 mg organic compounds per liter of gasoline loaded, as referenced by MACT CC (§63.650(a)).
- Uncontrolled gasoline emissions are calculated as an input for the Vapor Combustion Unit (VCU) emissions calculation
- f. For the Fuels Truck Loading Rack (TL-4), the maximum hourly emissions are calculated based on all materials being loaded concurrently. For the other racks, the maximum hourly emissions reflect only the highest-emitting material being loaded in any hour.
- g. Annual controlled VOC emissions are calculated based on all materials being loaded, except for RLO-19, which reflect themaximum of the individual liquid values to reflect the physical limitations of the rack.
- h. H2S emissions estimated using Raoult's Law

Sample Calculations for Diesel Loading at the Fuels Truck Loading Rack (TL-4):

Loading Loss (lb/Mgal) = 12.46 * S * P * M / T (AP-42 Ch. 5.2)

Diesel Max. Loading Loss = 12.46 * 0.6 * 0.02 psia * 130 lb/lbmole / 560 R = 0.04 lb/Mgal

Diesel Avg. Loading Loss = 12.46 * 0.6 * 0.01 psia * 130 lb/lbmole / 524 R = 0.02 lb/Mgal

 $Uncontrolled \ VOC \ Emissions = Throughput \ (bbl) * 42 \ gal/bbl * (Mgal/1000 \ gal) * (Average \ Loading \ Loss, \ lb/Mgal)$

Diesel Max. Loading Uncontrolled VOC Emissions = 2,000 bbl/hr * 42gal/bbl * 1Mgal/1,000gal * 0.04 lb/Mgal = 3.22 lb/hr

 $Diesel Avg. Loading \ Uncontrolled \ VOC \ Emissions = 17,520,000 \ bbl/yr \ ^* 42gal/bbl \ ^* 1 Mgal/1,000gal \ ^* 0.01 \ bb/Mgal \ ^* 1 ton/2,000 \ lb = 5.04 \ lb/hr \ ^* 1 bb/mgal/1,000gal \ ^* 0.01 \ bb/mgal/1,000gal/1 \ ^* 1 bb/mgal/1,000gal/1 \$

Controlled VOC Emissions = Uncontrolled VOC Emissions * ((1 - % Capture Eff) + % Capt Eff * (1 - % Control Eff))

Diesel Max. Loading Controlled VOC Emissions = 3.22 lb/hr * ((1 - 0.99) + 0.99 * (1 - 0.95)) = 0.20 lb/hr

Diesel Avg. Loading Controlled VOC Emissions = 5.04 tpy * ((1 - 0.99) + 0.99 * (1 - 0.95)) = 0.31 tpy

Loading/Unloading Racks without emissions*

LUauiiig	Joinidaunig Racks Without emission	3
Loading Rack	Loading Rack Description	Material Loaded
TL-5	LPG Truck Loading Rack	LPG/PP mix
TLO-13	Butane Truck Loading & Off-Loading Rack	Butane
TLO-14	LPG Loading & Off-Loading Rack	LPG
TLO-17	Truck Off-Loading Rack	-
TO-10	Gasoline Blends Truck Off-Loading Rack	-
TO-11	Transmix Truck Off-Loading Rack	-
TO-12	HF Truck Off-Loading Rack	-
TO-15	Ethanol Truck Off-Loading Rack	-
TO-16	TEL Truck Off-Loading Rack	-
TO-18	Crude Truck Off-Loading Rack	-
TO-21	Gas Oil Truck Off-Loading for use with a	-
TO-3	Gas Oil Truck Off-Loading Rack	-
TO-6	Asphalt Truck Off-Loading Rack	-

^{*}Unloading emissions occur at the storage tank.

ton/yr

TRUCK AND RAILCAR LOADING PTE HAPS

Maximum Individual HAPs (n-Hexane) 1.00

Total HAPs 1.28 ton/yr

							CAS No.		540-84-1			83-32-9	
							Pi°, psia		0.79			4.3E-05	
Loading Rack	Loading Rack Description	Material Loaded	Surrogate for HAPs Speciation (API 4723A)	Vapor Molecular Weight, M _V (lb/lbmole)	Liquid Molecular Weight, M _L (lb/lbmole)	VOC (lb/hr) ^b	VOC (tpy) ^b	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy
TLO-1	Asphalt Truck Loading and Off-Loading Rack	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	84	1,000	14.6	14.5	0.04	6.0E-03	5.9E-03	-	-	-
TL-2	Asphalt Truck Loading Rack #2	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	84	1,000	12.5	3.8	0.04	5.1E-03	1.5E-03	-	-	-
	Fuels Truck Loading	Gasoline	Gasoline Blending - Reformulated Gasoline	62	92	4.3	4.5	0.56	0.024	0.025	-	-	-
TL-4	Rack	Diesel	Distillate Blending - Diesel Fuel	130	188	0.2	0.3		-		-	-	-
	NdCK	Jet Fuel	Kerosene treating - Commercial Jet Fuel	130	162	0.05	0.02	2.2E-03	1.0E-06	5.2E-07	-	-	-
TL-7	CBO/LCO Truck	Carbon Black Oil	Fluid Catalytic Cracker - Heavy Cat Gas Oil	130	188	7.5	1.8	-	-	-	2.6E-07	2.0E-08	4.8E-09
16-7	Loading Rack	Light Cycle Oil	Fluid Catalytic Cracker - Ligh Cat Gas Oil	130	162	12.2	0.0	4.0E-03	4.9E-04	7.2E-07	8.7E-07	1.1E-07	1.6E-10
		Carbon Black Oil	Fluid Catalytic Cracker - Heavy Cat Gas Oil	130	188	19.9	1.7	-	-	-	2.6E-07	5.2E-08	4.4E-09
RLO-8	Railcar Loading and Off-	Diesel	Distillate Blending - Diesel Fuel	130	188	0.8	0.8	-	-	-	-	-	-
KLU-0	Loading Rack	Jet Fuel	Kerosene treating - Commercial Jet Fuel	130	162	1.0	1.0	2.2E-03	2.2E-05	2.3E-05	-	-	-
		Asphalt	Asphalt Plant - (Feed) Pitch	84	1,000	12.5	3.0	0.04	5.1E-03	1.2E-03	-	-	-
	Railcar Loading and Off-	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	84	1,000	65.5	5.5	0.04	2.7E-02	2.3E-03	-		-
RLO-19	Loading Rack	Gas Oil	Vacuum Distillation - Light Vacuum Gas Oil	130	188	8.8	2.8	-	-	-	ND	-	-
	Loading Nack	Fuel Oil	Fluid Catalytic Cracker - Ligh Cat Gas Oil	130	188	3.1	3.5	4.7E-03	1.5E-04	1.6E-04	1.0E-06	3.2E-08	3.5E-08
TLO-20	Asphalt/Pitch Truck Loading Rack	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	84	1,000	25.0	3.8	0.04	1.0E-02	1.5E-03	-	-	-
					TOTAL	187.8	46.8			0.04			4.4E-08

Notes:

P_A 13.07 psia

2,2,4-Trimethylpentane

Acenaphthene

Sample Calculations for Gasoline Loading

HAP Vapor wt% = HAP Liquid I wt% * Pi° / Pa * ML/Mv

2,2,4-Trimethylpentane Vapor wt% in Gasoline = 6.2 * 0.79 psia / 13.07 psia * 92lb/lbmole / 62 lb/lbmole = 0.56 wt%

HAPs Loss = VOC * HAP wt%

2,2,4-Trimethylpentane Emissions on Gasoline Loading = 4.3 lb/hr * 0.56/100 = 0.024 lb/hr

2,2,4-Trimethylpentane Emissions on Gasoline Loading = 4.5 ton/yr * 0.56/100 = 0.025 ton/yr

a. HAP Speciation per API 4723A for each surrogate commodity. API liquid wt% converted to vapor wt% using Raoults Law and the

b. Controlled VOC Emissions per Commodity as calculated in Truck and Railcar Loading Potential to Emit worksheet and using AP-42, Ch. 5.2 (6/2008)

			Ac	enaphthyle	ene		Anthracen	e	Ben	z(a)anthra	cene		Benzene		Benzo	(a)phenan	threne
				208-96-8			120-12-7			56-55-3			71-43-2			218-01-9	
				9.3E-05			1.2E-05			4.1E-09			2.01			1.2E-10	
Loading Rack	Loading Rack Description	Material Loaded	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy
TLO-1	Asphalt Truck Loading and Off-Loading Rack	Asphalt/Pitch	-	-	-	3.0E-08	4.3E-09	4.3E-09	ND	-	-	0.33	0.05	0.05	3.1E-13	4.5E-14	4.5E-14
TL-2	Asphalt Truck Loading Rack #2	Asphalt/Pitch	-	-	-	3.0E-08	3.7E-09	1.1E-09	ND	-	-	0.33	0.04	0.01	3.1E-13	3.9E-14	1.2E-14
	Fuels Truck Loading	Gasoline	-	-	-	-	-	-	-	-	-	0.13	5.7E-03	6.0E-03	-	-	-
TL-4	Rack	Diesel	-	-	-	2.1E-06	4.3E-09	6.7E-09	-	-	-	4.9E-03	9.8E-06	1.5E-05	-	-	-
	Nack	Jet Fuel	-	-	-	-	-	-	-	-	-	1.9E-03	8.5E-07	4.4E-07	-	-	-
TL-7	CBO/LCO Truck	Carbon Black Oil	2.2E-08	1.6E-09	4.0E-10	4.7E-08	3.5E-09	8.7E-10	2.1E-11	1.6E-12	3.8E-13	2.5E-04	1.9E-05	4.7E-06	4.8E-13	3.6E-14	8.8E-15
16-7	Loading Rack	Light Cycle Oil	1.1E-07	1.4E-08	2.0E-11	2.9E-08	3.6E-09	5.2E-12	ND	-	-	1.9E-03	2.3E-04	3.4E-07	ND	-	-
		Carbon Black Oil	2.2E-08	4.3E-09	3.6E-10	4.7E-08	9.4E-09	7.9E-10	2.1E-11	4.1E-12	3.5E-13	2.5E-04	5.1E-05	4.2E-06	4.8E-13	9.6E-14	8.0E-15
RLO-8	Railcar Loading and Off-	Diesel				2.1E-06	1.6E-08	1.7E-08		-	-	4.9E-03	3.8E-05	3.9E-05	-	-	-
NLO-6	Loading Rack	Jet Fuel	-	-	-	-	-	-	-	-	-	1.9E-03	1.9E-05	1.9E-05	-	-	-
		Asphalt	-	-	-	3.0E-08	3.7E-09	8.8E-10	ND	-	-	0.33	0.04	0.01	3.1E-13	3.9E-14	9.1E-15
	Railcar Loading and Off-	Asphalt/Pitch	-	-	-	3.0E-08	1.9E-08	1.6E-09	ND	-	-	0.33	0.22	0.02	3.1E-13	2.0E-13	1.7E-14
RLO-19	Loading Rack	Gas Oil	ND	-	-	3.6E-09	3.2E-10	1.0E-10	5.3E-13	4.6E-14	1.5E-14	0.20	1.8E-02	5.5E-03	5.0E-14	4.4E-15	1.4E-15
	Loading Nack	Fuel Oil	1.3E-07	4.0E-09	4.5E-09	3.4E-08	1.1E-09	1.2E-09	ND	-	-	2.2E-03	6.9E-05	7.7E-05	ND	-	-
TLO-20	Asphalt/Pitch Truck Loading Rack	Asphalt/Pitch	-	-	-	3.0E-08	7.4E-09	1.1E-09	ND	-	-	0.33	0.08	0.01	3.1E-13	7.7E-14	1.2E-14
					5.3E-09			3.5E-08			7.5E-13			1.1E-01			1.1E-13

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

b. Controlled VOC Emissions per Commodity as calculated in $\mathsf{Tr} \mathsf{u}$

Sample Calculations for Gasoline Loading

HAP Vapor wt% = HAP Liquid I wt% * Pi° / Pa * ML/Mv 2,2,4-Trimethylpentane Vapor wt% in Gasoline = 6.2 * (

HAPs Loss = VOC * HAP wt%

2,2,4-Trimethylpentane Emissions on Gasoline Loading

			Ве	nzo(a)pyre	ene	Benzo	(b)fluoran	thene	Ве	nzo(e)pyre	ene	Benz	o(g,h,i)per	ylene	Benzo	o(k)fluoran	thene
				50-32-8			205-99-2			192-97-2			191-24-2			207-08-9	
				1.1E-10			9.7E-09			1.1E-10			1.9E-12			1.9E-11	
Loading Rack	Loading Rack Description	Material Loaded	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy
TLO-1	Asphalt Truck Loading and Off-Loading Rack	Asphalt/Pitch	ND	-	-	ND	-	-	-	-	-	5.0E-15	7.2E-16	7.2E-16	-	-	-
TL-2	Asphalt Truck Loading Rack #2	Asphalt/Pitch	ND	-	-	ND	-	-	-	-	-	5.0E-15	6.2E-16	1.9E-16	-	-	-
	Fuels Truck Loading	Gasoline	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TL-4	Rack	Diesel	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	Nack	Jet Fuel	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TL-7	CBO/LCO Truck	Carbon Black Oil	6.2E-14	4.6E-15	1.1E-15	3.4E-12	2.5E-13	6.2E-14	5.6E-14	4.2E-15	1.0E-15	6.3E-16	4.7E-17	1.2E-17	2.8E-15	2.1E-16	5.2E-17
16-7	Loading Rack	Light Cycle Oil	ND	-	-	ND	-	-	ND	-	-	9.1E-16	1.1E-16	1.6E-19	ND	-	-
		Carbon Black Oil	6.2E-14	1.2E-14	1.0E-15	3.4E-12	6.7E-13	5.6E-14	5.6E-14	1.1E-14	9.3E-16	6.3E-16	1.2E-16	1.0E-17	2.8E-15	5.6E-16	4.7E-17
RLO-8	Railcar Loading and Off-	Diesel	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NLO-6	Loading Rack	Jet Fuel	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
		Asphalt	ND	-	-	ND	-	-	-	-	-	5.0E-15	6.2E-16	1.5E-16	-	-	-
	Railcar Loading and Off-	Asphalt/Pitch	ND	-	-	ND	-	-	-	-	-	5.0E-15	3.2E-15	2.7E-16	-	-	-
RLO-19	Loading Rack	Gas Oil	1.2E-14	1.0E-15	3.3E-16	7.9E-13	7.0E-14	2.2E-14	4.4E-14	3.9E-15	1.2E-15	6.0E-16	5.3E-17	1.7E-17	ND	-	-
	Loading Nack	Fuel Oil	ND	-	-	ND	-	-	ND	-	-	1.1E-15	3.3E-17	3.6E-17	ND	-	-
TLO-20	Asphalt/Pitch Truck Loading Rack	Asphalt/Pitch	ND	-	-	ND	-	-	-	-	-	5.0E-15	1.2E-15	1.9E-16	-	-	-
					2.5E-15			1.4E-13			3.2E-15			1.6E-15			9.9E-17

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

b. Controlled VOC Emissions per Commodity as calculated in Tru

Sample Calculations for Gasoline Loading

HAP Vapor wt% = HAP Liquid I wt% * Pi° / Pa * ML/Mv 2,2,4-Trimethylpentane Vapor wt% in Gasoline = 6.2 * (

HAPs Loss = VOC * HAP wt%

2,2,4-Trimethylpentane Emissions on Gasoline Loading

				Biphenyl			Cumene		E	thylbenzer	ie	Fl	luoranther	пе		Fluorene	
				92-52-4			98-82-8			100-41-4			206-44-0			86-73-7	
				1.9E-04			0.12			2.2E-01			1.8E-07			1.2E-05	
Loading Rack	Loading Rack Description	Material Loaded	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy
TLO-1	Asphalt Truck Loading and Off-Loading Rack	Asphalt/Pitch	-	-	-	1.4E-03	2.0E-04	2.0E-04	2.6E-02	3.8E-03	3.7E-03	-	-	-	-	-	-
TL-2	Asphalt Truck Loading Rack #2	Asphalt/Pitch	-	-	-	1.4E-03	1.7E-04	5.2E-05	2.6E-02	3.2E-03	9.7E-04	-	-	-	-	-	-
	Fuels Truck Loading	Gasoline	ND	-	-	2.4E-04	1.0E-05	1.1E-05	1.0E-02	4.3E-04	4.5E-04	-	-	-	-	-	-
TL-4	Rack	Diesel	2.4E-07	4.8E-10	7.5E-10	2.8E-04	5.5E-07	8.7E-07	1.1E-03	2.2E-06	3.4E-06	-	-	-	-	-	-
	Nack	Jet Fuel	5.5E-08	2.5E-11	1.3E-11	9.8E-04	4.5E-07	2.3E-07	2.3E-03	1.0E-06	5.3E-07	-	-	-	-	-	-
TL-7	CBO/LCO Truck	Carbon Black Oil	1.5E-06	1.1E-07	2.8E-08	ND	-	-	1.3E-04	9.7E-06	2.4E-06	8.1E-10	6.1E-11	1.5E-11	9.1E-08	6.8E-09	1.7E-09
16-7	Loading Rack	Light Cycle Oil	6.5E-06	8.0E-07	1.2E-09	6.6E-05	8.0E-06	1.2E-08	1.1E-03	1.4E-04	2.0E-07	1.4E-11	1.7E-12	2.5E-15	1.5E-07	1.9E-08	2.8E-11
		Carbon Black Oil	1.5E-06	3.0E-07	2.5E-08	ND	-	-	1.3E-04	2.6E-05	2.2E-06	8.1E-10	1.6E-10	1.4E-11	9.1E-08	1.8E-08	1.5E-09
RLO-8	Railcar Loading and Off-	Diesel	2.4E-07	1.8E-09	1.9E-09	2.8E-04	2.2E-06	2.2E-06	1.1E-03	8.4E-06	8.6E-06	-	-	-	-	-	-
NLO-6	Loading Rack	Jet Fuel	5.5E-08	5.5E-10	5.6E-10	9.8E-04	9.7E-06	9.9E-06	2.3E-03	2.3E-05	2.3E-05	-	-	-	-	-	-
		Asphalt	-	-	-	1.4E-03	1.7E-04	4.1E-05	2.6E-02	3.2E-03	7.7E-04	-	-	-	-	-	-
	Railcar Loading and Off-	Asphalt/Pitch	-	-	-	1.4E-03	9.0E-04	7.6E-05	2.6E-02	1.7E-02	1.4E-03	-	-	-	-	-	-
RLO-19	Loading Rack	Gas Oil	-	-	-	-	-	-	-	-	-	4.5E-11	4.0E-12	1.3E-12	4.2E-09	3.7E-10	1.2E-10
	Loading Nack	Fuel Oil	7.6E-06	2.4E-07	2.6E-07	7.6E-05	2.4E-06	2.6E-06	1.3E-03	4.1E-05	4.5E-05	1.6E-11	5.1E-13	5.6E-13	1.8E-07	5.6E-09	6.2E-09
TLO-20	Asphalt/Pitch Truck Loading Rack	Asphalt/Pitch	-	-	-	1.4E-03	3.4E-04	5.2E-05	2.6E-02	6.5E-03	9.7E-04	-	-	-	-	-	-
					3.2E-07			4.5E-04			8.4E-03			3.0E-11			9.5E-09

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

b. Controlled VOC Emissions per Commodity as calculated in Tru

Sample Calculations for Gasoline Loading

HAP Vapor wt% = HAP Liquid I wt% * Pi° / Pa * ML/Mv 2,2,4-Trimethylpentane Vapor wt% in Gasoline = 6.2 * (

HAPs Loss = VOC * HAP wt%

2,2,4-Trimethylpentane Emissions on Gasoline Loading

			Indend	(1,2,3-cd) 193-39-5	pyrene	Lea	d compou 7439-92-1			Methanol			l tert-buty			m-Xylene 108-38-3	
								•						'			
				2.4E-12			3.4E-02			2.70			5.30			0.16	
Loading Rack	Loading Rack Description	Material Loaded	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy
TLO-1	Asphalt Truck Loading and Off-Loading Rack	Asphalt/Pitch	ND	-	-	3.9E-07	5.7E-08	5.7E-08	-	-	-	-	-	-	0.04	6.4E-03	6.4E-03
TL-2	Asphalt Truck Loading Rack #2	Asphalt/Pitch	ND	-	-	3.9E-07	4.9E-08	1.5E-08	-	-	-	-	-	-	0.04	5.5E-03	1.7E-03
	Fuels Truck Loading	Gasoline	-		-	ND		-	5.5E-03	2.4E-04	2.5E-04	3.7E-02	1.6E-03	1.6E-03	1.8E-04	7.7E-06	8.2E-06
TL-4		Diesel	-	-	-	-	-	-	-	-	-	-	-	-	2.4E-02	4.7E-05	7.4E-05
	Rack	Jet Fuel	-	-	-	-	-	-	-	-	-	-	-	-	3.8E-03	1.7E-06	8.9E-07
TL-7	CBO/LCO Truck	Carbon Black Oil	2.8E-16	2.1E-17	5.1E-18	2.9E-08	2.2E-09	5.4E-10	-	-	-	ND	-	-	2.0E-04	1.5E-05	3.6E-06
IL-7	Loading Rack	Light Cycle Oil	ND	-	-	-	-	-	ND	-	-	ND	-	-	3.8E-03	4.7E-04	6.8E-07
		Carbon Black Oil	2.8E-16	5.5E-17	4.7E-18	2.9E-08	5.8E-09	4.9E-10	-	-	-	ND	-	-	2.0E-04	3.9E-05	3.3E-06
RLO-8	Railcar Loading and Off-	Diesel	-	-	-	-	-	-	-	-	-	-	-	-	0.02	1.8E-04	1.9E-04
KLU-0	Loading Rack	Jet Fuel	-	-	-	-	-	-	-	-	-	-	-	-	3.8E-03	3.8E-05	3.8E-05
		Asphalt	ND	-	-	3.9E-07	4.9E-08	1.2E-08	-	-	-	-	-	-	0.04	5.5E-03	1.3E-03
	Dailean Landing and Off	Asphalt/Pitch	ND	-	-	3.9E-07	2.6E-07	2.2E-08	-	-	-	-	-	-	0.04	0.03	2.4E-03
RLO-19	Railcar Loading and Off-	Gas Oil	ND		-	ND		-	ND		-	ND	-	-	-	-	-
	Loading Rack	Fuel Oil	ND	-	-	-	-	-	ND	-	-	ND	-	-	4.4E-03	1.4E-04	1.5E-04
TLO-20	Asphalt/Pitch Truck Loading Rack	Asphalt/Pitch	ND	-	-	3.9E-07	9.8E-08	1.5E-08	-	-	-	-	-	-	0.04	1.1E-02	1.7E-03
					9.8E-18			1.2E-07			2.5E-04			1.6E-03			0.01

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

b. Controlled VOC Emissions per Commodity as calculated in Tru

Sample Calculations for Gasoline Loading

HAP Vapor wt% = HAP Liquid I wt% * Pi° / Pa * ML/Mv 2,2,4-Trimethylpentane Vapor wt% in Gasoline = 6.2 * (

HAPs Loss = VOC * HAP wt%

2,2,4-Trimethylpentane Emissions on Gasoline Loading

				laphthalen	е		n-Hexane			o-Xylene		Pl	nenanthre	ne		p-Xylene	
				91-20-3			110-54-3			95-47-6			85-01-8			106-42-3	
				0.01			3.14			0.13			2.3E-06			0.17	
Loading Rack	Loading Rack Description	Material Loaded	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy
TLO-1	Asphalt Truck Loading and Off-Loading Rack	Asphalt/Pitch	5.9E-05	8.6E-06	8.5E-06	3.3E+00	0.47	0.47	-	-	-	1.4E-08	2.0E-09	2.0E-09	8.1E-03	1.2E-03	1.2E-03
TL-2	Asphalt Truck Loading Rack #2	Asphalt/Pitch	5.9E-05	7.4E-06	2.2E-06	3.3E+00	0.41	0.12	-	-	-	1.4E-08	1.7E-09	5.1E-10	8.1E-03	1.0E-03	3.0E-04
	Fuels Truck Loading	Gasoline	1.2E-04	5.0E-06	5.3E-06	1.5E-01	6.4E-03	6.7E-03	0.03	1.1E-03	1.2E-03	2.1E-10	9.1E-12	9.6E-12	9.7E-05	4.1E-06	4.3E-06
TL-4	Rack	Diesel	9.4E-05	1.9E-07	3.0E-07	1.8E-03	3.6E-06	5.6E-06	8.5E-05	1.7E-07	2.7E-07	4.4E-10	8.8E-13	1.4E-12	0.02	3.5E-05	5.5E-05
	Nack	Jet Fuel	9.8E-04	4.5E-07	2.3E-07	0.01	5.8E-06	2.9E-06	3.1E-02	1.4E-05	7.2E-06	-	-	-	0.01	4.7E-06	2.4E-06
TL-7	CBO/LCO Truck	Carbon Black Oil	1.9E-05	1.4E-06	3.6E-07	ND	-	-	1.3E-04	9.6E-06	2.4E-06	4.6E-08	3.5E-09	8.5E-10	2.1E-04	1.6E-05	3.8E-06
16-7	Loading Rack	Light Cycle Oil	2.7E-04	3.2E-05	4.7E-08	1.9E-03	2.3E-04	3.4E-07	7.7E-04	9.3E-05	1.4E-07	4.6E-08	5.6E-09	8.2E-12	1.4E-03	1.7E-04	2.5E-07
		Carbon Black Oil	1.9E-05	3.9E-06	3.2E-07	ND	-	-	1.3E-04	2.6E-05	2.2E-06	4.6E-08	9.2E-09	7.8E-10	2.1E-04	4.1E-05	3.5E-06
RLO-8	Railcar Loading and Off-	Diesel	9.4E-05	7.3E-07	7.5E-07	1.8E-03	1.4E-05	1.4E-05	8.5E-05	6.6E-07	6.8E-07	4.4E-10	3.4E-12	3.5E-12	1.7E-02	1.4E-04	1.4E-04
NLO-6	Loading Rack	Jet Fuel	9.8E-04	9.7E-06	9.9E-06	0.01	1.3E-04	1.3E-04	0.03	3.1E-04	3.1E-04	-	-	-	1.0E-02	1.0E-04	1.0E-04
		Asphalt	5.9E-05	7.4E-06	1.7E-06	3.26	4.1E-01	9.7E-02	-	-	-	1.4E-08	1.7E-09	4.0E-10	8.1E-03	1.0E-03	2.4E-04
	Railcar Loading and Off-	Asphalt/Pitch	5.9E-05	3.9E-05	3.2E-06	3.26	2.1E+00	1.8E-01	-	-	-	1.4E-08	8.9E-09	7.4E-10	8.1E-03	5.3E-03	4.4E-04
RLO-19	Loading Rack	Gas Oil	ND	-	-	-	-	-	-	-	-	4.6E-09	4.1E-10	1.3E-10	-	-	-
	Loading Nack	Fuel Oil	3.1E-04	9.6E-06	1.1E-05	2.2E-03	7.0E-05	7.7E-05	8.9E-04	2.8E-05	3.1E-05	5.4E-08	1.7E-09	1.9E-09	1.7E-03	5.2E-05	5.8E-05
TLO-20	Asphalt/Pitch Truck Loading Rack	Asphalt/Pitch	5.9E-05	1.5E-05	2.2E-06	3.26	0.81	0.12	-	-	-	1.4E-08	3.4E-09	5.1E-10	8.1E-03	2.0E-03	3.0E-04
					4.6E-05			1.00			1.5E-03			7.8E-09			2.8E-03

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

b. Controlled VOC Emissions per Commodity as calculated in Tru

Sample Calculations for Gasoline Loading

HAP Vapor wt% = HAP Liquid I wt% * Pi° / Pa * ML/Mv 2,2,4-Trimethylpentane Vapor wt% in Gasoline = 6.2 * (

HAPs Loss = VOC * HAP wt%

2,2,4-Trimethylpentane Emissions on Gasoline Loading

				Pyrene 129-00-0			Toluene 108-88-3			(mixed iso 1330-20-7	
				8.7E-08			0.60			0.20	
Loading Rack	Loading Rack Description	Material Loaded	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy	Vapor wt%	lb/hr	tpy
TLO-1	Asphalt Truck Loading and Off-Loading Rack	Asphalt/Pitch	-	-	-	0.22	0.03	0.03	0.06	9.4E-03	9.3E-03
TL-2	Asphalt Truck Loading Rack #2	Asphalt/Pitch	-	-	-	0.22	0.03	0.01	0.06	8.1E-03	2.4E-03
	Fuels Truck Loading	Gasoline	-	-	-	0.13	0.01	0.01	0.16	0.01	0.01
TL-4	Rack	Diesel	-	-	-	4.3E-03	8.7E-06	1.4E-05	0.01	1.0E-05	1.6E-05
	Nack	Jet Fuel	-	-	-	3.9E-03	1.8E-06	9.1E-07	0.03	1.6E-05	8.1E-06
TL-7	CBO/LCO Truck	Carbon Black Oil	1.6E-09	1.2E-10	2.9E-11	7.4E-04	5.5E-05	1.4E-05	7.0E-04	5.3E-05	1.3E-05
16-7	Loading Rack	Light Cycle Oil	6.7E-11	8.1E-12	1.2E-14	0.00	4.7E-04	6.9E-07	0.01	6.2E-04	9.1E-07
		Carbon Black Oil	1.6E-09	3.1E-10	2.6E-11	7.4E-04	1.5E-04	1.2E-05	7.0E-04	1.4E-04	1.2E-05
RLO-8	Railcar Loading and Off-	Diesel	-	-	-	4.3E-03	3.4E-05	3.4E-05	0.01	4.0E-05	4.1E-05
NLO-0	Loading Rack	Jet Fuel	-	-	-	0.004	3.9E-05	4.0E-05	0.03	3.4E-04	3.5E-04
		Asphalt	-	-	-	0.22	0.03	0.01	0.06	8.1E-03	1.9E-03
	Railcar Loading and Off-	Asphalt/Pitch	-	-	-	0.22	0.14	0.01	0.06	0.04	0.004
RLO-19	Loading Rack	Gas Oil	4.6E-11	4.0E-12	1.3E-12	-	-	-	-	-	-
	Loading Nack	Fuel Oil	7.8E-11	2.4E-12	2.7E-12	0.00	1.4E-04	1.6E-04	0.01	1.8E-04	2.0E-04
TLO-20	Asphalt/Pitch Truck Loading Rack	Asphalt/Pitch	-	-	-	0.22	0.05	0.01	0.06	0.02	0.002
					5.9E-11			0.07			0.03

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

b. Controlled VOC Emissions per Commodity as calculated in Tru

Sample Calculations for Gasoline Loading

HAP Vapor wt% = HAP Liquid I wt% * Pi° / Pa * ML/Mv 2,2,4-Trimethylpentane Vapor wt% in Gasoline = 6.2 * (

HAPs Loss = VOC * HAP wt%

2,2,4-Trimethylpentane Emissions on Gasoline Loading

TRLO-9 POTENTIAL TO EMIT

Molten Sulfur Truck/Railcar Loading & Off-Loading Rack

Scrubber Emissions

			Stack	Exhaust			Exhaust H ₂ S	H₂S Em	issions
Loading	Loading Rack Description	Material	Diameter	Temp.	Exhaust	Flow Rate	Concentration	Max.	Annual
Rack	Loading Rack Description	Loaded	Diameter	remp.			Concentration	Hourly	Average
			ft	°F	acfm	scfh	ppmv	lb/hr	tpy
TRLO-9	Molten Sulfur Truck/Railcar	Molten	0.33	130	500	26.846	2	0.005	0.02
TKLU-9	Loading Rack	Sulfur	0.55	130	300	20,840	2	0.005	0.02

Notes

Standard Volume = 385.3 scf/lbmol H₂S Molecular Weight = 34.1 lb/lbmol

Fugitive Loading Emissions

			Loading Th	roughputs		Molten			Vapor	Liquid H ₂ S in	Vapor H ₂ S in	Standard		of Sulfur	Volume	-611.6	Load Rack	H ₂ S Em	nissions
Loading Rack	Loading Rack Description	Material Loaded	Maximum Hourly	Annual Average	Sulfur Specific	Sulfur Density	H ₂ S	Loading Rack Temp.	Pressure of H ₂ S ⁽¹⁾	Sulfur Stream (X _{H2S}) ⁽²⁾	Sulfur Stream (Y _{H2S}) ⁽³⁾	Molar Volume ⁽⁴⁾		isplaced ⁽⁵⁾	Vapor Dis	. 2	Scrubber Capture Eff.	Max. Hourly	Annual Average
			gal/hr	LTPD	Gravity	lb/ft^3	ppmw	°c	bar	ft^3 _{H2S} / ft^3 _S	ft^3 _{H2S} / ft^3 _S	ft^3/lbmol	ft^3 _s /hr	ft^3 _s /yr	ft^3 _{H2S} /hr	ft^3 _{H2S} /yr	%	lb/hr	tpy
TRLO-9	Molten Sulfur Truck/Railcar Loading Rack	Molten Sulfur	34,500	330	1.8	112.3	100	140.6	162	0.0001	0.02	611.5	4,612	2,402,623	77.9	40,597	99.0%	0.043	0.011

(1) Vapor pressure of H2S per Stull, Daniel R., Vapor Pressure of Pure Substances. Organic and Inorganic Compounds, Ind. Eng. Chem., 1947, 39, 4, 517-540. https://webbook.nist.gov/cgi/cbook.cgi?lD=C7783064&Mask=4&Type=ANTOINE&Plot=on $Log10(P^{\circ}) = A - B/(T + C)$, P in bar and T in K

A= 4.52887 unitless

B= 958.587 unitless

C= -0.539 K

(2) Liquid H2S in Sulfur Stream X_{H2S} = H₂S (ppmw)/10^6 * MW_S/MW_{H2S}

H₂S Molecular Weight = 34.1 lb/lbmol

Sulfur Molecular Weight = 32.1 lb/lbmol

(3) Vapor H2S in Sulfur Stream $Y_{H2S} = P_{H2S}/P_{atm} * X_{H2S}$

Atmospheric Pressure 0.9 bar Carlsbad, NM - Nearest Class II site

- (4) Standard molar volume n/v = R*T/P
- (5) Volume of Sulfur Vapor Displaced (ft^3/hr) = Sulfur Production (gal/hr) * Specific Gravity * 8.34 lb/gal / Sulfur Density (lb/ft^3) Volume of Sulfur Vapor Displaced (ft^3/yr) = Sulfur Production (LT/day) * 2,240 lb/LT * 365 day/yr / Sulfur Density (lb/ft^3)
- (6) Volume of H₂S Vapor Displaced (ft³H_{2S}/hr) = Volume of Sulfur Vapor Displaced (ft³S/hour) x YH₂S (ft³H₂S /ft³S) $Volume \ of \ H_2S \ Vapor \ Displaced \ (ft^3_{H2S}/yr) = Volume \ of \ Sulfur \ Vapor \ Displaced \ (ft^3_s/yr) \ x \ Y_{H2S} \ (ft^3_{H2S}/ft^3_s)$
- (7) Maximum Hourly H₂S Emissions = Volume of H₂S Vapor Displaced (ft³/hr) / Standard Molar Volume (ft³/lbmol) * MW_{H2S} (lb/lbmol) Annual Avg. H₂S Emissions = Volume of H₂S Vapor Displaced (ft³/yr) / Standard Molar Volume (ft³/lbmol) * MW_{H2}S (lb/lbmol) * 1 ton/2,000 lb

TL-4 VAPOR COMBUSTION UNIT (VCU) POTENTIAL TO EMIT

	Emissions I	Factors	
Pollutant	Assist Gas/ Pilot Gas (lb/MMscf)	HC Vapors (lb/MMBtu)	Reference
NO _x	100	0.14	Assist Gas/Pilot Gas EF per AP-42, Ch. 1.4 (7/98), Table 1.4-1 Small Boilers (<100 MMBtu/hr),
СО	CO 84 0.14 U		uncontrolled. HC EF per VCU manufacturer specifications.
VOC	5.5	Note b	Assist Gas/Pilot Gas EF per AP-42, Ch. 1.4 (7/98), Table 1.4-1 Small Boilers (<100 MMBtu/hr), uncontrolled. HC DRE per VCU manufacturer specifications.
SO ₂	20 gr/10	0scf	PSD-NM-0195-M39R1. C101.G Natural Gas definition
PM/PM ₁₀ /PM _{2.5}	7.6	0.0075	EF per AP-42, Ch. 1.4 (7/98), Table 1.4-2 PM (Total). The lb/MMscf EF is converted to lb/MMBtu by dividing by the average heating content, 1020 Btu/scf, of the natural gas basis for the EF.

	Heat Content-HHV)	Flow	to VCU	Heat Inp	ut to VCU	NO _x E	missions	CO Em	nissions	PM/PM ₁₀ /PN	M _{2.5} Emissions	VOC Er	nissions	SO ₂ En	nissions
Streams to VCU ^a	(Btu/scf or Btu/lb)	(scfm or lb/hr)	(MMscf/yr or ton/yr)	(MMBtu/hr)	(MMBtu/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)
Scenario 1 - Maximum A	ssist Gas Only														
Assist Gas	1,020 Btu/scf	150 scfm		9.18		0.90		0.76		0.07		0.05		0.51	
Scenario 2 - Maximum L	oading Throughputs, No	Assist Gas													
Pilot Gas	1,020 Btu/scf	0.9 scfm	0.5 MMscf/yr	0.06	482.5	0.005	0.02	0.005	0.02	0.0004	0.002	0.0003	0.001	0.003	0.014
Gasoline Vapor	23,214 Btu/lb	602.2 lb/hr	365.4 ton/yr	13.98	16,966	1.96	1.19	1.96	1.19	0.104	0.06	Note b	Note b		
Diesel Vapor	19,718 Btu/lb	3.2 lb/hr	5.0 ton/yr	0.06	196.2	0.01	0.01	0.01	0.01	0.0005	0.001	Note b	Note b		
Jet Fuel Vapor	19,286 Btu/lb	0.7 lb/hr	0.4 ton/yr	0.01	14.2	0.002	0.001	0.002	0.001	0.0001	0.0001	Note b	Note b		
				Scena	rio 2 Subtotals =	1.97	1.23	1.97	1.22	0.11	0.07	0.0003	0.001	0.003	0.01
			Potential to Emit =	Maximum of Sc	enarios 1 or 2 =	1.97	1.23	1.97	1.22	0.11	0.07	0.05	0.001	0.51	0.01

Notes:

a. Scenarios 1 and 2 reflect the two Vapor Combustion Unit (VCU) operating scenarios with the highest hourly products-of-combustion emissions. Scenario 1 reflects when the VCU is receiving minimal, if any, heat input contribution from the loading vapors and therefore assist gas flow is required. In actual operations, Scenario 1 will occur for a limited number of minutes each hour and at less than maximum assist gas flow. The Scenario 1 hourly emissions are conservatively calculated assuming maximum assist gas flow occurring continuously for an entire hour. Scenario 2 reflects maximum loading vapors to the VCU when no assist gas is required. "Flow to VCU" conservatively reflects the total calculated uncontrolled loading emissions routed to the VCU (98.7% of uncontrolled loading losses).

b. VOC losses from HC routed to the VCU are captured at Loading Potential to Emit calculation sheet for TL-4

Sample Calculations:

Gasoline Vapor Flow = (Uncontrolled Loading Emissions, Ib/hr) from Fuels Truck Loading Rack Potential to Emit-VOC calculations

= 602 2 lb/br

Gasoline Heat Input = Heat Content (Btu/lb)* Gasoline Vapor Flow (lb/hr) * 1MMBtu/10^6 Btu

= 23,214Btu/lb * 602.2 lb/hr * 1 MMBtu/1,000,000 Btu = 13.98 MMBtu/hr

Gasoline NOx = Emission Factor (lb/MMBtu) * Gasoline Heat Input (MMBtu/hr)

= 0.14 lb/MMBtu * 13.98 MMBtu/hr = 1.96 lb/hr

Assist Gas SO_2 = Assist Gas Flow (scf/min)* 60 min/hr * cscf/100 scf * Natural Gas Sulfur Content (gr/100scf) * 1 lb/7,000 gr * 64 lbSO2/32 lbS 150 scf/min * 60 min/hr * 1 cscf/100 scf * 20 gr/100scf * 1 lb/7,000 gr * 64 lbSO2/32 lbS = 0.51 lb/hr

TL-4 VCU POTENTIAL TO EMIT GHG

Streams to VCU	Heat Input to VCU	Emissi	on Factors (lb/MMB	tu) ^a	Annua	l Emissions (to	n/yr)	CHC
Streams to vco	(MMBtu/yr)	CO ₂	CH ₄	N ₂ O	CO ₂	CH ₄	N ₂ O	GHG (as CO2e)
	Table	A-1 TO 40 CFR 98, s	subpart A, Global Wa	rming Potentials	1	25	298	(as COZE)
Pilot Gas	482.5	116.98	0.002	0.0002	28.2	5.3E-04	5.3E-05	28.2
Gasoline Vapor	16,966.5	154.81	0.007	0.001	1,313	0.06	0.01	1,318
Diesel Vapor	196.2	163.05	0.007	0.001	16.0	6.5E-04	1.3E-04	16.0
Jet Fuel Vapor	14.2	159.22	0.007	0.001	1.1	4.7E-05	9.4E-06	1.1
					1,358.6	0.06	0.01	1,363

Notes:

a. Emission factors from Tables C-1 and C-2 to 40 CFR 98, subpart C, for corresponsing products

Flanges

31,584

Pump Seals

295

Valves

FUGITIVE PIPING COMPONENT POTENTIAL TO EMIT

				Ga	as	Light	Liquid	Heavy	Liquid	Al	I	Light	Liquid	Heavy	y Liquid
				Non-		Non-		Non-		Non-		Non-		Non-	
				Monitored											
	Emission Factor (lb/	hr-cpte)/Control	Efficiency (1),(2)	0.059	96%	0.024	95%	0.0005	0%	0.00055	81%	0.251	88%	0.046	0%
UNIT ID	PROCESS UNIT	Regulatory Applicability	LDAR Database						COMPONENT	COUNTS					
FUG-02-SP CRUDE	South Division Crude Unit	-	02-CRUDE	-	409	-	1,710	-	-	2,766	-	-	21	-	-
FUG-06-NHDU	Naphtha HDS Unit 06	-	06-NDU	-	257	-	676	-	-	2,110	-	-	13	-	-
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	-	07-AMINE	-	340	-	1,318	-	-	1,415	-	-	25	-	-
FUG-07-SWS1	Sour Water Stripper	-	07-SWS	-	107	-	37	6	-	217	-	-	2	-	-
FUG-08-TRUCK RK	Loading Racks	-	08-TRUCK	-	22	-	415	-	-	1,051	-	-	13	-	-
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	-	09-N-ALK	-	256	-	1,505	-	-	952	-	-	24	-	-
FUG-10-FCC	FCC w/CVS	-	10-FCCU	-	763	-	826	-	-	4,091	-	-	21	-	-
FUG-13-NHDU	Naphtha HDS Unit 13	-	13-NHD	-	671	-	880	-	-	1,146	-	-	21	-	-
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	-	18-MEROX	-	-	-	-	-	-	-	-	-	-	-	-
FUG-19-NAPHTHA	Naptha Merox	QQQ	19-NAPH	-	-	-	-	-	-	-	-	-	-	-	-
FUG-20-ISOM	BenFree Unit	-	20-ISOM	-	2	-	396	-	-	173	-	-	2	-	-
FUG-21-SP VACUUM	Flasher/Vacuum Unit	-	21-VAC	-	142	-	133	-	-	699	-	-	6	-	-
FUG-25-ROSE-2	ROSE Unit	-	25-ROSE	-	199	-	584	-	-	1,796	-	-	6	-	-
FUG-29-BLENDER/TK FARM	Light Oil Tankage	-	29-BLEND 08-TK-FA 03-ROSE	-	61	-	2,028	-	-	2,260	-	-	57	-	-
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	-	30-SRU-2 12-TGTU	-	156	-	274	45	-	403	-	-	8	-	-
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	-	31-SRU-3	-	195	-	281	-	-	769	-	-	8	-	-
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	-	33-DHDU	-	576	-	289	473	-	1,835	-	-	6	7	-
FUG-34-HYDROCRACKER	WX Hydrocracker	-	34-MHU	-	291	-	213	-	-	779	-	-	6	-	-
FUG-35-SAT GAS	Saturates Gas Plant	-	35-SAT-G 16-SKID	-	185	-	659	-	-	1,596	-	-	9	-	-
FUG-36-RO	Reverse Osmosis	QQQ	36-RO	-	-	-	-	-	-	-	-	-	-	-	-
FUG-37-NP-UT	North Plant Utilities	QQQ	37-NP-UT	-	-	-	-	-	-	-	-	-	-	-	-
FUG-41-PBC	PBC Unit	-	41-PBC	-	38	-	135	-	-	440	-	-	2	-	-
FUG-43-S ALKY	South Alky Unit (W-76)	-	43-W76	-	-	-	-	-	-	-	-	-	-	-	-
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	-	44-DHDU	-	536	-	125	6	-	1,268	-	-	5	-	-
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	-	45-DHDU	-	109	-	140	-	-	349	-	-	2	-	-
FUG-54-PRIMEG	Prime G Unit	-	54-PRIME	-	708	-	635	119	-	1,133	-	-	8	2	-
FUG-63-H2 PLANT-1	Hydrogen Plant	-	63-HYDRO	-	-	-	-	-	-	-	-	-	-	-	-
FUG-64-H2 PLANT-2	Hydrogen Plant	-	64-HYDRO	-	-	-	-	-	-	-	-	-	-	-	-
FUG-70-CCR	CCR Reformer (w/in battery limits)	-	70-CCR	-	1,306	-	726	6	-	2,828	-	-	14	-	-
FUG-73-SP UTIL	Utilities	-	73-SP-UT	-	-	-	-	-	-	-	-	-	-	-	-
FUG-80-WWTP CVS	Oil/Water Separator	-	80-WWTP	-	72	-	183	-	-	846	-	-	13	-	-
FUG-LPG	LPG Storage System	-	08-LPG-S	-	41	-	261	-	-	662	-	-	3	-	-

TOTAL

7,442

Notes:

14,429

⁽¹⁾ Emission factors (lb/hr-cpte) per "Protocol for Equipment Leak Estimates," EPA-453/R-95-017, Table 2-2 "Refinery Average Emission Factors", November 1995

⁽²⁾ Control efficiency per "Protocol for Equipment Leak Estimates," EPA-453/R-95-017, Table 5-3 "Control Effectiveness for an LDAR Program at a Refinery Process Unit", Nov. 1995; and TCEQ Air Permit Technical Guidance for Chemical Sources - Fugitive Guidance - APDG 6422 - June 2018

⁽³⁾ Maximum VOC% applies to all stream unless otherwise specified.

	Ag	itators	Relief	Valves	Compres	sor Seals	Sampling C	Connections	WW Drai	n System
	Ligh	t Liquid	А	.II	G	as	А	JI .	А	.II
	Non-		Non-		Non-		Non-		Non-	
	Monitored	Monitored			Monitored	Monitored	Monitored	Monitored	Monitored	Monitored
!),(2)	0.251	0%	0.353	97%	1.402	95%	0.033	0%	0.0705	50%
e				(COMPONENT	COUNTS				

	Emission Factor (lb/h	r-cpte)/Control	Efficiency (1),(2)	0.251	0%	0.353	97%	1.402	95%	0.033	0%	0.0705	50%
UNIT ID	PROCESS UNIT	Regulatory Applicability	LDAR Database					COMPONENT	COUNTS				
FUG-02-SP CRUDE	South Division Crude Unit	-	02-CRUDE	-	-	-	11	-	2	-	5	-	62
FUG-06-NHDU	Naphtha HDS Unit 06	-	06-NDU	-	-	-	18	-	-	-	2	-	25
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	-	07-AMINE	-	-	-	22	-	-	-	8	-	58
FUG-07-SWS1	Sour Water Stripper	-	07-SWS	-	-	-	3	-	-	-	-	-	-
FUG-08-TRUCK RK	Loading Racks	-	08-TRUCK	-	1	-	13	-	1	-	-	-	-
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	-	09-N-ALK	-	-	-	26	-	-	-	14	-	55
FUG-10-FCC	FCC w/CVS	-	10-FCCU	-	-	-	11	-	1	-	-	-	62
FUG-13-NHDU	Naphtha HDS Unit 13	-	13-NHD	-	-	-	26	-	-	-	9	-	30
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	-	18-MEROX	-	-	-	-	-	-	-	-	-	5
FUG-19-NAPHTHA	Naptha Merox	QQQ	19-NAPH	-	-	-	-	-	-	-	-	-	6
FUG-20-ISOM	BenFree Unit	-	20-ISOM	-	-	-	15	-	-	-	5	-	21
FUG-21-SP VACUUM	Flasher/Vacuum Unit	-	21-VAC	-	-	-	3	-	2	-	1	-	32
FUG-25-ROSE-2	ROSE Unit	-	25-ROSE	-	-	-	6	-	-	-	7	-	56
			29-BLEND										
FUG-29-BLENDER/TK FARM	Light Oil Tankage	-	08-TK-FA	-	2	-	18	-	-	-	2	-	76
			03-ROSE										
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS		30-SRU-2	_	_		10	_	_		1	_	40
100-30-31(02) 1010	31102/3113 W/CV3		12-TGTU	_	_		10	_	_		1	_	40
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	-	31-SRU-3	-	-	-	9	-	-	-	1	-	31
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	-	33-DHDU	-	-	5	22	-	4	-	4	-	79
FUG-34-HYDROCRACKER	WX Hydrocracker	-	34-MHU	-	-	-	5	-	-	-	4	-	61
FUG-35-SAT GAS	Saturates Gas Plant	-	35-SAT-G 16-SKID	-	-	-	14	-	-	-	8	-	49
FUG-36-RO	Reverse Osmosis	QQQ	36-RO	-	-	-	-	-	-	-	-	-	2
FUG-37-NP-UT	North Plant Utilities	QQQ	37-NP-UT	-	-	-	-	-	-	-	-	-	38
FUG-41-PBC	PBC Unit	-	41-PBC	-	-	-	1	-	-	-	-	-	7
FUG-43-S ALKY	South Alky Unit (W-76)	-	43-W76	-	-	-	-	-	-	-	-	-	18
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	-	44-DHDU	-	-	-	15	-	-	-	-	-	41
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	-	45-DHDU	-	-	-	2	-	-	-	2	-	21
FUG-54-PRIMEG	Prime G Unit	-	54-PRIME	-	-	-	14	-	1	1	8	-	16
FUG-63-H2 PLANT-1	Hydrogen Plant	-	63-HYDRO	-	-	-	-	-	-	-	-	-	16
FUG-64-H2 PLANT-2	Hydrogen Plant	-	64-HYDRO	-	-	-	-	-	-	-	-	-	36
FUG-70-CCR	CCR Reformer (w/in battery limits)	-	70-CCR	-	-	-	36	-	4	-	6	-	52
FUG-73-SP UTIL	Utilities	-	73-SP-UT	-	-	-	-	-	-	-	-	-	8
FUG-80-WWTP CVS	Oil/Water Separator	-	80-WWTP	-	-	-	19	-	-	-	-	-	44
FUG-LPG	LPG Storage System	-	08-LPG-S	-	-	-	10	-	-	-	-	-	-
	-		TOTAL	0	3	5	329	0	15	1	87	0	1,047
Notes:													

Notes:

(1) Emission factors (lb/hr-cpte) per "Protocol for Equipment Leak Estimates," EPA-453/R-95-017, Table 2-2 "Refinery Average Emission Factors", November 1995

(2) Control efficiency per "Protocol for Equipment Leak Estimates," EPA-453/R-95-017, Table 5-3 "Control Effectiveness for an LDAR Program at a Refinery Process Unit", Nov. 1995; and TCEQ Air Permit Technical Guidance for Chemical Sources - Fugitive Guidance - APDG 6422 - June 2018

(3) Maximum VOC% applies to all stream unless otherwise specified.

							EMISSI	ONS (lb/hr)							
	Emission Factor (lb/h	ar-cate)/Control	Efficiency (1),(2)	Valves	Flanges	Pump Seals	Agitators	Relief	Compressor	Sampling	WW Drain	VOC Content ⁽³⁾	VOC Content ⁽³⁾	VOC Er	nissions
UNIT ID	PROCESS UNIT	Regulatory Applicability	LDAR Database	valves	rianges	rump Jeans	Agitators	Valves	Seals	Connections	WWV Diam	%	%	(lb/hr)	(tons/yr)
FUG-02-SP CRUDE	South Division Crude Unit	-	02-CRUDE	3.021	1.524	0.633	-	0.116	0.140	0.165	2.187	100%		7.79	34.11
FUG-06-NHDU	Naphtha HDS Unit 06	-	06-NDU	1.420	1.163	0.392	-	0.190	-	0.066	0.882	100%		4.11	18.02
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	-	07-AMINE	2.387	0.780	0.754	-	0.233	-	0.265	2.046	100%		6.46	28.31
FUG-07-SWS1	Sour Water Stripper	-	07-SWS	0.300	0.120	0.060	-	0.032	-	-	-	100%		0.51	2.24
FUG-08-TRUCK RK	Loading Racks	-	08-TRUCK	0.551	0.579	0.392	0.251	0.138	0.070	-	-	100%		1.98	8.68
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	-	09-N-ALK	2.413	0.525	0.724	-	0.275	-	0.463	1.940	100%		6.34	27.77
FUG-10-FCC	FCC w/CVS	-	10-FCCU	2.796	2.255	0.633	-	0.116	0.070	-	2.187	100%		8.06	35.29
FUG-13-NHDU	Naphtha HDS Unit 13	-	13-NHD	2.643	0.632	0.633	-	0.275	-	0.298	1.058	100%		5.54	24.26
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	-	18-MEROX	-	-	-	-	-	-	-	0.176	100%		0.18	0.77
FUG-19-NAPHTHA	Naptha Merox	QQQ	19-NAPH	-	-	-	-	-	-	-	0.212	100%		0.21	0.93
FUG-20-ISOM	BenFree Unit	-	20-ISOM	0.481	0.095	0.060	-	0.159	-	0.165	0.741	100%		1.70	7.45
FUG-21-SP VACUUM	Flasher/Vacuum Unit	-	21-VAC	0.495	0.385	0.181	-	0.032	0.140	0.033	1.129	100%		2.40	10.49
FUG-25-ROSE-2	ROSE Unit	-	25-ROSE	1.172	0.990	0.181	-	0.063	-	0.231	1.975	100%		4.61	20.21
FUG-29-BLENDER/TK FARM	Light Oil Tankage	-	29-BLEND 08-TK-FA 03-ROSE	2.581	1.246	1.719	0.503	0.190	-	0.066	2.681	100%		8.99	39.36
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	-	30-SRU-2 12-TGTU	0.721	0.222	0.241	-	0.106	-	0.033	1.411	100%		2.73	11.97
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	-	31-SRU-3	0.798	0.424	0.241	-	0.095	-	0.033	1.093	100%		2.69	11.76
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	-	33-DHDU	1.948	1.011	0.505	-	1.996	0.280	0.132	2.787	100%		8.66	37.93
FUG-34-HYDROCRACKER	WX Hydrocracker	-	34-MHU	0.944	0.429	0.181	-	0.053	-	0.132	2.152	100%		3.89	17.04
FUG-35-SAT GAS	Saturates Gas Plant	-	35-SAT-G 16-SKID	1.229	0.880	0.271	-	0.148	-	0.265	1.728	100%		4.52	19.80
FUG-36-RO	Reverse Osmosis	QQQ	36-RO	-	-	-	-	-	-	-	0.071	100%		0.07	0.31
FUG-37-NP-UT	North Plant Utilities	QQQ	37-NP-UT	-	-	-	-	-	-	-	1.340	100%		1.34	5.87
FUG-41-PBC	PBC Unit	-	41-PBC	0.252	0.243	0.060	-	0.011	-	-	0.247	100%		0.81	3.56
FUG-43-S ALKY	South Alky Unit (W-76)	-	43-W76	-	-	-	-	-	-	-	0.635	100%		0.63	2.78
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	-	44-DHDU	1.420	0.699	0.151	-	0.159	-	-	1.446	100%		3.87	16.97
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	-	45-DHDU	0.426	0.192	0.060	-	0.021	-	0.066	0.741	100%		1.51	6.60
FUG-54-PRIMEG	Prime G Unit	-	54-PRIME	2.497	0.624	0.334	-	0.148	0.070	0.298	0.564	100%		4.54	19.86
FUG-63-H2 PLANT-1	Hydrogen Plant	-	63-HYDRO	-	-	-	-	-	-	-	0.564	100%		0.56	2.47
FUG-64-H2 PLANT-2	Hydrogen Plant	-	64-HYDRO	-	-	-	-	-	-	-	1.270	100%		1.27	5.56
FUG-70-CCR	CCR Reformer (w/in battery limits)	-	70-CCR	3.962	1.559	0.422	-	0.381	0.280	0.198	1.834	100%		8.64	37.83
FUG-73-SP UTIL	Utilities	-	73-SP-UT	-	-	-	-	-	-	-	0.282	100%		0.28	1.24
FUG-80-WWTP CVS	Oil/Water Separator	-	80-WWTP	0.390	0.466	0.392	-	0.201	-	-	1.552	100%		3.00	13.15
FUG-LPG	LPG Storage System	-	08-LPG-S	0.410	0.365	0.090	-	0.106	-	-	-	100%		0.97	4.26
Notes:	, , ,		TOTAL	35.256	17.407	9.313	0.754	5.245	1.052	2.910	36.931			108.87	476.85

Notes:

(1) Emission factors (lb/hr-cpte) per "Protocol for Equipment Leak Estimates," EPA-453/R-95-017, Table 2-2 "Refinery Average Emission Factors", November 1995

(2) Control efficiency per "Protocol for Equipment Leak Estimates," EPA-453/R-95-017, Table 5-3 "Control Effectiveness for an LDAR Program at a Refinery Process Unit", Nov. 1995; and TCEQ Air Permit Technical Guidance for Chemical Sources - Fugitive Guidance - APDG 6422 - June 2018

(3) Maximum VOC% applies to all stream unless otherwise specified.

$$CH_{4} = \left(0.4 \times N_{CD} + 0.2 \times N_{PU1} + 0.1 \times N_{PU2} + 4.3 \times N_{H2} + 6 \times N_{FGS}\right) \qquad (\text{Eq. Y-21})$$

CH₄ = Annual methane emissions from equipment leaks (metric tons/yr).

N_{CD} = Number of atmospheric crude distillation columns at the facility.

N_{PU1} = Cumulative number of catalytic cracking units, coking units, hydrocracking, and full-range distillation columns at the facility.

N_{PU2} = Cumulative number of hydrotreating/hydrorefining units, catalytic reforming units, and visbreaking units at the facility.

 N_{H2} = Total number of hydrogen plants at the facility.

N_{FGS} = Total number of fuel gas systems at the facility.

Variable	Number of Units	Unit Descriptions
N _{CD}	1	South Division Crude Unit 02
N _{PU1}	9	FCC Unit 10, Rose Unit 25, and Hydrocracker Unit 34. Sat Gas Unit 35 - 4 columns, PBC Unit 41 - 2 columns.
N _{PU2}	10	Kerosene HDS Unit 05, Naphtha HDS Units 06 and 13, Merox/Merichem Treating Unit 18, Diesel HDS Unit 33, GOH Unit 44, GOH Unit 45, CCR Unit 70, Skid Treaters Unit 16, and Prime G Unit 54.
N _{H2}	2	Hydrogen Units 63 and 64.
N _{FGS}	2	Unit 7 HP and LP systems

CH₄ = 23.8 metric tons/yr 26.2 tons/yr

The CCR catalytic reforming unit only has fugitive emission sources reported in the permit. Additional GHG emissions associated with catalyst regeneration is included with the fugitive emissions. The maximum reported rate between 2011 and 2015 was increased by 100% to estimate the potential to emit.

Fugitive GHG TOTAL GHG (ton/yr) (as CO₂e) CH₄ CO, N_2O (ton/yr) 25 298 Table A-1 to 40 CFR 98, subpart A, Global Warming Potentials 1 **Fugitive Components** 26.23 656 CCR 816.52 0.024 0.005 819 816.52 26.26 0.005 1,474 Total

Maximum Individual HAPs (2,2,4-Trimethylpentane) 16.85 ton/yr

Total HAPs 49.42 ton/yr

						1	L,3-Butadien	e	2,2,4-1	rimethylp	entane	A	cenaphthe	ne
							106-99-0			540-84-1			83-32-9	
UNIT ID	PROCESS UNIT	LDAR Database	Surrogate	VOC (lb/hr)	VOC (tpy)	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy
FUG-02-SP CRUDE	South Division Crude Unit	02-CRUDE	Supply System - Crude Oil	7.8	34.1	ND	-		5.5E-02	4.3E-03	1.9E-02	5.9E-04	4.6E-05	2.0E-04
FUG-06-NHDU	Naphtha HDS Unit 06	06-NDU	Atmospheric Distillation - Straight Run Naphtha	4.1	18.0	ND	-	-	4.5E-02	1.9E-03	8.1E-03	ND	-	-
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	07-AMINE	Amine Treating - Sour Gas	6.5	28.3	ND	-	-	-	-	-	-	-	-
FUG-07-SWS1	Sour Water Stripper	07-SWS	Amine Treating - Sour Gas	0.5	2.2	ND	-	-	-	-	-	-	-	-
FUG-08-TRUCK RK	Loading Racks	08-TRUCK	Gasoline Blending - Reformulated Gasoline	2.0	8.7	ND	-	-	6.2E+00	1.2E-01	5.4E-01	-	-	-
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	09-N-ALK	Alkylation - Alkylate/NOT C4 Olefin feed	6.3	27.8	-	-	-	2.8E+01	1.7E+00	7.7E+00	-	-	-
FUG-10-FCC	FCC w/CVS	10-FCCU	Gasoline Blending - Reformulated Gasoline	8.1	35.3	ND	-	-	6.2E+00	5.0E-01	2.2E+00	-	-	-
FUG-13-NHDU	Naphtha HDS Unit 13	13-NHD	Atmospheric Distillation - Straight Run Naphtha	5.5	24.3	ND	-	-	4.5E-02	2.5E-03	1.1E-02	ND	-	-
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	18-MEROX	Gasoline Blending - Reformulated Gasoline	0.2	0.8	ND	-	-	6.2E+00	1.1E-02	4.8E-02	-	-	-
FUG-19-NAPHTHA	Naptha Merox	19-NAPH	Atmospheric Distillation - Straight Run Naphtha	0.2	0.9	ND	-	-	4.5E-02	9.6E-05	4.2E-04	ND	-	-
FUG-20-ISOM	BenFree Unit	20-ISOM	Catalytic Isomerization - Isom Naphtha/Isomerate	1.7	7.5	-	-	-	1.9E-01	3.2E-03	1.4E-02	-	-	-
FUG-21-SP VACUUM	Flasher/Vacuum Unit	21-VAC	Vacuum Distillation - Light Vacuum Gas Oil	2.4	10.5	-	-	-	-	-	-	ND	-	-
FUG-25-ROSE-2	ROSE Unit	25-ROSE	Asphalt Plant - Asphalt	4.6	20.2	ND	-	-	ND	-	-	-	-	-
FUG-29-BLENDER/TK FARM	Light Oil Tankage	29-BLEND 08-TK-FA 03-ROSE	Gasoline Blending - Reformulated Gasoline	9.0	39.4	ND	-	-	6.2E+00	5.6E-01	2.5E+00	-	-	-
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	30-SRU-2 12-TGTU	Amine Treating - Sour Gas	2.7	12.0	ND	-	-	-	-	-	-	-	-
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	31-SRU-3	Amine Treating - Sour Gas	2.7	11.8	ND	-	-	-	-	-	-	-	-
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	33-DHDU	Catalytic Hydrocracker - Light H/C Distillate	8.7	37.9	-	-	-	1.4E-01	1.2E-02	5.2E-02	-	-	-
FUG-34-HYDROCRACKER	WX Hydrocracker	34-MHU	Atmospheric Distillation - Straight Run Naphtha	3.9	17.0	ND	-	-	4.5E-02	1.8E-03	7.7E-03	ND	-	-
FUG-35-SAT GAS	Saturates Gas Plant	35-SAT-G 16-SKID	Atmospheric Distillation - Straight Run Naphtha	4.5	19.8	ND	-	-	4.5E-02	2.0E-03	9.0E-03	ND	-	-
FUG-36-RO	Reverse Osmosis	36-RO	Atmospheric Distillation - Straight Run Naphtha	0.1	0.3	ND	-	-	4.5E-02	3.2E-05	1.4E-04	ND	-	-
FUG-37-NP-UT	North Plant Utilities	37-NP-UT	Atmospheric Distillation - Straight Run Naphtha	1.3	5.9	ND	-	-	4.5E-02	6.1E-04	2.7E-03	ND	-	-
FUG-41-PBC	PBC Unit	41-PBC	Catalytic Isomerization - Isobutane	0.8	3.6	1.2E-01	9.7E-04	4.2E-03	-	-	-	-	-	-
FUG-43-S ALKY	South Alky Unit (W-76)	43-W76	Gasoline Blending - Reformulated Gasoline	0.6	2.8	ND	-	-	6.2E+00	4.0E-02	1.7E-01	-	-	-
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	44-DHDU	Catalytic Hydrocracker - Light H/C Distillate	3.9	17.0	-	-	-	1.4E-01	5.3E-03	2.3E-02	-	-	-
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	45-DHDU	Catalytic Hydrocracker - Light H/C Distillate	1.5	6.6	-	-	-	1.4E-01	2.1E-03	9.0E-03	-	-	-
FUG-54-PRIMEG	Prime G Unit	54-PRIME	Gasoline Blending - Reformulated Gasoline	4.5	19.9	ND	-	-	6.2E+00	2.8E-01	1.2E+00	-	-	-
FUG-63-H2 PLANT-1	Hydrogen Plant	63-HYDRO	N/A	0.6	2.5									
FUG-64-H2 PLANT-2	Hydrogen Plant	64-HYDRO	N/A	1.3	5.6									
FUG-70-CCR	CCR Reformer (w/in battery limits)	70-CCR	Gasoline Blending - Reformulated Gasoline	8.6	37.8	ND	-	-	6.2E+00	5.4E-01	2.4E+00	-	-	-
FUG-73-SP UTIL	Utilities	73-SP-UT	N/A	0.3	1.2									
FUG-80-WWTP CVS	Oil/Water Separator	80-WWTP	Various Units - Slop Oil	3.0	13.1	ND	-	-	4.1E-02	1.2E-03	5.4E-03	3.0E-02	8.9E-04	3.9E-03
FUG-LPG	LPG Storage System	08-LPG-S	N/A	1.0	4.3					ĺ				
			TOTAL		476.8			4.2E-03			1.7E+01			4.1E-03

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

			Ac	enaphthyl	ene		Anthracen	e		Antimony	,		Arsenic		Ben	z(a)anthra	cene		Benzene	
				208-96-8			120-12-7			7440-36-0)		7440-38-2			56-55-3			71-43-2	
UNIT ID	PROCESS UNIT	LDAR Database	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy									
FUG-02-SP CRUDE	South Division Crude Unit	02-CRUDE	4.1E-04	3.2E-05	1.4E-04	3.8E-04	2.9E-05	1.3E-04	4.1E-05	3.2E-06	1.4E-05	6.5E-06	5.0E-07	2.2E-06	2.9E-03	2.3E-04	1.0E-03	1.6E-01	1.3E-02	5.5E-02
FUG-06-NHDU	Naphtha HDS Unit 06	06-NDU	ND	-	-	ND	-	-	-	-	-	-	-	-	ND	-	-	1.2E+00	4.9E-02	2.2E-01
FUG-07-N AMINE	Amine Unit-Treating/Regen. ²	07-AMINE	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-07-SWS1	Sour Water Stripper	07-SWS	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-08-TRUCK RK	Loading Racks	08-TRUCK	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	5.8E-01	1.2E-02	5.1E-02
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	09-N-ALK	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	2.4E-01	1.5E-02	6.7E-02
FUG-10-FCC	FCC w/CVS	10-FCCU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	5.8E-01	4.7E-02	2.1E-01
FUG-13-NHDU	Naphtha HDS Unit 13	13-NHD	ND	-	-	ND	-	-	-	-	-	-	-	-	ND	-	-	1.2E+00	6.6E-02	2.9E-01
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	18-MEROX	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	5.8E-01	1.0E-03	4.5E-03
FUG-19-NAPHTHA	Naptha Merox	19-NAPH	ND	-	-	ND	-	-	-	-	-	-	-	-	ND	-	-	1.2E+00	2.5E-03	1.1E-02
FUG-20-ISOM	BenFree Unit	20-ISOM	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	6.6E-01	1.1E-02	4.9E-02
FUG-21-SP VACUUM	Flasher/Vacuum Unit	21-VAC	ND	-	-	2.8E-03	6.7E-05	2.9E-04	-	-	-	4.6E-06	1.1E-07	4.8E-07	1.2E-03	2.8E-05	1.2E-04	9.0E-01	2.2E-02	9.5E-02
FUG-25-ROSE-2	ROSE Unit	25-ROSE	-	-	-	ND	-	-	2.1E-04	9.7E-06	4.2E-05	ND	-	-	ND	-	-	2.5E-04	1.2E-05	5.1E-05
FUG-29-BLENDER/TK FARM	Light Oil Tankage	29-BLEND 08-TK-FA	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	5.8E-01	5.2E-02	2.3E-01
		03-ROSE																		
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	30-SRU-2 12-TGTU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	31-SRU-3	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	33-DHDU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	2.5E+00	2.2E-01	9.5E-01
FUG-34-HYDROCRACKER	WX Hydrocracker	34-MHU	ND	-	-	ND	-	-	-	-	-	-	-	-	ND	-	-	1.2E+00	4.7E-02	2.0E-01
FUG-35-SAT GAS	Saturates Gas Plant	35-SAT-G 16-SKID	- ND	-	-	ND	-	-	-	-	-	-	-	-	ND	-	-	1.2E+00	5.4E-02	2.4E-01
FUG-36-RO	Reverse Osmosis	36-RO	ND	-	-	ND	-	-	-	-	-	-	-	-	ND	-	-	1.2E+00	8.5E-04	3.7E-03
FUG-37-NP-UT	North Plant Utilities	37-NP-UT	ND	-	-	ND	-	-	-	-	-	-	-	-	ND	-	-	1.2E+00	1.6E-02	7.0E-02
FUG-41-PBC	PBC Unit	41-PBC	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	2.6E-01	2.1E-03	9.2E-03
FUG-43-S ALKY	South Alky Unit (W-76)	43-W76	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	5.8E-01	3.7E-03	1.6E-02
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	44-DHDU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	2.5E+00	9.7E-02	4.3E-01
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	45-DHDU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	2.5E+00	3.8E-02	1.7E-01
FUG-54-PRIMEG	Prime G Unit	54-PRIME	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	5.8E-01	2.6E-02	1.2E-01
FUG-63-H2 PLANT-1	Hydrogen Plant	63-HYDRO																		
FUG-64-H2 PLANT-2	Hydrogen Plant	64-HYDRO																		
FUG-70-CCR	CCR Reformer (w/in battery limits)	70-CCR	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	5.8E-01	5.0E-02	2.2E-01
FUG-73-SP UTIL	Utilities	73-SP-UT																		1
FUG-80-WWTP CVS	Oil/Water Separator	80-WWTP	1.7E-02	5.2E-04	2.3E-03	1.1E-01	3.2E-03	1.4E-02	ND	-	-	ND	-	-	1.1E-03	3.2E-05	1.4E-04	3.5E-01	1.1E-02	4.6E-02
FUG-LPG	LPG Storage System	08-LPG-S																		1
					2.4E-03			1.4E-02			5.6E-05			2.7E-06			0.001			3.74

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

			Benzo	(a)phenan	threne	Be	nzo(a)pyre	ene	Benzo	o(b)fluoran	thene	Be	nzo(e)pyre	ne	Benz	o(g,h,i)per	ylene		Biphenyl	
				218-01-9			50-32-8			205-99-2			192-97-2			191-24-2			92-52-4	
UNIT ID	PROCESS UNIT	LDAR Database	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy
FUG-02-SP CRUDE	South Division Crude Unit	02-CRUDE	1.1E-03	8.4E-05	3.7E-04	2.9E-03	2.3E-04	1.0E-03	4.1E-03	3.2E-04	1.4E-03	8.0E-04	6.2E-05	2.7E-04	3.3E-04	2.6E-05	1.1E-04	2.4E-02	1.9E-03	8.2E-03
FUG-06-NHDU	Naphtha HDS Unit 06	06-NDU	ND	-	-	ND	-	-	ND	-	-	ND	-	-	ND	-	-	1.6E-02	6.6E-04	2.9E-03
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	07-AMINE	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-07-SWS1	Sour Water Stripper	07-SWS	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-08-TRUCK RK	Loading Racks	08-TRUCK	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	09-N-ALK	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	1.0E-02	6.3E-04	2.8E-03
FUG-10-FCC	FCC w/CVS	10-FCCU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-13-NHDU	Naphtha HDS Unit 13	13-NHD	ND	-	-	ND	-	-	ND	-	-	ND	-	-	ND	-	-	1.6E-02	8.9E-04	3.9E-03
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	18-MEROX	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-19-NAPHTHA	Naptha Merox	19-NAPH	ND	-	-	ND	-	-	ND	-	-	ND	-	-	ND	-	-	1.6E-02	3.4E-05	1.5E-04
FUG-20-ISOM	BenFree Unit	20-ISOM	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	4.9E-02	8.3E-04	3.7E-03
FUG-21-SP VACUUM	Flasher/Vacuum Unit	21-VAC	3.8E-03	9.0E-05	3.9E-04	1.0E-03	2.4E-05	1.1E-04	7.4E-04	1.8E-05	7.8E-05	3.6E-03	8.6E-05	3.8E-04	2.8E-03	6.7E-05	2.9E-04	-	-	-
FUG-25-ROSE-2	ROSE Unit	25-ROSE	ND	-	-	ND	-	-	ND	-	-	-	-	-	2.8E-03	1.3E-04	5.7E-04	ND	-	-
FUG-29-BLENDER/TK FARM	Light Oil Tankage	29-BLEND 08-TK-FA 03-ROSE	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	30-SRU-2 12-TGTU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	31-SRU-3	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	33-DHDU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-34-HYDROCRACKER	WX Hydrocracker	34-MHU	ND	-	-	ND	-	-	ND	-	-	ND	-	-	ND	-	-	1.6E-02	6.2E-04	2.7E-03
FUG-35-SAT GAS	Saturates Gas Plant	35-SAT-G 16-SKID	ND	-	-	ND	-	-	ND	-	-	ND	-	-	ND	-	-	1.6E-02	7.2E-04	3.2E-03
FUG-36-RO	Reverse Osmosis	36-RO	ND	-	-	ND	-	-	ND	-	-	ND	-	-	ND	-	-	1.6E-02	1.1E-05	4.9E-05
FUG-37-NP-UT	North Plant Utilities	37-NP-UT	ND	-	-	ND	-	-	ND	-	-	ND	-	-	ND	-	-	1.6E-02	2.1E-04	9.4E-04
FUG-41-PBC	PBC Unit	41-PBC	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-43-S ALKY	South Alky Unit (W-76)	43-W76	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	44-DHDU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	45-DHDU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-54-PRIMEG	Prime G Unit	54-PRIME	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-63-H2 PLANT-1	Hydrogen Plant	63-HYDRO																		
FUG-64-H2 PLANT-2	Hydrogen Plant	64-HYDRO																		
FUG-70-CCR	CCR Reformer (w/in battery limits)	70-CCR	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	ND	-	-
FUG-73-SP UTIL	Utilities	73-SP-UT																		
FUG-80-WWTP CVS	Oil/Water Separator	80-WWTP	8.5E-04	2.5E-05	1.1E-04	9.6E-04	2.9E-05	1.3E-04	1.5E-03	4.4E-05	1.9E-04	1.4E-03	4.2E-05	1.9E-04	ND	-	-	1.4E+00	4.2E-02	1.9E-01
FUG-LPG	LPG Storage System	08-LPG-S																		
					0.001			0.001			0.002			8.4E-04			0.001			0.21

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

				Cadmium)	Ca	rbon disulf	fide	Ca	rbonyl sulf	fide		Chromium			Cobalt		Creso	I (mixed is	omers)
				7440-43-9)		75-15-0			463-58-1			7440-47-3			7440-48-4			1319-77-3	
UNIT ID	PROCESS UNIT	LDAR Database	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy
FUG-02-SP CRUDE	South Division Crude Unit	02-CRUDE	2.9E-07	2.2E-08		ND	-	-	ND	-	-	5.7E-06	4.5E-07	2.0E-06	ND	-	-	-	-	-
FUG-06-NHDU	Naphtha HDS Unit 06	06-NDU	-	-	-	1.3E-03	5.2E-05	2.3E-04	-	-	-	-	-	-	-	-	-	-	-	-
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	07-AMINE	-	-	-	-	-	-	1.2E-02	7.7E-04	3.4E-03	-	-	-	-	-	-	-	-	-
FUG-07-SWS1	Sour Water Stripper	07-SWS	-	-	-	-	-	-	1.2E-02	6.1E-05	2.7E-04	-	-	-	-	-	-	-	-	-
FUG-08-TRUCK RK	Loading Racks	08-TRUCK	-	-	-	ND	-	-	ND	-	-	ND	-	-	-	-	-	-	-	-
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	09-N-ALK	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-10-FCC	FCC w/CVS	10-FCCU	-	-	-	ND	-	-	ND	-	-	ND	-	-	-	-	-	-	-	-
FUG-13-NHDU	Naphtha HDS Unit 13	13-NHD	-	-	-	1.3E-03	7.0E-05	3.1E-04	-	-	-	-	-	-	-	-	-	-	-	-
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	18-MEROX	-	-	-	ND	-	-	ND	-	-	ND	-	-	-	-	-	-	-	-
FUG-19-NAPHTHA	Naptha Merox	19-NAPH	-	-	-	1.3E-03	2.7E-06	1.2E-05	-	-	-	-	-	-	-	-	-	-	-	-
FUG-20-ISOM	BenFree Unit	20-ISOM	-	-	-	-	-	-	ND	-	-	-	-	-	-	-	-	-	-	-
FUG-21-SP VACUUM	Flasher/Vacuum Unit	21-VAC	ND	-	-	-	-	-	-	-	-	5.7E-05	1.4E-06	6.0E-06	-	-	-	-	-	-
FUG-25-ROSE-2	ROSE Unit	25-ROSE	4.0E-05	1.8E-06	8.0E-06	ND	-	-	ND	-	-	2.5E-05	1.1E-06	5.0E-06	2.8E-05	1.3E-06	5.7E-06	-	-	-
FUG-29-BLENDER/TK FARM	Light Oil Tankage	29-BLEND 08-TK-FA 03-ROSE	-	-	-	ND	-	-	ND	-	-	ND	-	-	-	-	-	-	-	-
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	30-SRU-2 12-TGTU	-	-	-	-	-	-	1.2E-02	3.3E-04	1.4E-03	-	-	-	-	-	-	-	-	-
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	31-SRU-3	-	-	-	-	-	-	1.2E-02	3.2E-04	1.4E-03	-	-	-	-	-	-	-	-	-
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	33-DHDU	-	-	-	ND	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-34-HYDROCRACKER	WX Hydrocracker	34-MHU	-	-	-	1.3E-03	4.9E-05	2.2E-04	-	-	-	-	-	-	-	-	-	-	-	-
FUG-35-SAT GAS	Saturates Gas Plant	35-SAT-G 16-SKID	-	-	-	1.3E-03	5.7E-05	2.5E-04	-	-	-	-	-	-	-	-	-	-	-	-
FUG-36-RO	Reverse Osmosis	36-RO	-	-	-	1.3E-03	9.0E-07	3.9E-06	-	-	-	-	-	-	-	-	-	-	-	-
FUG-37-NP-UT	North Plant Utilities	37-NP-UT	-	-	-	1.3E-03	1.7E-05	7.5E-05	-	-	-	-	-	-	-	-	-	-	-	-
FUG-41-PBC	PBC Unit	41-PBC	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-43-S ALKY	South Alky Unit (W-76)	43-W76	-	-	-	ND	-	-	ND	-	-	ND	-	-	-	-	-	-	-	-
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	44-DHDU	-	-	-	ND	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	45-DHDU	-	-	-	ND	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-54-PRIMEG	Prime G Unit	54-PRIME	-	-	-	ND	-	-	ND	-	-	ND	-	-	-	-	-	-	-	-
FUG-63-H2 PLANT-1	Hydrogen Plant	63-HYDRO																		
FUG-64-H2 PLANT-2	Hydrogen Plant	64-HYDRO																		
FUG-70-CCR	CCR Reformer (w/in battery limits)	70-CCR	-	-	-	ND	-	-	ND	-	-	ND	-	-	-	-	-	-	-	-
FUG-73-SP UTIL	Utilities	73-SP-UT																		
FUG-80-WWTP CVS	Oil/Water Separator	80-WWTP	3.2E-05	9.5E-07	4.2E-06	ND	-	-	ND	-	-	3.2E-05	9.5E-07	4.1E-06	ND	-	-	7.4E-02	2.2E-03	9.8E-03
FUG-LPG	LPG Storage System	08-LPG-S																		
					1.2E-05			0.001			6.5E-03			1.7E-05			5.7E-06			9.8E-03

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

				Cumene		Dibenz	o(a,h)anth	racene	E	thylbenzei	ne	FI	uoranther	ie		Fluorene		Lea	d compou	nds
				98-82-8			53-70-3			100-41-4			206-44-0			86-73-7			7439-92-1	
UNIT ID	PROCESS UNIT	LDAR Database	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy
FUG-02-SP CRUDE	South Division Crude Unit	02-CRUDE	2.4E-02	1.9E-03	8.2E-03	3.1E-04	2.4E-05	1.1E-04	1.7E-01	1.3E-02	5.7E-02	4.2E-04	3.3E-05	1.4E-04	3.4E-03	2.7E-04	1.2E-03	1.6E-07	1.2E-08	5.5E-08
FUG-06-NHDU	Naphtha HDS Unit 06	06-NDU	1.3E-01	5.4E-03	2.4E-02	ND	-	-	5.9E-01	2.4E-02	1.1E-01	ND	-	-	ND	-	-	-	-	-
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	07-AMINE	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-07-SWS1	Sour Water Stripper	07-SWS	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-08-TRUCK RK	Loading Racks	08-TRUCK	1.7E-02	3.4E-04	1.5E-03	-	-	-	4.1E-01	8.1E-03	3.5E-02	-	-	-	-	-	-	ND	-	-
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	09-N-ALK	2.5E-02	1.6E-03	6.8E-03	-	-	-	2.8E-02	1.7E-03	7.6E-03	-	-	-	-	-	-	-	-	-
FUG-10-FCC	FCC w/CVS	10-FCCU	1.7E-02	1.4E-03	6.1E-03	-	-	-	4.1E-01	3.3E-02	1.4E-01	-	-	-	-	-	-	ND	-	-
FUG-13-NHDU	Naphtha HDS Unit 13	13-NHD	1.3E-01	7.3E-03	3.2E-02	ND	-	-	5.9E-01	3.2E-02	1.4E-01	ND	-	-	ND	-	-	-	-	-
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	18-MEROX	1.7E-02	3.1E-05	1.3E-04	-	-	-	4.1E-01	7.2E-04	3.2E-03	-	-	-	-	-	-	ND	-	-
FUG-19-NAPHTHA	Naptha Merox	19-NAPH	1.3E-01	2.8E-04	1.2E-03	ND	-	-	5.9E-01	1.2E-03	5.4E-03	ND	-	-	ND	-	-	-	-	-
FUG-20-ISOM	BenFree Unit	20-ISOM	1.0E-01	1.8E-03	7.7E-03	-	-	-	5.0E-01	8.5E-03	3.7E-02	-	-	-	-	-	-	-	-	-
FUG-21-SP VACUUM	Flasher/Vacuum Unit	21-VAC	-	-	-	ND	-	-	-	-	-	2.3E-03	5.5E-05	2.4E-04	3.3E-03	7.8E-05	3.4E-04	ND	-	-
FUG-25-ROSE-2	ROSE Unit	25-ROSE	ND	-	-	-	-	-	2.9E-04	1.3E-05	5.9E-05	-	-	-	-	-	-	6.1E-05	2.8E-06	1.2E-05
FUG-29-BLENDER/TK FARM	Light Oil Tankage	29-BLEND 08-TK-FA	1.7E-02	1.6E-03	6.8E-03	-	-	-	4.1E-01	3.7E-02	1.6E-01	-	-	-	-	-	-	ND	-	-
		03-ROSE																		
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	30-SRU-2 12-TGTU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	31-SRU-3	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	33-DHDU	4.0E-02	3.5E-03	1.5E-02	-	-	-	3.1E-01	2.7E-02	1.2E-01	-	-	-	-	-	-	-	-	-
FUG-34-HYDROCRACKER	WX Hydrocracker	34-MHU	1.3E-01	5.1E-03	2.2E-02	ND	-	-	5.9E-01	2.3E-02	1.0E-01	ND	-	-	ND	-	-	-	-	-
FUG-35-SAT GAS	Saturates Gas Plant	35-SAT-G 16-SKID	1.3E-01	5.9E-03	2.6E-02	ND	-	-	5.9E-01	2.6E-02	1.2E-01	ND	-	-	ND	-	-	-	-	-
FUG-36-RO	Reverse Osmosis	36-RO	1.3E-01	9.2E-05	4.0E-04	ND	-	-	5.9E-01	4.1E-04	1.8E-03	ND	-	-	ND	-	-	-	-	-
FUG-37-NP-UT	North Plant Utilities	37-NP-UT	1.3E-01	1.8E-03	7.7E-03	ND	-	-	5.9E-01	7.9E-03	3.4E-02	ND	-	-	ND	-	-	-	-	-
FUG-41-PBC	PBC Unit	41-PBC	2.5E-02	2.0E-04	8.7E-04	-	-	-	8.6E-01	7.0E-03	3.1E-02	-	-	-	-	-	-	-	-	-
FUG-43-S ALKY	South Alky Unit (W-76)	43-W76	1.7E-02	1.1E-04	4.8E-04	-	-	-	4.1E-01	2.6E-03	1.1E-02	-	-	-	-	-	-	ND	-	-
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	44-DHDU	4.0E-02	1.6E-03	6.8E-03	-	-	-	3.1E-01	1.2E-02	5.3E-02	-	-	-	-	-	-	-	-	-
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	45-DHDU	4.0E-02	6.1E-04	2.7E-03	-	-	-	3.1E-01	4.7E-03	2.0E-02	-	-	-	-	-	-	-	-	-
FUG-54-PRIMEG	Prime G Unit	54-PRIME	1.7E-02	7.8E-04	3.4E-03	-	-	-	4.1E-01	1.9E-02	8.1E-02	-	-	-	-	-	-	ND	-	-
FUG-63-H2 PLANT-1	Hydrogen Plant	63-HYDRO																		
FUG-64-H2 PLANT-2	Hydrogen Plant	64-HYDRO																		
FUG-70-CCR	CCR Reformer (w/in battery limits)	70-CCR	1.7E-02	1.5E-03	6.5E-03	-	-	-	4.1E-01	3.5E-02	1.5E-01	-	-		-	-	-	ND	-	-
FUG-73-SP UTIL	Utilities	73-SP-UT																		
FUG-80-WWTP CVS	Oil/Water Separator	80-WWTP	3.1E-02	9.2E-04	4.0E-03	ND	-	-	2.0E-01	6.1E-03	2.7E-02	5.4E-03	1.6E-04	7.2E-04	4.3E-02	1.3E-03	5.7E-03	ND	-	-
FUG-LPG	LPG Storage System	08-LPG-S																		
					0.19			1.1E-04			1.45			1.1E-03			0.007			1.2E-05

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

				Manganes	e	Merc	cury compo	ounds		Methanol		Methy	l tert-buty	l ether		m-Xylene		ı	Naphthaler	ne
				7439-96-5	;		7439-97-6	;		67-56-1			1634-04-4			108-38-3			91-20-3	
UNIT ID	PROCESS UNIT	LDAR Database	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy
FUG-02-SP CRUDE	South Division Crude Unit	02-CRUDE	6.4E-06	5.0E-07	2.2E-06	3.2E-07	2.5E-08	1.1E-07	ND	-	-	-	-	-	4.7E-01	3.6E-02	1.6E-01	2.3E-02	1.8E-03	7.8E-03
FUG-06-NHDU	Naphtha HDS Unit 06	06-NDU	-	-	-	4.0E-08	1.6E-09	7.2E-09	5.6E-02	2.3E-03	1.0E-02	8.8E-02	3.6E-03	1.6E-02	2.1E+00	8.8E-02	3.9E-01	5.2E-03	2.1E-04	9.3E-04
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	07-AMINE	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-07-SWS1	Sour Water Stripper	07-SWS	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-08-TRUCK RK	Loading Racks	08-TRUCK	-	-	-	-	-	-	1.8E-02	3.6E-04	1.6E-03	6.1E-02	1.2E-03	5.3E-03	1.0E-02	2.0E-04	8.7E-04	1.9E-01	3.8E-03	1.6E-02
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	09-N-ALK	-	-	-	-	-	-	ND	-	-	8.0E-02	5.0E-03	2.2E-02	1.6E-01	1.0E-02	4.4E-02	5.1E-02	3.2E-03	1.4E-02
FUG-10-FCC	FCC w/CVS	10-FCCU	-	-	-	-	-	-	1.8E-02	1.5E-03	6.4E-03	6.1E-02	4.9E-03	2.1E-02	1.0E-02	8.1E-04	3.5E-03	1.9E-01	1.5E-02	6.7E-02
FUG-13-NHDU	Naphtha HDS Unit 13	13-NHD	-	-	-	4.0E-08	2.2E-09	9.7E-09	5.6E-02	3.1E-03	1.3E-02	8.8E-02	4.8E-03	2.1E-02	2.1E+00	1.2E-01	5.2E-01	5.2E-03	2.9E-04	1.3E-03
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	18-MEROX	-	-	-	-	-	-	1.8E-02	3.2E-05	1.4E-04	6.1E-02	1.1E-04	4.7E-04	1.0E-02	1.8E-05	7.7E-05	1.9E-01	3.4E-04	1.5E-03
FUG-19-NAPHTHA	Naptha Merox	19-NAPH	-	-	-	4.0E-08	8.5E-11	3.7E-10	5.6E-02	1.2E-04	5.1E-04	8.8E-02	1.9E-04	8.1E-04	2.1E+00	4.5E-03	2.0E-02	5.2E-03	1.1E-05	4.8E-05
FUG-20-ISOM	BenFree Unit	20-ISOM	-	-	-	-	-	-	-	-	-	-	-	-	3.8E-01	6.5E-03	2.8E-02	2.7E-02	4.5E-04	2.0E-03
FUG-21-SP VACUUM	Flasher/Vacuum Unit	21-VAC	ND	-	-	ND	-	-	ND	-	-	ND	-	-	-	-	-	ND	-	-
FUG-25-ROSE-2	ROSE Unit	25-ROSE	-	-	-	-	-	-	ND	-	-	ND	-	-	1.5E-02	6.9E-04	3.0E-03	ND	-	-
FUG-29-BLENDER/TK FARM	Light Oil Tankage	29-BLEND 08-TK-FA 03-ROSE	-	-	-	-	-	-	1.8E-02	1.6E-03	7.1E-03	6.1E-02	5.5E-03	2.4E-02	1.0E-02	9.0E-04	3.9E-03	1.9E-01	1.7E-02	7.5E-02
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	30-SRU-2 12-TGTU	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	31-SRU-3	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	33-DHDU	-	-	-	-	-	-	-	-	-	-	-	-	1.3E+00	1.1E-01	4.9E-01	-	-	-
FUG-34-HYDROCRACKER	WX Hydrocracker	34-MHU	-	-	-	4.0E-08	1.6E-09	6.8E-09	5.6E-02	2.2E-03	9.5E-03	8.8E-02	3.4E-03	1.5E-02	2.1E+00	8.3E-02	3.6E-01	5.2E-03	2.0E-04	8.8E-04
FUG-35-SAT GAS	Saturates Gas Plant	35-SAT-G 16-SKID	-	-	-	4.0E-08	1.8E-09	7.9E-09	5.6E-02	2.5E-03	1.1E-02	8.8E-02	4.0E-03	1.7E-02	2.1E+00	9.7E-02	4.2E-01	5.2E-03	2.3E-04	1.0E-03
FUG-36-RO	Reverse Osmosis	36-RO	-	-	-	4.0E-08	2.8E-11	1.2E-10	5.6E-02	3.9E-05	1.7E-04	8.8E-02	6.2E-05	2.7E-04	2.1E+00	1.5E-03	6.6E-03	5.2E-03	3.7E-06	1.6E-05
FUG-37-NP-UT	North Plant Utilities	37-NP-UT	-	-	-	4.0E-08	5.4E-10	2.3E-09	5.6E-02	7.4E-04	3.3E-03	8.8E-02	1.2E-03	5.1E-03	2.1E+00	2.9E-02	1.3E-01	5.2E-03	6.9E-05	3.0E-04
FUG-41-PBC	PBC Unit	41-PBC	-	-	-	-	-	-	-	-	-	-	-	-	1.3E+00	1.0E-02	4.4E-02	-	-	-
FUG-43-S ALKY	South Alky Unit (W-76)	43-W76	-	-	-	-	-	-	1.8E-02	1.1E-04	5.0E-04	6.1E-02	3.9E-04	1.7E-03	1.0E-02	6.3E-05	2.8E-04	1.9E-01	1.2E-03	5.3E-03
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	44-DHDU	-	-	-	-	-	-	-	-	-	-	-	-	1.3E+00	5.0E-02	2.2E-01	-	-	-
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	45-DHDU	-	-	-	-	-	-	-	-	-	-	-	-	1.3E+00	1.9E-02	8.4E-02	-	-	-
FUG-54-PRIMEG	Prime G Unit	54-PRIME	-	-	-	-	-	-	1.8E-02	8.2E-04	3.6E-03	6.1E-02	2.8E-03	1.2E-02	1.0E-02	4.5E-04	2.0E-03	1.9E-01	8.6E-03	3.8E-02
FUG-63-H2 PLANT-1	Hydrogen Plant	63-HYDRO																		
FUG-64-H2 PLANT-2	Hydrogen Plant	64-HYDRO																		
FUG-70-CCR	CCR Reformer (w/in battery limits)	70-CCR	-	-	-	-	-	-	1.8E-02	1.6E-03	6.8E-03	6.1E-02	5.3E-03	2.3E-02	1.0E-02	8.6E-04	3.8E-03	1.9E-01	1.6E-02	7.2E-02
FUG-73-SP UTIL	Utilities	73-SP-UT																		
FUG-80-WWTP CVS	Oil/Water Separator	80-WWTP	-	-	-	-	-	-	3.5E-01	1.1E-02	4.6E-02	ND	-	-	1.3E+00	3.8E-02	1.6E-01	8.6E-02	2.6E-03	1.1E-02
FUG-LPG	LPG Storage System	08-LPG-S																		
					2.2E-06			1.4E-07			0.12			0.19			3.09			0.31

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

FUGITIVE PIPING COMPONENT POTENTIAL TO EMIT HAPS

				n-Hexane			Nickel			o-Xylene		PI	enanthre	ne		p-Xylene			Pyrene	
				110-54-3			7440-02-0	1		95-47-6			85-01-8			106-42-3			129-00-0	
UNIT ID	PROCESS UNIT	LDAR Database	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy
FUG-02-SP CRUDE	South Division Crude Unit	02-CRUDE	9.6E-01	7.5E-02	3.3E-01	1.8E-03	1.4E-04	6.1E-04	2.4E-02	1.9E-03	8.2E-03	-	-	-	1.1E-01	8.6E-03	3.8E-02	9.2E-04	7.2E-05	3.2E-04
FUG-06-NHDU	Naphtha HDS Unit 06	06-NDU	5.7E+00	2.4E-01	1.0E+00	ND	-	-	7.1E-01	2.9E-02	1.3E-01	ND	-	-	7.2E-01	2.9E-02	1.3E-01	ND	-	-
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	07-AMINE	ND	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-07-SWS1	Sour Water Stripper	07-SWS	ND	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-08-TRUCK RK	Loading Racks	08-TRUCK	4.2E-01	8.3E-03	3.6E-02	-	-	-	1.8E+00	3.5E-02	1.6E-01	8.0E-04	1.6E-05	7.0E-05	5.0E-03	9.9E-05	4.3E-04	-	-	-
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	09-N-ALK	8.3E-02	5.3E-03	2.3E-02	-	-	-	1.2E-01	7.5E-03	3.3E-02	-	-	-	8.6E-02	5.5E-03	2.4E-02	-	-	-
FUG-10-FCC	FCC w/CVS	10-FCCU	4.2E-01	3.4E-02	1.5E-01	-	-	-	1.8E+00	1.4E-01	6.3E-01	8.0E-04	6.5E-05	2.8E-04	5.0E-03	4.0E-04	1.8E-03	-	-	-
FUG-13-NHDU	Naphtha HDS Unit 13	13-NHD	5.7E+00	3.2E-01	1.4E+00	ND	-	-	7.1E-01	3.9E-02	1.7E-01	ND	-	-	7.2E-01	4.0E-02	1.7E-01	ND	-	-
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	18-MEROX	4.2E-01	7.4E-04	3.2E-03	-	-	-	1.8E+00	3.2E-03	1.4E-02	8.0E-04	1.4E-06	6.2E-06	5.0E-03	8.8E-06	3.9E-05	-	-	-
FUG-19-NAPHTHA	Naptha Merox	19-NAPH	5.7E+00	1.2E-02	5.3E-02	ND	-	-	7.1E-01	1.5E-03	6.5E-03	ND	-	-	7.2E-01	1.5E-03	6.6E-03	ND	-	-
FUG-20-ISOM	BenFree Unit	20-ISOM	7.6E+00	1.3E-01	5.6E-01	-	-	-	8.1E-01	1.4E-02	6.0E-02	ND	-	-	4.4E-01	7.5E-03	3.3E-02	-	-	-
FUG-21-SP VACUUM	Flasher/Vacuum Unit	21-VAC	-	-	-	2.0E-05	4.8E-07	2.1E-06	-	-	-	1.8E-02	4.3E-04	1.9E-03	-	-	-	4.7E-03	1.1E-04	5.0E-04
FUG-25-ROSE-2	ROSE Unit	25-ROSE	7.1E-03	3.3E-04	1.4E-03	9.7E-03	4.5E-04	2.0E-03	3.0E-04	1.4E-05	6.1E-05	ND	-	-	7.9E-04	3.6E-05	1.6E-04	-	-	-
FUG-29-BLENDER/TK FARM	Light Oil Tankage	29-BLEND 08-TK-FA 03-ROSE	4.2E-01	3.8E-02	1.7E-01	-	-	-	1.8E+00	1.6E-01	7.0E-01	8.0E-04	7.2E-05	3.2E-04	5.0E-03	4.5E-04	2.0E-03	-	-	-
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	30-SRU-2 12-TGTU	ND	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	31-SRU-3	ND	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	33-DHDU	8.3E+00	7.2E-01	3.1E+00	-	-	-	7.6E-01	6.6E-02	2.9E-01	-	-	-	5.3E-01	4.6E-02	2.0E-01	-	-	-
FUG-34-HYDROCRACKER	WX Hydrocracker	34-MHU	5.7E+00	2.2E-01	9.7E-01	ND	-	-	7.1E-01	2.7E-02	1.2E-01	ND	-	-	7.2E-01	2.8E-02	1.2E-01	ND	-	-
FUG-35-SAT GAS	Saturates Gas Plant	35-SAT-G 16-SKID	5.7E+00	2.6E-01	1.1E+00	ND	-	-	7.1E-01	3.2E-02	1.4E-01	ND	-	-	7.2E-01	3.2E-02	1.4E-01	ND	-	-
FUG-36-RO	Reverse Osmosis	36-RO	5.7E+00	4.0E-03	1.8E-02	ND	-	-	7.1E-01	5.0E-04	2.2E-03	ND	-	-	7.2E-01	5.1E-04	2.2E-03	ND	-	-
FUG-37-NP-UT	North Plant Utilities	37-NP-UT	5.7E+00	7.7E-02	3.4E-01	ND	-	-	7.1E-01	9.5E-03	4.1E-02	ND	-	-	7.2E-01	9.6E-03	4.2E-02	ND	-	-
FUG-41-PBC	PBC Unit	41-PBC	2.0E+00	1.6E-02	7.0E-02	-	-	-	7.6E-01	6.2E-03	2.7E-02	-	-	-	5.9E-01	4.8E-03	2.1E-02	-	-	-
FUG-43-S ALKY	South Alky Unit (W-76)	43-W76	4.2E-01	2.7E-03	1.2E-02	-	-	-	1.8E+00	1.1E-02	5.0E-02	8.0E-04	5.1E-06	2.2E-05	5.0E-03	3.2E-05	1.4E-04	-	-	-
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	44-DHDU	8.3E+00	3.2E-01	1.4E+00	-	-	-	7.6E-01	3.0E-02	1.3E-01	-	-	-	5.3E-01	2.1E-02	9.0E-02	-	-	-
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	45-DHDU	8.3E+00	1.2E-01	5.5E-01	-	-	-	7.6E-01	1.1E-02	5.0E-02	-	-	-	5.3E-01	8.0E-03	3.5E-02	-	-	-
FUG-54-PRIMEG	Prime G Unit	54-PRIME	4.2E-01	1.9E-02	8.3E-02	-	-	-	1.8E+00	8.1E-02	3.6E-01	8.0E-04	3.6E-05	1.6E-04	5.0E-03	2.3E-04	9.9E-04	-	-	-
FUG-63-H2 PLANT-1	Hydrogen Plant	63-HYDRO																		
FUG-64-H2 PLANT-2	Hydrogen Plant	64-HYDRO																		
FUG-70-CCR	CCR Reformer (w/in battery limits)	70-CCR	4.2E-01	3.6E-02	1.6E-01	-	-	-	1.8E+00	1.5E-01	6.8E-01	8.0E-04	6.9E-05	3.0E-04	5.0E-03	4.3E-04	1.9E-03	-	-	-
FUG-73-SP UTIL	Utilities	73-SP-UT																		
FUG-80-WWTP CVS	Oil/Water Separator	80-WWTP	4.9E-01	1.5E-02	6.5E-02	5.4E-04	1.6E-05	7.2E-05	3.2E-01	9.6E-03	4.2E-02	7.3E-02	2.2E-03	9.5E-03	-	-	-	ND	-	-
FUG-LPG	LPG Storage System	08-LPG-S																		
					11.67			0.003			3.84			0.01			1.07			0.001

Notes:

a. HAP Speciation per API 4723A for each surrogate commodity.

FUGITIVE PIPING COMPONENT POTENTIAL TO EMIT HAPS

				Selenium			Toluene		Xylene	(mixed is	omers)
				7782-49-2	!		108-88-3			1330-20-7	,
UNIT ID	PROCESS UNIT	LDAR Database	wt%	lb/hr	tpy	wt%	lb/hr	tpy	wt%	lb/hr	tpy
FUG-02-SP CRUDE	South Division Crude Unit	02-CRUDE	6.9E-06	5.4E-07	2.4E-06	4.3E-01	3.4E-02	1.5E-01	4.8E-01	3.7E-02	1.6E-01
FUG-06-NHDU	Naphtha HDS Unit 06	06-NDU	-	-	-	3.0E+00	1.2E-01	5.4E-01	1.5E+00	6.2E-02	2.7E-01
FUG-07-N AMINE	Amine Unit-Treating/Regen. 2	07-AMINE	-	-	-	-	-	-	-	-	-
FUG-07-SWS1	Sour Water Stripper	07-SWS	-	-	-	-	-	-	-	-	-
FUG-08-TRUCK RK	Loading Racks	08-TRUCK	-	-	-	1.9E+00	3.8E-02	1.7E-01	7.0E+00	1.4E-01	6.1E-01
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	09-N-ALK	-	-	-	5.3E-01	3.3E-02	1.5E-01	1.4E-01	9.1E-03	4.0E-02
FUG-10-FCC	FCC w/CVS	10-FCCU	-	-	-	1.9E+00	1.6E-01	6.8E-01	7.0E+00	5.6E-01	2.5E+00
FUG-13-NHDU	Naphtha HDS Unit 13	13-NHD	-	-	-	3.0E+00	1.7E-01	7.3E-01	1.5E+00	8.4E-02	3.7E-01
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	18-MEROX	-	-	-	1.9E+00	3.4E-03	1.5E-02	7.0E+00	1.2E-02	5.4E-02
FUG-19-NAPHTHA	Naptha Merox	19-NAPH	-	-	-	3.0E+00	6.4E-03	2.8E-02	1.5E+00	3.2E-03	1.4E-02
FUG-20-ISOM	BenFree Unit	20-ISOM	-	-	-	7.4E-01	1.3E-02	5.5E-02	2.8E-02	4.8E-04	2.1E-03
FUG-21-SP VACUUM	Flasher/Vacuum Unit	21-VAC	-	-	-	-	-	-	-	-	-
FUG-25-ROSE-2	ROSE Unit	25-ROSE	ND	-	-	9.3E-04	4.3E-05	1.9E-04	1.1E-03	5.1E-05	2.2E-04
		29-BLEND									
FUG-29-BLENDER/TK FARM	Light Oil Tankage	08-TK-FA	1 -	-	-	1.9E+00	1.7E-01	7.6E-01	7.0E+00	6.3E-01	2.8E+00
		03-ROSE									
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	30-SRU-2				_	_				_
FUG-30-3KU2/TGTU	SRU2/SWS W/CVS	12-TGTU	1 -	-	-	-	-	-	-	-	-
FUG-31-SRU3/TGTU3/TGI3	SRU3 Unit	31-SRU-3	-	-	-	-	-	-	-	-	-
FUG-33-DIST HDU	Diesel HDS Unit w/CVS	33-DHDU	-	-	-	1.2E+00	1.0E-01	4.6E-01	4.6E-01	3.9E-02	1.7E-01
FUG-34-HYDROCRACKER	WX Hydrocracker	34-MHU	-	-	-	3.0E+00	1.2E-01	5.1E-01	1.5E+00	5.9E-02	2.6E-01
FUG-35-SAT GAS	Saturates Gas Plant	35-SAT-G 16-SKID	-	-	-	3.0E+00	1.4E-01	6.0E-01	1.5E+00	6.8E-02	3.0E-01
FUG-36-RO	Reverse Osmosis	36-RO	-	-	-	3.0E+00	2.1E-03	9.3E-03	1.5E+00	1.1E-03	4.7E-03
FUG-37-NP-UT	North Plant Utilities	37-NP-UT	-	-	-	3.0E+00	4.0E-02	1.8E-01	1.5E+00	2.0E-02	8.9E-02
FUG-41-PBC	PBC Unit	41-PBC	-	-	-	1.9E+00	1.6E-02	6.8E-02	-	-	-
FUG-43-S ALKY	South Alky Unit (W-76)	43-W76	-	-	-	1.9E+00	1.2E-02	5.4E-02	7.0E+00	4.4E-02	1.9E-01
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	44-DHDU	-	-	-	1.2E+00	4.7E-02	2.1E-01	4.6E-01	1.8E-02	7.7E-02
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	45-DHDU	-	-	-	1.2E+00	1.8E-02	8.0E-02	4.6E-01	6.9E-03	3.0E-02
FUG-54-PRIMEG	Prime G Unit	54-PRIME	-	-	-	1.9E+00	8.8E-02	3.8E-01	7.0E+00	3.2E-01	1.4E+00
FUG-63-H2 PLANT-1	Hydrogen Plant	63-HYDRO									
FUG-64-H2 PLANT-2	Hydrogen Plant	64-HYDRO									
FUG-70-CCR	CCR Reformer (w/in battery limits)	70-CCR	-	-	-	1.9E+00	1.7E-01	7.3E-01	7.0E+00	6.0E-01	2.6E+00
FUG-73-SP UTIL	Utilities	73-SP-UT									
FUG-80-WWTP CVS	Oil/Water Separator	80-WWTP	ND	-	-	5.0E-01	1.5E-02	6.5E-02	4.1E-01	1.2E-02	5.4E-02
FUG-LPG	LPG Storage System	08-LPG-S									
		-			2.4E-06			6.62			11.95

notes

a. HAP Speciation per API 4723A for each surrogate commodity.

FIXED ROOF TANKS POTENTIAL TO EMIT

Tank ID		Stored Commodity	Most Volatile Category of Allowable Liquids to be	Regulatory Vapor Pressure Limitation (MACT CC, NSPS K, Ka, Kb)	MACT CC Group	Maximum Hourly Throughput	Net Throughput	H2S in Liquid
	CHEMICAL NAME FOR VOC LOSSES	CHEMICAL NAME FOR HAPS LOSSES SPECIATION	Stored			Q _H	Q	H2S _{liq}
	CALCULATION	SIECIATION				bbl/hr	bbl/yr	ppm
								API 4723A
T-0040	Spent Caustic	Caustic Treating - Spent Caustic	Low VP	No limit (Pre-NSPS, HAPs<4wt%)	Group 2	240	28,000	
T-0040	Spent Caustic	Caustic Treating - Spent Caustic	Low VP	No limit (NSPS K/Ka, HAPs<4wt%, V<40,000gal)	Group 2	240	28,000	-
T-0049	Slop Oil	Various Units - Slop Oil	Moderate VP	TVP < 1.9 psia (MACT CC, HAPs>4wt%, V>20,000 gal)	Group 2	300	449,590	3,200
T-0055	Stripped Sour Water	Caustic Treating - Spent Caustic	Low VP	TVP < 1.5 psia (NSPS K/Ka, HAPs<4wt%, V>40,000gal)	Group 2	420	1,088,772	- 3,200
T-0059	Light Cycle Oil (LCO)	Fluid Catalytic Cracker - Light Cat Gas Oil	Low VP	No limit (Pre-NSPS, HAPs<4wt%)	Group 2	120	47,578	2.19
T-0053	Light Cycle Oil (LCO)	Fluid Catalytic Cracker - Light Cat Gas Oil	Low VP	No limit (Pre-NSPS, HAPS<4wt%)	Group 2	180	1,011,690	2.19
T-0063	Heavy Cycle Oil (HCO)	Fluid Catalytic Cracker - Light Cat Gas Oil	Low VP	No limit (Pre-NSPS, HAPS<4wt%)	Group 2	600	430.537	8.50
T-0065	Heavy Cycle Oil (HCO)	Fluid Catalytic Cracker - Heavy Cat Gas Oil	Low VP	TVP < 0.75 psia (NSPS Kb, HAPs<4wt%, V>40,000gal)	Group 2	600	430,537	8.50
T-0075	Heavy Cycle Oil (HCO)	Fluid Catalytic Cracker - Heavy Cat Gas Oil	Low VP	TVP < 0.75 psia (NSPS Kb, HAPs<4wt%, V>40,000gal)	Group 2	600	430,537	8.50
T-0073	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	Low VP	TVP < 0.75 psia (NSPS Kb, HAPs<4wt%, V>40,000gal)	Group 2	2.400	5,000,000	500
T-0082	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	Low VP	TVP < 0.75 psia (NSPS Kb, HAPs<4wt%, V>40,000gal)	Group 2	2,400	6,000,000	500
T-0110	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	Low VP	No limit (Pre-NSPS, HAPs<4wt%)	Group 2	600	5,256,000	500
T-0400	Gas Oil	Vacuum Distillation - Light Vacuum Gas Oil	Low VP	TVP < 1.5 psia (NSPS K/Ka, HAPs<4wt%, V>40,000gal)	Group 2	2,400	7,300,000	1.34
T-0410	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	Low VP	TVP < 1.5 psia (NSPS K/Ka, HAPs<4wt%, V>40,000gal)	Group 2	600	5,256,000	500
T-0419	No. 2 Fuel Oil (Diesel)	Distillate Blending - Diesel Fuel	Low VP	TVP < 0.5 psia (MACT CC, HAPs>4wt%, V>40,000 gal)	Group 2	240	3,650,000	3.54
T-0420	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	Low VP	No limit (Pre-NSPS, HAPs<4wt%)	Group 2	600	97.022	500
T-0420	Light Cycle Oil (LCO)	Fluid Catalytic Cracker - Light Cat Gas Oil	Low VP	No limit (Pre-NSPS, HAPS<4wt%)	Group 2	600	1,002,055	2.19
T-0423	Light Cycle Oil (LCO)	Fluid Catalytic Cracker - Light Cat Gas Oil	Low VP	No limit (Pre-NSPS, HAPS<4wt%)	Group 2	600	1,011,690	2.19
T-0431	Fuel Oil	Fluid Catalytic Cracker - Light Cat Gas Oil	Low VP	No limit (Pre-NSPS, HAPs<4wt%)	Group 2	1,600	394,200	2.19
T-0431	Fuel Oil	Fluid Catalytic Cracker - Light Cat Gas Oil	Low VP	No limit (Pre-NSPS, HAPS<4wt%)	Group 2	1,600	461,214	2.19
T-0433	Straight Run Gas Oil	Vacuum Distillation - Light Vacuum Gas Oil	Low VP	No limit (Pre-NSPS, HAPs<4wt%)	Group 2	600	4,125,000	1.34
T-0433	Straight Run Diesel	Distillate Blending - Diesel Fuel	Low VP	TVP < 0.75 psia (MACT CC, HAPs>4wt%, V>40,000 gal)	Group 2	2,400	7,500,000	3.54
T-0434	Straight Run Gas Oil	Vacuum Distillation - Light Vacuum Gas Oil	Low VP	TVP < 1.5 psia (MSPS K/Ka, HAPs<4wt%, V>40,000 gal)	Group 2	600	4,125,000	1.34
T-0438	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	Low VP	TVP < 0.75 psia (NSPS Kb, HAPs<4wt%, V>40,000gal)	Group 2	600	3,360,000	500
T-0814	No. 2 Fuel Oil (Diesel)	Distillate Blending - Diesel Fuel	Low VP	TVP < 0.5 psia (MACT CC, HAPs>4wt%, V>40,000gal)	Group 2	3,600	26,097,500	3.54
T-0813	No. 2 Fuel Oil (Diesel)	Distillate Blending - Diesel Fuel	Low VP	TVP < 0.75 psia (MACT CC, HAPs>4wt%, V>40,000 gal)	Group 2	660	15,695,000	3.54
T-1227	Asphalt/Pitch	Asphalt Plant - (Feed) Pitch	Low VP	TVP < 0.75 psia (WACT CC, TIATS 24WC/8, V > 40,000 gal)	Group 2	1,200	876.000	500

			TANK	CHARACTERISTIC	:S					TANK PAINT				СН	EMICAL PRO	PERTIES		
Tank ID	Tank Type	Tank Insulated	Tank Construction	Tank Diameter	Tank Shell Height	Tank Effective Diameter (HFR ONLY)	Effective Tank Height (HFR ONLY)	Shell Capacity	Tank Shell Paint	Tank Roof Paint		Roof Paint Condition	Product Category	Liquid Molecular Weight	Vapor Molecular Weight	Density of the Liquid	Stock Vapor Density (P _{VA})	Stock Vapor Density (TVP Limit)
				D	H _s	D _E	H _E							ML	M _v	W _L	w _v	
				ft	ft	ft	ft	gallons						lb/lbmole	lb/lbmole	lb/gal	lb/ft3	lb/ft ³
	CR DM HFR	YES-ALL-CTE YES-ALL-CYCLE YES-SHELL NO	Riveted-Bolted Welded	HFR: diam of vertical cross-section	HFR: length	AP-42 Ch. 7.1 Eq. 1-14	AP-42 Ch. 7.1 Eq. 1-15				New Average Aged	New Average Aged	Crude Oil Petroleum Stock Organic Liquids				AP-42, Ch. 7.1, Eq. 1-22	AP-42, Ch. 7.1, Eq. 1-22
T-0040	CR	NO	-	9.0	72.0	-	-	34,440	White	White	Aged	Aged	Petroleum Stock	188	130	7.10	1.9E-04	-
T-0041	CR	NO	-	9.0	72.0	-	-	34,440	White	White	Aged	Aged	Petroleum Stock	188	130	7.10	1.9E-04	_
T-0049	HFR	NO	-	11.0	36.0	22.5	8.6	25,620	White	White	Aged	Aged	Petroleum Stock	188	130	7.10	3.6E-02	
T-0055	CR	NO	-	45.0	36.0	-	-	428,400	White	White	Average	Average	Petroleum Stock	188	130	7.10	8.2E-04	
T-0059	CR	NO	-	35.0	30.0	-	-	215,880	Black	Black	Average	Average	Petroleum Stock	162	130	7.00	3.0E-04	
T-0061	CR	NO	-	50.0	30.0	-	-	440,580	Black	Black	Average	Average	Petroleum Stock	162	130	7.00	3.0E-04	
T-0063	CR	NO	-	51.0	30.0	-	-	458,220	Black	Black	Average	Average	Petroleum Stock	188	130	7.10	2.6E-04	
T-0065	CR	NO	-	50.0	30.0	-	-	440,580	Black	Black	Average	Average	Petroleum Stock	188	130	7.10	2.7E-04	_
T-0075	CR	NO	-	65.0	32.0	-	-	794,220	Black	Black	Aged	Aged	Petroleum Stock	188	130	7.10	2.3E-04	
T-0081	CR	YES-ALL-CTE	-	108.5	40.0	-	-	2,766,540	Aluminum - Specular	Aluminum - Specular	Average	Average	Asphalt/Pitch	1,000	84	-	4.1E-05	
T-0082	CR	YES-ALL-CTE	-	140.0	40.0	-	-	4,605,720	Aluminum - Specular	Aluminum - Specular	Average	Average	Asphalt/Pitch	1,000	84	-	1.3E-05	_
T-0110	CR	YES-ALL-CTE	-	108.0	35.0	-	-	2,398,200	Aluminum - Specular	Aluminum - Specular	Average	Average	Asphalt/Pitch	1,000	84	-	4.6E-04	
T-0400	CR	NO	-	120.0	48.0	-	-	4,060,560	Black	Black	Aged	Aged	Petroleum Stock	188	130	7.10	1.7E-03	
T-0410	CR	YES-ALL-CTE	-	79.0	40.0	-	-	1,466,640	Aluminum - Specular	Aluminum - Specular	Average	Average	Asphalt/Pitch	1,000	84	- 7.40	3.4E-04	
T-0419	CR	NO	-	53.0	28.0	-	-	462,000	White	White	Average	Average	Petroleum Stock	188	130	7.10	2.4E-04	
T-0420	CR	YES-ALL-CTE	-	50.0	30.0	-	-	440,580	Aluminum - Specular	Aluminum - Specular	Average	Average	Asphalt/Pitch	1,000	84	- 7.00	2.5E-06	
T-0422	CR CR	NO NO	-	50.0	30.0	-	-	440,580	White	White	New	New	Petroleum Stock	162 162	130 130	7.00	6.3E-04	
T-0423	-	NO NEC ALL CTE		50.0	30.0			440,580	White	White	New	New	Petroleum Stock			7.00	7.5E-04	
T-0431	CR	YES-ALL-CTE	-	109.0	32.0	-	-	2,233,560	Aluminum - Specular	Aluminum - Specular	Average	Average	Petroleum Stock	188	130	7.10	2.9E-03	
T-0432	CR	YES-ALL-CTE	-	109.0	32.0	-	-	2,233,560	Aluminum - Specular	Aluminum - Specular	Average	Average	Petroleum Stock	188	130	7.10	3.5E-03	_
T-0433	CR	NO	-	117.0	42.0	-	-	3,377,640	Rust - Red Iron Oxide	Rust - Red Iron Oxide	Aged	Aged	Petroleum Stock	188	130	7.10	1.3E-03	
T-0434	CR	NO	-	117.0	42.0	-	-	3,377,640	White	White	New	New	Petroleum Stock	188	130	7.10	8.0E-03	-
T-0438	CR	NO VEC ALL CTE	-	90.0	48.0	-	-	2,283,960	Black	Black	Aged	Aged	Petroleum Stock	188	130	7.10	6.8E-04	
T-0814	CR	YES-ALL-CTE	-	50.0	32.0	-	-	469,980	Aluminum - Specular	Aluminum - Specular	Average	Average	Asphalt/Pitch	1,000	84	- 7.40	2.9E-03	
T-0815	CR	NO NO	-	116.0	43.0	-	-	3,399,060	White	White	New	New	Petroleum Stock	188	130	7.10	1.8E-04	
T-0838	CR	NO	-	74.0	40.0	-	-	1,286,880	White	White	New	New	Petroleum Stock	188	130	7.10	2.7E-04	
T-1227	CR	YES-ALL-CTE	-	77.0	40.0	-	-	1,393,140	Aluminum - Specular	Aluminum - Specular	Average	Average	Asphalt/Pitch	1,000	84	-	3.9E-03	6.9E-03

		ME	TEOROLOGICAL DA	ATA								TANK TEMPERATU	JRE VARIABLES				
Tank ID	Average Wind Speed	Atmosph. Pressure	Daily Maximum Ambient Temp.	Daily Minimum Ambient Temp.	Daily Total Solar Insulation Factor	Tank Shell Surface Solar	Tank Roof Surface Solar Absorptance	Daily Average Temp.	Liquid Bulk Temp. based on Ambient Met Data	Monthly Liquid Bulk Temperature Monitored	Liquid Bulk Temp.	Daily Average Liquid Surface Temp.	Average Vapor Temp.	Daily Temp. Range	Avg. Daily Vapor Temp. Range	Daily Maximum Liquid Surface Temp.	Daily Minimum Liquid Surfa Temp.
	v	P _A	T _{AX}	T _{AN}	ı	αs	α_{R}	T _{AA}	T _B (AP-42)	T _B (Monitored)	T _B	T _{LA}	T _v	ΔΤΑ	ΔT _V	T _{LX}	T _{LN}
	mph	psia	°F	°F	Btu/ft^2d	unitless	unitless	°R	°R	°R	°R	°R	°R	°R	°R	°R	°R
						AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Eq. 1-30	AP-42, Ch. 7.1, Eq. 1-31	Ops Data	Max. Monitored vs AP- 42 Estimate	AP-42, Ch. 7.1, T _B Full-Insul Eq. 1-29 Shell-Insul Eq. 1-27 Non-Insul	AP-42, Ch. 7.1, T _B Full-Insul Eq. 1-34 Shell-Insul Eq. 1-32 Non-Insul	AP-42, Ch. 7.1, Eq. 1-11	AP-42, Ch. 7-1, Eq. 1-6 Non-Insul Eq. 1-8 Shell-Insul $\Delta T_{\nu} = 0$ Full-Insul and Constant Temp Eq. 8-1 Full-Insul and Cycle Temp	AP-42, Chp 7.1, Fig 7.1-17 For Full-Insul T _{LX} = T _{BX}	AP-42, Chp 7.1, Fig 7.1-17 For Full-Insul T _{LN} = T _{BN}
T-0040	9.0	13.1	77.9	50.0	1,711.9	0.34	0.34	523.6	525.4	524.57	525.4	526.4	527.4	27.9	34.2	535.0	517.9
T-0040	9.0	13.1	77.9	50.0	1,711.9	0.34	0.34	523.6	525.4	524.57	525.4	526.4	527.4	27.9	34.2	535.0	517.
T-0041	9.0	13.1	77.9	50.0	1,711.9	0.34	0.34	523.6	525.4	524.57	525.4	526.6	527.9	27.9	33.6	535.0	518.
T-0045	9.0	13.1	77.9	50.0	1,711.9	0.34	0.25	523.6	524.9	610.38	610.4	578.3	546.3	27.9	29.2	585.6	571.
T-0059	9.0	13.1	77.9	50.0	1,711.9	0.23	0.23	523.6	528.6	529.54	529.5	534.3	539.0	27.9	50.2	546.8	521.
T-0053	9.0	13.1	77.9	50.0	1,711.9	0.97	0.97	523.6	528.6	529.54	529.5	534.7	540.0	27.9	50.7	547.4	522.
T-0063	9.0	13.1	77.9	50.0	1,711.9	0.97	0.97	523.6	528.6	534.88	534.9	538.1	541.3	27.9	50.7	550.8	525.4
T-0065	9.0	13.1	77.9	50.0	1,711.9	0.97	0.97	523.6	528.6	536.56	536.6	539.1	541.7	27.9	50.7	551.8	526.
T-0075	9.0	13.1	77.9	50.0	1,711.9	0.97	0.97	523.6	528.6	459.70	528.6	534.4	540.2	27.9	50.9	547.2	521.
T-0081	9.0	13.1	77.9	50.0	1,711.9	0.44	0.44	523.6	525.9	668.03	668.0	668.0	668.0	27.9	-	789.2	769.
T-0082	9.0	13.1	77.9	50.0	1,711.9	0.44	0.44	523.6	525.9	633.37	633.4	633.4	633.4	27.9	-	780.5	731.
T-0110	9.0	13.1	77.9	50.0	1,711.9	0.44	0.44	523.6	525.9	749.02	749.0	749.0	749.0	27.9	-	776.4	756.
T-0400	9.0	13.1	77.9	50.0	1,711.9	0.97	0.97	523.6	528.6	616.00	616.0	590.9	565.9	27.9	51.2	603.7	578.
T-0410	9.0	13.1	77.9	50.0	1,711.9	0.44	0.44	523.6	525.9	738.22	738.2	738.2	738.2	27.9	-	771.5	748.0
T-0419	9.0	13.1	77.9	50.0	1,711.9	0.25	0.25	523.6	524.9	539.24	539.2	535.4	531.6	27.9	28.4	542.5	528.
T-0420	9.0	13.1	77.9	50.0	1,711.9	0.44	0.44	523.6	525.9	591.10	591.1	591.1	591.1	27.9	-	799.0	589.
T-0422	9.0	13.1	77.9	50.0	1,711.9	0.17	0.17	523.6	524.5	579.06	579.1	559.5	540.0	27.9	26.2	566.1	553.
T-0423	9.0	13.1	77.9	50.0	1,711.9	0.17	0.17	523.6	524.5	589.55	589.6	566.1	542.6	27.9	26.2	572.6	559.
T-0431	9.0	13.1	77.9	50.0	1,711.9	0.44	0.44	523.6	525.9	637.50	637.5	637.5	637.5	27.9	-	725.9	620.
T-0432	9.0	13.1	77.9	50.0	1,711.9	0.44	0.44	523.6	525.9	646.24	646.2	646.2	646.2	27.9	-	718.4	643.
T-0433	9.0	13.1	77.9	50.0	1,711.9	0.50	0.50	523.6	526.2	604.85	604.8	580.4	556.0	27.9	36.0	589.4	571.
T-0434	9.0	13.1	77.9	50.0	1,711.9	0.17	0.17	523.6	524.5	459.70	524.5	525.6	526.7	27.9	25.2	531.9	519.
T-0438	9.0	13.1	77.9	50.0	1,711.9	0.97	0.97	523.6	528.6	567.35	567.3	558.7	550.1	27.9	50.8	571.4	546.
T-0814	9.0	13.1	77.9	50.0	1,711.9	0.44	0.44	523.6	525.9	829.95	830.0	830.0	830.0	27.9	-	866.6	832.
T-0815	9.0	13.1	77.9	50.0	1,711.9	0.17	0.17	523.6	524.5	459.70	524.5	525.6	526.7	27.9	25.2	531.9	519.
T-0838	9.0	13.1	77.9	50.0	1,711.9	0.17	0.17	523.6	524.5	544.82	544.8	538.3	531.8	27.9	26.0	544.8	531.
T-1227	9.0	13.1	77.9	50.0	1,711.9	0.44	0.44	523.6	525.9	845.04	845.0	845.0	845.0	27.9	-	909.4	839.9

		TANK PRESSURE	VARIABLES		BREAT	HER VENT SE	TTINGS				STANDIN	IG LOSSES			
Tank ID	True Vapor Pressure at Daily Avg Temp. (T _{LA})	True Vapor Pressure at Daily Max. Liq. Surface Temp (T _{LX})	True Vapor Pressure at Daily Min. Liq. Surface Temp (T _{LN})	Avg. Daily Vapor Pressure Range	Breather Vent Pressure Setting	Breather Vent Vacuum Setting	Breather Vent Pressure Setting Range	Avg. Liquid Height	Tank Roof Height	Roof Outage	Vapor Space Outage	Volume of the Vapor Space	Vapor Space Expansion Factor	Vented Vapor Saturation Factor	Standing Loss
	P _{VA}	P _{VX}	P _{VN}	ΔP_{V}	P _{BP}	P _{BV}	ΔP_B	HL	H _R	H _{RO}	H _{vo}	v _v	K _E	Ks	L _S
	psia	psia	psia	psia	psig	psig	psia	ft	ft	ft	ft	ft^3	unitless	unitless	lb/yr
		AP-42, Ch. 7.1, Eq. 1-25 Petroleum Eq. 1-26 Org Liq Trumbore Asphalts		AP-42, Ch. 7.1, Eq. 1-9 §7.1.3.8.4	AP-42 Ch. 7.1, Note to Eq. 1-10	AP-42 Ch. 7.1, Note to Eq. 1-10	AP-42, Ch. 7.1, Eq. 1-10	AP-42, Ch. 7.1 Eq. 1-16	AP-42, Ch. 7.1, Eq. 1-18 for CR, Eq. 1-20 for DR	AP-42, Ch. 7.1, Eq. 1-17 for CR, Eq. 1-18 for DR	AP-42, Ch. 7.1 Eq. 1-16	AP-42, Ch. 7.1, Eq. 1-3	AP-42, Ch. 7.1 Eq. 1-5	AP-42, Ch. 7.1 Eq. 1-21	AP-42, Ch. 7.1, Eq. 1-2
T-0040	0.008	0.011	0.006	0.004	0.03	(0.03)	0.1	36.0	0.28	0.09	36.1	2,296	0.061	1.0	9.3
T-0040	0.008	0.011	0.006	0.004	0.03	(0.03)	0.1	36.0	0.28	0.09	36.1	2,296	0.061	1.0	9.3
T-0041	1.557	1.876	1.285	0.004	0.03	(0.03)	0.1	18.0	0.28	0.09	4.3	1,711	0.001	0.7	1,809.2
T-0049	0.037	0.045	0.030	0.392	0.03	(0.03)	0.1	18.0	1.41	0.47	18.5	29,373	0.110	1.0	397.0
T-0059	0.013	0.019	0.009	0.014	0.03	(0.03)	0.1	15.0	1.09	0.36	15.4	14,782	0.090	1.0	142.5
T-0055	0.013	0.019	0.009	0.011	0.03	(0.03)	0.1	15.0	1.56	0.52	15.5	30,475	0.091	1.0	300.3
T-0063	0.012	0.017	0.008	0.009	0.03	(0.03)	0.1	15.0	1.59	0.53	15.5	31,728	0.090	1.0	270.5
T-0065	0.012	0.018	0.008	0.010	0.03	(0.03)	0.1	15.0	1.56	0.52	15.5	30,475	0.090	1.0	267.2
T-0075	0.010	0.015	0.007	0.008	0.03	(0.03)	0.1	16.0	2.03	0.68	16.7	55,340	0.091	1.0	426.6
T-0081	0.004	0.122	0.075	-	0.03	(0.03)	0.1	20.0	3.39	1.13	21.1	195.368	-	1.0	-
T-0082	0.001	0.099	0.026	-	0.03	(0.03)	0.1	20.0	4.38	1.46	21.5	330,325	-	1.0	-
T-0110	0.044	0.089	0.053	-	0.03	(0.03)	0.1	17.5	3.38	1.13	18.6	170,621	-	1.0	-
T-0400	0.080	0.113	0.055	0.058	0.03	(0.03)	0.1	24.0	3.75	1.25	25.3	285,571	0.086	0.9	13,871.3
T-0410	0.032	0.079	0.043	-	0.03	(0.03)	0.1	20.0	2.47	0.82	20.8	102,067	-	1.0	-
T-0419	0.011	0.013	0.009	0.005	0.03	(0.03)	0.1	14.0	1.66	0.55	14.6	32,105	0.049	1.0	138.8
T-0420	0.000	0.153	0.000	-	0.03	(0.03)	0.1	15.0	1.56	0.52	15.5	30,475	-	1.0	-
T-0422	0.028	0.034	0.023	0.011	0.03	(0.03)	0.1	15.0	1.56	0.52	15.5	30,475	0.043	1.0	293.9
T-0423	0.034	0.040	0.028	0.012	0.03	(0.03)	0.1	15.0	1.56	0.52	15.5	30,475	0.043	1.0	347.0
T-0431	0.154	0.845	0.105	-	0.03	(0.03)	0.1	16.0	3.41	1.14	17.1	159,896	-	0.9	-
T-0432	0.186	0.743	0.176	-	0.03	(0.03)	0.1	16.0	3.41	1.14	17.1	159,896	-	0.9	-
T-0433	0.059	0.076	0.045	0.031	0.03	(0.03)	0.1	21.0	3.66	1.22	22.2	238,881	0.060	0.9	6,261.8
T-0434	0.348	0.410	0.294	0.116	0.03	(0.03)	0.1	21.0	3.66	1.22	22.2	238,881	0.052	0.7	25,871.3
T-0438	0.031	0.045	0.021	0.025	0.03	(0.03)	0.1	24.0	2.81	0.94	24.9	158,646	0.088	1.0	3,333.4
T-0814	0.305	0.643	0.322	-	0.03	(0.03)	0.1	16.0	1.56	0.52	16.5	32,439	-	0.8	-
T-0815	0.008	0.010	0.006	0.003	0.03	(0.03)	0.1	21.5	3.63	1.21	22.7	239,989	0.044	1.0	685.0
T-0838	0.012	0.014	0.010	0.005	0.03	(0.03)	0.1	20.0	2.31	0.77	20.8	89,332	0.044	1.0	378.5
T-1227	0.418	0.750	0.376	-	0.03	(0.03)	0.1	20.0	2.41	0.80	20.8	96,868	-	0.7	-

					WOI	RKING LOSSI	ESS													
Tank ID	Sum of Increases in Liquid Level	Max. Hourly Working Loss Throughput	Net Working Loss Throughput	Maximum Liquid Height	Minimum Liquid Height	Turnovers per Year	Working Losss Turnover (Saturation) Factor	Working Loss Product Factor	Vent Setting Correction Factor	Working Loss Max. Hourly	Working Loss	CONTROL EFFICIENCY	MAXIMUM HOURLY FIXED ROOF LOSSES	TOTAL FIXED ROOF TANKS LOSSES	VC Emis:		H2 Emiss		HA Emiss	
	ΣH ^ď		$\mathbf{v}_{\mathbf{q}}$	H _{LX}	H _{LN}	N	K _N	K _P	K _B		L _w			LT						
	ft/yr	ft^3/hr	ft^3/yr	ft	ft	unitless	unitless	unitless	unitless	lb/hr	lb/yr		lb/hr	lb/yr	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
	AP-42, Ch. 7.1 Eq. 1-37	AP-42, Ch. 7.1 Eq. 1-38/1-39	AP-42, Ch. 7.1 Eq. 1-38/1-39	AP-42, Ch. 7.1 Eq. 1-37 Notes	AP-42, Ch. 7.1 Eq. 1-37 Notes	AP-42, Ch. 7.1 Eq. 1-36	AP-42, Ch. 7.1 Eq. 1-35 Notes	AP-42, Ch. 7.1 Eq. 1-35 Notes	AP-42, Ch. 7.1 Eq. 1-41 Eq. 1-40	AP-42, Ch. 7.1 Eq. 1-35	AP-42, Ch. 7.1 Eq. 1-35		AP-42, Ch. 7.1 Eq. 1-35 @P _{VX} , K _N =1 with control	AP-42, Ch. 7.1 Eq. 1-1	AP- Ch. David T Trumbo	7.1	Raoult	s Law	Raoult	s Law
T-0040	2,470.9	1,348	157,192	71.0	1.0	35.3	1.0	1.0	1.0	0.33	29.1		0.33	38.5	0.33	0.02	-	-	4.08E-04	2.39E-05
T-0041	2,470.9	1,348	157,192	71.0	1.0	35.3	1.0	1.0	1.0	0.33	29.1	-	0.33	38.5	0.33	0.02	-	- 1	4.08E-04	2.39E-05
T-0049	6,373.7	1,684	2,524,001	8.6	-	737.8	0.2	1.0	1.0	73.44	18,702.1	95%	3.67	1,025.6	3.67	0.51	3.88E-01	4.45E-02	0.02	0.002
T-0055	3,843.2	2,358	6,112,364	35.0	1.0	113.0	0.4	1.0	1.0	78.43	2,159.4	-	78.43	2,556.4	78.43	1.28	-	-	0.10	0.002
T-0059	277.6	674	267,104	29.0	1.0	9.9	1.0	1.0	1.0	0.29	79.0	-	0.29	221.5	0.29	0.11	1.82E-05	5.66E-06	7.12E-05	2.70E-05
T-0061	2,892.6	1,011	5,679,630	29.0	1.0	103.3	0.5	1.0	1.0	0.45	778.4	-	0.45	1,078.7	0.45	0.54	2.78E-05	2.76E-05	1.09E-04	1.31E-04
T-0063	1,183.2	3,368	2,417,033	29.0	1.0	42.3	0.9	1.0	1.0	1.29	553.0	-	1.29	823.5	1.29	0.41	3.61E-04	9.49E-05	3.06E-05	9.79E-06
T-0065	1,231.0	3,368	2,417,033	29.0	1.0	44.0	0.8	1.0	1.0	56.50	552.3	-	56.50	819.5	56.50	0.41	1.59E-02	9.44E-05	0.001	9.74E-06
T-0075	728.4	3,368	2,417,033	31.0	1.0	24.3	1.0	1.0	1.0	56.65	563.9	-	56.65	990.6	56.65	0.50	1.59E-02	1.14E-04	0.001	1.18E-05
T-0081	3,035.9	13,474	28,070,000	39.0	1.0	79.9	0.5	1.0	1.0	118.41	626.0	-	118.41	626.0	118.41	0.31	5.92E-02	1.56E-04	4.73	0.01
T-0082	2,188.2	13,474	33,684,000	39.0	1.0	57.6	0.7	1.0	1.0	124.89	293.3	-	124.89	293.3	124.89	0.15	6.24E-02	7.33E-05	4.98	0.01
T-0110	3,221.0	3,368	29,507,184	34.0	1.0	97.6	0.5	1.0	1.0	3.13	6,375.8	-	3.13	6,375.8	3.13	3.19	1.57E-03	1.59E-03	0.12	0.13
T-0400	3,623.6	13,474	40,982,200	47.0	1.0	78.8	0.5	1.0	1.0	432.68	38,228.3	-	432.68	52,099.5	432.68	26.05	1.91E-02	9.46E-04	0.87	0.05
T-0410	6,019.8	3,368	29,507,184	39.0	1.0	158.4	0.4	1.0	1.0	53.58	3,598.8	-	53.58	3,598.8	53.58	1.80	2.68E-02	9.00E-04	2.14	0.07
T-0419	9,288.0	1,347	20,491,100	27.0	1.0	357.2	0.3	1.0	1.0	15.35	1,256.3	-	15.35	1,395.1	15.35	0.70	1.79E-03	6.69E-05	0.01	4.09E-04
T-0420	277.4	3,368	544,684	29.0	1.0	9.9	1.0	1.0	1.0	6.83	1.4	-	6.83	1.4	6.83	0.00	3.42E-03	3.38E-07	0.27	2.70E-05
T-0422	2,865.1	3,368	5,625,538	29.0	1.0	102.3	0.5	1.0	1.0	2.55	1,625.9	-	2.55	1,919.8	2.55	0.96	1.59E-04	4.91E-05	6.20E-04	2.34E-04
T-0423	2,892.6	3,368	5,679,630	29.0	1.0	103.3	0.5	1.0	1.0	3.04	1,953.1	-	3.04	2,300.1	3.04	1.15	1.89E-04	5.88E-05	7.39E-04	2.80E-04
T-0431	237.2	8,982	2,213,039	31.0	1.0	7.9	1.0	1.0	1.0	144.21	6,477.1	-	144.21	6,477.1	144.21	3.24	1.04E-02	1.92E-04	0.04	9.15E-04
T-0432	277.5	8,982	2,589,255	31.0	1.0	9.2 53.8	0.7	1.0	1.0	125.04	9,030.0	-	125.04	9,030.0	125.04	4.51 13.91	9.04E-03	2.68E-04	0.04	0.001
T-0433 T-0434	2,153.9 3,916.3	3,368 13,474	23,157,750 42,105,000	41.0 41.0	1.0	97.9	0.7	1.0	1.0	5.60 232.44	21,563.2 159,403.1	-	5.60 232.44	27,825.0 185,274.4	5.60 232.44	92.64	2.48E-04 2.72E-02	5.05E-04 8.89E-03	0.01	0.03
T-0434	-	3,368	23,157,750	47.0	1.0	79.1	0.5	1.0	1.0	111.27	8,576.0	-	111.27	11,909.3	111.27	5.95	4.92E-03	2.16E-04	0.14	0.05
T-0438	3,640.2 9,606.9	3,368	18,863,040	31.0	1.0	320.2	0.5	1.0	1.0	23.83	14,133.5	-	23.83	11,909.3	23.83	7.07	4.92E-03 1.19E-02	3.53E-03	0.22	0.01
T-0814	13,863.3	20,210	146,511,365	42.0	1.0	338.1	0.3	1.0	1.0	23.83	6,766.6	-	232.44	7,451.7	23.83	3.73	2.72E-02	3.53E-03 3.57E-04	0.95	0.28
T-0838	20,487.1	3,705	88,111,730	39.0	1.0	539.1	0.3	1.0	1.0	63.31	5,233.4	-	63.31	5,612.0	63.31	2.81	7.40E-03	2.69E-04	0.14	0.002
T-1227	1,056.1	6,737	4,917,864	39.0	1.0	27.8	1.0	1.0	1.0	46.80	19,049.2	-	46.80	19,049.2	46.80	9.52	2.34E-02	4.76E-03	1.87	0.002
	1,033.1	0,.51	1,527,004	55.0	2.0	27.0	1.0	1.0	2.0	.0.30	15,0 .5.2			HOURLY, lb/hr	1.943	3.32	0.72	02 00	16.68	0.30
														ANNUAL, tpy	1,543	181.48	0.72	0.07	20.00	1.04

FIXED ROOF TANKS POTENTIAL TO EMIT HAPS

Maximum individual HAPs (n-Hexane), tpy = 0.72 Total HAPS, tpy = 1.04

	2,2,4- Trimethylp entane	Acenaphth ene	Acenaphth ylene	Acetaldehy de	Anthracen e	Benz(a)ant hracene	Benzene	Benzo(a)phe nanthrene	Benzo(a)pyr ene	Benzo(b)flu oranthene	Benzo(e)py rene		Benzo(k)flu oranthene	Biphenyl	Cresol (mixed isomers)	Cumene	Ethylbenze ne	Fluoranthe ne	Fluorene
CAS No.	540-84-1	83-32-9	208-96-8	75-07-0	120-12-7	56-55-3	71-43-2	218-01-9	50-32-8	205-99-2	192-97-2	191-24-2	207-08-9	92-52-4	1319-77-3	98-82-8	100-41-4	206-44-0	86-73-7
Pi°, psia	7.85E-01	4.26E-05	9.28E-05	1.74E+01	1.16E-05	4.06E-09	2.01E+00	1.21E-10	1.06E-10	9.67E-09	1.10E-10	1.93E-12	1.87E-11	1.93E-04	3.48E-03	1.20E-01	2.17E-01	1.78E-07	1.16E-05
Tank	Speciated	Potential to	Emit, tpy					•											
T-0040	-	-	1.20E-11	5.57E-08	-	-	1.20E-08	4.74E-21	5.65E-21	-	-	-	-	-	6.94E-10	3.57E-10	1.23E-10	-	- 1
T-0041	-	-	1.20E-11	5.57E-08	-	-	1.20E-08	4.74E-21	5.65E-21	-	-	-	-	-	6.94E-10	3.57E-10	1.23E-10	-	-
T-0049	1.83E-05	7.12E-10	9.06E-10	-	6.91E-10	2.44E-15	3.99E-04	5.81E-17	5.77E-17	7.96E-15	8.82E-17	-	-	1.55E-07	1.47E-07	2.08E-06	2.49E-05	5.51E-13	2.86E-10
T-0055	-	-	8.00E-10	3.70E-06	-	-	7.96E-07	3.15E-19	3.76E-19	-	-	-	-	-	4.61E-08	2.38E-08	8.19E-09	-	- 1
T-0059	4.48E-06	9.66E-10	1.24E-10	-	3.26E-11	-	2.12E-06	-	-	-	-	1.01E-18	-	7.25E-09	-	7.26E-08	1.25E-06	1.55E-14	1.72E-10
T-0061	2.18E-05	4.71E-09	6.02E-10	-	1.59E-10	-	1.03E-05	-	-	-	-	4.90E-18	-	3.53E-08	-	3.54E-07	6.08E-06	7.57E-14	8.36E-10
T-0063	-	1.08E-09	8.93E-11	-	1.94E-10	8.55E-14	1.04E-06	1.98E-15	2.54E-16	1.39E-14	2.29E-16	2.57E-18	1.16E-17	6.26E-09	-	-	5.33E-07	3.34E-12	3.73E-10
T-0065	-	1.08E-09	8.88E-11	-	1.93E-10	8.51E-14	1.04E-06	1.97E-15	2.53E-16	1.38E-14	2.28E-16	2.56E-18	1.15E-17	6.23E-09	-	-	5.30E-07	3.32E-12	3.71E-10
T-0075	-	1.30E-09	1.07E-10	-	2.33E-10	1.03E-13	1.26E-06	2.38E-15	3.06E-16	1.67E-14	2.76E-16	3.10E-18	1.39E-17	7.52E-09	-	-	6.41E-07	4.02E-12	4.48E-10
T-0081	1.28E-04	-	-	-	9.30E-11	-	1.03E-03	9.65E-16	-	-	-	1.55E-17	-	-	-	4.31E-06	8.10E-05	-	-
T-0082	6.02E-05	-	-	-	4.36E-11	-	4.83E-04	4.52E-16	-	-	-	7.26E-18	-	-	-	2.02E-06	3.80E-05	-	-
T-0110	1.31E-03	-	-	-	9.47E-10	-	1.05E-02	9.83E-15	-	-	-	1.58E-16	-	-	-	4.39E-05	8.25E-04	-	-
T-0400	-	-	-	-	9.40E-10	1.37E-13	5.23E-02	1.31E-14	3.09E-15	2.07E-13	1.15E-14	1.57E-16	-	-	-	-	-	1.18E-11	1.09E-09
T-0410	7.39E-04	-	-	-	5.34E-10	-	5.93E-03	5.55E-15	-	-	-	8.91E-17	-	-	-	2.48E-05	4.66E-04	-	-
T-0419	-	-	-	-	1.48E-08	-	3.41E-05	-	-	-	-	-	-	1.66E-09	-	1.93E-06	7.54E-06	-	-
T-0420	2.78E-07	-	-	-	2.01E-13	-	2.23E-06	2.09E-18	-	-	-	3.35E-20	-	-	-	9.32E-09	1.75E-07	-	-
T-0422	3.88E-05	8.37E-09	1.07E-09	-	2.83E-10	-	1.84E-05	-	-	-	-	8.73E-18	-	6.28E-08	-	6.29E-07	1.08E-05	1.35E-13	1.49E-09
T-0423	4.65E-05	1.00E-08	1.28E-09	-	3.38E-10	-	2.20E-05	-	-	-	-	1.05E-17	-	7.53E-08	-	7.54E-07	1.30E-05	1.61E-13	1.78E-09
T-0431	1.52E-04	3.28E-08	4.19E-09	-	1.11E-09	-	7.20E-05	-	-	-	-	3.42E-17	-	2.46E-07	-	2.46E-06	4.24E-05	5.27E-13	5.82E-09
T-0432	2.12E-04	4.57E-08	5.84E-09	-	1.54E-09	-	1.00E-04	-	-	-	-	4.76E-17	-	3.43E-07	-	3.44E-06	5.91E-05	7.35E-13	8.12E-09
T-0433	-	-	-	-	5.02E-10	7.32E-14	2.79E-02	6.98E-15	1.65E-15	1.10E-13	6.13E-15	8.37E-17	-	-	-	-	-	6.32E-12	5.82E-10
T-0434	-	-	-	-	1.96E-06	-	4.53E-03	-	-	-	-	-	-	2.20E-07	-	2.56E-04	1.00E-03	-	-
T-0438	-	-	-	-	2.15E-10	3.13E-14	1.20E-02	2.99E-15	7.07E-16	4.73E-14	2.62E-15	3.58E-17	-	-	-	-	-	2.70E-12	2.49E-10
T-0814	2.90E-03	-	-	-	2.10E-09	-	2.33E-02	2.18E-14	-	-	-	3.50E-16	-	-	-	9.73E-05	1.83E-03	-	-
T-0815	-	-	-	-	7.89E-08	-	1.82E-04	-	-	-	-	-	-	8.85E-09	-	1.03E-05	4.03E-05	-	-
T-0838		-		-	5.94E-08	-	1.37E-04		-	-			-	6.66E-09	-	7.75E-06	3.03E-05	-	-
T-1227	3.91E-03	-	-	-	2.83E-09	-	3.14E-02	2.94E-14	-	-	-	4.72E-16	-	-	-	1.31E-04	2.47E-03	-	-
Sum HAPs, tpy	9.54E-03	1.07E-07	1.51E-08	3.81E-06	2.13E-06	5.17E-13	1.70E-01	9.74E-14	6.32E-15	4.17E-13	2.10E-14	1.48E-15	3.70E-17	1.18E-06	1.94E-07	5.89E-04	6.94E-03	3.37E-11	2.16E-08

 $\begin{aligned} &\text{Raoult's Law} &&P_i = x_i * \mathsf{TVP}_i \\ &&P_i = y_i * \mathsf{TVP} \\ &y_i = x_i * \mathsf{TVP}_i / \mathsf{TVP} \\ &\text{Liquid molar fraction} &&\text{xi } (\mathsf{mole_i/mole_T}) = \mathsf{mi} \ (g_i/g_T) * \ \mathsf{MW}_{liq} \ (g_T/\mathsf{moles_T}) \ / \ \mathsf{MW}_i \ (g_i/\mathsf{moles_i}) = \mathsf{wt}\%_{liq} * \ \mathsf{MW}_{liq} / \mathsf{MW}_i \\ &\text{Gas molar fraction} &&\text{yi } (\mathsf{mole_i/mole_T}) = \mathsf{mi} \ (g_i/g_T) * \ \mathsf{MW}_{vap} \ (g_T/\mathsf{moles_T}) \ / \ \mathsf{MW}_i \ (g_i/\mathsf{moles_i}) = \mathsf{wt}\%_{vap} * \ \mathsf{MW}_{vap} / \mathsf{MW}_i \\ && y_i = x_i * \mathsf{TVPi} / \mathsf{TVP} \\ && w_i \%_{vap} * \ \mathsf{MW}_{vap} / \mathsf{MW}_i = \ \mathsf{wt}\%_{liq} * \ \mathsf{MW}_{liq} / \mathsf{MW}_i * \ \mathsf{TVPi} / \mathsf{TVP} \\ && w_i \%_{vap} = \ \mathsf{wt}\%_{liq} * \ \mathsf{TVP_i} / \mathsf{TVP} * \ \mathsf{MW}_{liq} / \mathsf{MW}_{vap} \end{aligned}$

	Indeno(1,2, 3-	compound	m-Cresol	Methanol	Methyl ethyl	Methyl isobutyl ketone	m-Xylene	Naphthale ne	n-Hexane	o-Cresol	o-Xylene	PAH Total	Phenanthr ene	Phenol	p-Xylene	Pyrene	Toluene	Xylene (mixed
CAS No.	cd)pyrene 193-39-5	7439-92-1	108-39-4	67-56-1	78-93-3	108-10-1	108-38-3	91-20-3	110-54-3	95-48-7	95-47-6	PAH	85-01-8	108-95-2	106-42-3	129-00-0	108-88-3	isomers) 1330-20-7
Pi°, psia		3.42E-02	2.13E-03	2.70E+00	1.75E+00	3.85E-01	1.60E-01	5.44E-03	3.14E+00	3.48E-03	1.29E-01	1.93E-12	2.34E-06	8.42E-03	1.71E-01	8.70E-08	6.00E-01	1.96E-01
Tank	2.722 12	3.422 02	2.132 03	2.702.00	1.752.00	3.03L 01	1.002 01	3.442 03	3.142.00	3.402 03	1.232 01	1.552 12	2.542 00	0.422 03	1.712 01	0.702 00	0.002 01	1.502 01
T-0040	_		_	2.35E-05	6.82E-08	2.91E-08	_	3.21E-13	_	3.95E-11	3.15E-10	_	7.77E-17	2.53E-07	_	_	2.44E-09	4.02E-10
T-0041	_	_	-	2.35E-05	6.82E-08	2.91E-08	_	3.21E-13	-	3.95E-11	3.15E-10	_	7.77E-17	2.53E-07	-	_	2.44E-09	4.02E-10
T-0049	_	_	8.96E-08	5.35E-04	-	-	1.14E-04	2.66E-07	8.75E-04	1.46E-07	2.34E-05	_	9.64E-11	-	_	_	1.69E-04	4.59E-05
T-0055	_	_	-	1.56E-03	4.54E-06	1.93E-06	-	2.13E-11	-	2.62E-09	2.09E-08	_	5.16E-15	1.68E-05	_	_	1.62E-07	2.67E-08
T-0059	-	-	-	-	-	-	4.23E-06	2.95E-07	2.14E-06	-	8.49E-07	-	5.14E-11	-	1.59E-06	7.41E-14	4.28E-06	5.65E-06
T-0061	-	-	-	-	-	-	2.06E-05	1.44E-06	1.04E-05	-	4.13E-06	-	2.50E-10	_	7.74E-06	3.61E-13	2.09E-05	2.75E-05
T-0063	1.15E-18	1.20E-10	-	-	-	-	8.04E-07	7.96E-08	-	-	5.30E-07	-	1.91E-10	-	8.57E-07	6.39E-12	3.03E-06	2.90E-06
T-0065	1.14E-18	1.19E-10	-	-	-	-	8.00E-07	7.92E-08	-	-	5.28E-07	-	1.90E-10	-	8.53E-07	6.35E-12	3.02E-06	2.89E-06
T-0075	1.38E-18	1.44E-10	-	-	-	-	9.67E-07	9.57E-08	-	-	6.38E-07	-	2.30E-10	-	1.03E-06	7.68E-12	3.65E-06	3.49E-06
T-0081	-	1.23E-09	-	-	-	-	1.38E-04	1.85E-07	1.02E-02	-	-	-	4.23E-11	-	2.52E-05	-	6.74E-04	2.02E-04
T-0082	-	5.76E-10	-	-	-	-	6.47E-05	8.65E-08	4.78E-03	-	-	-	1.98E-11	-	1.18E-05	-	3.16E-04	9.48E-05
T-0110	-	1.25E-08	-	-	-	-	1.41E-03	1.88E-06	1.04E-01	-	-	-	4.31E-10	-	2.57E-04	-	6.86E-03	2.06E-03
T-0400	-	-	-	-	-	-	-	-	-	-	-	-	1.20E-09	-	-	1.19E-11	-	-
T-0410	-	7.07E-09	-	-	-	-	7.94E-04	1.06E-06	5.87E-02	-	-	-	2.43E-10	-	1.45E-04	-	3.87E-03	1.16E-03
T-0419	-	-	-	-	-	-	1.65E-04	6.55E-07	1.25E-05	-	5.96E-07	1.81E-15	3.07E-12	-	1.21E-04	-	3.02E-05	3.59E-05
T-0420	-	2.66E-12	-	-	-	-	2.99E-07	3.99E-10	2.21E-05	-	-	-	9.15E-14	-	5.45E-08	-	1.46E-06	4.38E-07
T-0422	-	-	-	-	-	-	3.67E-05	2.55E-06	1.85E-05	-	7.36E-06	-	4.46E-10	-	1.38E-05	6.42E-13	3.71E-05	4.90E-05
T-0423	-	-	-	-	-	-	4.40E-05	3.06E-06	2.22E-05	-	8.82E-06	-	5.34E-10	-	1.65E-05	7.69E-13	4.45E-05	5.87E-05
T-0431	-	-	-	-	-	-	1.44E-04	1.00E-05	7.25E-05	-	2.88E-05	-	1.74E-09	-	5.39E-05	2.51E-12	1.45E-04	1.92E-04
T-0432	-	-	-	-	-	-	2.00E-04	1.39E-05	1.01E-04	-	4.02E-05	-	2.43E-09	-	7.52E-05	3.51E-12	2.03E-04	2.67E-04
T-0433	-	-	-	-	-	-	-	-	-	-	-	-	6.41E-10	-	-	6.34E-12	-	-
T-0434	-	-					2.19E-02	8.70E-05	1.66E-03	-	7.91E-05	2.40E-13	4.08E-10		1.61E-02		4.01E-03	4.76E-03
T-0438	-	-	-	-	-	-	-	-	-	-	-	-	2.75E-10	-	-	2.71E-12	-	-
T-0814	-	2.78E-08	-	-	-	-	3.12E-03	4.17E-06	2.30E-01	-	-	-	9.55E-10	-	5.69E-04	-	1.52E-02	4.57E-03
T-0815	-	-	-	-	-	-	8.79E-04	3.50E-06	6.67E-05	-	3.18E-06	9.65E-15	1.64E-11	-	6.48E-04	-	1.61E-04	1.92E-04
T-0838	-	-	-	-	-	-	6.62E-04	2.64E-06	5.02E-05	-	2.40E-06	7.27E-15	1.24E-11	-	4.88E-04	-	1.21E-04	1.44E-04
T-1227	-	3.74E-08	-	-	-	-	4.20E-03	5.62E-06	3.11E-01	-	-	-	1.29E-09	-	7.67E-04	-	2.05E-02	6.16E-03
Sum HAPs, tpy	3.66E-18	8.70E-08	8.96E-08	2.15E-03	4.67E-06	1.99E-06	3.39E-02	1.39E-04	7.22E-01	1.49E-07	2.01E-04	2.59E-13	1.17E-08	1.73E-05	1.93E-02	4.92E-11	5.24E-02	2.00E-02

FLOATING ROOF TANKS (EXT, INT) POTENTIAL TO EMIT

Tank ID	Stor	red Commodity	Most Volatile Category of Allowable Liquids to be	Regulatory Vapor Pressure Limitation (MACT CC, NSPS K, Ka, Kb)	MACT CC Group	Maximum Hourly Throughput	Net Throughput	Are Seal Gap Is Maintained with Gaps	H2S in Liquid
	CHEMICAL NAME FOR VOC LOSSES	CHEMICAL NAME FOR HAPS LOSSES SPECIATION	Stored			Q _H	Q	< 1/8 in.?	H2S _{liq}
	CALCULATION					bbl/hr	bbl/yr	-	ppm
								No - Avg. Fitting Yes - Tight Fitting	API 4723A
T-0011	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	624.29	2,000,000	Avg. Fitting	-
T-0012	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	624.29	2,000,000	Avg. Fitting	-
T-0020	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	624.29	1,800,000	Avg. Fitting	-
T-0021	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	624.29	1,800,000	Avg. Fitting	-
T-0022	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	624.29	1,800,000	Avg. Fitting	-
T-0023	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	624.29	1,800,000	Avg. Fitting	-
T-0056	Sweet Naphtha	Catalytic Hydrocracker - Heavy H/C Naphtha	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	600.00	9,855,000	Avg. Fitting	-
T-0079	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	5,200.00	5,780,000	Avg. Fitting	-
T-0106	Sour Water	Various Units - Slop Oil	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	2,400.00	2,390,000	Avg. Fitting	3,200
T-0107	Gasolines & Gasoline Blendstocks	Atmospheric Distillation - Straight Run Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	1200	3,197,400	Avg. Fitting	0.035
T-0108	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	300.00	2,796,814	Avg. Fitting	-
T-0109	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	1,200.00	3,452,000	Avg. Fitting	-
T-0111	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	600.00	1,415,000	Avg. Fitting	-
T-0112	Sweet Naphtha	Catalytic Hydrocracker - Heavy H/C Naphtha	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	600.00	30,000	Avg. Fitting	-
T-0117	Sweet Naphtha	Catalytic Hydrocracker - Heavy H/C Naphtha	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	2,400.00	1,292,000	Avg. Fitting	-
T-0124	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	1,200.00	2,308,000	Avg. Fitting	-
T-0401	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	600.00	5,110,000	Avg. Fitting	-
T-0402	Light Cat Naphtha	Fluid Catalytic Cracker - Cracked Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	600.00	6,205,000	Avg. Fitting	0.80
T-0411	Gasolines & Gasoline Blendstocks	Atmospheric Distillation - Straight Run Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	2400	3,197,400	Avg. Fitting	0.03

FLOATING ROOF TANKS (EXT, INT) POTENTIAL TO EMIT

Tank ID	Store	ed Commodity	Most Volatile Category of Allowable	Regulatory Vapor Pressure Limitation (MACT CC, NSPS K, Ka, Kb)	MACT CC Group	Maximum Hourly Throughput	Net Throughput	Are Seal Gap Is Maintained with Gaps	H2S in Liquid
	CHEMICAL NAME FOR VOC LOSSES CALCULATION	CHEMICAL NAME FOR HAPS LOSSES SPECIATION	Liquids to be Stored			Q _H	Q	< 1/8 in.?	H2S _{liq}
	CALCULATION					bbl/hr	bbl/yr		ppm
								No - Avg. Fitting Yes - Tight Fitting	API 4723A
T-0412	Sweet Naphtha	Catalytic Hydrocracker - Heavy H/C Naphtha	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	2,520.00	1,292,000	Avg. Fitting	
T-0413	Straight Run Kerosene	Atmospheric Distillation - Straight Run Kerosene	High VP	No limit (Pre-NSPS, HAPs<4wt%)	Group 2	2,520.00	4,927,500	Avg. Fitting	
T-0415	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	2,160.00	3,452,000	Avg. Fitting	
T-0417	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	1,200.00	1,415,000	Avg. Fitting	-
T-0418	Straight Run Kerosene	Atmospheric Distillation - Straight Run Kerosene	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 2	240.00	4,200,000	Avg. Fitting	-
T-0435	Sour Water	Various Units - Slop Oil	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	300.00	2,628,000	Avg. Fitting	3,200
T-0437	Crude Oil	Supply System - Crude Oil	High VP	TVP < 11.1 psia (NSPS Kb, HAPs<4wt%,V>20,000gal)	Group 2	4,200.00	16,754,000	Avg. Fitting	12.50
T-0439	Sour Naphtha	Atmospheric Distillation - Straight Run Naphtha	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	4,200.00	18,067,500	Avg. Fitting	1.67
T-0450	Sour Naphtha	Atmospheric Distillation - Straight Run Naphtha	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	5,200.00	9,855,000	Avg. Fitting	1.67
T-0451	Straight Run Diesel	Distillate Blending - Diesel Fuel	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 2	225.71	949,000	Avg. Fitting	3.54
T-0452	Ethanol	-	High VP	TVP < 11.1 psia (NSPS Kb, HAPs<4wt%,V>20,000gal)	Group 2	1,024.29	142,350	Avg. Fitting	-
T-0737	Sour Water	Various Units - Slop Oil	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	572.00	5,006,000	Avg. Fitting	3,200
T-0802	Sour Water	Various Units - Slop Oil	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	572.00	5,006,000	Avg. Fitting	3,200
T-0821	Light Cat Naphtha	Fluid Catalytic Cracker - Cracked Gasoline	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 1	730.00	6,394,800	Avg. Fitting	0.80
T-0834	Straight Run Diesel	Distillate Blending - Diesel Fuel	Moderate VP	TVP < 1.9 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 2	660.00	15,695,000	Avg. Fitting	3.54
T-0835	Straight Run Diesel	Distillate Blending - Diesel Fuel	High VP	TVP < 11.1 psia (MACT CC, HAPs>4wt%, V>20,000gal)	Group 2	960.00	15,695,000	Avg. Fitting	3.54
T-1225	Crude Oil	Supply System - Crude Oil	High VP	TVP < 11.1 psia (NSPS Kb, HAPs<4wt%,V>20,000gal)	Group 2	1,714.29	38,106,000	Avg. Fitting	12.50

				TANK CHARACTI	ERISTICS						TANK CHARAC	TERISTICS			
Tank ID	Tank Type	Tank Diameter	Tank Shell Height	Shell Capacity	Tank Insulated	Tank Construction	Deck Construction	Deck Type	Deck Type (EFR)	Rim Seal System Primary Seal	Rim Seal System	Deck Seam Type	Deck Seam Length	Self or Column	Column Construction Details
		D	Hs		insulated	Construction	Construction			Primary Seai	Secondary Seal		L _{seam}	Supported Roof?	Details
		ft	ft	gallons									ft		
	INT EXT EXT-GEO EXT-CR				YES-ALL-CTE YES-ALL-CYCLE YES-SHELL NO	Riveted-Bolted Welded	Riveted-Bolted Welded	Continous Sheet Panel Unknown	Steel Peripheral Pontoon (SPP) Steel Double Deck (SDD)	Mechanical Shoe Liquid-mounted Vapor-mounted	None Shoe-mounted Rim-mounted	5 ft wide; 6 ft wide; 7 ft wide; 5 x 7.5 ft rectangular; 5 x 12 ft rectangular Unknown		Self-Supported Column	9"x7" built-up columns 8" diameter pipe columns Tank Specific Unknown
T-0011	INT	89.00	29.00	1,349,460	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0012	INT	89.00	29.00	1,349,460	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0020	INT	90.00	48.00	2,283,960	NO	Welded	Welded	Unknown	SPP	Mechanical Shoe	Shoe-mounted	Unknown	-	Column	Unknown
T-0021	INT	90.00	48.00	2,283,960	NO	Welded	Welded	Unknown	SPP	Mechanical Shoe	Shoe-mounted	Unknown	-	Column	Unknown
T-0022	INT	75.00	48.00	1,586,340	NO	Welded	Welded	Unknown	SPP	Mechanical Shoe	Shoe-mounted	Unknown	-	Column	Unknown
T-0023	INT	75.00	48.00	1,586,340	NO	Welded	Welded	Unknown	SPP	Mechanical Shoe	Shoe-mounted	Unknown	-	Column	Unknown
T-0056	INT	48.00	36.00	487,200	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0079	EXT	125.00	40.00	3,671,640	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-0106	INT	67.00	40.00	1,055,040	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0107	INT	67.00	40.00	1,055,040	NO	Welded	Riveted-Bolted	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0108	INT	67.00	40.00	1,055,040	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0109	INT	67.00	40.00	1,055,040	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0111	INT	49.00	30.00	423,360	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0112	INT	48.00	30.00	406,140	NO	Welded	Riveted-Bolted	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0117	EXT	48.00	48.00	649,740	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-0124	INT	40.00	30.00	281,820	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0401	EXT-GEO	90.00	50.00	2,379,300	NO	Welded	Welded	Unknown	SPP	Mechanical Shoe	Rim-mounted	Unknown	-	Self-Support	-
T-0402	EXT	90.00	50.00	2,379,300	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-0411	EXT	100.00	40.00	2,349,900	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-

				TANK CHARACTE	RISTICS						TANK CHARACT	TERISTICS			
Tank ID	Tank Type	Tank Diameter	Tank Shell Height	Shell Capacity	Tank	Tank	Deck	Deck Type	Deck Type (EFR)	Rim Seal System	Rim Seal System	Deck Seam Type	Deck Seam Length	Self or Column	Column Constructio
		D	H _s		Insulated	Construction	Construction			Primary Seal	Secondary Seal		L _{seam}	Supported Roof?	Details
		ft	ft	gallons									ft		
	INT EXT EXT-GEO EXT-CR				YES-ALL-CTE YES-ALL-CYCLE YES-SHELL NO	Riveted-Bolted Welded	Riveted-Bolted Welded	Continous Sheet Panel Unknown	Steel Peripheral Pontoon (SPP) Steel Double Deck (SDD)	Mechanical Shoe Liquid-mounted Vapor-mounted	None Shoe-mounted Rim-mounted	5 ft wide; 6 ft wide; 7 ft wide; 5 x 7.5 ft rectangular; 5 x 12 ft rectangular Unknown		Self-Supported Column	9"x7" built-up columns 8" diameter pipe columns Tank Specific Unknown
T-0412	EXT	100.00	40.00	2,349,900	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-0413	INT	67.00	39.00	1,028,580	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0415	INT	67.00	40.00	1,055,040	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0417	INT	50.00	30.00	440,580	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0418	INT	67.00	33.00	870,240	NO	Welded	Welded	Unknown	SPP	Vapor-mounted	Rim-mounted	Unknown	-	Column	Unknown
T-0435	EXT	30.00	40.00	211,680	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-0437	EXT	120.00	45.00	3,806,880	NO	Welded	Welded	-	SPP	Liquid-mounted	Rim-mounted	-	-	-	-
T-0439	INT	130.00	46.00	4,567,080	NO	Welded	Welded	Unknown	SPP	Mechanical Shoe	Rim-mounted	Unknown	-	Column	Unknown
T-0450	EXT	120.00	40.00	3,383,940	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-0451	INT	35.00	40.00	287,700	YES-ALL-CTE	Welded	Welded	Unknown	SPP	Mechanical Shoe	Rim-mounted	Unknown	-	Column	Unknown
T-0452	INT	35.00	40.00	287,700	NO	Welded	Welded	Unknown	SPP	Mechanical Shoe	Rim-mounted	Unknown	-	Column	Unknown
T-0737	EXT	63.00	40.00	932,820	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-0802	EXT	45.00	40.00	475,860	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-0821	EXT	106.00	50.00	3,300,360	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-0834	EXT	85.00	40.00	1,697,640	NO	Welded	Welded	-	SPP	Mechanical Shoe	None	-	-	-	-
T-0835	EXT	111.00	40.00	2,895,480	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-
T-1225	EXT	150.00	40.00	5,287,380	NO	Welded	Welded	-	SPP	Mechanical Shoe	Rim-mounted	-	-	-	-

		TANK PAII	NT			СН	EMICAL PRO	PERTIES			METE	OROLOGICAL	. DATA	
Tank ID	Tank Shell Paint	Tank Roof Paint	Shell Paint	Roof Paint	Internal Shell	Product Category	Liquid Molecular Weight	Vapor Molecular Weight	Density of the Liquid	Average Wind Speed	Atmosph. Pressure	Daily Maximum Ambient Temp.	Daily Minimum Ambient Temp.	Daily Total Solar Insulation Factor
			Condition	Condition	Condition		ML	M _v	W _L	v	PA	T _{AX}	T _{AN}	ı
							lb/lbmole	lb/lbmole	lb/gal	mph	psia	°F	°F	Btu/ft^2d
			New Average Aged	New Average Aged	Light Rust Dense Rust Gunite Lining	Organic Liquids Crude Oil Petroleum Stock								
T-0011	White	White	New	New	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0012	White	White	New	New	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0020	White	White	New	New	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0021	White	White	New	New	Light Rust	Petroleum Stock	92 92	62 62	5.60 5.60	9.0	13.1	77.9	50.0	1,711.9
T-0022 T-0023	White White	White	New	New	Light Rust	Petroleum Stock Petroleum Stock	92	62	5.60	9.0	13.1	77.9 77.9	50.0 50.0	1,711.9
		White	New	New	Light Rust		-				-			1,711.9
T-0056 T-0079	White	White White	Average	Average	Light Rust	Petroleum Stock Petroleum Stock	120	80 62	6.40 5.60	9.0	13.1	77.9 77.9	50.0 50.0	1,711.9
T-0079	White White	White	New	New	Light Rust	Crude Oil	92 92	66	5.60	9.0	13.1	77.9	50.0	1,711.9 1.711.9
T-0106	White	White	New	New	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0107	White	White	Average	Average	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0108	White	White	Aged	Aged	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0103	White	White	Aged	Aged	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0111	White	White	Average	Average	Light Rust	Petroleum Stock	120	80	6.40	9.0	13.1	77.9	50.0	1,711.9
T-0112	White	White	New	New	Light Rust	Petroleum Stock	120	80	6.40	9.0	13.1	77.9	50.0	1,711.9
T-0117	White	White	New	New	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0401	White	White	New	New	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0402	White	White	New	New	Light Rust	Petroleum Stock	92	66	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0411	White	White	Average	Average	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
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		TANK PAII	NT			СН	EMICAL PRO	PERTIES			METE	OROLOGICAI	LDATA	
Tank ID	Tank Shell Paint	Tank Roof Paint	Shell Paint Condition	Roof Paint	Internal Shell	Product Category	Liquid Molecular Weight	Vapor Molecular Weight	Density of the Liquid	Average Wind Speed	Atmosph. Pressure	Daily Maximum Ambient Temp.	Daily Minimum Ambient Temp.	Daily Total Solar Insulation Factor
			Condition	Condition	Condition		ML	M _v	W _L	v	PA	T _{AX}	T _{AN}	ı
							lb/lbmole	lb/lbmole	lb/gal	mph	psia	°F	°F	Btu/ft^2d
			New Average Aged	New Average Aged	Light Rust Dense Rust Gunite Lining	Organic Liquids Crude Oil Petroleum Stock								
T-0412	White	White	Average	Average	Light Rust	Petroleum Stock	120	80	6.40	9.0	13.1	77.9	50.0	1,711.9
T-0413	White	White	New	New	Light Rust	Petroleum Stock	162	130	7.00	9.0	13.1	77.9	50.0	1,711.9
T-0415	White	White	New	New	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0417	White	White	Aged	Aged	Light Rust	Petroleum Stock	92	62	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0418	White	White	New	New	Light Rust	Petroleum Stock	162	130	7.00	9.0	13.1	77.9	50.0	1,711.9
T-0435	White	White	New	New	Light Rust	Crude Oil	92	66	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0437	White	White	New	New	Light Rust	Crude Oil	207	58	7.10	9.0	13.1	77.9	50.0	1,711.9
T-0439	White	White	Average	Average	Light Rust	Petroleum Stock	92	66	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0450	White	White	New	New	Light Rust	Petroleum Stock	92	66	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0451	Aluminum - Specular	Aluminum - Specular	Average	Average	Light Rust	Petroleum Stock	188	130	7.10	9.0	13.1	77.9	50.0	1,711.9
T-0452	White	White	Average	Average	Light Rust	Organic Liquids	-	46	6.59	9.0	13.1	77.9	50.0	1,711.9
T-0737	White	White	New	New	Light Rust	Crude Oil	92	66	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0802	White	White	New	New	Light Rust	Crude Oil	92	66	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0821	White	White	Average	Average	Light Rust	Petroleum Stock	92	66	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0834	White	White	Average	Average	Light Rust	Petroleum Stock	188	130	7.10	9.0	13.1	77.9	50.0	1,711.9
T-0835	White	White	Average	Average	Light Rust	Petroleum Stock	188	130	7.10	9.0	13.1	77.9	50.0	1,711.9
T-1225	White	White	Average	Average	Light Rust	Crude Oil	207	58	7.10	9.0	13.1	77.9	50.0	1,711.9

			TA	NK TEMPERATURE V	ARIABLES			1	TANK PRESSURE VA	ARIABLES	
Tank ID	Tank Shell Surface Solar Absorptance	Tank Roof Surface Solar Absorptance	Daily Average Temp.	Liquid Bulk Temp. based on Ambient Met Data	Monthly Liquid Bulk Temperature Monitored	Liquid Bulk Temp.	Daily Average Liquid Surface Temp.	Max. True Vapor Pressure	True Vapor Pressure at Daily Avg Temp. (T _{LA})	Vapor Pressure Function (P _{VA})	Vapor Pressure Function (TVP Limit)
	α_{s}	α_{R}	T _{AA}	T _B (AP-42)	T _B (Monitored)	T _B	T _{LA}	P _{vmax}	P _{VA}	P*	P*max
	unitless	unitless	°R	°R	°R	°R	°R	psia	psia	unitless	unitless
	AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Eq. 1-30	AP-42, Ch. 7.1, Eq. 1-31 INT, EXT-GEO, EXT-CR Eq. 2-8 EXT w/ SPP Eq. 2-11 EXT w/ SDD	Ops Data	Max. Monitored vs AP-42 Estimate	AP-42, Ch. 7.1, Eq. 2-5 INT, EXT-GEO, EXT-CR Eq. 2.7 EXT w/ SPP Eq. 2-10 EXT w/ SDD		AP-42, Ch. 7.1, Eq. 1-25 Petroleum Eq. 1-26 Org Liq	AP-42 Ch. 7.1 Eq. 2-4	AP-42 Ch. 7.1 Eq. 2-4
T-0011	0.17	0.17	523.6	524.5	534.38	534.4	532.2	11.1	9.1	0.289	0.441
T-0012	0.17	0.17	523.6	524.5	527.71	527.7	527.7	11.1	8.4	0.251	0.441
T-0020	0.17	0.17	523.6	524.5	-	524.5	525.4	11.1	8.1	0.235	0.441
T-0021	0.17	0.17	523.6	524.5	-	524.5	525.4	11.1	8.1	0.235	0.441
T-0022	0.17	0.17	523.6	524.5	-	524.5	525.4	11.1	8.0	0.235	0.441
T-0023	0.17	0.17	523.6	524.5	-	524.5	525.4	11.1	8.0	0.235	0.441
T-0056	0.25	0.25	523.6	524.9	526.74	526.7	527.3	11.1	1.9	0.039	0.441
T-0079	0.17	0.17	523.6	525.9	545.55	545.5	532.5	11.1	9.1	0.292	0.441
T-0106	0.17	0.17	523.6	524.5	532.10	532.1	530.4	11.1	7.0	0.191	0.441
T-0107	0.17	0.17	523.6	524.5	533.57	533.6	531.3	11.1	9.0	0.281	0.441
T-0108	0.25	0.25	523.6	524.9	544.62	544.6	539.1	11.1	10.3	0.366	0.441
T-0109	0.34	0.34	523.6	525.4	542.01	542.0	538.0	11.1	10.1	0.352	0.441
T-0111	0.34	0.34	523.6	525.4	541.40	541.4	537.6	11.1	10.0	0.347	0.441
T-0112	0.25	0.25	523.6	524.9	525.91	525.9	526.9	11.1	1.9	0.039	0.441
T-0117	0.17	0.17	523.6	525.2	528.39	528.4	527.4	11.1	1.9	0.039	0.441
T-0124	0.17	0.17	523.6	524.5	528.23	528.2	527.7	11.1	8.4	0.252	0.441
T-0401	0.17	0.17	523.6	524.5	532.24	532.2	530.5	11.1	8.8	0.274	0.441
T-0402	0.17	0.17	523.6	525.5	538.33	538.3	530.4	11.1	6.3	0.163	0.441
T-0411	0.25	0.25	523.6	526.7	525.12	526.7	528.0	11.1	8.4	0.254	0.441

			TA	NK TEMPERATURE V	ARIABLES			1	ANK PRESSURE VA	RIABLES	
Tank ID	Tank Shell Surface Solar Absorptance	Tank Roof Surface Solar Absorptance	Daily Average Temp.	Liquid Bulk Temp. based on Ambient Met Data	Monthly Liquid Bulk Temperature Monitored	Liquid Bulk Temp.	Daily Average Liquid Surface Temp.	Max. True Vapor Pressure	True Vapor Pressure at Daily Avg Temp. (T _{LA})	Vapor Pressure Function (P _{VA})	Vapor Pressure Function (TVP Limit
	αs	α_{R}	T _{AA}	T _B (AP-42)	T _B (Monitored)	T _B	T _{LA}	P _{vmax}	P _{VA}	P*	P*max
	unitless	unitless	°R	°R	°R	°R	°R	psia	psia	unitless	unitless
	AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Eq. 1-30	AP-42, Ch. 7.1, Eq. 1-31 INT, EXT-GEO, EXT-CR Eq. 2-8 EXT w/ SPP Eq. 2-11 EXT w/ SDD	Ops Data	Max. Monitored vs AP-42 Estimate	AP-42, Ch. 7.1, Eq. 2-5 INT, EXT-GEO, EXT-CR Eq. 2.7 EXT w/ SPP Eq. 2-10 EXT w/ SDD		AP-42, Ch. 7.1, Eq. 1-25 Petroleum Eq. 1-26 Org Liq	AP-42 Ch. 7.1 Eq. 2-4	AP-42 Ch. 7.1 Eq. 2-4
T-0412	0.25	0.25	523.6	526.7	526.39	526.7	528.0	11.1	1.9	0.040	0.441
T-0413	0.17	0.17	523.6	524.5	535.45	535.5	532.6	11.1	0.5	0.009	0.441
T-0415	0.17	0.17	523.6	524.5	527.18	527.2	527.1	11.1	8.3	0.247	0.441
T-0417	0.34	0.34	523.6	525.4	531.21	531.2	531.0	11.1	8.9	0.278	0.441
T-0418	0.17	0.17	523.6	524.5	539.63	539.6	535.4	11.1	0.5	0.010	0.441
T-0435	0.17	0.17	523.6	525.0	524.57	525.0	526.4	11.1	6.6	0.173	0.441
T-0437	0.17	0.17	523.6	525.8	533.44	533.4	528.9	11.1	6.9	0.184	0.441
T-0439	0.25	0.25	523.6	524.9	531.80	531.8	531.0	11.1	7.5	0.209	0.441
T-0450	0.17	0.17	523.6	525.9	531.26	531.3	528.3	11.1	7.1	0.194	0.441
T-0451	0.44	0.44	523.6	525.9	534.20	534.2	534.2	11.1	0.4	0.008	0.441
T-0452	0.25	0.25	523.6	524.9	515.12	524.9	526.0	11.1	0.8	0.016	0.441
T-0737	0.17	0.17	523.6	525.4	524.57	525.4	526.5	11.1	6.6	0.174	0.441
T-0802	0.17	0.17	523.6	525.2	524.57	525.2	526.4	11.1	6.6	0.174	0.441
T-0821	0.25	0.25	523.6	526.6	520.65	526.6	527.9	11.1	6.0	0.153	0.441
T-0834	0.25	0.25	523.6	526.6	541.9	541.9	532.5	1.9	0.4	0.008	0.039
T-0835	0.25	0.25	523.6	526.8	542.05	542.1	532.6	11.1	0.4	0.008	0.441
T-1225	0.25	0.25	523.6	527.1	530.25	530.3	529.0	11.1	6.9	0.185	0.441

			RIM SEAL	LOSSES				DEC	K FITTING LOSSES			DECK SEAM	LOSSES (IFR)	
Tank ID	Zero Wind Speed Rim Seal Loss Factor	Wind Speed Dependent Rim Seal Loss Factor	Seal-Related Wind Speed Exponent	Average Ambient Wind Speed at the Tank Site	Product Factor	Rim Seal Loss Max Hourly	Rim Seal Loss	Total Deck Fitting Loss Factor	Deck Fitting Loss Max Hourly	Deck Fitting Loss	Deck Seam Loss per Unit Seam Length Factor	Deck Seam Length Factor	Deck Seam Loss Max Hourly	Deck Seam Loss
	K _{Ra}	K _{Rb}	n	V _{tank}	Kc		L _R	$F_{\rm F} = \sum (N_{\rm Fi} * K_{\rm fi})$		L _F	K _D	S _D		L_{D}
	lbmole/ft*yr	lbmole/(mph) ⁿ ft*yr	unitless	mph	unitless	lb/hr	lb/month	lbmole/yr	lb/hr	lb/month	lbmole/ft-yr	ft/ft^2	lb/hr	lb/month
	AP-42 CH. 7.1 Table 7.1-8 Varies if fittings are avg. or tight	AP-42 CH. 7.1 Table 7.1-8 Varies if fittings are avg. or tight	AP-42 CH. 7.1 Table 7.1-8 Varies if fittings are avg. or tight	AP-42 Ch. 7.1 Eq. 2-3 Note 1	AP-42 Ch. 7.1 Eq. 2-3 Notes	AP-42 Ch. 7.1 Eq. 2-3	AP-42 Ch. 7.1 Eq. 2-3	AP-42, Ch. 7.1, Eq. 2-14	AP-42, Ch. 7.1, Eq. 2-13	AP-42, Ch. 7.1, Eq. 2-13	AP-42, Ch. 7.1, Eq. 2-18 Note	AP-42, Ch. 7.1, Eq. 2-18 Notes	AP-42, Ch. 7.1, Eq. 2-18	AP-42, Ch. 7.1, Eq. 2-18
T-0011	2.20	0.003	4.3	-	1.0	0.61	3,510.1	568.5	1.77	10,190.9	-	-	-	-
T-0012	2.20	0.003	4.3	-	1.0	0.61	3,051.0	560.6	1.75	8,734.9	-	-	-	-
T-0020	1.60	0.300	1.6	-	1.0	0.45	2,098.3	89.3	0.28	1,300.8	-	-	-	-
T-0021	1.60	0.300	1.6	-	1.0	0.45	2,098.3	89.3	0.28	1,300.8	-	-	-	-
T-0022	1.60	0.300	1.6	-	1.0	0.37	1,746.6	80.3	0.25	1,168.3	-	-	-	-
T-0023	1.60	0.300	1.6	-	1.0	0.37	1,746.6	80.3	0.25	1,168.3	-	-	-	-
T-0056	2.20	0.003	4.3	-	1.0	0.43	332.4	292.9	1.18	921.8	-	-	-	-
T-0079	0.60	0.400	1.0	9.0	1.0	1.64	9,551.7	346.1	1.08	6,272.3	-	-	-	-
T-0106	2.20	0.003	4.3	-	0.4	0.20	742.2	340.3	0.45	1,713.3	-	-	-	-
T-0107	2.20	0.003	4.3	-	1.0	0.46	2,568.9	614.2	1.92	10,704.3	0.14	0.20	0.39	2,191
T-0108	2.20	0.003	4.3	-	1.0	0.46	3,348.8	340.3	1.06	7,730.6	-	-	-	-
T-0109	2.20	0.003	4.3	-	1.0	0.46	3,219.6	538.3	1.68	11,757.4	-	-	-	-
T-0111	2.20	0.003	4.3	-	1.0	0.34	2,319.0	292.9	0.91	6,300.2	-	-	-	-
T-0112	2.20	0.003	4.3	-	1.0	0.43	328.8	236.9	0.95	737.5	0.14	0.20	0.26	201
T-0117	0.60	0.400	1.0	9.0	1.0	0.81	637.9	751.3	3.02	2,368.1	-	-	-	-
T-0124	2.20	0.003	4.3	-	1.0	0.27	1,373.7	340.3	1.06	5,311.8	-	-	-	-
T-0401	0.60	0.400	1.0	-	1.0	0.17	916.9	77.2	0.24	1,311.2	-	-	-	-
T-0402	0.60	0.400	1.0	9.0	1.0	1.26	4,070.7	334.3	1.11	3,586.1	-	-	-	-
T-0411	0.60	0.400	1.0	9.0	1.0	1.32	6,630.5	775.2	2.42	12,190.6	-	-	-	-

			RIM SEAI	LOSSES				DEC	K FITTING LOSSES			DECK SEAM	LOSSES (IFR)	
Tank ID	Zero Wind Speed Rim Seal Loss Factor	Wind Speed Dependent Rim Seal Loss Factor	Seal-Related Wind Speed Exponent	Average Ambient Wind Speed at the Tank Site	Product Factor	Rim Seal Loss Max Hourly	Rim Seal Loss	Total Deck Fitting Loss Factor	Deck Fitting Loss Max Hourly	Deck Fitting Loss	Deck Seam Loss per Unit Seam Length Factor	Deck Seam Length Factor	Deck Seam Loss Max Hourly	Deck Seam Loss
	K _{Ra}	K _{Rb}	n	V _{tank}	K _c		L _R	$F_{\rm F} = \sum (N_{\rm Fi} * K_{\rm fi})$		L _F	K _D	S _D		L _D
	lbmole/ft*yr	lbmole/(mph) ⁿ ft*yr	unitless	mph	unitless	lb/hr	lb/month	lbmole/yr	lb/hr	lb/month	lbmole/ft-yr	ft/ft^2	lb/hr	lb/month
	AP-42 CH. 7.1 Table 7.1-8 Varies if fittings are avg. or tight	AP-42 CH. 7.1 Table 7.1-8 Varies if fittings are avg. or tight	AP-42 CH. 7.1 Table 7.1-8 Varies if fittings are avg. or tight	AP-42 Ch. 7.1 Eq. 2-3 Note 1	AP-42 Ch. 7.1 Eq. 2-3 Notes	AP-42 Ch. 7.1 Eq. 2-3	AP-42 Ch. 7.1 Eq. 2-3	AP-42, Ch. 7.1, Eq. 2-14	AP-42, Ch. 7.1, Eq. 2-13	AP-42, Ch. 7.1, Eq. 2-13	AP-42, Ch. 7.1, Eq. 2-18 Note	AP-42, Ch. 7.1, Eq. 2-18 Notes	AP-42, Ch. 7.1, Eq. 2-18	AP-42, Ch. 7.1, Eq. 2-18
T-0412	0.60	0.400	1.0	9.0	1.0	1.70	1,347.8	775.2	3.12	2,478.0	-	-	-	
T-0413	2.20	0.003	4.3	-	1.0	0.96	174.5	664.3	4.35	786.5	-	-	-	
T-0415	2.20	0.003	4.3	-	1.0	0.46	2,259.8	300.8	0.94	4,611.2	-	-	-	
T-0417	2.20	0.003	4.3	-	1.0	0.34	1,896.3	506.2	1.58	8,725.9	-	-	-	
T-0418	2.20	0.003	4.3	-	1.0	0.96	187.6	885.3	5.79	1,126.9	-	-	-	
T-0435	0.60	0.400	1.0	9.0	0.4	0.17	578.6	301.1	0.40	1,377.4	-	-	-	
T-0437	0.30	0.600	0.3	9.0	0.4	0.20	749.1	885.3	1.03	3,781.6	-	-	-	
T-0439	0.60	0.400	1.0	-	1.0	0.26	1,078.3	784.6	2.61	10,846.2	-	-	-	
T-0450	0.60	0.400	1.0	9.0	1.0	1.68	6,480.9	741.7	2.46	9,499.9	-	-	-	
T-0451	0.60	0.400	1.0	-	1.0	0.14	23.1	271.4	1.78	298.5	-	-	-	
T-0452	0.60	0.400	1.0	-	1.0	0.05	15.4	271.4	0.63	198.7	-	-	-	
T-0737	0.60	0.400	1.0	9.0	0.4	0.35	1,218.5	86.6	0.12	397.2	-	-	-	
T-0802	0.60	0.400	1.0	9.0	0.4	0.25	869.1	61.2	0.08	280.5	-	-	-	
T-0821	0.60	0.400	1.0	9.0	1.0	1.48	4,503.5	426.6	1.42	4,298.7	-	-	-	
T-0834	5.80	0.300	2.1	9.0	1.0	1.80	3,255.9	764.3	0.45	805.1	-	-	-	
T-0835	0.60	0.400	1.0	9.0	1.0	3.06	493.6	751.3	4.92	792.4	-	-	-	
T-1225	0.60	0.400	1.0	9.0	0.4	0.74	2,710.5	756.3	0.88	3,241.3	-	-	-	

		V	VORKING (WITHD	RAWAL) LOSSE	S		MAXIMUM							
Tank ID	Sum of the Decreases in Liquid Level	Shell Clingage Factor	No. of Roof Support Columns	Effective Column Diameter	Working (Withdrawal) Loss Max Hourly	Working (Withdrawal) Loss	FLOATING	TOTAL FLOATING ROOF TANKS VOC LOSSES	VC Emis		H: Emis		HA Emiss	
	ΣH _{QD}	Cs	N _c	F _c		L _w		L _T						
	ft/month	bbl/1,000 ft^2	ft	ft	lb/hr	lb/month	lb/hr	lb/month	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
	AP-42, Ch. 7.1, Eq. 2-20	AP-42, Ch. 7.1, Table 7.1-10	Site-Specific If unknown AP-42 Ch. 7.1 Eq. 2-19 Note 3 Table 7.1-11 (IFR)	AP-42, Ch. 7.1, Eq. 2-19 Note 4		AP-42, Ch. 7.1, Eq. 2-19	AP-42, Ch. 7.1 Eq. 2-1 & 2-2 (@ P*max)	AP-42, Ch. 7.1 Eq. 2-1 & 2-2			Raoul	rs Law	Raoult	s Law
T-0011	1,804.8	0.0015	6.0	1.0		190.0	2.44	13,891	2.44	6.95	-	-	0.05	0.14
T-0012	1,804.8	0.0015	6.0	1.0		190.0	2.42	11,976	2.42	5.99	-	-	0.05	0.12
T-0020	1,588.4	0.0015	1.0	1.0		160.2	0.78	3,559	0.78	1.78	-	-	0.02	0.04
T-0021	1,588.4	0.0015	1.0	1.0		160.2	0.78	3,559	0.78	1.78	-	-	0.02	0.04
T-0022	2,287.3	0.0015	1.0	1.0		192.6	0.69	3,108	0.69	1.55	-	-	0.01	0.03
T-0023	2,287.3	0.0015	1.0	1.0		192.6	0.69	3,108	0.69	1.55	-	-	0.01	0.03
T-0056	30,574.3	0.0015	1.0	1.0		1,897.4	1.72	3,152	1.72	1.58	-	-	0.01	0.01
T-0079	2,644.2	0.0015	-	-	0.33	366.3	3.05	16,190	3.05	8.10	-	-	0.06	0.16
T-0106	3,805.7	0.0060	1.0	1.0	1.15	1,147.1	1.80	3,603	1.80	1.80	9.17E-05	1.51E-01	0.01	0.01
T-0107	5,091.3	0.0015	7.0	1.0		417.5	2.93	15,881	2.93	7.94	1.71E-09	7.64E-06	0.11	0.30
T-0108	4,453.4	0.0015	1.0	1.0		335.6	1.56	11,415	1.56	5.71	-	-	0.03	0.11
T-0109	5,496.7	0.0015	7.0	1.0		450.8	2.30	15,428	2.30	7.71	-	-	0.05	0.16
T-0111	4,212.6	0.0015	1.0	1.0		233.4	1.35	8,853	1.35	4.43	-	-	0.03	0.09
T-0112	93.1	0.0015	1.0	1.0		5.8	1.75	1,273	1.75	0.64	-	-	0.01	0.003
T-0117	4,008.3	0.0015	-	-	0.45	243.7	4.29	3,250	4.29	1.62	-	-	0.02	0.01
T-0124	10,310.9	0.0015	1.0	1.0		468.5	1.58	7,154	1.58	3.58	-	-	0.03	0.07
T-0401	4,509.4	0.0015	-	-	0.05	449.7	0.46	2,678	0.46	1.34	-	-	0.01	0.03
T-0402	5,475.7	0.0015	-	-	0.05	546.1	2.42	8,203	2.42	4.10	3.07E-08	8.52E-05	0.03	0.05
T-0411	2,285.5	0.0015	-	-	0.19	253.3	3.92	19,074	3.92	9.54	2.30E-09	9.18E-06	0.15	0.36

		V	VORKING (WITHD	RAWAL) LOSSES	5		MAXIMUM							
Tank ID	Sum of the Decreases in Liquid Level	Shell Clingage Factor	No. of Roof Support Columns	Effective Column Diameter	Working (Withdrawal) Loss Max Hourly	Working (Withdrawal) Loss	FLOATING	TOTAL FLOATING ROOF TANKS VOC LOSSES	VC Emiss		H2 Emiss		HA Emiss	
	ΣH _{QD}	Cs	N _c	F _c		L _w		L _T						
	ft/month	bbl/1,000 ft^2	ft	ft	lb/hr	lb/month	lb/hr	lb/month	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
	AP-42, Ch. 7.1, Eq. 2-20	AP-42, Ch. 7.1, Table 7.1-10	Site-Specific If unknown AP-42 Ch. 7.1 Eq. 2-19 Note 3 Table 7.1-11 (IFR)	AP-42, Ch. 7.1, Eq. 2-19 Note 4		AP-42, Ch. 7.1, Eq. 2-19	AP-42, Ch. 7.1 Eq. 2-1 & 2-2 (@ P*max)	AP-42, Ch. 7.1 Eq. 2-1 & 2-2			Raoult	s Law	Raoult	s Law
T-0412	923.5	0.0015			0.23	117.0	5.05	3,943	5.05	1.97			0.03	0.01
T-0412	7.846.2	0.0015	7.0	1.0	0.23	804.3	5.72	1,765	5.72	0.88			0.003	0.0004
T-0415	5,496.7	0.0015	1.0	1.0	0.41	414.2	1.66	7,285	1.66	3.64			0.003	0.0004
T-0417	4,045.7	0.0015	1.0	1.0	0.19	228.7	2.12	10,851	2.12	5.43	_	_	0.04	0.11
T-0418	6,687.8	0.0015	1.0	1.0	0.04	630.0	6.79	1,944	6.79	0.97	-	_	0.003	0.0004
T-0435	20,872.1	0.0060	-	_	0.32	2,775.6	0.88	4,732	0.88	2.37	4.51E-05	1.98E-01	0.004	0.01
T-0437	8,316.5	0.0060	-	-	1.41	5,608.7	2.64	10,139	2.64	5.07	1.35E-06	4.24E-03	0.03	0.05
T-0439	7,641.8	0.0015	8.0	1.0	0.27	1,168.6	3.14	13,093	3.14	6.55	8.34E-08	2.86E-04	0.08	0.17
T-0450	4,891.9	0.0015	-	-	0.34	650.5	4.49	16,631	4.49	8.32	1.19E-07	3.63E-04	0.11	0.21
T-0451	5,537.5	0.0015	1.0	1.0	0.07	280.1	1.98	602	1.98	0.30	1.16E-07	2.89E-05	0.001	0.0002
T-0452	830.6	0.0015	1.0	1.0	0.28	39.0	0.96	253	0.96	0.13	-	-	-	-
T-0737	9,015.6	0.0060	-	-	0.29	2,517.7	0.76	4,133	0.76	2.07	3.85E-05	1.73E-01	0.003	0.01
T-0802	17,670.5	0.0060	-	-	0.40	3,524.8	0.74	4,674	0.74	2.34	3.75E-05	1.95E-01	0.003	0.01
T-0821	4,068.2	0.0015	-	-	0.05	477.9	2.96	9,280	2.96	4.64	3.74E-08	9.64E-05	0.03	0.05
T-0834	15,527.7	0.0015	-	-	0.08	1,854.4	2.32	5,915	2.32	2.96	1.36E-07	2.84E-04	0.001	0.002
T-0835	9,105.4	0.0015	-	-	0.09	1,420.0	8.06	2,706	8.06	1.35	4.71E-07	1.30E-04	0.005	0.001
T-1225	12,105.8	0.0060	-	-	0.46	10,205.2	2.08	16,157	2.08	8.08	1.06E-06	6.75E-03	0.02	0.09
							MA	X. HOURLY, lb/hr	89.29		2.16E-04		1.09	
								ANNUAL, tpy		134.73		0.73		2.53

Maximum individual HAPs (n-Hexane), tpy = 0.06
Total HAPS (assumes 51.5% tanks landed per year), 0.08

HAPs	1,3- Butadiene	2,2,4- Trimethylp entane	Acenaphth ene	Acenaphth ylene	Anthracene	Benz(a)ant hracene	Benzene	Benzo(a)phe nanthrene	Benzo(a)py rene	Benzo(b)fl uoranthen e	Benzo(e)py rene	Benzo(g,h,i)perylene	Biphenyl	Cresol (mixed isomers)	Cumene	Ethylbenze ne	Fluoranthe ne	Fluorene	Lead compound s
CAS No.	106-99-0	540-84-1	83-32-9	208-96-8	120-12-7	56-55-3	71-43-2	218-01-9	50-32-8	205-99-2	192-97-2	191-24-2	92-52-4	1319-77-3	98-82-8	100-41-4	206-44-0	86-73-7	7439-92-1
Pi°, psia	57.00	0.79	4.26E-05	9.28E-05	1.16E-05	4.06E-09	2.01	1.21E-10	1.06E-10	9.67E-09	1.10E-10	1.93E-12	1.93E-04	0.00	0.12	0.22	1.78E-07	1.16E-05	0.03
Tank	Speciated F	otential to	Emit, tpy																
T-0011	6.47E-04	2.44E-03	-	-	3.61E-13	-	6.90E-04	-	-	-	-	-	2.54E-09	-	6.28E-06	1.13E-04	-	-	-
T-0012	6.12E-04	2.31E-03	-	-	3.42E-13	-	6.53E-04	-	-	-	-	-	2.41E-09	-	5.95E-06	1.07E-04	-	-	-
T-0020	6.09E-04	2.29E-03	-	-	3.40E-13	-	6.50E-04	-	-	-	-	-	2.40E-09	-	5.92E-06	1.06E-04	-	-	-
T-0021	6.09E-04	2.29E-03	-	-	3.40E-13	-	6.50E-04	-	-	-	-	-	2.40E-09	-	5.92E-06	1.06E-04	-	-	-
T-0022	4.23E-04	1.59E-03	-	-	2.36E-13	-	4.51E-04	-	-	-	-	-	1.66E-09	-	4.11E-06	7.36E-05	-	-	-
T-0023	4.23E-04	1.59E-03	-	-	2.36E-13	-	4.51E-04	-	-	-	-	-	1.66E-09	-	4.11E-06	7.36E-05	-	-	-
T-0056	-	3.30E-07	-	-	-	-	3.07E-05	-	-	-	-	-	-	-	1.08E-06	1.08E-05	-	-	-
T-0079	1.40E-03	5.27E-03	-	-	7.82E-13	-	1.49E-03	-	-	-	-	-	5.51E-09	-	1.36E-05	2.44E-04	-	-	-
T-0106	-	1.69E-07	6.59E-12	8.38E-12	6.39E-12	2.26E-17	3.69E-06	5.37E-19	5.33E-19	7.36E-17	8.16E-19	-	1.43E-09	1.36E-09	1.92E-08	2.30E-07	5.09E-15	2.64E-12	-
T-0107	6.52E-04	9.60E-06	-	-	-	-	6.59E-04	-	-	-	-	-	-	-	1.69E-06	1.72E-05	-	-	-
T-0108	3.99E-04	1.50E-03	-	-	2.23E-13	-	4.25E-04	-	-	-	-	-	1.57E-09	-	3.87E-06	6.95E-05	-	-	-
T-0109	3.94E-04	1.48E-03	-	-	2.20E-13	-	4.20E-04	-	-	-	-	-	1.55E-09	-	3.83E-06	6.86E-05	-	-	-
T-0111	2.10E-04	7.89E-04	-	-	1.17E-13	-	2.24E-04	-	-	-	-	-	8.25E-10	-	2.04E-06	3.65E-05	-	-	-
T-0112	-	3.29E-07	-	-	-	-	3.06E-05	-	-	-	-	-	-	-	1.07E-06	1.08E-05	-	-	-
T-0117	-	3.31E-07	-	-	-	-	3.08E-05	-	-	-	-	-	-	-	1.08E-06	1.08E-05	-	-	-
T-0124	1.24E-04	4.66E-04	-	-	6.90E-14	-	1.32E-04	-	-	-	-	-	4.86E-10	-	1.20E-06	2.15E-05	-	-	-
T-0401	6.48E-04	2.44E-03	-	-	3.61E-13	-	6.91E-04	-	-	-	-	-	2.55E-09	-	6.29E-06	1.13E-04	-	-	-
T-0402	2.40E-04	3.22E-05	8.48E-12	8.25E-11	-	-	5.68E-04	-	-	-	-	-	4.17E-10	-	2.43E-06	6.86E-05	-	-	-
T-0411	1.37E-03	2.02E-05	-	-	-	-	1.39E-03	-	-	-	-	-	-	-	3.55E-06	3.62E-05	-	-	-
T-0412	-	1.43E-06	-	-	-	-	1.33E-04	-	-	-	-	-	-	-	4.68E-06	4.69E-05	-	-	-
T-0413	-	3.54E-06	-	-	-	-	3.09E-06	-	-	-	-	-	3.04E-11	-	3.19E-07	2.42E-06	-	-	-
T-0415	3.45E-04	1.30E-03	-	-	1.92E-13	-	3.67E-04	-	-	-	-	-	1.36E-09	-	3.35E-06	6.00E-05	-	-	-
T-0417	2.01E-04	7.58E-04	-	-	1.12E-13	-	2.15E-04	-	-	-	-	-	7.92E-10	-	1.96E-06	3.51E-05	-	-	-
T-0418	-	3.79E-06	-	-	-	-	3.31E-06	-	-	-	-	-	3.25E-11	-	3.42E-07	2.59E-06	-	-	-
T-0435	-	3.29E-08	1.29E-12	1.63E-12	1.25E-12	4.41E-18	7.20E-07	1.05E-19	1.04E-19	1.44E-17	1.59E-19	-	2.79E-10	2.64E-10	3.75E-09	4.49E-08	9.93E-16	5.16E-13	-
T-0437	-	2.13E-06	1.24E-12	1.88E-12	2.14E-13	5.85E-16	1.60E-05	6.40E-18	1.53E-17	1.96E-15	4.33E-18	3.12E-20	2.28E-10	-	1.42E-07	1.79E-06	3.66E-15	1.96E-12	2.69E-13
T-0439	-	2.86E-05	-	-	-	-	1.94E-03	-	-	-	-	-	2.49E-09	-	1.27E-05	1.02E-04	-	-	-
T-0450	-	2.40E-05	-	-	-	-	1.63E-03	-	-	-	-	-	2.10E-09	-	1.06E-05		-	-	-
T-0451	-	-	-	-	4.45E-10	-	1.03E-06	-	-	-	-	-	4.99E-11	-	5.80E-08	2.27E-07	-	-	-
T-0452	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
T-0737	-	1.45E-07	5.67E-12		5.51E-12	1.95E-17	3.18E-06	4.62E-19	4.59E-19	6.34E-17	7.02E-19	-	1.23E-09		1.65E-08		4.38E-15	2.28E-12	-
T-0802	-	7.42E-08	2.89E-12	3.68E-12	2.81E-12	9.92E-18	1.62E-06	2.36E-19	2.34E-19	3.23E-17	3.58E-19	-	6.28E-10	5.95E-10	8.43E-09	1.01E-07	2.24E-15	1.16E-12	-
T-0821	3.03E-04	4.06E-05	1.07E-11	1.04E-10		-	7.17E-04	-	-	-	-	-	5.27E-10	-	3.07E-06	8.66E-05	-	-	-
T-0834	-	-	-	-	2.84E-09	-	6.55E-06	-	-	-	-	-	3.18E-10	-	3.70E-07	1.45E-06	-	-	-
T-0835	-	-	-	-	4.88E-09	-	1.13E-05	-	-	-	-	-	5.48E-10	-	6.37E-07	2.49E-06	-	-	-
T-1225	-	3.31E-06	1.92E-12	2.92E-12	3.33E-13	9.09E-16	2.49E-05	9.94E-18	2.38E-17	3.04E-15	6.73E-18	4.84E-20	3.54E-10	-	2.21E-07	2.78E-06	5.69E-15	3.05E-12	4.18E-13
Sum HAPs, tpy	9.61E-03	2.67E-02	3.88E-11	2.12E-10	8.19E-09	1.55E-15	1.47E-02	1.77E-17	4.04E-17	5.18E-15	1.31E-17	7.96E-20	3.84E-08	3.38E-09	1.12E-04	1.72E-03	2.21E-14	1.16E-11	6.87E-13

 $\begin{aligned} \text{Raoult's Law} & P_i = x_i * \text{TVP}_i \\ P_i = y_i * \text{TVP} \\ y_i = x_i * \text{TVP}_i / \text{TVP} \\ y_i = x_i * \text{TVP}_i / \text{TVP} \end{aligned}$ Liquid molar fraction $\text{xi (mole}_i / \text{mole}_T) = \text{mi (g}_i / \text{g}_T) * \text{MW}_{iiq} \left(\text{g}_T / \text{moles}_T \right) / \text{MW}_i \left(\text{g}_i / \text{moles}_i \right) = \text{wt\%}_{iiq} * \text{MW}_{iiq} / \text{MW}_i \\ \text{Gas molar fraction} & \text{yi (mole}_i / \text{mole}_T) = \text{mi (g}_i / \text{g}_T) * \text{MW}_{vap} \left(\text{g}_T / \text{moles}_T \right) / \text{MW}_i \left(\text{g}_i / \text{moles}_i \right) = \text{wt\%}_{vap} * \text{MW}_{vap} / \text{MW}_i \\ & \text{yi = xi * TVPi/TVP} \\ \text{wt\%}_{vap} * \text{MW}_{vap} / \text{MWi} = \text{wt\%}_{iiq} * \text{MW}_{iiq} / \text{MW}_i * \text{TVPi/TVP} \\ \text{wt\%}_{vap} = \text{wt\%}_{iiq} * \text{TVP}_i / \text{TVP} * \text{MW}_{iiq} / \text{MW}_{vap} \end{aligned}$

m-Cresol	Mercury compound s	Methanol	Methyl tert butyl ether	m-Xylene	Naphthale ne	n-Hexane	o-Cresol	o-Xylene	PAH Total	Phenanthr ene	p-Xylene	Pyrene	Styrene	Toluene	Xylene (mixed isomers)
108-39-4	7439-97-6	67-56-1	1634-04-4	108-38-3	91-20-3	110-54-3	95-48-7	95-47-6	30-31-1	85-01-8	106-42-3	129-00-0	100-42-5	108-88-3	1330-20-7
2.13E-03	2.32E-05	2.70	5.30	0.16	0.01	3.14	3.48E-03	0.13	1.93E-12	2.34E-06	0.17	8.70E-08	0.12	0.60	0.20
-	-	6.29E-06	4.36E-05	1.32E-04	3.18E-07	1.09E-03	-	8.49E-05	1.78E-16	8.32E-14	8.28E-05	-	1.06E-05	1.76E-03	7.00E-04
-	-	5.95E-06	4.13E-05	1.25E-04	3.01E-07	1.03E-03	-	8.04E-05	1.68E-16	7.88E-14	7.83E-05	-	1.01E-05	1.67E-03	6.63E-04
-	-	5.92E-06	4.11E-05	1.24E-04	3.00E-07	1.03E-03	-	7.99E-05	1.67E-16	7.83E-14	7.79E-05	-	1.00E-05	1.66E-03	6.59E-04
-	-	5.92E-06	4.11E-05	1.24E-04	3.00E-07	1.03E-03	-	7.99E-05	1.67E-16	7.83E-14	7.79E-05	-	1.00E-05	1.66E-03	6.59E-04
-	-	4.11E-06	2.85E-05	8.62E-05	2.08E-07	7.12E-04	-	5.55E-05	1.16E-16	5.44E-14	5.41E-05	-	6.94E-06	1.15E-03	4.58E-04
-	-	4.11E-06	2.85E-05	8.62E-05	2.08E-07	7.12E-04	-	5.55E-05	1.16E-16	5.44E-14	5.41E-05	-	6.94E-06	1.15E-03	4.58E-04
-	-	9.68E-06	1.94E-05	1.53E-05	-	2.88E-05	-	1.20E-07	-	-	1.34E-05	-	-	1.42E-04	2.09E-05
-	-	1.36E-05	9.44E-05	2.86E-04	6.89E-07	2.36E-03	-	1.84E-04	3.85E-16	1.80E-13	1.79E-04	-	2.30E-05	3.82E-03	1.52E-03
8.28E-10	-	4.95E-06	-	1.05E-06	2.46E-09	8.09E-06	1.35E-09	2.17E-07	-	8.92E-13	-	-	-	1.56E-06	4.25E-07
-	4.84E-15	-	-	4.35E-05	-	6.43E-03	-	1.43E-05	-	-	1.54E-05	-	-	2.45E-04	-
-	-	3.88E-06	2.69E-05	8.14E-05	1.96E-07	6.72E-04	-	5.23E-05	1.10E-16	5.13E-14	5.10E-05	-	6.55E-06	1.09E-03	4.32E-04
-	-	3.83E-06	2.66E-05	8.04E-05	1.94E-07	6.64E-04	-	5.17E-05	1.08E-16	5.07E-14	5.04E-05	-	6.47E-06	1.07E-03	4.27E-04
-	-	2.04E-06	1.41E-05	4.28E-05	1.03E-07	3.53E-04	-	2.75E-05	5.77E-17	2.70E-14	2.68E-05	-	3.44E-06	5.71E-04	2.27E-04
-	-	9.65E-06	1.93E-05	1.52E-05	-	2.87E-05	-	1.19E-07	-	-	1.34E-05	-	-	1.41E-04	2.08E-05
-	-	9.71E-06	1.94E-05	1.53E-05	-	2.89E-05	-	1.20E-07	-	-	1.34E-05	-	-	1.42E-04	2.09E-05
-	-	1.20E-06	8.34E-06	2.52E-05	6.09E-08	2.08E-04	-	1.62E-05	3.40E-17	1.59E-14	1.58E-05	-	2.03E-06	3.37E-04	1.34E-04
-	-	6.29E-06	4.37E-05	1.32E-04	3.19E-07	1.09E-03	-	8.50E-05	1.78E-16	8.33E-14	8.28E-05	-	1.06E-05	1.76E-03	7.01E-04
-	-	-	5.91E-04	9.92E-05	2.43E-07	1.78E-03	-	6.01E-06	-	-	4.78E-05	-	-	-	2.65E-04
-	1.02E-14	-	-	9.15E-05	-	1.35E-02	-	3.02E-05	-	-	3.24E-05	-	-	5.16E-04	-
-	-	4.20E-05	8.42E-05	6.63E-05	-	1.25E-04	-	5.20E-07	-	-	5.82E-05	-	-	6.14E-04	9.07E-05
-	-	-	-	2.30E-06	1.08E-06	1.17E-05	-	-	-	-	1.17E-06	-	-	5.04E-06	5.57E-06
-	-	3.35E-06	2.32E-05	7.03E-05	1.70E-07	5.81E-04	-	4.52E-05	9.48E-17	4.43E-14	4.41E-05	-	5.66E-06	9.39E-04	3.73E-04
-	-	1.96E-06	1.36E-05	4.11E-05	9.91E-08	3.39E-04	-	2.64E-05	5.54E-17	2.59E-14	2.58E-05	-	3.31E-06	5.49E-04	2.18E-04
-	-	-	-	2.47E-06	1.16E-06	1.25E-05	-	-	-	-	1.26E-06	-	-	5.40E-06	5.97E-06
1.62E-10	-	9.66E-07	-	2.05E-07	4.80E-10	1.58E-06	2.64E-10	4.23E-08	-	1.74E-13	-	-	-	3.05E-07	8.29E-08
-	3.64E-16	-	-	3.67E-06	6.10E-09	1.48E-04	-	1.52E-07	-	-	9.33E-07	3.95E-15	-	1.27E-05	4.58E-06
-	7.47E-16	1.20E-04	3.73E-04	2.76E-04	2.27E-08	1.45E-02	-	7.31E-05	-	-	9.85E-05	-	-	1.46E-03	2.38E-04
-	6.29E-16	1.01E-04	3.14E-04	2.32E-04	1.91E-08	1.22E-02	-	6.15E-05	-	-	8.29E-05	-	-	1.23E-03	2.00E-04
-	-	-	-	4.96E-06	1.97E-08	3.76E-07	-	1.79E-08	5.44E-17	9.25E-14	3.65E-06	-	-	9.09E-07	1.08E-06
-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
7.13E-10	-	4.26E-06	-	9.06E-07	2.12E-09	6.97E-06	1.17E-09	1.87E-07	-	7.68E-13	-	-	-	1.35E-06	3.66E-07
3.64E-10	-	2.17E-06	-	4.62E-07	1.08E-09	3.55E-06	5.95E-10	9.51E-08	-	3.92E-13	-	-	-	6.87E-07	1.87E-07
-	-	-	7.46E-04	1.25E-04	3.06E-07	2.25E-03	-	7.59E-06	-	-	6.03E-05	-	-	-	3.35E-04
-	-	-	-	3.16E-05	1.26E-07	2.40E-06	-	1.14E-07	3.47E-16	5.89E-13	2.33E-05	-	-	5.79E-06	6.88E-06
-	-	-	-	5.44E-05	2.17E-07	4.13E-06	-	1.97E-07	5.97E-16	1.02E-12	4.01E-05	-	-	9.98E-06	1.19E-05
-	5.65E-16	-	-	5.71E-06	9.47E-09	2.30E-04	-	2.36E-07	-	-	1.45E-06	6.14E-15	-	1.97E-05	7.12E-06
2.07E-09	1.73E-14	3.74E-04	2.64E-03	2.52E-03	6.69E-06	6.31E-02	3.38E-09	1.12E-03	2.94E-15	4.83E-12	1.41E-03	1.01E-14	1.16E-04	2.37E-02	8.86E-03

TANKS POTENTIAL TO EMIT GHG

$$CH_4 = 0.1 \times Q_{Ref}$$

CH ₄	6.05	ton/yr	1.10231 tons/metric ton, Table A-2 to Subpart
C11 ₄	0.03	tony yr	A of Part 98
CH₄	5.49	metric ton/yr	40 CFR §98.253(m)(1) equation Y-22 annual
CII4	3.49	metric tonyyi	methane emissions from storage tanks
FF	0.10	metric ton _{CH4} /MMbbl	40 CFR §98.253(m)(1) default emission factor
E F	0.10	THECHIC COHCH4/ IVIIVIDDI	for storage tanks
			Quantity of crude oil plus the quantity of
Q _{ref}	54.86	MMbbl/yr	intermediate products received from off site
			that are processed at the facility

SSM POTENTIAL TO EMIT SUMMARY

Unit No.	Description	N	O _X	С	0	V	oc	S	O ₂	P	М	PN	/ 1 ₁₀	PN	1 _{2.5}	Н	I ₂ S
Offit NO.	Description	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
	Startup and Shutdown Emissions from																
SSM H-9851	Unit 64 Hydrogen Plant Reformer	11.23	1.35	20.22	2.43	2.02	0.24	6.32	0.30	2.79	0.33	2.79	0.33	2.79	0.33	-	-
	(SCR downtime)																
SSM H-0473	Startup and Shutdown Emissions from	6.50	0.03	27.70	0.12	0.10	4.50E-04	135.00	0.38	1.20	0.0054	11.53	0.03	11.53	0.03	1.44	4.00E-03
(SRU2 TGI)	the SRU2 TGI	0.50	0.03	27.70	0.12	0.10	4.30E-04	155.00	0.56	1.20	0.0054	11.55	0.03	11.55	0.03	1.44	4.006-03
SSM H-3103	Startup and Shutdown Emissions from	6.50	0.03	15.00	0.07	0.10	4.50E-04	50.00	0.23	1.10	0.0050	4.93	0.02	4.93	0.02	0.53	2.39E-03
(SRU3 TGI)	the SRU3 TGI	0.50	0.03	15.00	0.07	0.10	4.30E-04	30.00	0.23	1.10	0.0030	4.93	0.02	4.93	0.02	0.55	2.39E-03
	Emissions from venting MSS activity																
SSM Flare Cap	gases to FL-400, FL-401, FL-402, FL-403,	162.90	18.30	1,243.00	77.00	1,376.3	68.70	1,133.40	14.90							12.04	0.16
	or FL-404																
	Holly Energy Partners (HEP) control																
SSM FL-HEP-PORT	flare for pipeline mainteance and	11.56	0.09	50.12	0.38	106.70	0.80	0.11	8.24E-04							1.19E-03	8.93E-06
	pigging activities																
SSM Tanks	Storage tanks (roof landings)					51.90	8.09									0.02	3.60E-03
SSM T-0737	Sour water tank roof landing					0.24	4.24E-03									0.02	7.33E-04
SSM Tank VCU	Floating roof tanks landings control	0.17	0.037	0.17	0.033	2.60	0.21	0.05	0.017	9.39E-03	2.50E-03	9.39E-03	2.50E-03	9.39E-03	2.50E-03	1.24E-03	9.26E-05
SSM Misc 1	Catalyst handling activities											Ехе	mpt				
SSM Misc 2	Low-emitting maintenance activities	17.00	1.90	127.10	7.80	137.70	6.90	129.30	1.60	0.06	0.02	0.06	0.02	0.06	0.02	0.70	0.10
SSM Pigging	Crude Oil Pigging					24.57	0.64										
SSM Cap		215.87	21.73	1,483.31	87.83	1,701.98	85.58	1,454.18	17.42	5.16	0.37	19.32	0.41	19.32	0.41	14.74	0.27
Malfunction Cap			10.00		10.00		10.00		10.00		-		-		-		1.00
	TOTAL		31.73		97.83		95.58		27.42		0.37		0.41		0.41		1.27

H-9851 STARTUP AND SHUTDOWN EMISSIONS

Routine or Predictable Startup, Shtudown, and Scheduled Maintenance (SSM) Emissions

		Design	Design				E	mission Factors ^a	l							S	SM Poten	itial to Em	nit			
		Capacity (LHV)	Capacity (HHV)	со	NO _x	PM/PM ₁₀ / PM _{2.5}		:	SO ₂			voc	C	:0	N	O _x	PM/PM	₁₀ /PM _{2.5}	S	02	V	ос
ID	Description	(2110)	(11117)			/ PIVI _{2.5}	H2S	non-H2S Sulfur		non-H2S	\vdash											1
		MMBtu/hr	MMBtu/hr	lb/MMBtu	MMBtu lb/MMBtu lb/MM			Species	H2S avg gr/dscf	Sulfur Species		lb/MMBtu	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
H-9851	Unit 64 Hydrogen Plant	337	374	0.060 k	0.03	0.0075	-	0.00032	-	0.00032		0.0054	20.2	2.4	11.2	1.2	2.8	0.2	6.3	0.3	2.0	0.2
11-3631	Reformer	337	374	0.000	0.03	0.0073	0.10	0.00391	0.037	0.00391		0.0034	20.2	2.4	11.2	1.5	2.0	0.3	0.5	0.3	2.0	0.2

Notes:

a. Unless otherwise noted, the emission factors are from AP-42 Tables 1.4-1 and 1.4-2, dated 7/98. Factors are converted to lb/MMBtu by dividing by 1020 Btu/scf as specified in AP-42 and are based on HHV.

b. Based on manufacturer guarantee on LHV basis.

c. H-9851 will combust a mixture of PSA Offgas and amine-treated refinery fuel gas (RFG). It has been conservatively assumed 50/50 mix for SO2 emissions calculation.

d. Expected annual hours during H-9851 SCR downtime (SSM hours per year) = 240

SRUS STARTUP AND SHUTDOWN EMISSIONS

		H-0473	(SRU2 TGI)	H-3103 (SR	U3 TGI)
		Startup	Shutdown	Startup	Shutdown
Sulfur Feed	lbmol/event	52.7	9.6	19.5	6.2
Duration	hr/event	1	8	1	8
Sulfur Recovery Efficiency		96%		96%	
Unconverted H2S		2%	2%	2%	2%

Pollutant	MW			H-0473 (SRU2 TGI)		
Pollutalit	IVIVV	Sta	rtup	Shut	down	SS	M
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
NOx	46	6.5	0.003	6.5	0.03	6.5	0.03
СО	28	27.7	0.01	27.7	0.11	27.7	0.12
VOC	44	0.1	0.0001	0.1	0.0004	0.1	4.50E-04
SO2	64	135.0	0.1	77.0	0.3	135.0	0.4
H2S	34	1.4	0.001	0.8	0.003	1.4	4.00E-03
SAM	98	10.3	0.01	5.9	0.02	10.3	0.03
PM	-	1.2	0.001	1.2	0.005	1.2	0.01
PM ₁₀ /PM _{2.5}	-	11.5	0.01	7.1	0.03	11.5	0.03

Dallatant	B 4347			H-3103 (SRU3 TGI)		
Pollutant	MW	Sta	rtup	Shut	down	SS	SM
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
NOx	46	6.5	0.003	6.5	0.03	6.5	0.03
СО	28	15.0	0.01	15.0	0.06	15.0	0.07
VOC	44	0.1	0.0001	0.1	0.0004	0.1	4.50E-04
SO2	64	50.0	0.03	50.0	0.2	50.0	0.2
H2S	34	0.5	0.0003	0.5	0.002	0.5	2.39E-03
SAM	98	3.8	0.002	3.8	0.02	3.8	0.02
PM	-	1.1	0.001	1.1	0.004	1.1	0.005
PM ₁₀ /PM _{2.5}	-	4.9	0.002	4.9	0.02	4.9	0.02

Notes

(1) NO_{xy} CO, VOC and PM emissions during SSM are expected to be within the proposed limits for normal operations

(2) SAM assumed 5% conversion SO2 to SO3 and 100% SO3 to H2SO4. $PM_{10}/PM_{2.5}$ assumed to be PM + SAM

Sample Calculation H-0473 (SRU 2 TGI)

Houlry SO2 Startup = 52.7 lbmol/event / 1 hr/event * 64 lb/lbmol * (1 - 0.96) = 135.0 lb/hr Annual SO2 Startup = 135.0 lb/hr * 1 hr/event * 1 event/yr * 1 ton/2,000 lb = 0.1 ton/yr Houlry SO2 Shutdown = 9.6 lbmol/event / 8 hr/event * 64 lb/lbmol = 77.0 lb/hr Annual SO2 Shutdown = 77.0 lb/hr * 8 hr/event * 1 event/yr * 1 ton/2,000 lb = 0.3 ton/yr

Houlry H2S Startup = 52.7 lbmol/event / 1 hr/event * 34 lb/lbmol * (1 - 0.96) * 0.02 = 1.4 lb/hr Annual H2S Startup = 1.4 lb/hr * 1 hr/event * 1 event/yr * 1 ton/2,000 lb = 0.001 ton/yr Houlry H2S Shutdown = 9.6 lbmol/event / 8 hr/event * 34 lb/lbmol * 0.02 = 0.8 lb/hr Annual H2S Startup = 0.8 lb/hr * 8 hr/event * 1 event/yr * 1 ton/2,000 lb = 0.003 ton/yr

FLARES STARTUP AND SHUTDOWN EMISSIONS

FLARES SSM

Emission Calculations for Proposed Permit 0195-M40 Emission Limits - SSM

	NO _x	СО	voc	SO ₂	H ₂ S
			lb/hr		
PROPOSED SSM CAP:	162.9	1,243.0	1,376.3	1,133.4	12.0
CURRENT SSM CAP:	162.9	1,243.0	1,376.3	1,133.4	0.4
PROPOSED CAP INCREASE:	0.0	0.0	0.0	0.0	11.6
			tpy		
PROPOSED SSM CAP:	18.3	77.0	68.7	14.9	0.2
CURRENT SSM CAP:	18.3	77.0	68.7	14.9	0.1
PROPOSED CAP INCREASE:	0.0	0.0	0.0	0.0	0.1

FL-HEP-PORT STARTUP AND SHUTDOWN EMISSIONS

Holly Energy Partners (HEP) control flare for pipeline mainteance and pigging activities

Parameter	Value	Units	Reference
Flaring Event Duration	15.00	hr	
Flaring Flowrate (Flare _p)	2,500,000	scf	Total estimated flow to flare per event
	170	MMBtu/hr (HHV)	MMBtu/hr = Flow (scf/event) / Duration (hr/event) *
	162	MMBtu/hr (LHV)	Heat Content (Btu/scf) * 1 MMBtu/1,000,000 Btu
Natural gas heat content (HHV _p)	1,020	Btu/scf (HHV)	
	970	Btu/scf (LHV)	
Flare Destruction Efficiency	98%		
NO _X Emission Factor	0.068	lb/MMBtu (HHV)	AP-42, Ch. 13.5 (2/2018), Table 13.5-1
CO Emission Factor	0.31	lb/MMBtu (LHV)	AP-42, Ch. 13.5 (2/2018), Table 13.5-2
VOC Emission Factor	0.66	lb/MMBtu (LHV)	AP-42, Ch. 13.5 (2/2018), Table 13.5-2
H ₂ S in Natural Gas	0.25	gr/100 dscf	
CO ₂ Emission Factor	60	kg/MMBtu (HHV)	40 CFR §98.253(b)(1), default flare gas
CH₄ Emission Factor	1.00E-03	kg/MMBtu (HHV)	Table C-2 to Subpart C to Part 98, Natural Gas
N ₂ O Emission Factor	1.00E-04	kg/MMBtu (HHV)	Table C-2 to Subpart C to Part 98, Natural Gas
Metric tons to short tons	1.10231	short ton/metric ton	Table A-2 to Subpart C of Part 98
Weight Fraction of Carbon in Flare	0.40	kg/kg	40 CFR §98.253(b)(1), default flare gas
Gas (f _{CH4})	0.40	Ng/ Ng	40 CFN 938.233(b)(1), detault flate gas
CO ₂ GWP	1		Table A-1 to Subpart C of Part 98
CH₄ GWP	25		Table A-1 to Subpart C of Part 98
N₂O GWP	298		Table A-1 to Subpart C of Part 98

Flare	N(Ох	С	0	V	oc	SC	D2	Н	₂ S	CO2	CH4	N2O	CO2e
riale	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	ton/yr	ton/yr	ton/yr	ton/yr
FL-HEP-PORT	11.56	0.09	50.12	0.38	106.70	0.80	0.1	0.001	1.19E-03	8.93E-06	165.3	0.54	3.04E-04	179.0

Notes:

(1) GHG emissions per 40 CFR Part 98, Subpart Y:

Eq. Y-2
$$CO_2 = 0.98 \times 0.001 \times \sum_{p=1}^{n} Flare_p \times HHV_p \times EF_{CO2}$$
 Eq. Y-4
$$CH_4 = \left(CO_2 \times \frac{EF_{CH_4}}{EF_{CO_2}}\right) + \left(CO_2 \times \frac{0.02}{0.98} \times \frac{16}{44} \times f_{CH_4}\right)$$
 Eq. Y-5
$$N_2O = CO_2 \times \frac{EF_{N_2O}}{EF_{CO_2}}$$

Where

Flare_o: volume of flare gas combusted (scf)

HHVp: Higher heating value for the flare gas combusted during measurement period (Btu/scf)

EF_{CO2}: default CO2 emissionf actor for flare gas:

EF_{CH4}: default emission factor for fuel gas for CH4, per Table C-2 to Part 98:

EF_{N2O}: default emission factor for fuel gas for N2O, per Table C-2 to Part 98:

 f_{CH4} : weight fraction of carbon in the flare gas, monitored or default 0.4 $kg_{\text{CCH4}}/kg_{\text{Cflaregas}}$

Tank ID	Stor	red Commodity	H2S in Liquid	Type of Landing	Number of Days Tank Stands Idle	Deck Leg Height at the Tank Shell	Height of Liquid at the Tank Shell	VCU Capture Efficiency
	CHEMICAL NAME FOR VOC LOSSES CALCULATION	CHEMICAL NAME FOR HAPS LOSSES SPECIATION	H2S _{liq}		n _d days/event	h _d	h _i	%
			API 4723A	Full Heel Partial Heel Drain Dry		Gauge Height - Height Roof Landed	AP-42 Ch. 7.1 Table 7.1-4 Figure 7.1-23 Figure 7.1-24	
T-0011	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0012	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0020	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0021	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0022	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0023	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0056	Sweet Naphtha	Catalytic Hydrocracker - Heavy H/C Naphtha	-	Drain Dry	1.00	6.00	0.25	
T-0079	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0106	Sour Water	Various Units - Slop Oil	3,200	Drain Dry	1.00	6.00	0.25	98.7%
T-0107	Gasolines & Gasoline Blendstocks	Atmospheric Distillation - Straight Run Gasoline	0.03	Drain Dry	1.00	6.00	0.25	
T-0108	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0109	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0111	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0112	Sweet Naphtha	Catalytic Hydrocracker - Heavy H/C Naphtha	-	Drain Dry	1.00	6.00	0.25	
T-0117	Sweet Naphtha	Catalytic Hydrocracker - Heavy H/C Naphtha	-	Drain Dry	1.00	6.00	0.25	
T-0124	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0401	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	

Tank ID	Sto	red Commodity	H2S in Liquid	Type of Landing	Number of Days Tank Stands Idle	Deck Leg Height at the Tank Shell	Height of Liquid at the Tank Shell	VCU Capture Efficiency
	CHEMICAL NAME FOR VOC LOSSES		H2S _{liq}		n _d	h _d	hı	
	CALCULATION	CHEMICAL NAME FOR HAPS LOSSES SPECIATION	ppm		days/event	ft	ft	%
			API 4723A	Full Heel Partial Heel Drain Dry		Gauge Height - Height Roof Landed	AP-42 Ch. 7.1 Table 7.1-4 Figure 7.1-23 Figure 7.1-24	
T-0402	Light Cat Naphtha	Fluid Catalytic Cracker - Cracked Gasoline	0.80	Drain Dry	1.00	6.00	0.25	
T-0411	Gasolines & Gasoline Blendstocks	Atmospheric Distillation - Straight Run Gasoline	0.03	Drain Dry	1.00	6.00	0.25	
T-0412	Sweet Naphtha	Catalytic Hydrocracker - Heavy H/C Naphtha	-	Drain Dry	1.00	6.00	0.25	
T-0413	Straight Run Kerosene	Atmospheric Distillation - Straight Run Kerosene	-	Drain Dry	1.00	6.00	0.25	
T-0415	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0417	Gasolines & Gasoline Blendstocks	Gasoline Blending - Conventional Gasoline	-	Drain Dry	1.00	6.00	0.25	
T-0418	Straight Run Kerosene	Atmospheric Distillation - Straight Run Kerosene	-	Drain Dry	1.00	6.00	0.25	
T-0435	Sour Water	Various Units - Slop Oil	3,200	Drain Dry	1.00	6.00	0.25	98.7%
T-0437	Crude Oil	Supply System - Crude Oil	12.50	Drain Dry	1.00	6.00	0.25	98.7%
T-0439	Sour Naphtha	Atmospheric Distillation - Straight Run Naphtha	1.67	Drain Dry	1.00	6.00	0.25	
T-0450	Sour Naphtha	Atmospheric Distillation - Straight Run Naphtha	1.67	Drain Dry	1.00	6.00	0.25	
T-0451	Straight Run Diesel	Distillate Blending - Diesel Fuel	3.54	Drain Dry	1.00	6.00	0.25	
T-0452	Ethanol	-	-	Drain Dry	1.00	6.00	0.25	
T-0737	Sour Water	Various Units - Slop Oil	3,200	Drain Dry	1.00	6.00	0.25	98.7%
T-0802	Sour Water	Various Units - Slop Oil	3,200	Drain Dry	1.00	6.00	0.25	98.7%
T-0821	Light Cat Naphtha	Fluid Catalytic Cracker - Cracked Gasoline	0.80	Drain Dry	1.00	6.00	0.25	
T-0834	Straight Run Diesel	Distillate Blending - Diesel Fuel	3.54	Drain Dry	1.00	6.00	0.25	
T-0835	Straight Run Diesel	Distillate Blending - Diesel Fuel	3.54	Drain Dry	1.00	6.00	0.25	
T-1225	Crude Oil	Supply System - Crude Oil	12.50	Drain Dry	1.00	6.00	0.25	98.7%

		TA	NK CHARACTERI	STICS			TANK PAINT							
Tank ID	Tank Type	Tank Insulated	Tank Construction	Tank Diameter	Tank Shell Height	Shell Capacity	Tank Shell Paint	Tank Roof Paint	Shell Paint Condition	Roof Paint Condition	Internal Shell Condition			
				D	Hs									
				ft	ft	gallons								
	CR DM HFR	YES-ALL-CTE YES-ALL-CYCLE YES-SHELL NO	Riveted-Bolted Welded	HFR: diam of vertical cross-section	HFR: length				New Average Aged	New Average Aged	Light Rust Dense Rust Gunite Lining			
T-0011	INT	NO	Welded	89.0	29.0	1,349,460	White	White	New	New	Light Rust			
T-0012	INT	NO	Welded	89.0	29.0	1,349,460	White	White	New	New	Light Rust			
T-0020	INT	NO	Welded	90.0	48.0	2,283,960	White	White	New	New	Light Rust			
T-0021	INT	NO	Welded	90.0	48.0	2,283,960	White	White	New	New	Light Rust			
T-0022	INT	NO	Welded	75.0	48.0	1,586,340	White	White	New	New	Light Rust			
T-0023	INT	NO	Welded	75.0	48.0	1,586,340	White	White	New	New	Light Rust			
T-0056	INT	NO	Welded	48.0	36.0	487,200	White	White	Average	Average	Light Rust			
T-0079	EXT	NO	Welded	125.0	40.0	3,671,640	White	White	New	New	Light Rust			
T-0106	INT	NO	Welded	67.0	40.0	1,055,040	White	White	New	New	Light Rust			
T-0107	INT	NO	Welded	67.0	40.0	1,055,040	White	White	New	New	Light Rust			
T-0108	INT	NO	Welded	67.0	40.0	1,055,040	White	White	Average	Average	Light Rust			
T-0109	INT	NO	Welded	67.0	40.0	1,055,040	White	White	Aged	Aged	Light Rust			
T-0111	INT	NO	Welded	49.0	30.0	423,360	White	White	Aged	Aged	Light Rust			
T-0112	INT	NO	Welded	48.0	30.0	406,140	White	White	Average	Average	Light Rust			
T-0117	EXT	NO	Welded	48.0	48.0	649,740	White	White	New	New	Light Rust			
T-0124	INT	NO	Welded	40.0	30.0	281,820	White	White	New	New	Light Rust			
T-0401	EXT-GEO	NO	Welded	90.0	50.0	2,379,300	White	White	New	New	Light Rust			

		TA	NK CHARACTERI	STICS				TANK PA	INT		
Tank ID	Tank Type	Tank Insulated	Tank Construction	Tank Diameter	Tank Shell Height	Shell Capacity	Tank Shell Paint	Tank Roof Paint	Shell Paint Condition	Roof Paint Condition	Internal Shell Condition
	,,			D	Hs						
				ft	ft	gallons					
	CR DM HFR	YES-ALL-CTE YES-ALL-CYCLE YES-SHELL NO	Riveted-Bolted Welded	HFR: diam of vertical cross-section	HFR: length				New Average Aged	New Average Aged	Light Rust Dense Rust Gunite Lining
T-0402	EXT	NO	Welded	90.0	50.0	2,379,300	White	White	New	New	Light Rust
T-0411	EXT	NO	Welded	100.0	40.0	2,349,900	White	White	Average	Average	Light Rust
T-0412	EXT	NO	Welded	100.0	40.0	2,349,900	White	White	Average	Average	Light Rust
T-0413	INT	NO	Welded	67.0	39.0	1,028,580	White	White	New	New	Light Rust
T-0415	INT	NO	Welded	67.0	40.0	1,055,040	White	White	New	New	Light Rust
T-0417	INT	NO	Welded	50.0	30.0	440,580	White	White	Aged	Aged	Light Rust
T-0418	INT	NO	Welded	67.0	33.0	870,240	White	White	New	New	Light Rust
T-0435	EXT	NO	Welded	30.0	40.0	211,680	White	White	New	New	Light Rust
T-0437	EXT	NO	Welded	120.0	45.0	3,806,880	White	White	New	New	Light Rust
T-0439	INT	NO	Welded	130.0	46.0	4,567,080	White	White	Average	Average	Light Rust
T-0450	EXT	NO	Welded	120.0	40.0	3,383,940	White	White	New	New	Light Rust
T-0451	INT	YES-ALL-CTE	Welded	35.0	40.0	287,700	Aluminum - Specular	Aluminum - Specular	Average	Average	Light Rust
T-0452	INT	NO	Welded	35.0	40.0	287,700	White	White	Average	Average	Light Rust
T-0737	EXT	NO	Welded	63.0	40.0	932,820	White	White	New	New	Light Rust
T-0802	EXT	NO	Welded	45.0	40.0	475,860	White	White	New	New	Light Rust
T-0821	EXT	NO	Welded	106.0	50.0	3,300,360	White	White	Average	Average	Light Rust
T-0834	EXT	NO	Welded	85.0	40.0	1,697,640	White	White	Average	Average	Light Rust
T-0835	EXT	NO	Welded	111.0	40.0	2,895,480	White	White	Average	Average	Light Rust
T-1225	EXT	NO	Welded	150.0	40.0	5,287,380	White	White	Average	Average	Light Rust

Tank ID		CHEMICAL PROP	ERTIES		METEOROLOGICAL DATA						
	Product Category	Liquid Molecular Weight	Vapor Molecular Weight	Density of the Liquid	Average Wind Speed	Atmosph. Pressure	Daily Maximum Ambient Temp.	Daily Minimum Ambient Temp.	Daily Total Solar Insulation Factor		
		ML	M _V		v	P _A	T _{AX}	T _{AN}			
		lb/lbmole	lb/lbmole	lb/gal	mph	psia	°F	°F			
	Crude Oil Petroleum Stock Organic Liquids										
T-0011	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0012	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0020	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0021	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0022	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0023	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0056	Petroleum Stock	120.0	80.0	6.40	9.0	13.1	77.9	50.0	1,711.9		
T-0079	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0106	Crude Oil	92.0	66.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0107	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0108	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0109	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0111	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0112	Petroleum Stock	120.0	80.0	6.40	9.0	13.1	77.9	50.0	1,711.9		
T-0117	Petroleum Stock	120.0	80.0	6.40	9.0	13.1	77.9	50.0	1,711.9		
T-0124	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		
T-0401	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9		

Tank ID		METEOROLOGICAL DATA							
	Product Category	Liquid Molecular Weight	Vapor Molecular Weight M _V	Density of the Liquid	Average Wind Speed	Atmosph. Pressure	Daily Maximum Ambient Temp.	Daily Minimum Ambient Temp.	Daily Total Solar Insulation Factor I Btu/ft^2d
		ML			v	P _A	T _{AX}	T _{AN}	
		lb/lbmole	lb/lbmole	lb/gal	mph	psia	°F	°F	
	Crude Oil Petroleum Stock Organic Liquids								
T-0402	Petroleum Stock	92.0	66.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0411	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0412	Petroleum Stock	120.0	80.0	6.40	9.0	13.1	77.9	50.0	1,711.9
T-0413	Petroleum Stock	162.0	130.0	7.00	9.0	13.1	77.9	50.0	1,711.9
T-0415	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0417	Petroleum Stock	92.0	62.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0418	Petroleum Stock	162.0	130.0	7.00	9.0	13.1	77.9	50.0	1,711.9
T-0435	Crude Oil	92.0	66.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0437	Crude Oil	207.0	58.0	7.10	9.0	13.1	77.9	50.0	1,711.9
T-0439	Petroleum Stock	92.0	66.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0450	Petroleum Stock	92.0	66.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0451	Petroleum Stock	188.0	130.0	7.10	9.0	13.1	77.9	50.0	1,711.9
T-0452	Organic Liquids	-	46.1	6.59	9.0	13.1	77.9	50.0	1,711.9
T-0737	Crude Oil	92.0	66.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0802	Crude Oil	92.0	66.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0821	Petroleum Stock	92.0	66.0	5.60	9.0	13.1	77.9	50.0	1,711.9
T-0834	Petroleum Stock	188.0	130.0	7.10	9.0	13.1	77.9	50.0	1,711.9
T-0835	Petroleum Stock	188.0	130.0	7.10	9.0	13.1	77.9	50.0	1,711.9
T-1225	Crude Oil	207.0	58.0	7.10	9.0	13.1	77.9	50.0	1,711.9

	TANK TEMPERATURE VARIABLES												
Tank ID	Tank Shell Surface Solar Absorptance	Tank Roof Surface Solar Absorptance	Daily Average Temp.	Liquid Bulk Temp. based on Ambient Met Data	Monthly Liquid Bulk Temperature Monitored	Liquid Bulk Temp.	Daily Average Liquid Surface Temp.	Average Vapor Temp.	Daily Temp. Range	Avg. Daily Vapor Temp. Range	Daily Maximum Liquid Surface Temp.	Daily Minimum Liquid Surface Temp.	
	αs	α_{R}	T _{AA}	T _B (AP-42)	T _B (Monitored)	T _B	TLA	T _V	ΔΤΑ	ΔΤ _V	T _{LX}	T _{LN}	
	unitless	unitless	°R	°R	°R	°R	°R	°R	°R	°R	°R	°R	
	AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Eq. 1-30	AP-42, Ch. 7.1, Eq. 1-31	Ops Data	Max. Monitored vs AP- 42 Estimate	AP-42, Ch. 7.1, TB Full-Insul Eq. 1-29 Shell-Insul Eq. 1-27 Non-Insul	AP-42, Ch. 7.1, TB Full-Insul Eq. 1-34 Shell-Insul Eq. 1-32 Non-Insul	AP-42, Ch. 7.1, Eq. 1-11	AP-42, Ch. 7.1, Eq. 1-6 Non-Insul Eq. 1-8 Shell-Insul ΔTV = 0 Full-Insul and Constant Temp Eq. 8-1 Full-Insul and Cycle Temp	AP-42, Chp 7.1, Fig 7.1-17 For Full-Insul TLX = TBX	AP-42, Chp 7.1, Fig 7.1-17 For Full-Insul TLN = TBN	
T-0011	0.17	0.17	523.6	524.5	534.38	534.4	532.1	529.7	27.9	25.0	538.3	525.8	
T-0012	0.17	0.17	523.6	524.5	527.71	527.7	527.7	527.7	27.9	25.0	533.9	521.4	
T-0020	0.17	0.17	523.6	524.5	-	524.5	525.5	526.5	27.9	25.9	532.0	519.0	
T-0021	0.17	0.17	523.6	524.5	-	524.5	525.5	526.5	27.9	25.9	532.0	519.0	
T-0022	0.17	0.17	523.6	524.5	-	524.5	525.5	526.4	27.9	26.3	532.1	518.9	
T-0023	0.17	0.17	523.6	524.5	-	524.5	525.5	526.4	27.9	26.3	532.1	518.9	
T-0056	0.25	0.25	523.6	524.9	526.74	526.7	527.4	528.0	27.9	29.0	534.7	520.1	
T-0079	0.17	0.17	523.6	524.5	545.55	545.5	539.4	533.2	27.9	25.0	545.6	533.1	
T-0106	0.17	0.17	523.6	524.5	532.10	532.1	530.2	528.4	27.9	26.2	536.8	523.7	
T-0107	0.17	0.17	523.6	524.5	533.57	533.6	531.1	528.7	27.9	26.2	537.7	524.6	
T-0108	0.25	0.25	523.6	524.9	544.62	544.6	538.7	532.7	27.9	28.6	545.8	531.5	
T-0109	0.34	0.34	523.6	525.4	542.01	542.0	537.7	533.4	27.9	31.4	545.6	529.9	
T-0111	0.34	0.34	523.6	525.4	541.40	541.4	537.3	533.2	27.9	31.4	545.2	529.4	
T-0112	0.25	0.25	523.6	524.9	525.91	525.9	527.0	528.0	27.9	28.7	534.1	519.8	
T-0117	0.17	0.17	523.6	524.5	528.39	528.4	527.7	527.0	27.9	27.3	534.5	520.9	
T-0124	0.17	0.17	523.6	524.5	528.23	528.2	527.7	527.2	27.9	26.7	534.4	521.0	
T-0401	0.17	0.17	523.6	524.5	532.24	532.2	530.4	528.5	27.9	26.0	536.9	523.9	

						TANK TE	MPERATURE VARI	ABLES				
Tank ID	Tank Shell Surface Solar Absorptance	Tank Roof Surface Solar Absorptance	Daily Average Temp.	Liquid Bulk Temp. based on Ambient Met Data	Monthly Liquid Bulk Temperature Monitored	Liquid Bulk Temp.	Daily Average Liquid Surface Temp.	Average Vapor Temp.	Daily Temp. Range	Avg. Daily Vapor Temp. Range	Daily Maximum Liquid Surface Temp.	Daily Minimum Liquid Surface Temp.
	αs	α_{R}	T _{AA}	T _B (AP-42)	T _B (Monitored)	T _B	T _{LA}	T _V	ΔΤΑ	ΔT _V	T _{LX}	T _{LN}
	unitless	unitless	°R	°R	°R	°R	°R	°R	°R	°R	°R	°R
	AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Table 7.1-6	AP-42, Ch. 7.1, Eq. 1-30	AP-42, Ch. 7.1, Eq. 1-31	Ops Data	Max. Monitored vs AP- 42 Estimate	AP-42, Ch. 7.1, TB Full-Insul Eq. 1-29 Shell-Insul Eq. 1-27 Non-Insul	AP-42, Ch. 7.1, TB Full-Insul Eq. 1-34 Shell-Insul Eq. 1-32 Non-Insul	AP-42, Ch. 7.1, Eq. 1-11	AP-42, Ch. 7.1, Eq. 1-6 Non-Insul Eq. 1-8 Shell-Insul ΔTV = 0 Full-Insul Insul and Constant Temp Eq. 8-1 Full-Insul and Cycle Temp	AP-42, Chp 7.1, Fig 7.1-17 For Full-Insul TLX = TBX	AP-42, Chp 7.1, Fig 7.1-17 For Full-Insul TLN = TBN
T-0402	0.17	0.17	523.6	524.5	538.33	538.3	534.2	530.0	27.9	26.0	540.7	527.7
T-0411	0.25	0.25	523.6	524.9	525.12	525.1	526.6	528.1	27.9	28.0	533.6	519.6
T-0412	0.25	0.25	523.6	524.9	526.39	526.4	527.4	528.5	27.9	28.0	534.4	520.4
T-0413	0.17	0.17	523.6	524.5	535.45	535.5	532.3	529.2	27.9	26.1	538.9	525.8
T-0415	0.17	0.17	523.6	524.5	527.18	527.2	527.2	527.1	27.9	26.2	533.7	520.6
T-0417	0.34	0.34	523.6	525.4	531.21	531.2	531.0	530.7	27.9	31.4	538.8	523.1
T-0418	0.17	0.17	523.6	524.5	539.63	539.6	535.1	530.6	27.9	25.8	541.6	528.7
T-0435	0.17	0.17	523.6	524.5	524.57	524.6	525.3	526.1	27.9	27.9	532.3	518.4
T-0437	0.17	0.17	523.6	524.5	533.44	533.4	531.4	529.3	27.9	25.3	537.7	525.1
T-0439	0.25	0.25	523.6	524.9	531.80	531.8	531.0	530.2	27.9	27.8	537.9	524.0
T-0450	0.17	0.17	523.6	524.5	531.26	531.3	530.0	528.8	27.9	25.0	536.3	523.7
T-0451	0.44	0.44	523.6	525.9	534.20	534.2	534.2	534.2	27.9	11.4	543.9	532.5
T-0452	0.25	0.25	523.6	524.9	515.12	524.9	526.1	527.3	27.9	29.8	533.6	518.7
T-0737	0.17	0.17	523.6	524.5	524.57	524.6	525.5	526.4	27.9	26.3	532.1	518.9
T-0802	0.17	0.17	523.6	524.5	524.57	524.6	525.4	526.3	27.9	27.0	532.2	518.7
T-0821	0.25	0.25	523.6	524.9	520.65	524.9	526.4	527.9	27.9	28.2	533.5	519.4
T-0834	0.25	0.25	523.6	524.9	541.90	541.9	537.2	532.6	27.9	28.2	544.3	530.2
T-0835	0.25	0.25	523.6	524.9	542.05	542.1	537.6	533.2	27.9	27.8	544.6	530.7
T-1225	0.25	0.25	523.6	524.9	530.25	530.3	530.1	530.0	27.9	27.4	537.0	523.3

		TANK PRI	ESSURE VARIABLES					HEEL PARAM	TETERS CALCULA	ATION		
Tank ID	True Vapor Pressure at Daily Avg Temp. (T _{LA})	True Vapor Pressure at Daily Max. Liq. Surface Temp (T _{LX})		Avg. Daily Vapor Pressure Range	Vapor Pressure Function	Slope of Tank Bottom	Effective Liquid Height During Roof Landing	Vapor Space Height under Landed Floating Roof	Volume of the Vapor Space	Vapor Space Expansion Factor	Filling Saturation Factor	Vented Vapor Saturation Factor
	P _{VA}	P _{vx}	P _{VN}	ΔP _V	P*	S _B	h _{le}	hv	V _v	K _E	Sat	Ks
	psia	psia	psia	psia	unitless	ft/ft	ft	ft	ft^3	unitless	unitless	unitless
	AP-42, Ch. 7.1, Eq. 1-25 Petroleum Eq. 1-26 Org Liq	AP-42, Ch. 7.1, Eq. 1-25 Petroleum Eq. 1-26 Org Liq	AP-42, Ch. 7.1, Eq. 1-25 Petroleum Eq. 1-26 Org Liq	AP-42, Ch. 7.1, Eq. 1-9 §7.1.3.8.4	AP-42 Ch. 7.1 Eq. 3-9	SB < 0 (Cone-Up) SB = 0 (Flat) SB > 0 (Cone-Down)	AP-42 Ch. 7.1 Table 7.1-4	AP-42 Ch. 7.1 Table 7.1-4	AP-42, Ch. 7.1, Eq. 3-22	AP-42, Ch. 7.1 Eq. 1-5	AP-42, Ch. 7.1, Tables 7.1-17 7.1-18 and 7.1-19	AP-42, Ch. 7.1 Table 7.1-17 Eq. 1-21 Hvo=hv
T-0011	9.07	10.12	8.11	2.01	0.29	-	0.25	5.75	35,772	0.550	0.2	0.15
T-0012	8.39	9.38	7.49	1.89	0.25	-	0.25	5.75	35,772	0.452	0.2	0.15
T-0020	8.07	9.06	7.16	1.90	0.24	-	0.25	5.75	36,580	0.430	0.2	0.15
T-0021	8.07	9.06	7.16	1.90	0.24	-	0.25	5.75	36,580	0.430	0.2	0.15
T-0022	8.06	9.07	7.14	1.93	0.24	-	0.25	5.75	25,403	0.435	0.2	0.15
T-0023	8.06	9.07	7.14	1.93	0.24	-	0.25	5.75	25,403	0.435	0.2	0.15
T-0056	1.91	2.23	1.63	0.60	0.04	-	0.25	5.75	10,405	0.109	0.2	0.15
T-0079	10.31	11.10	9.24	1.86	0.37	-	0.25	5.75	70,563	0.719	0.2	0.15
T-0106	7.02	7.81	6.28	1.53	0.19	-	0.25	5.75	20,273	0.302	0.2	0.15
T-0107	8.93	10.01	7.93	2.08	0.28	-	0.25	5.75	20,273	0.551	0.2	0.15
T-0108	10.18	11.10	8.98	2.12	0.36	-	0.25	5.75	20,273	0.787	0.2	0.15
T-0109	10.02	11.10	8.72	2.38	0.35	-	0.25	5.75	20,273	0.837	0.2	0.15
T-0111	9.95	11.10	8.66	2.44	0.34	-	0.25	5.75	10,843	0.840	0.2	0.15
T-0112	1.89	2.20	1.61	0.59	0.04	-	0.25	5.75	10,405	0.107	0.2	0.15
T-0117	1.92	2.22	1.65	0.57	0.04	-	0.25	5.75	10,405	0.103	0.2	0.15
T-0124	8.39	9.45	7.43	2.02	0.25	-	0.25	5.75	7,226	0.482	0.2	0.15
T-0401	8.80	9.87	7.83	2.04	0.27	-	0.25	5.75	36,580	0.528	0.2	0.15

		TANK PRI	ESSURE VARIABLES					HEEL PARAM	IETERS CALCULA	ATION		
Tank ID	True Vapor Pressure at Daily Avg Temp. (T _{LA})	True Vapor Pressure at Daily Max. Liq. Surface Temp (T _{LX})	True Vapor Pressure at Daily Min. Liq. Surface Temp (T _{LN})	Avg. Daily Vapor Pressure Range	Vapor Pressure Function	Slope of Tank Bottom	Effective Liquid Height During Roof Landing	Vapor Space Height under Landed Floating Roof	Volume of the Vapor Space	Vapor Space Expansion Factor	Filling Saturation Factor	Vented Vapor Saturation Factor
	P _{VA}	P _{vx}	P _{VN}	ΔP _V	P*	S _B	h _{le}	hv	V _v	K _E	Sat	Ks
	psia	psia	psia	psia	unitless	ft/ft	ft	ft	ft^3	unitless	unitless	unitless
	AP-42, Ch. 7.1, Eq. 1-25 Petroleum Eq. 1-26 Org Liq	AP-42, Ch. 7.1, Eq. 1-25 Petroleum Eq. 1-26 Org Liq	AP-42, Ch. 7.1, Eq. 1-25 Petroleum Eq. 1-26 Org Liq	AP-42, Ch. 7.1, Eq. 1-9 §7.1.3.8.4	AP-42 Ch. 7.1 Eq. 3-9	SB < 0 (Cone-Up) SB = 0 (Flat) SB > 0 (Cone-Down)	AP-42 Ch. 7.1 Table 7.1-4	AP-42 Ch. 7.1 Table 7.1-4	AP-42, Ch. 7.1, Eq. 3-22	AP-42, Ch. 7.1 Eq. 1-5	AP-42, Ch. 7.1, Tables 7.1-17 7.1-18 and 7.1-19	AP-42, Ch. 7.1 Table 7.1-17 Eq. 1-21 Hvo=hv
T-0402	6.75	7.59	5.98	1.62	0.18	-	0.25	5.75	36,580	0.304	0.2	0.15
T-0411	8.23	9.32	7.24	2.08	0.24	-	0.25	5.75	45,160	0.483	0.2	0.15
T-0412	1.91	2.21	1.64	0.58	0.04	-	0.25	5.75	45,160	0.105	0.2	0.15
T-0413	0.46	0.55	0.39	0.15	0.01	-	0.25	5.75	20,273	0.061	0.2	0.15
T-0415	8.31	9.34	7.37	1.97	0.25	-	0.25	5.75	20,273	0.463	0.2	0.15
T-0417	8.90	10.21	7.72	2.49	0.28	-	0.25	5.75	11,290	0.656	0.2	0.15
T-0418	0.50	0.58	0.42	0.16	0.01	-	0.25	5.75	20,273	0.061	0.2	0.15
T-0435	6.46	7.26	5.73	1.53	0.17	-	0.25	5.75	4,064	0.285	0.2	0.15
T-0437	7.15	7.93	6.43	1.50	0.20	-	0.25	5.75	65,031	0.300	0.2	0.15
T-0439	7.48	8.47	6.58	1.89	0.21	-	0.25	5.75	76,321	0.391	0.2	0.15
T-0450	7.35	8.23	6.54	1.68	0.20	-	0.25	5.75	65,031	0.341	0.2	0.15
T-0451	0.43	0.55	0.42	0.14	0.01	-	0.25	5.75	5,532	0.032	0.2	0.15
T-0452	0.81	1.03	0.63	0.41	0.02	-	0.25	5.75	5,532	0.090	0.2	0.15
T-0737	6.48	7.24	5.79	1.44	0.17	-	0.25	5.75	17,924	0.269	0.2	0.15
T-0802	6.47	7.25	5.77	1.48	0.17	-	0.25	5.75	9,145	0.276	0.2	0.15
T-0821	5.84	6.66	5.10	1.56	0.15	-	0.25	5.75	50,742	0.270	0.2	0.15
T-0834	0.47	0.56	0.39	0.17	0.01	-	0.25	5.75	32,628	0.066	0.2	0.15
T-0835	0.47	0.56	0.40	0.17	0.01	-	0.25	5.75	55,642	0.065	0.2	0.15
T-1225	7.00	7.84	6.24	1.59	0.19	-	0.25	5.75	101,611	0.315	0.2	0.15

		: LANDING LOSS L DRAIN-DRY TA		TOTAL ROOF	RE	FILLING LOSSES		Voc	Voc	H2S	H2S	HAPs
Tank ID	Clingage Factor	Limit on Standing Idle Loss (Clingage)	Standing Idle Loss (Clingage)	LANDING LOSSES	Filling Saturation Correction Factor for Wind	Limit on Filling Loss	Filling Loss	Emissions	Emissions	Emissions	Emissions	Emissions
	Cs	L _{SLmax}	L _{SLclingage}	L _{TL}	C _{sf}	L _{FLmax}	L _{FL}					
	bbl/1000 ft^2	lb/event	lb/event	lb/event	unitless	lb/event	lb/event	lb/hr	ton/event	lb/hr	ton/event	ton/event
	AP-42 Ch. 7.1 Table 7.1-10	AP-42 Ch. 7.1 Table 7.1-19 Eq. 3-15	AP-42 Ch. 7.1 Table 7.1-19 Eq. 3-11	AP-42 Ch. 7.1 Eq. 3-1	AP-42, Ch. 7.1, Table 7.1-18 Eq. 3-21	AP-42, Ch. 7.1, Table 7.1-17 Eq. 3-16					Raoults Law	Raoults Law
T-0011	0.15	2,148.1	219.5	219.5	1.00	-	555.7	23.2	0.4	-	-	7.81E-03
T-0012	0.15	1,987.3	219.5	219.5	1.00	-	514.1	21.4	0.4	-	-	7.39E-03
T-0020	0.15	1,953.4	224.4	224.4	1.00	-	505.3	21.1	0.4	-	-	7.35E-03
T-0021	0.15	1,953.4	224.4	224.4	1.00	-	505.3	21.1	0.4	-	-	7.35E-03
T-0022	0.15	1,355.5	155.9	155.9	1.00	-	350.6	14.6	0.3	-	-	5.10E-03
T-0023	0.15	1,355.5	155.9	155.9	1.00	-	350.6	14.6	0.3	-	-	5.10E-03
T-0056	0.15	169.4	73.0	73.0	1.00	-	43.8	3.0	0.1	-	-	2.92E-04
T-0079	0.15	4,814.9	433.0	433.0	1.00	-	1,245.5	51.9	0.8	-	-	1.69E-02
T-0106	0.60	1,002.4	497.5	497.5	1.00	-	259.3	0.3	0.005	2.48E-02	8.42E-04	2.04E-05
T-0107	0.15	1,197.9	124.4	124.4	1.00	-	309.9	12.9	0.2	1.38E-05	3.41E-07	8.08E-03
T-0108	0.15	1,366.5	124.4	124.4	1.00	-	353.5	14.7	0.2	-	-	4.81E-03
T-0109	0.15	1,344.4	124.4	124.4	1.00	-	347.8	14.5	0.2	-	-	4.75E-03
T-0111	0.15	713.9	66.5	66.5	1.00	-	184.7	7.7	0.1	-	-	2.53E-03
T-0112	0.15	167.8	73.0	73.0	1.00	-	43.4	3.0	0.1	-	-	2.91E-04
T-0117	0.15	170.5	73.0	73.0	1.00	-	44.1	3.0	0.1	-	-	2.93E-04
T-0124	0.15	401.5	44.3	44.3	1.00	-	103.9	4.3	0.1	-	-	1.49E-03
T-0401	0.15	2,131.4	224.4	224.4	1.00	-	551.4	23.0	0.4	-	-	7.81E-03

		: LANDING LOSS L DRAIN-DRY TA		TOTAL ROOF	RE	FILLING LOSSES		VOC	VOC	H2S	H2S	HAPs
Tank ID	Clingage Factor	Limit on Standing Idle Loss (Clingage)	Standing Idle Loss (Clingage)	LANDING LOSSES	Filling Saturation Correction Factor for Wind	Limit on Filling Loss	Filling Loss	Emissions	Emissions	Emissions	Emissions	Emissions
	C _s	L _{SLmax}	L _{SLclingage}	L _{TL}	C _{sf}	L _{FLmax}	L _{FL}					
	bbl/1000 ft^2	lb/event	lb/event	lb/event	unitless	lb/event	lb/event	lb/hr	ton/event	lb/hr	ton/event	ton/event
	AP-42 Ch. 7.1 Table 7.1-10	AP-42 Ch. 7.1 Table 7.1-19 Eq. 3-15	AP-42 Ch. 7.1 Table 7.1-19 Eq. 3-11	AP-42 Ch. 7.1 Eq. 3-1	AP-42, Ch. 7.1, Table 7.1-18 Eq. 3-21	AP-42, Ch. 7.1, Table 7.1-17 Eq. 3-16					Raoults Law	Raoults Law
T-0402	0.15	1,738.9	224.4	224.4	1.00	-	449.8	18.7	0.3	4.52E-04	1.58E-05	3.70E-03
T-0411	0.15	2,460.0	277.1	277.1	1.00	-	636.3	26.5	0.5	2.66E-05	7.29E-07	1.70E-02
T-0412	0.15	736.0	316.7	316.7	1.00	-	190.4	13.2	0.3	-	-	1.27E-03
T-0413	0.15	130.8	130.8	130.8	1.00	-	33.8	5.5	0.082	-	-	3.63E-05
T-0415	0.15	1,115.2	124.4	124.4	1.00	-	288.5	12.0	0.2	-	-	4.16E-03
T-0417	0.15	665.0	69.3	69.3	1.00	-	172.0	7.2	0.1	-	-	2.43E-03
T-0418	0.15	140.1	140.1	140.1	1.00	-	36.3	5.8	0.1	-	-	3.88E-05
T-0435	0.60	185.1	99.8	99.8	1.00	-	47.9	0.05	0.0010	4.63E-03	1.66E-04	3.98E-06
T-0437	0.60	2,879.5	2,023.5	2,023.5	1.00	-	744.9	1.1	0.02	1.02E-03	3.07E-05	1.90E-04
T-0439	0.15	4,022.9	468.3	468.3	1.00	-	1,040.6	43.4	0.8	2.10E-03	6.39E-05	1.92E-02
T-0450	0.15	3,367.3	399.0	399.0	1.00	-	871.0	36.3	0.6	1.74E-03	5.40E-05	1.61E-02
T-0451	0.15	33.4	33.4	33.4	1.00	-	8.6	1.4	0.02	1.55E-04	7.04E-05	1.23E-05
T-0452	0.00	22.0	0.4	0.4	1.00	-	5.7	0.2	0.003	-	-	0.00E+00
T-0737	0.60	818.9	439.9	439.9	1.00	-	211.8	0.2	0.004	2.05E-02	7.33E-04	1.76E-05
T-0802	0.60	417.2	224.4	224.4	1.00	-	107.9	0.1	0.002	1.04E-02	3.74E-04	8.97E-06
T-0821	0.15	2,087.6	311.3	311.3	1.00	-	540.0	22.5	0.4	4.87E-04	2.06E-05	4.68E-03
T-0834	0.15	212.7	212.7	212.7	1.00	-	55.0	8.9	0.1	1.03E-03	4.33E-04	7.86E-05
T-0835	0.15	366.3	366.3	366.3	1.00	-	94.8	15.3	0.2	1.79E-03	7.43E-04	1.35E-04
T-1225	0.60	4,407.0	3,161.8	3,161.8	1.00	-	1,140.0	1.7	0.03	1.57E-03	4.79E-05	2.95E-04
				MAX HOUR	LY (assumes only	one landing a	t time), lb/hr	51.9		0.02		
							ANNUAL, tpy		8.09		0.004	0.16

FLOATING ROOF TANKS (EXT, INT) POTENTIAL TO EMIT HAPS

Maximum individual HAPs (n-Hexane), tpy = 1.14
Total HAPS, tpy = 2.53

HAPs	1,3- Butadiene	2,2,4- Trimethylp entane	Acenaphth ene	Acenaphth ylene	Anthracen e	Benz(a)ant hracene	Benzene	Benzo(a)ph enanthren e	Benzo(a)py rene	Benzo(b)fl uoranthen e	Benzo(e)py rene	Benzo(g,h,i)perylene	Biphenyl	Cresol (mixed isomers)	Cumene	Ethylbenze ne	Fluoranthe ne	Fluorene	Lead compound s	m-Cresol
CAS No.	106-99-0	540-84-1	83-32-9	208-96-8	120-12-7	56-55-3	71-43-2	218-01-9	50-32-8	205-99-2	192-97-2	191-24-2	92-52-4	1319-77-3	98-82-8	100-41-4	206-44-0	86-73-7	7439-92-1	108-39-4
Pi°, psia	57.00	0.79	4.26E-05	9.28E-05	1.16E-05	4.06E-09	2.01	1.21E-10	1.06E-10	9.67E-09	1.10E-10	1.93E-12	1.93E-04	0.00	0.12	0.22	1.78E-07	1.16E-05	0.03	2.13E-03
Tank	Speciated F	Potential to	Emit, tpy																	
T-0011	1.16E-02	4.36E-02	-	-	6.47E-12	-	1.24E-02	-	-	-	-	-	4.56E-08	-	1.13E-04	2.02E-03	-	-	-	-
T-0012	1.00E-02	3.76E-02	-	-	5.58E-12	-	1.07E-02	-	-	-	-	-	3.93E-08	-	9.71E-05	1.74E-03	-	-	-	-
T-0020	2.97E-03	1.12E-02	-	-	1.66E-12	-	3.17E-03	-	-	-	-	-	1.17E-08	-	2.89E-05	5.17E-04	-	-	-	-
T-0021	2.97E-03	1.12E-02	-	-	1.66E-12	-	3.17E-03	-	-	-	-	-	1.17E-08	-	2.89E-05	5.17E-04	-	-	-	-
T-0022	2.59E-03	9.76E-03	-	-	1.45E-12	-	2.77E-03	-	-	-	-	-	1.02E-08	-	2.52E-05	4.52E-04	-	-	-	-
T-0023	2.59E-03	9.76E-03	-	-	1.45E-12	-	2.77E-03	-	-	-	-	-	1.02E-08	-	2.52E-05	4.52E-04	-	-	-	-
T-0056	-	8.92E-06	-	-	-	-	8.29E-04	-	-	-	-	-	-	-	2.91E-05	2.92E-04	-	-	-	-
T-0079	1.35E-02	5.09E-02	-	-	7.54E-12	-	1.44E-02	-	-	-	-	-	5.31E-08	-	1.31E-04	2.35E-03	-	-	-	-
T-0106	-	6.18E-05	2.41E-09	3.07E-09	2.34E-09	8.27E-15	1.35E-03	1.97E-16	1.95E-16	2.69E-14	2.99E-16	-	5.24E-07	4.96E-07	7.03E-06	8.42E-05	1.86E-12	9.68E-10	-	3.03E-07
T-0107	2.38E-02	3.51E-04	-	-	-	-	2.41E-02	-	-	-	-	-	-	-	6.17E-05	6.30E-04	-	-	-	-
T-0108	9.53E-03	3.59E-02	-	-	5.32E-12	-	1.02E-02	-	-	-	-	-	3.75E-08	-	9.25E-05	1.66E-03	-	-	-	-
T-0109	1.29E-02	4.85E-02	-	-	7.19E-12	-	1.37E-02	-	-	-	-	-	5.06E-08	-	1.25E-04	2.24E-03	-	-	-	-
T-0111	7.39E-03	2.78E-02	-	-	4.12E-12	-	7.88E-03	-	-	-	-	-	2.91E-08	-	7.18E-05	1.29E-03	-	-	-	-
T-0112	-	3.60E-06	-	-	-	-	3.35E-04	-	-	-	-	-	-	-	1.17E-05	1.18E-04	-	-	-	-
T-0117	-	9.20E-06	-	-	-	-	8.55E-04	-	-	-	-	-	-	-	3.00E-05	3.01E-04	-	-	-	-
T-0124	5.97E-03	2.25E-02	-	-	3.33E-12	-	6.37E-03	-	-	-	-	-	2.35E-08	-	5.80E-05	1.04E-03	-	-	-	-
T-0401	2.24E-03	8.41E-03	-	-	1.25E-12	-	2.38E-03	-	-	-	-	-	8.79E-09	-	2.17E-05	3.89E-04	-	-	-	-
T-0402	2.92E-03	3.92E-04	1.03E-10	1.00E-09	-	-	6.91E-03	-	-	-	-	-	5.08E-09	-	2.96E-05	8.34E-04	-	-	-	-
T-0411	2.86E-02	4.22E-04	-	-	-	-	2.90E-02	-	-	-	-	-	-	-	7.41E-05	7.57E-04	-	-	-	-
T-0412	-	1.12E-05	-	-	-	-	1.04E-03	-	-	-	-	-	-	-	3.64E-05	3.65E-04	-	-	-	-
T-0413	-	3.79E-05	-	-	-	-	3.32E-05	-	-	-	-	-	3.26E-10	-	3.42E-06	2.59E-05	-	-	-	-
T-0415	6.08E-03	2.29E-02	-	-	3.39E-12	-	6.48E-03	-	-	-	-	-	2.39E-08	-	5.91E-05	1.06E-03	-	-	-	-
T-0417	9.06E-03	3.41E-02	-	-	5.05E-12	-	9.66E-03	-	-	-	-	-	3.56E-08	-	8.80E-05	1.58E-03	-	-	-	-
T-0418	-	4.18E-05	-	-	-	-	3.65E-05	-	-	-	-	-	3.59E-10	-	3.77E-06	2.86E-05	-	-	-	-
T-0435	-	8.12E-05	3.17E-09	4.03E-09	3.07E-09	1.09E-14	1.78E-03	2.58E-16	2.56E-16	3.54E-14	3.92E-16	-	6.88E-07	6.52E-07	9.24E-06	1.11E-04	2.45E-12	1.27E-09	-	3.98E-07
T-0437	-	6.00E-04	3.48E-10	5.30E-10	6.04E-11	1.65E-13	4.51E-03	1.80E-15	4.31E-15	5.52E-13	1.22E-15	8.78E-18	6.43E-08	-	4.00E-05	5.05E-04	1.03E-12	5.53E-10	7.58E-11	-
T-0439	-	2.48E-04	-	-	-	-	1.68E-02	-	-	-	-	-	2.16E-08	-	1.10E-04	8.88E-04	-	-	-	-
T-0450	-	3.15E-04	-	-	-	-	2.14E-02	-	-	-	-	-	2.74E-08	-	1.39E-04	1.13E-03	-	-	-	-
T-0451	-	-	-	-	6.37E-09	-	1.47E-05	-	-	-	-	-	7.15E-10	-	8.31E-07	3.25E-06	-	-	-	-
T-0452	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
T-0737	-	7.10E-05	2.77E-09	3.52E-09	2.69E-09	9.49E-15	1.55E-03	2.26E-16	2.24E-16	3.09E-14	3.43E-16	-	6.01E-07	5.69E-07	8.07E-06	9.66E-05	2.14E-12	1.11E-09	-	3.48E-07
T-0802	-	8.02E-05	3.13E-09	3.98E-09	3.04E-09	1.07E-14	1.75E-03	2.55E-16	2.53E-16	3.50E-14	3.88E-16	-	6.80E-07	6.44E-07	9.12E-06	1.09E-04	2.42E-12	1.26E-09	-	3.94E-07
T-0821	3.30E-03	4.43E-04	1.17E-10	1.14E-09	-	-	7.82E-03	-	-	-	-	-	5.74E-09	-	3.34E-05	9.44E-04	-	-	-	-
T-0834	-	-	-	-	6.27E-08	-	1.45E-04	-	-	-	-	-	7.03E-09	-	8.17E-06	3.20E-05	-	-	-	-
T-0835	-	-	-	-	2.87E-08	-	6.62E-05	-	-	-	-	-	3.21E-09	-	3.74E-06	1.46E-05	-	-	-	-
T-1225	-	9.56E-04	5.55E-10	8.44E-10	9.63E-11	2.63E-13	7.18E-03	2.87E-15	6.86E-15	8.79E-13	1.94E-15	1.40E-17	1.02E-07	-	6.38E-05	8.04E-04	1.64E-12	8.81E-10	1.21E-10	-
Sum HAPs, tpy	1.58E-01	3.78E-01	1.26E-08	1.81E-08	1.09E-07	4.67E-13	2.33E-01	5.61E-15	1.21E-14	1.56E-12	4.58E-15	2.28E-17	3.12E-06	2.36E-06	1.68E-03	2.54E-02	1.15E-11	6.04E-09	1.97E-10	1.44E-06

 $\begin{aligned} \text{Raoult's Law} & P_i = x_i * \text{TVP}_i \\ P_i = y_i * \text{TVP}_i \\ Y_j = x_i * \text{TVP}_j \text{TVP} \end{aligned}$ $\text{Liquid molar fraction} & \text{xi (mole_i/mole_T)} = \text{mi (g_i/g_T)} * \text{MW}_{iiq} \left(g_T/\text{moles}_T \right) / \text{MW}_i \left(g_i/\text{moles}_i \right) = \text{wt}\%_{iiq} * \text{MW}_{iiq} / \text{MW}_i \end{aligned}$ $\text{Gas molar fraction} & \text{yi (mole_i/mole_T)} = \text{mi (g_i/g_T)} * \text{MW}_{vap} \left(g_T/\text{moles}_T \right) / \text{MW}_i \left(g_i/\text{moles}_i \right) = \text{wt}\%_{vap} * \text{MW}_{vap} / \text{MW}_i \end{aligned}$ $\text{yi = xi * TVPi/TVP} \\ & \text{wt}\%_{vap} * \text{MW}_{vap} / \text{MW} = \text{wt}\%_{iiq} * \text{MW}_{iiq} / \text{MW}_i * \text{TVPi/TVP} \\ & \text{wt}\%_{vap} = \text{wt}\%_{iiq} * \text{TVPi/TVP} * \text{MW}_{iiq} / \text{MW}_{vap} \end{aligned}$

HAPs	Mercury compound s	Methanol	Methyl tert	m-Xylene	Naphthale ne	n-Hexane	o-Cresol	o-Xylene	PAH Total	Phenanthr ene	p-Xylene	Pyrene	Styrene	Toluene	Xylene (mixed isomers)
CAS No.	7439-97-6	67-56-1	1634-04-4	108-38-3	91-20-3	110-54-3	95-48-7	95-47-6	PAH	85-01-8	106-42-3	129-00-0	100-42-5	108-88-3	1330-20-7
Pi°, psia	2.32E-05	2.70	5.30	0.16	0.01	3.14	3.48E-03	0.13	1.93E-12	2.34E-06	0.17	8.70E-08	0.12	0.60	0.20
Tank															
T-0011	-	1.13E-04	7.82E-04	2.36E-03	5.71E-06	1.95E-02	-	1.52E-03	3.19E-15	1.49E-12	1.48E-03	-	1.90E-04	3.16E-02	1.26E-02
T-0012	-	9.71E-05	6.74E-04	2.04E-03	4.92E-06	1.68E-02	-	1.31E-03	2.75E-15	1.29E-12	1.28E-03	-	1.64E-04	2.72E-02	1.08E-02
T-0020	-	2.89E-05	2.00E-04	6.06E-04	1.46E-06	5.01E-03	-	3.90E-04	8.17E-16	3.82E-13	3.80E-04	-	4.88E-05	8.10E-03	3.22E-03
T-0021	-	2.89E-05	2.00E-04	6.06E-04	1.46E-06	5.01E-03	-	3.90E-04	8.17E-16	3.82E-13	3.80E-04	-	4.88E-05	8.10E-03	3.22E-03
T-0022	-	2.52E-05	1.75E-04	5.29E-04	1.28E-06	4.37E-03	-	3.40E-04	7.13E-16	3.34E-13	3.32E-04	-	4.26E-05	7.07E-03	2.81E-03
T-0023	-	2.52E-05	1.75E-04	5.29E-04	1.28E-06	4.37E-03	-	3.40E-04	7.13E-16	3.34E-13	3.32E-04	-	4.26E-05	7.07E-03	2.81E-03
T-0056	-	2.61E-04	5.23E-04	4.12E-04	-	7.78E-04	-	3.23E-06	-	-	3.62E-04	-	-	3.82E-03	5.64E-04
T-0079	-	1.31E-04	9.11E-04	2.76E-03	6.65E-06	2.28E-02	-	1.77E-03	3.72E-15	1.74E-12	1.73E-03	-	2.22E-04	3.68E-02	1.46E-02
T-0106	-	1.81E-03	-	3.85E-04	9.01E-07	2.96E-03	4.96E-07	7.93E-05	-	3.26E-10	-	-	-	5.73E-04	1.56E-04
T-0107	1.77E-13	-	-	1.59E-03	-	2.35E-01	-	5.24E-04	-	-	5.63E-04	-	-	8.98E-03	-
T-0108	-	9.26E-05	6.42E-04	1.94E-03	4.69E-06	1.61E-02	-	1.25E-03	2.62E-15	1.23E-12	1.22E-03	-	1.56E-04	2.60E-02	1.03E-02
T-0109	-	1.25E-04	8.68E-04	2.63E-03	6.34E-06	2.17E-02	-	1.69E-03	3.54E-15	1.66E-12	1.65E-03	-	2.11E-04	3.51E-02	1.39E-02
T-0111	-	7.18E-05	4.98E-04	1.51E-03	3.64E-06	1.25E-02	-	9.70E-04	2.03E-15	9.50E-13	9.45E-04	-	1.21E-04	2.01E-02	8.00E-03
T-0112	-	1.06E-04	2.11E-04	1.66E-04	-	3.14E-04	-	1.31E-06	-	-	1.46E-04	-	-	1.54E-03	2.28E-04
T-0117	-	2.69E-04	5.40E-04	4.25E-04	-	8.02E-04	-	3.33E-06	-	-	3.73E-04	-	-	3.94E-03	5.81E-04
T-0124	-	5.80E-05	4.03E-04	1.22E-03	2.94E-06	1.01E-02	-	7.84E-04	1.64E-15	7.68E-13	7.64E-04	-	9.80E-05	1.63E-02	6.46E-03
T-0401	-	2.17E-05	1.51E-04	4.56E-04	1.10E-06	3.77E-03	-	2.93E-04	6.15E-16	2.88E-13	2.86E-04	-	3.67E-05	6.09E-03	2.42E-03
T-0402	-	-	7.19E-03	1.21E-03	2.95E-06	2.17E-02	-	7.32E-05	-	-	5.81E-04	-	-	-	3.22E-03
T-0411	2.13E-13	-	-	1.91E-03	-	2.82E-01	-	6.30E-04	-	-	6.76E-04	-	-	1.08E-02	-
T-0412	-	3.27E-04	6.55E-04	5.15E-04	-	9.73E-04	-	4.05E-06	-	-	4.53E-04	-	-	4.78E-03	7.05E-04
T-0413	-	-	-	2.47E-05	1.16E-05	1.26E-04	-	-	-	-	1.26E-05	-	-	5.40E-05	5.97E-05
T-0415	-	5.91E-05	4.10E-04	1.24E-03	2.99E-06	1.02E-02	-	7.98E-04	1.67E-15	7.82E-13	7.78E-04	-	9.98E-05	1.66E-02	6.58E-03
T-0417	-	8.80E-05	6.11E-04	1.85E-03	4.46E-06	1.53E-02	-	1.19E-03	2.49E-15	1.16E-12	1.16E-03	-	1.49E-04	2.47E-02	9.80E-03
T-0418	-	-	-	2.72E-05	1.28E-05	1.38E-04	-	-	-	-	1.39E-05	-	-	5.95E-05	6.58E-05
T-0435	-	2.38E-03	-	5.06E-04	1.18E-06	3.89E-03	6.51E-07	1.04E-04	-	4.29E-10	-	-	-	7.52E-04	2.04E-04
T-0437	1.02E-13	-	-	1.03E-03	1.72E-06	4.17E-02	-	4.27E-05	-	-	2.63E-04	1.11E-12	-	3.58E-03	1.29E-03
T-0439	6.48E-15	1.04E-03	3.24E-03	2.40E-03	1.97E-07	1.25E-01	-	6.34E-04	-	-	8.55E-04	-	-	1.26E-02	2.07E-03
T-0450	8.23E-15	1.33E-03	4.11E-03	3.04E-03	2.50E-07	1.59E-01	-	8.05E-04	-	-	1.09E-03	-	-	1.61E-02	2.63E-03
T-0451	-	-	-	7.10E-05	2.83E-07	5.38E-06	-	2.57E-07	7.79E-16	1.32E-12	5.23E-05	-	-	1.30E-05	1.55E-05
T-0452	-		-		-			-	-		-	-	-		-
T-0737	-	2.08E-03	-	4.42E-04	1.03E-06	3.40E-03	5.69E-07	9.10E-05	-	3.75E-10	-	-	-	6.57E-04	1.78E-04
T-0802	-	2.35E-03	-	5.00E-04	1.17E-06	3.84E-03	6.43E-07	1.03E-04	-	4.24E-10	-	-	-	7.43E-04	2.02E-04
T-0821	-	-	8.13E-03	1.37E-03	3.34E-06	2.46E-02	-	8.28E-05	-	-	6.58E-04	-	-	-	3.65E-03
T-0834	-	-	-	6.98E-04	2.78E-06	5.29E-05	-	2.53E-06	7.66E-15	1.30E-11	5.14E-04	-	-	1.28E-04	1.52E-04
T-0835	-	-	-	3.19E-04	1.27E-06	2.42E-05	-	1.16E-06	3.50E-15	5.96E-12	2.35E-04	-	-	5.86E-05	6.96E-05
T-1225	1.63E-13	-	-	1.65E-03	2.74E-06	6.64E-02	-	6.81E-05	-	-	4.19E-04	1.77E-12	-	5.70E-03	2.06E-03
Sum HAPs, tpy	6.70E-13	1.29E-02	3.13E-02	3.90E-02	9.32E-05	1.14E+00	2.36E-06	1.63E-02	3.93E-14	1.59E-09	2.00E-02	2.89E-12	1.63E-03	3.46E-01	1.26E-01

TANK LANDINGS VAPOR COMBUSTION UNIT (TVCU) - STARTUP AND SHUTDOWN EMISSIONS

	Emissions Fact	tors	
Pollutant	Assist Gas/ Pilot Gas (lb/MMscf)	HC Vapors (lb/MMBtu)	Reference
NO _X	100	0.14	Assist Gas/Pilot Gas EF per AP-42, Ch. 1.4 (7/98), Table 1.4-1 Small Boilers (<100 MMBtu/hr), uncontrolled.
CO	84	0.14	HC EF per VCU manufacturer specifications.
voc	5.5	95%	Assist Gas/Pilot Gas EF per AP-42, Ch. 1.4 (7/98), Table 1.4-1 Small Boilers (<100 MMBtu/hr), uncontrolled. HC DRE per VCU manufacturer specifications.
SO ₂	20 gr/100scf	95%	PSD-NM-0195-M39R1. C101.G Natural Gas definition
PM/PM ₁₀ /PM _{2.5}	7.6	0.0075	EF per AP-42, Ch. 1.4 (7/98), Table 1.4-2 PM (Total). The lb/MMscf EF is converted to lb/MMBtu by dividing by the average heating content, 1020 Btu/scf, of the natural gas basis for the EF.

Streams to VCU ^a	Heat Content-HHV)		v to VCU ses to VCU ^{b,c}	H ₂ S Loss	es to VCU	Heat Inp	ut to VCU	NO _x En	nissions	CO Em	issions	PM/PM Emis	₁₀ /PM _{2.5} sions	VOC En	nissions	SO ₂ Em	nissions	H ₂ S Em	nissions
51. ca5 to 1 co	(Btu/scf, Btu/lb, or	(scfm or	(MMscf/yr	lb/hr	ton/yr	(MMBtu/hr)	(MMBtu/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)
	MMBtu/bbl)	lb/hr)	or ton/yr)	,	, ,.	((, , - ,	(,,	(10.17)	(,,	(, ,,	(,,	(101.77.7	(,	(,	(,,	(10.17)	(,,	(, ,.,
Assist Gas/Pilot Gas	1,020 Btu/scf	0.9 scfm	0.5 MMscf/yr			0.06	482.50	5.40E-03	2.37E-02	4.54E-03	1.99E-02	4.10E-04	1.80E-03	2.97E-04	1.30E-03	3.09E-03	1.35E-02		
Gasolines & Gasoline				0.00003	0.000001											5.01E-05	2.01E-06	1.33E-06	5.35E-08
Blendstocks	23,214 Btu/lb	51.9 lb/hr	4.89 ton/yr	0.00003	0.000001	1.20	227.19	1.69E-01	1.59E-02	1.69E-01	1.59E-02	8.98E-03	8.46E-04	2.59E+00	2.45E-01	J.01L-03	2.011-00	1.331-00	J.33L-08
Crude Oil	5.69 MMBtu/bbl	1.7 lb/hr	0.05 ton/yr	0.0016	0.0001	0.03	0.53	4.58E-03	3.70E-05	4.58E-03	3.70E-05	2.44E-04	1.97E-06	8.56E-02	2.30E-03	2.95E-03	1.48E-04	7.86E-05	3.93E-06
Light Cat Naphtha	23,214 Btu/lb	22.5 lb/hr	0.76 ton/yr	0.0005	0.00004	0.52	35.42	7.31E-02	2.48E-03	7.31E-02	2.48E-03	3.89E-03	1.32E-04	1.13E+00	3.81E-02	9.15E-04	6.84E-05	2.43E-05	1.82E-06
Sour Naphtha	23,214 Btu/lb	43.4 lb/hr	1.39 ton/yr	0.0021	0.0001	1.01	64.51	1.41E-01	4.52E-03	1.41E-01	4.52E-03	7.50E-03	2.40E-04	2.17E+00	6.95E-02	3.95E-03	2.22E-04	1.05E-04	5.89E-06
Sweet Naphtha	20,313 Btu/lb	13.2 lb/hr	0.43 ton/yr	-	-	0.27	17.41	3.75E-02	1.22E-03	3.75E-02	1.22E-03	2.00E-03	6.49E-05	6.60E-01	2.14E-02	-	-	-	-
Gas Oil	21,127 Btu/lb	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Straight Run Diesel	19,718 Btu/lb	15.3 lb/hr	0.39 ton/yr	0.0018	0.0012	0.30	15.20	4.21E-02	1.06E-03	4.21E-02	1.06E-03	2.24E-03	5.66E-05	7.63E-01	1.93E-02	3.36E-03	2.34E-03	8.93E-05	6.23E-05
Straight Run Kerosene	19,286 Btu/lb	5.8 lb/hr	0.17 ton/yr	-	-	0.11	6.58	1.58E-02	4.60E-04	1.58E-02	4.60E-04	8.39E-04	2.45E-05	2.92E-01	8.53E-03	-	-	-	-
Sour Water	26,786 Btu/lb	0.3 lb/hr	0.01 ton/yr	0.025	0.002	0.01	0.66	1.01E-03	4.60E-05	1.01E-03	4.60E-05	5.38E-05	2.45E-06	1.35E-02	6.14E-04	4.66E-02	3.98E-03	1.24E-03	1.06E-04
			MAX	(HOURLY (a	ssumes only	one landing a	t time), lb/hr	0.17		0.17		9.39E-03		2.60		0.05		1.24E-03	
	ANNUAL (assumes 51.5% tanks landed per year),						per year), tpy		0.04		0.03		2.50E-03		0.21		0.02		9.26E-05

Notes:

a. VCU may be used for the control of floating roof tanks landings. Temporary units may be rented or brought onsite as necessary

b. HC losses will not occur simoultanously.

c. A maximum annual of 51.5% landings will occur

Sample Calculations:

Gasoline Vapor Flow = (Uncontrolled Loading Emissions, lb/hr) from Fuels Truck Loading Rack Potential to Emit-VOC calculations

= 51.9 lb/hr

Gasoline Heat Input = Heat Content (Btu/lb)* Gasoline Vapor Flow (lb/hr) * 1MMBtu/10^6 Btu

= 23,214Btu/lb * 51.9 lb/hr * 1 MMBtu/1,000,000 Btu = 1.20 MMBtu/hr

Gasoline NOx = Emission Factor (lb/MMBtu) * Gasoline Heat Input (MMBtu/hr)

= 0.14 lb/MMBtu * 1.20 MMBtu/hr = 0.17 lb/hr

TVCU POTENTIAL TO EMIT GHG

Streams to VCU	Heat Input to VCU	Emissi	on Factors (kg/M	MBtu) ^a	Emissio	n Factors (lb/	MMBtu) ^a	Annua	I Emissions (ton/yr)	CHC
Streams to vco	(MMBtu/yr)	CO ₂	CH ₄	N ₂ O	CO2	CH ₄	N ₂ O	CO2	CH ₄	N ₂ O	GHG (as CO2e)
			Table A-1	TO 40 CFR 98	, subpart A, C	Global Warmi	ng Potentials	1	25	298	(as COZE)
Pilot Gas	482.50	53.06	0.001	0.0001	116.98	0.002	0.0002	28.2	5.3E-04	5.3E-05	28.25
Gasolines & Gasoline											
Blendstocks	227.19	70.22	0.003	0.001	154.81	0.007	0.001	17.6	7.5E-04	1.5E-04	17.65
Crude Oil	0.53	74.54	0.003	0.001	164.33	0.007	0.001	0.0	1.7E-06	3.5E-07	0.04
Light Cat Naphtha	35.42	68.02	0.003	0.001	149.96	0.007	0.001	2.7	1.2E-04	2.3E-05	2.67
Sour Naphtha	64.51	68.02	0.003	0.001	149.96	0.007	0.001	4.8	2.1E-04	4.3E-05	4.85
Sweet Naphtha	17.41	68.02	0.003	0.001	149.96	0.007	0.001	1.3	5.8E-05	1.2E-05	1.31
Gas Oil	0.00	75.10	0.003	0.001	165.56	0.007	0.001	0.0	0.0E+00	0.0E+00	0.00
Straight Run Diesel	15.20	73.96	0.003	0.001	163.05	0.007	0.001	1.2	5.0E-05	1.0E-05	1.24
Straight Run Kerosene	6.58	75.20	0.003	0.001	165.78	0.007	0.001	0.5	2.2E-05	4.4E-06	0.55
Sour Water	0.66	75.10	0.003	0.001	165.56	0.007	0.001	0.1	2.2E-06	4.3E-07	0.05
		•					TOTAL	42.8	0.001	0.0002	42.86

a. Emission factors from Tables C-1 and C-2 to 40 CFR 98, subpart C, for corresponsing products

CATALYST HANDLING STARTUP AND SHUTDOWN EMISSIONS (SSM MISC1)

(Exempt)

 $E(lb/ton) = k (0.0032) * (U/5)^{1.3} / (M/2)^{1.4}$ AP-42, Ch. 13.2.4 (11/06)

U, mean wind speed = 9.04 mph (annual average for Carlsbad, NM in AP-42 Table 7.1-9.)

M, material moisture content = 1 %
2015 Catalyst Handling Weight = 1,118 tons

Pollutant	k	Emission Factor	2015	PTE ^a
Tollutant	Dimensionless	lb/ton	tpy	tpy
PM	0.74	0.0135	0.008	0.015
PM10	0.35	0.0064	0.004	0.007
PM2.5	0.053	0.0010	0.001	0.001

a. PTE 2x the 2015 Rate.

Actuals from 2015:

Unit	Vessel	Task	Start	End	Weight (lbs)	Hours
33	D-0662	Unloading	1/14/15 2:00	1/15/15 8:00	307,725	30
33	D-0663	Unloading	1/14/15 4:00	1/15/15 10:00	282,153	30
33	D-0661	Unloading	1/15/15 6:00	1/16/15 12:00	164,519	30
33	D-0663	Loading	1/17/15 4:30	1/17/15 16:45	188,102	12.2
33	D-0662	Loading	1/18/15 10:20	1/18/15 19:45	205,150	9.4
33	D-0661	Loading	1/20/15 17:00	1/20/15 23:45	109,679	6.8
09	D-626	Unloading	2/17/15 0:00	2/18/15 0:00	9,000	24
09	D-626	Loading	2/20/15 0:00	2/21/15 0:00	9,000	24
09	D-627	Unloading	2/24/15 0:00	2/25/15 0:00	9,000	24
09	D-627	Loading	2/25/15 0:00	2/26/15 0:00	9,000	24
09	D-626	Loading	5/30/15 0:00	5/31/15 0:00	8,820	24
09	D-627	Unloading	6/3/15 0:00	6/4/15 0:00	13,230	24
09	D-627	Loading	6/4/15 0:00	6/5/15 0:00	8,820	24
09	D-626	Unloading	7/28/15 0:00	7/29/15 0:00	13,230	24
09	D-626	Loading	7/30/15 0:00	7/31/15 0:00	8,820	24
63	D-8801/2	Unloading	8/4/15 2:00	8/4/15 14:00	33,641	12
63	H-8801/2	Unloading	8/4/15 6:00	8/7/15 6:00	98,040	72
63	D-8801/2	Loading	8/4/15 14:00	8/5/15 2:00	22,427	12
09	D-627	Unloading	8/5/15 0:00	8/6/15 0:00	13,230	24
63	D-8803	Unloading	8/5/15 10:00	8/5/15 22:00	78,456	12
63	D-8803	Loading	8/5/15 22:00	8/6/15 12:00	52,304	14
09	D-627	Loading	8/7/15 0:00	8/8/15 0:00	8,820	24
63	H-8801/2	Loading	8/7/15 6:00	8/9/15 10:00	65,360	52
13	D-0042	Unloading	8/25/15 0:00	8/26/15 0:00	11,496	24
13	D-0042	Loading	9/2/15 0:00	9/3/15 0:00	7,664	24
20	D-0282	Unloading	10/19/15 21:00	10/21/15 14:00	43,886	41
20	D-0282	Loading	10/21/15 14:00	10/23/15 17:00	34,776	51
09	D-626	Unloading	10/26/15 0:00	10/27/15 0:00	13,230	24
09	D-626	Loading	10/27/15 0:00	10/28/15 0:00	8,820	24
6	D-0063	Unloading	11/3/15 2:00	11/3/15 14:00	36,580	12
6	D-0063	Loading	11/4/15 2:00	11/4/15 16:00	31,139	14
09	D-627	Unloading	11/8/15 0:00	11/9/15 0:00	13,230	24
09	D-627	Loading	11/9/15 0:00	11/10/15 0:00	8,820	24
45	D-2479	Unloading	12/12/15 20:00	12/17/15 13:00	169,572	113
45	D-2479	Loading	12/19/15 7:00	12/21/15 3:00	124,038	44
09	D-626	Unloading	12/31/15 0:00	1/1/16 0:00	13,230	24

TOTAL: 2,235,006 999

CRUDE OIL LINE PIGGING

Chamber Length, L	20	ft	Field specification
Chamber Diameter, D	1.33	ft	Field specification
Chamber Volume, V	27.93	ft3	V = pi()/4*D^2*L
Chamber Gage Pressure, P	100	psig	Field specification
Chamber Temperature, T	529.67	°R	Field specification
Molecular Weight of Gas Mixture, MW	50	lb/lbmol	AP-42, Ch. 7.1(6/20) Table 7.1-2
Compressibility Factor, C _Z	1		
Pressurized Density, ρ _{press}	1.01	lb/ft ³	ρ_{press} =(P+14.7)*MW/(10.73*T*C _z)
Atmospheric Density, ρ _{atm}	0.13	lb/ft ³	ρ_{atm} =14.7*MW/(10.73*T*C _z)
Delta Density, Δρ	0.88	lb/ft ³	$\Delta \rho = \rho_{press} - \rho_{atm}$
Amount of Gas Vented per Event, m _E	24.57	lbs	$m_E = \Delta \rho * V$
# of Events	52		
# of Purges per Event	1		
Event Duration	1	hr	
Controlled? (Y/N)	No		
Control Type	n/a		
Control Efficiency	0%		
Total Amount of Gas Vented, m _T	1,278	lb/yr	m _T = m _E * # Events * # Purges/Event * (1 - Control Eff)
Total VOC Weight Fraction	100%		
VOC Hourly Emissions	24.57	lb/hr	VOC Hourly Emissions = m _E * VOC% / Event Duration
VOC Annual Emissions	0.64	tpy	VOC Annual Emissions = m _T * VOC% * 1 ton/2000 lb

Section 7

Information Used To Determine Emissions

Information Used to Determine Emissions shall include the following:

If manufacturer data are used, include specifications for emissions units <u>and</u> control equipment, including control efficiencies specifications and sufficient engineering data for verification of control equipment operation, including design drawings, test reports, and design parameters that affect normal operation.
If test data are used, include a copy of the complete test report. If the test data are for an emissions unit other than the one
being permitted, the emission units must be identical. Test data may not be used if any difference in operating conditions of the unit being permitted and the unit represented in the test report significantly effect emission rates.
If the most current copy of AP-42 is used, reference the section and date located at the bottom of the page. Include a copy of the page containing the emissions factors, and clearly mark the factors used in the calculations.
If an older version of AP-42 is used, include a complete copy of the section.
If an EPA document or other material is referenced, include a complete copy.
Fuel specifications sheet.
If computer models are used to estimate emissions, include an input summary (if available) and a detailed report, and a disk containing the input file(s) used to run the model. For tank-flashing emissions, include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., permit or major source (NSPS, PSD or Title V)),
accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any

assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis.

The information used to determine emissions is as follows:

ROUTINE OPERATIONS

- Boilers and Heaters

- NO_X emissions from boilers and heaters are based on each unit design capacity, 8,760 hours per year operation, and the manufacturers' guaranteed NO_X emissions except as follows:
 - NO_X emissions from South Crude Charge Heaters H-0019 and H-0020, Unit 21 Heater H-0028, Unit 54 HDS Reactor Heater H-5401, Unit 70 CCR Reformer Heaters H-0352, H-0353, and H-0354, Unit 70 CCR Heaters H-0362, H-0363, and H-0364, are estimated using stack testing data.
 - NO_X emissions from H-8001/8002 are based on CEMS data.
 - NO_X emissions Unit 21 Vacuum Unit Heater H-0011 are estimated using NO_X emission factor from AP-42, Section 1.4 (5/74).
- O CO (except as noted below), VOC (except as noted below), and PM/PM₁₀/PM_{2.5} emissions are based on each unit design capacity, 8,760 hours per year operation, in combination with emission factors from AP-42, Section 1.4 (7/98) Tables 1.4-1 and 1.4-2.
 - CO emissions from Boiler B-0009, Unit 25 ROSE Unit No. 2 Hot Oil Heater H-2501, Unit 54 HDS Reactor Heater H-5401, and Unit 64 Hydrogen Plant Reformer H-9851 are based on the manufacturers' guaranteed CO emissions.
 - VOC emissions from Boiler B-0009 is based on manufacturer's guaranteed VOC emissions.
- SO₂ emissions, except as noted below, are based on the NSPS subpart Ja limit of 162 ppm_{H2S} (0.1 gr_{H2S}/dscf) on 3-hr rolling, and the NSPS Ja limit of 60 ppmv_{H2S} (0.037 gr_{H2S}/dscf) on a 365-day calendar rolling average limit plus non-H₂S species present in the refinery fuel gas ("RFG") as determined based on sampling data.
 - B-0009 SO₂ emissions calculated as currently authorized: 0.035 gr_S/scf fuel and a HHV of 845 Btu/scf.
 - H-8801, H-8802, and H-9851 will combust a mixture of PSA Offgas and amine-treated RFG. It has been conservatively assumed 50/50 mix for SO₂ emissions calculation.

- HAPs emissions are based on each unit design capacity, 8,760 hours per year operation, and AP-42,
 Section 1.4 (7/98), Table 1.4-3 emissions factors.
- Ammonia slip emissions from Unit 64 Hydrogen Plant Reformer Heater H-9851 are based on 7 parts per million volume ("ppmv,") wet basis slip, and the heater exhaust flow rate of 73,500 standard cubic feet per minute.
- O GHG emissions are based on Tables C-1 and C-2 to Subpart C of Part 98 emission factors for fuel gas, and Table A-1 to Subpart A of Part 98 global warning potentials.

- SRU2 TGI (H-0473) and SRU3 TGI (H-3103)

- NO_X, CO, and VOC emissions are based on the tail gas incinerators maximum and average exhaust flow rate and estimated pollutant concentrations.
- o SO₂ and H₂S emissions are based on the tail gas incinerator maximum and average exhaust flow rate and continuous emission monitoring ("CEMS") data for SO₂ and continuous monitoring for H₂S.
- o SAM emissions from the SRUs are conservatively assumed to be equal to a 5% oxidation of SO₂ emissions. No reduction of the SO₂ emissions due to the conversion to SAM is proposed.
- o PM emissions are based on the tail gas incinerators maximum and average exhaust flow rate and the Chevron Pascagoula Refinery Emissions Test Data (2007) as included in AP-42, Chapter 8.13 (4/15.) PM₁₀/PM_{2.5} emissions are conservatively assumed to be equal to the sum of PM and SAM emissions.
- O GHG emissions from the SRUs are based on maximum sour gas volumetric flow rate to each SRU 2 and SRU3 and Subpart Y to Part 98 default mole fraction of carbon in the sour gas.

FCC Regen

- NO_X emissions from the FCC are calculated based on the FCC stack exhaust flow rate and the Artesia Refinery's Consent Decree NO_X maximum hourly emission limit of 87.3 ppmvd at 0% oxygen on a 7-day rolling average basis, and an annual limit of 58.1 ppmvd at 0% oxygen on a 365-day rolling average basis.
- O CO emissions from the FCC are calculated based on the FCC stack exhaust flow rate and NSPS Subpart J maximum hourly emissions standard of 500 ppmvd at 0% oxygen on a 1-hr average basis (40 CFR §§ 60.103(a) and 60.106(d)), and an annual emissions standard of 100 ppmvd at 0% oxygen on a 365-day rolling average basis (PSD-NM-0195-M39R4 A211.A(2)(b).)
- VOC emissions from the FCC are conservatively assumed to be 200% of the semi volatile and volatile HAPs.
- o SO₂ emissions from the FCC are calculated based on the FCC stack exhaust flow rate and the Artesia Refinery's Consent Decree SO₂ maximum hourly emission limit of 50 ppmvd at 0% oxygen, on a 7-day rolling average basis, and annual average limit of 25 ppmvd at 0% oxygen on a 365-day rolling avg. basis.
- o SAM emissions from the FCC are conservatively assumed to be equal to a 5% oxidation of SO₂ emissions. No reduction of the SO₂ emissions due to the conversion to SAM is proposed.
- o PM emissions are calculated based on the FCC maximum coke burn rate and NSPS Subpart J maximum hourly emission rate of 2 lb/ per ton of coke burn-off in the catalyst regenerator (§60.102(a)(1.)) PM₁₀/PM_{2.5} emissions are conservatively assumed to be equal to the sum of 83% of PM and 100% of SAM emissions. For annual PM2.5 is assumed to be 58.6% of PM and 100% of SAM.
- HAPs emissions are conservatively calculated using the worst-case emission factor as published in "Emissions Estimation Protocol for Petroleum Refineries, Version 3" (April 2015) and the highest reported emissions factor based on ICR reported FCCU data and NPRA capacities, and the FCC capacity and maximum coke burn rate.
- O GHG emissions associated with FCC are based on the maximum reported rate between 2011 and 2015 (calculated according to Subpart Y of Part 98) increased by 100% to estimate the potential to emit.

- Flares

Emissions of CO and NO_X from the flares (FL-0400 North Plant Flare, FL-0401 South Plant Flare, FL-0402 FCC Flare, FL-0403 Alky Flare, and FL-0404 GOHT Flare) are based on heat input to the flare in combination with emission factors from AP-42, Section 13.5 (2/18), Tables 13.5-1 and 13.5-2 respectively. Heat input is based on flare monitoring data required by NSPS Ja (i.e., 40 CFR Part 60, Subpart Ja).

- Emissions of VOC and SO₂ from the flares (FL-0400 North Plant Flare, FL-0401 South Plant Flare, FL-0402 FCC Flare, FL-0403 Alky Flare, and FL-0404 GOHT Flare) are based on mass balance calculations and flare monitoring data required by NSPS Ja (i.e., 40 CFR Part 60, Subpart Ja).
- GHG emissions are calculated using 40 CFR 98, Subpart Y, equations Y-1b, Y-4 and Y-5 for flares.

Engines

- NO_X, CO, VOC and PM/PM₁₀/PM_{2.5} emissions are based on each engine horsepower rating, hours of operation, and:
 - 40 CFR §89.112, Table 1 emission standards⁴ in accordance with 40 CFR §60.4204(b) for engines with a rating less than 3,000 hp, with a displacement less than 10 liters per cylinder, and manufactured prior to 2014 (i.e., portable air compressors MG-0001 and MG-0002, portable fire water pump engine MG-0004, and server backup generator SG-0102.)
 - 40 CFR §1039.101 emission standards in accordance with 40 CFR §60.4204(b) for engines with a rating less than 3,000 hp, with a displacement less than 10 liters per cylinder, and manufactured after 2014 (i.e., portable air compressor MG-0003.)
 - Table 4 to Subpart IIII of Part 60 emission standards per 40 CFR §60.4205(c) for firewater pump engines (i.e., FWG-0600, FWG-0601, FWG-0602, and FWG-0603.)
 - AP-42, Chapter 3.3 (10/96), Table 3.3-1 emission factors for engines manufactured prior to 2005 (i.e., UPS backup generators SG-0100 and SG-0101.)
- SO₂ emissions are based on each engine horsepower rating, hours of operation, and on a maximum sulfur content of 15 parts per million sulfur content in diesel oil per 40 CFR §§ 60.4207 and 1090.305.
- HAPs emissions are based on each engine horsepower rating in combination with emission factors from AP-42, Section 3.3 (10/96), Table 3.3-2 for diesel-fired engines.
- GHG emissions are based on Tables C-1 and C-2 to Subpart C of Part 98 emission factors for distillate fuel oil No. 2, and Table A-1 to Subpart A of Part 98 global warming potentials.

Cooling Towers

- PM/PM₁₀/PM_{2.5} emissions from the cooling towers are based on each cooling tower water circulation rate, annual hours of operation, total dissolved solids water concentration, and drift eliminator efficiency, in accordance with AP-42, Chapter 13.4 (1/95.). PM₁₀/PM_{2.5} emissions are calculated in accordance with NMED's Technical Memorandum "Calculating TSP, PM-10 and PM-2.5 from Cooling Towers" dated 9/9/2013.
- VOC emissions from the cooling towers are based on each cooling tower water circulation rate and AP-42, Chapter 5.1 (4/15) Table 5.1-3 emission factor.
- HAPs emissions are estimated assuming a worst-case HAP content in the VOC emitted at the cooling towers equivalent to the HAPs content in naphtha. The HAPs liquid weight percent was defined in accordance with the American Petroleum Institute ("API") Standard 4723-A "Refinery Stream Composition Data Update to *Speciation data in API 4723*" (12/2018)

Wastewater

VOC emissions are estimated using EPA Water9 V.3, and wastewater stream composition as determined from ToxChem and analytical data.

Truck and Rail Loading

- VOC loading losses from truck and railcar loading racks are based on maximum hourly and average annual loading throughputs, the commodities chemical specifications, type of loading, and in accordance with AP-42, Chapter 5.2 (6/2008).
- For gasoline loading at TL-4, VOC loading losses are based on 10 milligrams of total organic compounds per liter of gasoline loaded standard in 40 CFR §63.422(b) as required by Subpart CC to Part 63 (§63.650(a))
- H₂S from molten sulfur loading at TRLO-9 is based on sulfur production, loading rack capacity, loading temperatures, H₂S expected concentration in molten sulfur, Raoult's Law, and efficiency of proposed controls.
- HAPs emissions are estimated assuming a worst-case HAP content in each loaded commodity. The HAPs liquid weight percent was defined in accordance with the API Standard 4723-A "Refinery Stream

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⁴ A conversion factor of 1 hp = 0.7457 kW was used to convert emission standards in g/kWhr to g/hp-hr.

Composition Data Update to Speciation data in API 4723" (12/2018.) Raoult's Law is used to estimate vapor weight percent from liquid weight percent.

- Truck Loading Rack TL-4 Vapor Combustion Unit ("VCU")

- NOx, CO, and VOC emissions from the combustion of assist gas/pilot gas are based on a maximum flow to the VCU and AP-42, Section 1.4 (7/98), Table 1.4-1 small uncontrolled boilers.
- NO_X, CO, and VOC emissions from the combustion of hydrocarbon vapors are based on a maximum flow to the VCU and the manufacturer specifications.
- o PM/PM₁₀/PM_{2.5} emissions from the combustion of assist gas/pilot gas and hydrocarbon vapors are based on a maximum flow to the VCU and AP-42, Section 1.4 (7/98), Table 1.4-1 small uncontrolled boilers.
- o SO₂ emissions are based on the maximum flow to the VCU and a maximum of 20 grains per 100 scf of gas per PSD-NM-0195-M39R4, C101.G Natural Gas definition.
- o GHG emissions are based on Tables C-1 and C-2 to Subpart C of Part 98 emission factors as applicable to each stream, and Table A-1 to Subpart A of Part 98 global warning potentials.

- Fugitives

- O VOC emissions from equipment component leaks are based on the facilities latest Leak Detection and Repair ("LDAR") component counts, and the emission factors published in the "Protocol for Equipment Leak Estimates," EPA-453/R-95-017 (November 1995), Table 2-2 "Refinery Average Emission Factors", and the control efficiencies in Table 5-3 "Control Effectiveness for an LDAR Program at a Refinery Process Unit", and the Texas Commission on Environmental Quality ("TCEQ") Air Permit Technical Guidance for Chemical Sources Fugitive Guidance APDG 6422 June 2018.
- HAPs emissions are estimated assuming a worst-case HAP content in each process stream. The HAPs liquid weight percent was defined in accordance with the API Standard 4723-A "Refinery Stream Composition Data Update to Speciation data in API 4723" (12/2018.) Raoult's Law is used to estimate vapor weight percent from liquid weight percent.
- OGHG emissions from fugitive piping components are based on Subpart Y to Part 98, equation Y-21. The CCR catalytic reforming unit only has fugitive emission sources reported in the permit. Additional GHG emissions associated with catalyst regeneration is included with the fugitive emissions. The maximum reported rate between 2011 and 2015 was increased by 100% to estimate the potential to emit.

- Storage Tanks

- O VOC losses from fixed roof and floating roof tanks during tank routine operations and routine and predictable SSM are calculated based on annual tank throughputs, tanks construction specifications, stored commodities chemical specifications, and AP-42, Chapter 7.1 (6/2020) methodology and factors. The stored commodities chemical specifications were developed based on published data (i.e., AP-42, Chapter 7.1 (6/2020), API Manual of Petroleum Measurement Standards Chapter 19.4 (6/2017),) average storage temperatures, and facility analytical data.
- O HAPs emissions are estimated assuming a worst-case HAP content in each stored commodity. The HAPs liquid weight percent was defined in accordance with the API Standard 4723-A "Refinery Stream Composition Data Update to Speciation data in API 4723" (12/2018.) Raoult's Law is used to estimate vapor weight percent from liquid weight percent.
- o GHG emissions from storage tanks are based on Subpart Y to Part 98, equation Y-22.

STARTUP, SHUTDOWN, AND MAINTENANCE (SSM)

- Unit 64 Hydrogen Plant Reformer H-9851 SSM

- CO, VOC, PM/PM₁₀/PM_{2.5} and SO₂ emissions from H-9851 are expected to remain consistent with routine operations emissions. Therefore, the same calculation methodology is used for estimating emissions for these pollutants during SSM of H-9851.
- O During SSM, H-9851 selective catalytic reduction ("SCR") control for NO_X emissions will only achieve 0.03 lb/MMBtu NO_X per manufacturer specifications. Emissions for SSM may occur for no more than 240 hours per year.

- SRU2 ((H-0473) and SRU3 (H-3103) SSM

o Routine or predictable SSM emissions are not expected to differ from routine emissions for NO_X, CO, VOC and PM. SO₂ and H₂S emissions are based on the expected sulfur feed per event during startup and shutdown, and the duration of each event.

- Flares SSM

o SSM Flare emissions are calculated in the same manner as routine emissions, using flare stream monitoring required by NSPS Ja (i.e., 40 CFR Part 60, Subpart Ja).

- SSM FL-HEP-PORT

- o Emissions of NO_X, CO, and VOC from the FL-HEP-PORT flare are based on a maximum flaring flowrate per event and emission factors from AP-42, Section 13.5 (2/18), Tables 13.5-1 and 13.5-2 respectively. Heat input is based on a default 1,020 Btu/scf (HHV) for natural gas.
- o Emissions of SO₂ and H₂S are based on a maximum flaring flowrate per event and 0.25 grains of sulfur per dry standard cubic foot expected in natural gas.
- o GHG emissions are calculated using 40 CFR 98, Subpart Y, equation Y-2, Y-4 and Y-5 for CO₂, CH₄, and N₂O respectively, and 40 CFR §98.253(b)(1) CO₂ emission factor for flares, and Table C-2 to Part 98, Subpart C, default emission factors for CH₄ and N₂O for natural gas.

- Tanks SSM

Emissions for routine and predictable SSM from floating roof storage tanks were calculated using AP-42, Chapter 7 drain dry landings equations, as summarized in Table 7.1-19. During SSM activities, all standing liquid in the tank is removed. A small layer of liquid of approximately 3 inches may remain clinging, which is further reduced with a pump until suction is lost and the tank is safe to entry. Landing emissions from all internal and external floating roof tanks were estimated assuming 1 day landing event, and 0.25 ft of liquid at the tank shell.

- Floating Roof Tanks Landings Vapor Combustion Unit ("VCU")

During certain floating roof tank landings, a temporary VCU may be brought onsite to control losses from the roof landing activities. Emissions from combustion at the VCU are estimated as follows:

- o NOx, CO, and VOC emissions from the combustion of assist gas/pilot gas are based on a maximum flow to the VCU and AP-42, Section 1.4 (7/98), Table 1.4-1 small uncontrolled boilers.
- NO_X, CO, and VOC emissions from the combustion of hydrocarbon vapors are based on a maximum flow to the VCU and the manufacturer specifications.
- o PM/PM₁₀/PM_{2.5} emissions from the combustion of assist gas/pilot gas and hydrocarbon vapors are based on a maximum flow to the VCU and AP-42, Section 1.4 (7/98), Table 1.4-1 small uncontrolled boilers.
- o SO₂ emissions are based on the maximum flow to the VCU and a maximum of 20 grains per 100 scf of gas per PSD-NM-0195-M39R4, C101.G Natural Gas definition.
- o GHG emissions are based on Tables C-1 and C-2 to Subpart C of Part 98 emission factors as applicable to each stream, and Table A-1 to Subpart A of Part 98 global warning potentials.

- SSM MISC 1 – Catalyst Handling

- o Emissions of PM, PM₁₀ and PM_{2.5} are calculated using AP-42, Chapter 13.2.4 (11/06) and the expected amount of annual catalyst handling, based on double the amount handled in 2015.
- o The catalyst handling potential to emit is no more than one-half (1/2) ton per year of PM, PM₁₀ and PM_{2.5}, and therefore, emissions from this activity are exempt per 20.2.72.202.B(5) NMAC.

- SSM MISC 2 – Low Emitting Activities

Low-Emitting Maintenance Activities such as de-inventorying small equipment, clearing piping associated with emission units, and routine maintenance activities such as heat exchanger repair. Emissions are estimated as ten percent of the historical emissions from flares and the TGI.

- Crude Oil Pipeline Pigging Activities

Emissions from pigging activities in the crude oil pipelines are expected to occur weekly. Prior to blowdown, chamber is expected to be at approximately 100 psig and 70 degrees Fahrenheit. Annual mass emissions from each depressurization event is calculated assuming ideal gas law mass balance.

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Information Used to Determine Emissions

- Boilers and Heaters
- SRU
- FCC Regen
- Flares
- Engines
- Cooling Towers
- Fugitives

Boilers and Heaters

Table 1.4-1. EMISSION FACTORS FOR NITROGEN OXIDES (NO_x) AND CARBON MONOXIDE (CO) FROM NATURAL GAS COMBUSTION^a

Combustor Tyres	И	10^{x}	со	
Combustor Type (MMBtu/hr Heat Input) [SCC]	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
Large Wall-Fired Boilers (>100)				
[1-01-006-01, 1-02-006-01, 1-03-006-01]				
Uncontrolled (Pre-NSPS) ^c	280	A	84	В
Uncontrolled (Post-NSPS) ^c	190	A	84	В
Controlled - Low NO _x burners	140	A	84	В
Controlled - Flue gas recirculation	100	D	84	В
Small Boilers (<100) [1-01-006-02, 1-02-006-02, 1-03-006-02, 1-03-006-03]				
Uncontrolled	100	В	84	В
Controlled - Low NO _x burners	50	D	84	В
Controlled - Low NO _x burners/Flue gas recirculation	32	C	84	В
Tangential-Fired Boilers (All Sizes) [1-01-006-04]				
Uncontrolled	170	A	24	C
Controlled - Flue gas recirculation	76	D	98	D
Residential Furnaces (<0.3) [No SCC]				
Uncontrolled	94	В	40	В

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. To convert from lb/10 ⁶ scf to kg/10⁶ m³, multiply by 16. Emission factors are based on an average natural gas higher heating value of 1,020 Btu/scf. To convert from 1b/10 ⁶ scf to lb/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. SCC = Source Classification Code. ND = no data. NA = not applicable. Expressed as NO₂. For large and small wall fired boilers with SNCR control, apply a 24 percent reduction to the appropriate NO _X emission factor. For

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tangential-fired boilers with SNCR control, apply a 13 percent reduction to the appropriate NO x emission factor.

on NSPS=New Source Performance Standard as defined in 40 CFR 60 Subparts D and Db. Post-NSPS units are boilers with greater than 250 MMBtu/hr of heat input that commenced construction modification, or reconstruction after August 17, 1971, and units with heat input capacities between 100 and 250 MMBtu/hr that commenced construction modification, or reconstruction after June 19, 1984.

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TABLE 1.4-2. EMISSION FACTORS FOR CRITERIA POLLUTANTS AND GREENHOUSE GASES FROM NATURAL GAS COMBUSTION^a

Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
CO ₂ ^b	120,000	A
Lead	0.0005	D
N ₂ O (Uncontrolled)	2.2	Е
N ₂ O (Controlled-low-NO _X burner)	0.64	Е
PM (Total) ^c	7.6	D
PM (Condensable) ^c	5.7	D
PM (Filterable) ^c	1.9	В
SO_2^d	0.6	A
TOC	11	В
Methane	2.3	В
VOC	5.5	С

- a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from lb/10⁶ scf to kg/10⁶ m³, multiply by 16. To convert from lb/10⁶ scf to 1b/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. TOC = Total Organic Compounds. VOC = Volatile Organic Compounds.
- ^b Based on approximately 100% conversion of fuel carbon to CO_2 . $CO_2[lb/10^6 \text{ scf}] = (3.67)$ (CON) (C)(D), where CON = fractional conversion of fuel carbon to CO_2 , C = carbon content of fuel by weight (0.76), and D = density of fuel, $4.2 \times 10^4 \text{ lb}/10^6 \text{ scf}$.
- ^c All PM (total, condensible, and filterable) is assumed to be less than 1.0 micrometer in diameter. Therefore, the PM emission factors presented here may be used to estimate PM₁₀, PM_{2.5} or PM₁ emissions. Total PM is the sum of the filterable PM and condensible PM. Condensible PM is the particulate matter collected using EPA Method 202 (or equivalent). Filterable PM is the particulate matter collected on, or prior to, the filter of an EPA Method 5 (or equivalent) sampling train.
- d Based on 100% conversion of fuel sulfur to SO₂.

 Assumes sulfur content is natural gas of 2,000 grains/10⁶ scf. The SO₂ emission factor in this table can be converted to other natural gas sulfur contents by multiplying the SO₂ emission factor by the ratio of the site-specific sulfur content (grains/10⁶ scf) to 2,000 grains/10⁶ scf.

TABLE 1.4-3. EMISSION FACTORS FOR SPECIATED ORGANIC COMPOUNDS FROM NATURAL GAS COMBUSTION $^{\rm a}$

CAS No.	Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
91-57-6	2-Methylnaphthalene ^{b, c}	2.4E-05	D
56-49-5	3-Methylcholanthrene ^{b, c}	<1.8E-06	E
	7,12- Dimethylbenz(a)anthracene ^{b,c}	<1.6E-05	E
83-32-9	Acenaphthene ^{b,c}	<1.8E-06	Е
203-96-8	Acenaphthylene ^{b,c}	<1.8E-06	Е
120-12-7	Anthracene ^{b,c}	<2.4E-06	Е
56-55-3	Benz(a)anthracene ^{b,c}	<1.8E-06	Е
71-43-2	Benzene ^b	2.1E-03	В
50-32-8	Benzo(a)pyrene ^{b,c}	<1.2E-06	Е
205-99-2	Benzo(b)fluoranthene ^{b,c}	<1.8E-06	Е
191-24-2	Benzo(g,h,i)perylene ^{b,c}	<1.2E-06	Е
207-08-9	Benzo(k)fluoranthene ^{b,c}	<1.8E-06	E
106-97-8	Butane	2.1E+00	Е
218-01-9	Chrysene ^{b,c}	<1.8E-06	Е
53-70-3	Dibenzo(a,h)anthracene ^{b,c}	<1.2E-06	Е
25321-22- 6	Dichlorobenzene ^b	1.2E-03	E
74-84-0	Ethane	3.1E+00	Е
206-44-0	Fluoranthene ^{b,c}	3.0E-06	Е
86-73-7	Fluorene ^{b,c}	2.8E-06	Е
50-00-0	Formaldehyde ^b	7.5E-02	В
110-54-3	Hexane ^b	1.8E+00	Е
193-39-5	Indeno(1,2,3-cd)pyrene ^{b,c}	<1.8E-06	Е
91-20-3	Naphthalene ^b	6.1E-04	Е
109-66-0	Pentane	2.6E+00	E
85-01-8	Phenanathrene ^{b,c}	1.7E-05	D
74-98-6	Propane	1.6E+00	Е

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CAS No.	Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
129-00-0	Pyrene ^{b, c}	5.0E-06	E
108-88-3	Toluene ^b	3.4E-03	С

- ^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from lb/10⁶ scf to kg/10⁶ m³, multiply by 16. To convert from 1b/10⁶ scf to lb/MMBtu, divide by 1,020. Emission Factors preceded with a less-than symbol are based on method detection limits.
- ^b Hazardous Air Pollutant (HAP) as defined by Section 112(b) of the Clean Air Act.
- ^c HAP because it is Polycyclic Organic Matter (POM). POM is a HAP as defined by Section 112(b) of the Clean Air Act.
- ^d The sum of individual organic compounds may exceed the VOC and TOC emission factors due to differences in test methods and the availability of test data for each pollutant.

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TABLE 1.4-4. EMISSION FACTORS FOR METALS FROM NATURAL GAS COMBUSTION^a

CAS No.	Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
7440-38-2	Arsenic ^b	2.0E-04	Е
7440-39-3	Barium	4.4E-03	D
7440-41-7	Beryllium ^b	<1.2E-05	Е
7440-43-9	Cadmium ^b	1.1E-03	D
7440-47-3	Chromium ^b	1.4E-03	D
7440-48-4	Cobalt ^b	8.4E-05	D
7440-50-8	Copper	8.5E-04	C
7439-96-5	Manganese ^b	3.8E-04	D
7439-97-6	Mercury ^b	2.6E-04	D
7439-98-7	Molybdenum	1.1E-03	D
7440-02-0	Nickel ^b	2.1E-03	C
7782-49-2	Selenium ^b	<2.4E-05	Е
7440-62-2	Vanadium	2.3E-03	D
7440-66-6	Zinc	2.9E-02	E

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. Emission factors preceded by a less-than symbol are based on method detection limits. To convert from $lb/10^6$ scf to $kg/10^6$ m³, multiply by l6. To convert from $lb/10^6$ scf to 1b/MMBtu, divide by 1,020.

^b Hazardous Air Pollutant as defined by Section 112(b) of the Clean Air Act.

NO_X Emissions Unit 21 Vacuum Unit Heater H-0011

Revised by Thomas Lahre

1.4 NATURAL GAS COMBUSTION

1.4.1 General 1,2

Natural gas has become one of the major fuels used throughout the country. It is used mainly for power generation, for industrial process steam and heat production, and for domestic and commercial space heating. The primary component of natural gas is methane, although varying amounts of ethane and smaller amounts of nitrogen, helium, and carbon dioxide are also present. The average gross heating value of natural gas is approximately 1050 Btu/stdft³ (9350 kcal/Nm³), varying generally between 1000 and 1100 Btu/stdft³ (8900 to 9800 kcal/Nm³).

Because natural gas in its original state is a gaseous, homogenous fluid, its combustion is simple and can be precisely controlled. Common excess air rates range from 10 to 15 percent; however, some large units operate at excess air rates as low as 5 percent to maximize efficiency and minimize nitrogen oxide (NO_x) emissions.

1.4.2 Emissions and Controls 3-16

Even though natural gas is considered to be a relatively clean fuel, some emissions can occur from the combustion reaction. For example, improper operating conditions, including poor mixing, insufficient air, etc., may cause large amounts of smoke, carbon monoxide, and hydrocarbons to be produced. Moreover, because a sulfur-containing mercaptan is added to natural gas for detection purposes, small amounts of sulfur oxides will also be produced in the combustion process.

Nitrogen oxides are the major pollutants of concern when burning natural gas. Nitrogen oxide emissions are a function of the temperature in the combustion chamber and the rate of cooling of the combustion products. Emission levels generally vary considerably with the type and size of unit and are also a function of loading.

In some large boilers, several operating modifications have been employed for NO_X control. Staged combustion, for example, including off-stoichiometric firing and/or two-stage combustion, can reduce NO_X emissions by 30 to 70 percent. In off-stoichiometric firing, also called "biased firing," some burners are operated fuel-rich, some fuel-lean, while others may supply air only. In two-staged combustion, the burners are operated fuel-rich (by introducing only 80 to 95 percent stoichiometric air) with combustion being completed by air injected above the flame zone through second-stage "NO-ports." In staged combustion, NO_X emissions are reduced because the bulk of combustion occurs under fuel-rich, reducing conditions.

Other NO_x-reducing modifications include low excess air firing and flue gas recirculation. In low excess air firing, excess air levels are kept as low as possible without producing unacceptable levels of unburned combustibles (carbon monoxide, hydrocarbons, and smoke) and/or other operational problems. This technique can reduce NO_x emissions by 10 to 30 percent primarily because of the lack of availability of oxygen during combustion. Flue gas recirculation into the primary combustion zone, because the flue gas is relatively cool and oxygen deficient, can also lower NO_x emissions by 20 to 60 percent depending on the amount of gas recirculated. At present only a few systems have this capability, however.

Combinations of the above combustion modifications may also be employed to further reduce NO_x emissions. In some boilers, for instance, NO_x reductions as high as 70 to 90 percent have been produced as a result of employing several of these techniques simultaneously. In general, however, because the net effect of any of these combinations varies greatly, it is difficult to predict what the overall reductions will be in any given unit.

Emission factors for natural gas combustion are presented in Table 1.4-1. Flue gas cleaning equipment has not been utilized to control emissions from natural gas combustion equipment.

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External Combustion Sources

1.4-1

Table 1.4-1. EMISSION FACTORS FOR NATURAL-GAS COMBUSTION EMISSION FACTOR RATING: A

	Type of unit					
			Industria	l process	Domes	tic and
	Power	r plant	bo	iler	commerc	ial heating
Pollutant	lb/106 ft ³	kg/106 m ³	lb/106 ft3	kg/106 m ³	lb/106 ft ³	kg/106 m ³
Particulates ^a	5-15	80-240	5-15	80-240	5-15	80-240
Sulfur oxides (SO ₂)b	0.6	9.6	0.6	9.6	0.6	9.6
Carbon monoxidec	17	272	17	272	20	320
Hydrocarbons (as CH ₄) ^d	1	16	3	48	8	128
Nitrogen oxides (NO ₂) ^e	700f-h	11,200 ^{f-h}	(120-230) ⁱ	(1920- 3680) [†]	(80-120)i.	(1280- 1920)i

^aReferences 4,7,8,12,

J Use 80 (1280) for domestic heating units and 120 (1920) for commercial units.

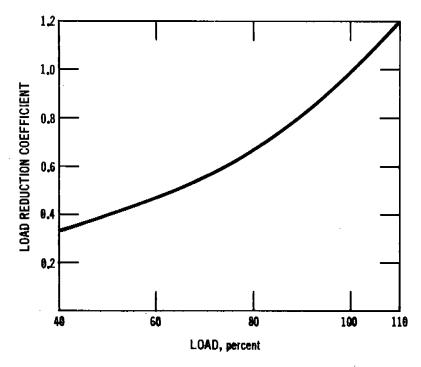


Figure 1.4-1. Load reduction coefficient as function of boiler load. (Used to determine NO_X reductions at reduced loads in large boilers.)

bReference 4 (based on an average sulfur content of natural gas of 2000 gr/106 stdft3 (4600 g/106 Nm3).

^CReferences 5, 8-12.

dReferences 8, 9, 12,

e References 3-9, 12-16.

 $^{^{\}rm f}$ Use 300 lb/10 $^{\rm \acute{e}}$ stdft $^{\rm 3}$ (4800 kg/10 $^{\rm 6}$ Nm $^{\rm 3}$) for tangentially fired units.

⁹At reduced loads, multiply this factor by the load reduction coefficient given in Figure 1.4-1.

hSee text for potential NO_X reductions due to combustion modifications. Note that the NO_X reduction from these modifications will also occur at reduced load conditions.

ⁱ This represents a typical range for many industrial boilers. For large industrial units (> 100 MMBtu/hr) use the NO_X factors presented for power plants.

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1.4-3

Sulfur Recovery Units

EMISSIONS TEST REPORT

For Particulate Matter and Gaseous Pollutants on Sulfur Recovery Units 2 and 3

Designated as F-2745 and F2765

at the ChevronTexaco Pascagoula Refinery

Located in Pascagoula, Mississippi

Prepared for CHEVRON PRODUCTS USA

TRC Project No. 155910 Test Date: November 27 and 28, 2007

Summary of Results F-2745

Plant:

Chevron Pascagoula

Location:

Pascagoula, MS F-2745

Source: Technicians:

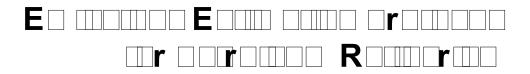
JPB, MAB, DM

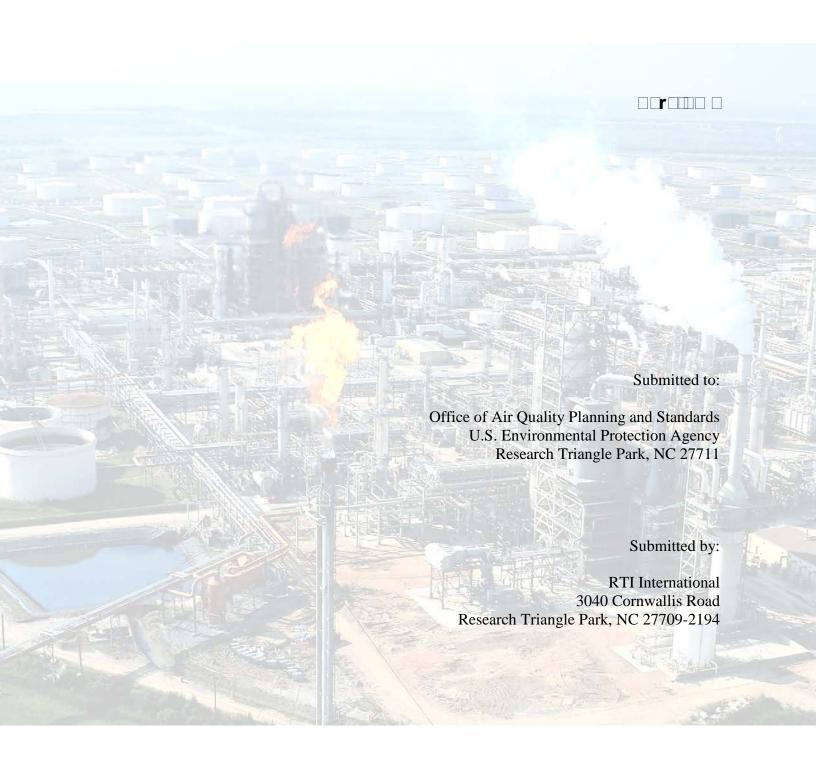
	or D, MAD, D	AFE.		
Test Run Designation	Run 1	Run 2	Run 3]
Date	11/27/2007	11/27/2007	11/27/2007	=
Start Time (24 hr)	15:52	17:40	19:15	
Stop Time (24 hr)	16:52	18:40	20:15	
Stack Gas Sampling Data				-
Box No.	2	4	2	1
Sample Time Length (min)	60	60	60	
Atmospheric Pressure (" Hg)	30.38	30.36	30.38	
Avg. Stack Temperature (°F)	846	829	843	
Avg. Meter Temperature (°F)	75.7	73.0	72.2	
Average √∆P	0.081	0.085	0.087	
Average ΔH	1.89	3.13	3.25	
Sample Volume at STP (DSCF)	44.097	58.668	59.523	
Moisture (% volume)	2.01	2.81	6.85	
Dry Gas Fraction (unitless)	0.980	0.972	0.931	
Molecular Weight (lb/lb-mole)	28.615	28.524	28.077	
Static Pressure (in. H2O)	-1.13	-1.13	-1.13	
Stack Velocity (ft/min @ stack conditions)	430	446	465	
Stack Flow, dry (DSCFH)	1.17E+06	1.22E+06	1.21E+06	
% Isokinetic	78.3	100.0	102.5	
Emissions Results				Averages
O2 (%)	5.38	5.31	5.22	5.30
CO2 (%)	3.86	3.85	3.81	3.84
NOx (ppmv)	23.70	21.15	23.16	22.67
CO (ppmv	40.11	36.72	37.62	38.15
SO2 (ppmv)	39.16	38.58	36.31	38.02
SO2 (ppmv) (@ 0% O2)	52.73	51.72	48.40	50.95
Calculated Mass Emissions				
NOx (lbs/hr)	3.31	3.08	3.34	3.24
CO (lbs/hr)	3.41	3.25	3.30	3.32
SO2 (lbs/hr)	7.62	7.81	7.28	7.57
NOx (tons/yr)	14.51	13.48	14.62	14.21
CO (tons/yr)	14.95	14.25	14.46	14.56
SO2 (tons/yr)	33.36	34.22	31.89	33.15
Calculated Particulate Emissions				
Filterable Particulate Matter Collected (g)	0.0211	0.0085	0.0273	0.0190
Filterable Analysis (lb/dscf)	1.05E-06	3.21E-07	1.01E-06	7.95E-07
Filterable Analysis (lb/hr)	1.23	0.39	1.22	0.95
Filterable Analysis (tons/yr)	5.40	1.71	5.34	4.15

FCC Regen

April 2015

Saved Date: 1/24/2022





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For most organic HAP (e.g., formaldehyde, benzene, benzo[a]pyrene, dioxin/furans) and other pollutants such as hydrogen cyanide and Hg, default emissions factors may be all that are available. When direct emissions monitoring or site-specific emissions factors are not available, then the default emissions factors presented in **Table 5-4** should be used to calculate the emissions from the CCU regenerator vent. Note that all CCU are considered "controlled for organics" if they meet the 500 ppmv CO emissions limit.

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The emission factors presented in Table 5-4 are based primarily on the emission data collected to support the Refinery MACT 2 rule; however, emissions factors for hydrogen cyanide and mercury were updated based on source tests conducted in response to EPA's 2011 ICR for the petroleum refining industry. While there appear to be slight differences in how outlier and non-detect values were handled, the emission factors in Table 5-4 agree well with the average emission factors developed by Bertrand and Siegell (2002).

Based on the lack of data for PAH and furan emissions, the emissions estimates for these compounds have high uncertainties, likely an order-of-magnitude either high or low. The California Air Resources Board (CARB), with EPA's support, conducted an emissions source test at a complete combustion FCCU (without a post-combustion device). The only dioxin isomer detected in all runs was octachloro-dibenzo-p-dioxin (OCDD); octachloro-dibenzo-furan (OCDF) and heptachloro-dibenzo-p-dioxin (hepta-CDD) were detected in one run. All dioxin/furan quantities that were detected were detected at levels below the method quantitation limit for the analysis. All polychlorinated biphenyls (PCBs) isomers were below detection limits. This additional source test was not included in the development of the Petroleum Refinery MACT II emissions factors, but it confirms low emissions of dioxins/furans and PCBs from the CCU catalyst regenerator vent.

5.2 Fluid Coking Units

Coking units use heat to thermally crack heavy hydrocarbon streams to form lighter, more useful distillates such as heating oils or gasoline. There are three basic types of coking units: traditional fluid coking units, flexicoking units, and delayed coking units. Traditional fluid coking units are one of the largest vent emissions sources at a refinery, being comparable to emissions from the CCU regenerator. However, there are only a handful of traditional fluid coking units currently in operation in the United States. Flexicoking units, which are also rare, do not have a direct atmospheric vent. Instead, these units produce a low heating value syngas that can be subsequently used as fuel in process heaters or boilers. Emissions from the combustion of flexicoking syngas should be determined using the methods described

Technical Memorandum

TO: Brenda Shine, Environmental Engineer

Refining and Chemicals Group, SPPD (E143-01)

FROM: Eric Goehl, Environmental Protection Specialist

Refining and Chemicals Group, SPPD (E143-01)

DATE: October 16, 2012

SUBJECT: Summary of Fluid Catalytic Cracking Unit Emission Source Test Reports

I. Purpose

The objective of this document is to provide a summary of the Fluid Catalytic Cracking Unit (FCCU) emission source test reports received by the EPA from the 2011 Information Collection Request (ICR) of the Petroleum Refinery industry.

II. Background

On April 1, 2011, the EPA sent an ICR to facilities in the U.S. petroleum refining industry. The ICR was comprehensive and designed to collect information on processing characteristics, crude slate characteristics, emissions inventories and source testing to bolster our current data and fill known data gaps. The ICR had four components: (1) a questionnaire on processes and controls to be completed by all petroleum refineries (Component 1); (2) an emissions inventory to be developed by all petroleum refineries using the emissions estimation protocol developed for this effort (Component 2); (3) distillation feed sampling and analysis to be conducted by all petroleum refineries (Component 3); and (4) emissions source testing to be completed in accordance with an EPA-approved protocol for specific sources at specific petroleum refineries (Component 4).

Component 4 of the ICR required source testing for twelve different types of emission sources or units: fluid catalytic cracking units (FCCU), thermal catalytic cracking units, catalytic reforming units, sulfur recovery units, delayed coking units, fluid coking units, hydrocracking units, hydrogen plants, asphalt blowing units, fuel gas systems, cooling water systems, and wastewater treatment systems. This memorandum summarizes the results of the FCCU sources tests. A similar memorandum is available for the other sources required to be tested as a result of

this ICR. Facilities often claimed specific process information as CBI, and included that information in the CBI version of the emission source test report stored in the EPA's CBI office in Research Triangle Park, NC. However, emissions data cannot be claimed as CBI. This memorandum summarizes and presents only non-CBI data.

III. Source-specific Testing Program

Below is a list of the ten facilities required to perform an emission source test on their FCCU.

- Marathon Oil Robinson, IL (IL2A0420)
- Flint Hills Rosemount, MN (MN2B0720)
- Motiva Norco, LA (LA3C0630)
- Citgo Lake Charles, LA (LA3C0560)
- Hovensa St. Croix, USVI (VI6A1530)
- Valero Port Arthur, TX (TX3B1250)
- Chevron Barbers Point, HI (HI5A0380)
- BP Whiting, IN (IN2A0440)
- ExxonMobil Torrance, CA (CA5A0190)
- Sunoco Philadelphia, PA (PA1A1030)

Owners or operators of the FCCU at these facilities were required to test for:

- Speciated volatile organic hazardous air pollutants (HAP)
- Speciated semi-volatile organic HAP
- Total hydrocarbons, methane, and ethane
- Aldehydes
- Carbon monoxide
- Dioxins, furans, and polychlorinated biphenyls
- Hydrogen chloride, chlorine, hydrogen fluoride, and hydrogen cyanide
- Mercury (speciated)
- Hexavalent chromium and multiple metals
- Particulate matter (PM, PM_{2.5} filterable, and PM condensable) and ammonia
- NO_X, SO₂, O₂, CO₂, moisture, and gas flow rate.

The EPA required that the data collected from the emission source testing to be reported using the EPA Electronic Reporting Tool (ERT). The ERT is a Microsoft® Access database application. If the facility conducted testing using a method not currently supported by the ERT, the facility was required to report the results in the Refinery Testing Supplement, a Microsoft® Excel spreadsheet. After completing the Refinery Testing Supplement, the refineries were also to submit an electronic copy of the emission test report, preferably in PDF format.

IV. Results

A summary of the emission results for the FCCU are provided in attached spreadsheet. In order to better characterize the reported data from the emission test reports, detection level information was provided in the attached summary spreadsheet. The following designations were used to describe the detection levels of the reported emissions data.

- DLL = Detection Level Limited = 1 or 2 runs below detection limit
- BDL = Below Detection Limit = All three runs are below detection limit
- No designation = All three runs are above detection limit

While reviewing the reported FCCU test data for Motiva in Norco, LA, we found conflicting data between the Refinery Testing Supplement and the PDF emission test report. A phone call to the facility clarified that the information contained in the PDF emission test report reflected the correct data.

			0 - ExxonMobil		.0440 - BP niting, IN	LA3C0630 - Motiva Norco LA		L2A0420 - Marathon obinson, IL	VI6A1530 - Hovensa Christiansted, USVI	TX3B1250 - Valero Port Arthur, TX		PA1A1030 - Sunoco Iladelphia, PA		C0560 - Citgo e Charles, LA		B0720 - Flint Rosemount, MN		0380 - Chevron (apolei, Hl
CAS#	Compound	Detection Level (DL)			lb/hr	DL lb/hr		Ib/hr	DL lb/hr	DL lb/hr		lb/hr		lb/hr	DI	lb/hr	DL	•
	•	Level (DL)		DL			DL											
75-07-0 50-00-0	Acetaldehyde Formaldehyde		8.00E-02 1.34E+00		8.40E-01 2.10E-01	BDL 1.90E-01 DLL 4.70E-02		3.62E-03 2.05E-03	2.52E-02 DLL 1.55E-01	4.04E-01 BDL 5.99E-02		3.31E-03 1.08E-02		6.27E-04 5.91E-03	BDL	6.80E-04		1.70E-01 2.00E-02
74-90-8	Hydrogen cyanide		1.20E+01		4.60E-01	BDL 7.00E-01		2.03E-03 2.07E+00	1.05E+02	4.20E+01		0.00E+00		3.22E+01		3.33E+00	DUL	5.36E+00
	Propanal				3.70E-01	BDL 2.50E-01		2.83E-03	1.10E-03	DLL 4.39E-02		0.00E+00				6.73E-04	BDL	1.80E-01
7647-01-0 7782-50-5	Hydrogen Chloride Chlorine	BDL	1.01E+00 2.00E-02		3.55E-01 5.20E-02	2.36E-01	BDI	3.12E-02 1.70E-03	9.90E-01 BDL 1.00E-02	BDL 7.20E-02 BDL 3.57E-02		7.78E-01 0.00E+00		1.96E-01 1.30E+00			BDI	5.75E-02 2.90E-03
7782-30-3	Hydrogen Fluoride	BDL	2.00E-02		1.40E-02	3.63E-02	BDL	2.02E-03	BDL 3.00E-02	BDL 9.85E-03		0.00E+00		2.60E-02			DUL .	1.49E-02
	VOLATILE ORGANIC HAP																	
67-64-1	Acetone		1.68E+00		3.79E+00	BDL 8.20E-04		2.86E+00	BDL 1.57E+00	8.85E+01				4.89E-01		7.00E-01	BDL	4.10E-01
750-05-8	Acetonitrile	DDI	3.70E-01		1.20E-01			2.85E-01	BDL 1.93E+00	DLL 3.62E-01	DD1	0.005.00				2.80E-01		data rejected
107-02-8 107-13-1	Acrolein Acrylonitrile	BDL BDL	2.30E-01 2.30E-01	BDL BDL	1.20E-01 1.19E-01	BDL 6.77E-04 BDL 7.34E-04		2.85E-01 2.85E-01	BDL 1.38E+00	DLL 1.60E-01 DLL 1.92E-01	BDL	0.00E+00		2.59E-01 2.55E-01		4.13E-01 2.30E-01		5.40E-01 1.10E-02
71-43-2	Benzene	BDL	2.30E-01	BDL	1.22E-01	BDL 6.60E-04	BDL	2.85E-01	BDL 4.39E-01	BDL 1.49E-01		2.40E-01		2.32E-01		4.93E-01		5.10E-01
106-99-0	1,3-Butadiene	BDL	2.40E-01	BDL	1.22E-01			2.85E-01	BDL 8.57E-01	BDL 7.50E-01		0.00E+00		2.66E-01		4.00E-01		6.20E-01
75-15-0 108-90-7	Carbon Disulfide Chlorobenzene	BDL BDL	2.30E-01 2.30E-01	BDL BDL	1.19E-01 1.22E-01	BDL 4.60E-04 BDL 5.80E-03		2.85E-01 2.85E-01	BDL 8.63E-01	BDL 1.49E-01 BDL 1.49E-01		1.29E+00 0.00E+00		1.28E-01 7.00E-03		1.73E-01 6.53E-02		1.40E-01 1.10E-02
98-82-8	Cumene (Isopropylbenzene)	BDL	2.30E-01	BDL	1.22E-01	BDL 4.36E-03	BDL	2.85E-01	BDL 1.84E+00	BDL 1.49E-01		0.00E+00	BDL	5.00E-03	BDL	4.73E-02	BDL	1.10E-02
106-93-4	1,2-Dibromoethane	BDL	2.30E-01	DLL	1.42E-01	BDL 1.41E-03	BDL	2.85E-01	BDL 4.00E+00	BDL 1.49E-01	DC:	0.005.00	BDL	3.17E-01	BDL	1.27E+00	BDL	1.30E+00
100-41-4 110-54-3	Ethylbenzene Hexane	BDL BDL	2.30E-01 2.30E-01	BDL BDL	1.22E-01 1.19E-01	BDL 4.45E-03 BDL 6.60E-04		2.85E-01 2.85E-01	BDL 5.43E-01 BDL 2.20E+00	BDL 1.49E-01 BDL 1.49E-01		0.00E+00 0.00E+00		6.00E-03 2.15E-01		4.83E-02 5.80E-01		1.10E-02 4.40E-01
108-10-1	Methyl iso-Butyl Ketone	BDL	2.30E-01	BDL	1.23E-01		BDL	2.85E-01	BDL 1.43E+00	BDL 1.44E-01		0.00E+00	BDL	5.00E-03	BDL	5.00E-02	BDL	8.90E-03
1634-04-4	Methyl t-Butyl Ether (MTBE)	BDL	2.30E-01	BDL	1.19E-01	DD1 0 00= 00		2.85E-01	BDL 1.36E+00	BDL 1.49E-01			BDL	5.00E-03	BDL	4.73E-02	BDL	7.80E-03
75-09-2 98-95-3	Methylene Chloride Nitrobenzene	BDL BDL	2.30E-01 1.17E+00	BDL BDL	1.20E-01 6.30E-01	BDL 2.68E-03 BDL 6.96E-03	BDI	3.64E-01 1.42E+00	BDL 2.61E+00	1.43E+00 BDL 7.46E-01	RDL	0.00E+00		8.97E-01 7.00E-03		2.51E+00 7.20E-02		1.30E+00 1.30E-02
79-46-9		BDL	2.30E-01	BDL	1.22E-01			2.85E-01	BDL 3.19E+00	BDL 1.49E-01				8.00E-03		4.40E-01		1.10E-02
109-66-0	Pentane	BDL	2.30E-01	BDL	1.22E-01	BDL 6.63E-04	BDL	2.85E-01	BDL 1.84E+00	BDL 7.76E-01			BDL	2.14E-01	BDL	4.90E-01	BDL	7.90E-01
100-42-5 127-18-4	Styrene	BDL BDL	2.30E-01 2.30E-01	BDL BDL	1.22E-01	BDL 4.83E-03 BDL 1.42E-03			BDL 1.81E+00 BDL 2.37E+00	BDL 1.49E-01 BDL 1.49E-01	BDI	0.00E+00		6.00E-03 2.81E-01		5.23E-02		8.60E-02
108-88-3	Tetrachloroethene Toluene	BDL	2.30E-01 2.30E-01	BDL	1.22E-01 1.23E-01			2.85E-01 2.85E-01	BDL 2.37E+00 BDL 2.40E+00	BDL 1.49E-01	DUL	6.13E+00		2.26E-01		1.28E+00 5.63E-01		2.30E+00 8.60E-01
79-01-6	Trichloroethene	BDL	2.30E-01	BDL	1.23E-01	BDL 1.34E-03	BDL	2.85E-01	BDL 6.71E-01	BDL 1.50E-01			BDL	3.48E-01	BDL	1.21E+00	BDL	7.60E-01
540-84-1 1330-20-7	2,2,4-Trimethylpentane Xylene	BDL	2.30E-01	BDL BDL	1.22E-01 1.22E-01		BDL	2.85E-01	BDL 2.04E+00 BDL 5.43E-01	BDL 1.49E-01 BDL 1.49E-01	BDL	0.00E+00		4.00E-03 1.10E-02		4.10E-02 9.60E-02	BDL	7.00E-03
	o-Xylene m&p-Xylenes	BDL BDL	2.30E-01 2.30E-01			BDL 4.52E-03 BDL 4.40E-03		2.85E-01 2.85E-01			BDL	0.00E+00 0.00E+00						1.00E-02 1.00E-02
	Total VOC as propane	DDL	2.002 01			BBE 4.40E 00	DDL	2.00L 01	BDL 5.24E+01		DDL	0.002.00					DDL	1.002 02
	SVOC											1.93E-08						
83-32-9	Acenaphthene	BDL	1.92E-06		1.35E-05	BDL 1.48E-05	BDL	7.48E-06	BDL 1.18E-04	DLL 1.11E-04		1.502 00	BDL	1.06E-04	BDL	1.60E-05	BDL	2.10E-06
209-96-8	Acenaphthylene	DLL	8.95E-06		8.03E-06	BDL 1.49E-05		9.31E-06	BDL 1.12E-04	BDL 1.42E-04				3.37E-05		1.60E-05		2.10E-06
62-53-3 120-12-7	Aniline Anthracene	BDL	3.60E-04 1.72E-06	BDL	3.07E-04 1.67E-06	BDL 1.03E-03 BDL 1.49E-05	BDL	2.13E-04 3.73E-06	4.78E-01 7.57E-04	BDL 2.89E-07 DLL 2.28E-05				5.09E-04 3.37E-05		5.70E-03 1.60E-05		5.20E-04 2.10E-06
92-87-5	Benzidine	BDL	7.40E-03	BDL	6.31E-03	BDL 3.39E-02	BDL	4.49E-03	BDL 1.28E+00	BDL 5.94E-06				5.21E-05	BDL	1.90E-01		data rejected
56-55-3	Benzo(a)Anthracene	BDL	7.79E-07	BDL	9.60E-07			6.82E-07	9.40E-04	BDL 8.78E-07						1.60E-05		2.10E-06
205-99-2 207-08-9	Benzo(b)Fluoranthene Benzo(k)Fluoranthene	BDL BDL	7.79E-07 7.79E-07	BDL BDL	1.38E-06 1.00E-06	BDL 1.48E-05 BDL 1.48E-05		4.26E-06 6.98E-07	BDL 1.12E-04 BDL 1.12E-04	BDL 6.75E-07 BDL 6.26E-07	-			2.76E-05 4.14E-05		1.60E-05 1.60E-05		2.10E-06 2.10E-06
191-24-2	Benzo(ghi)Perylene	DUL	1.52E-06	BDL	6.60E-07	BDL 1.48E-05	BDL	4.73E-07	BDL 1.12E-04	DLL 3.04E-06	t			1.00E-04	BDL	1.60E-05	BDL .	2.10E-06
50-32-8	Benzo(a)Pyrene	BDL	7.79E-07	BDL	6.60E-07	BDL 1.48E-05	BDL	4.73E-07	BDL 1.12E-04	BDL 8.05E-06			BDL	9.35E-05	DLL	1.60E-05	BDL :	2.10E-06
192-97-2 92-52-4	Benzo(e)Pyrene Biphenyl	BDL	7.79E-07 2.18E-04	BDL	2.16E-06 1.16E-03	BDL 1.48E-05 BDL 1.48E-05	BDL	1.62E-06 3.00E-04	BDL 1.12E-04 BDL 5.62E-02	DLL 1.31E-05 BDL 9.08E-05	1			3.07E-05 3.07E-05		1.60E-05 8.20E-03		2.10E-06 2.10E-04
1319-77-3	Cresols		2. 10L-0 1	BDL	1.10E-03	DDL 1.70L-00		0.00L-04	6.49E+00	DDL 0.00L-00	1			1.80E-02		1.00E-02	JUL	L. 10L-0 1
218-01-9	Chrysene*		1.70E-06		2.93E-06	BDL 1.48E-05		1.21E-05	8.80E-04	BDL 1.31E-06			BDL	1.07E-04	DLL	1.60E-05		2.10E-06
53-70-3 132-64-9	Dibenzo(a,h)Anthracene* Dibenzofuran	BDL BDL	7.79E-07 4.48E-04	BDL BDL	7.70E-07 3.82E-04	BDL 1.48E-05 BDL 1.02E-03	BDL	4.73E-07 3.69E-04	BDL 1.12E-04 BDL 3.87E-02	BDL 7.29E-07 BDL 3.60E-07	1			9.12E-05 7.74E-05		1.60E-05 5.60E-03		2.10E-06 1.40E-04
192-65-4	Dibenzo(a,e)pyrene	DDL	¬.→∪∟=∪ +	BDL	6.60E-07	BDL 1.48E-05	BDL	4.73E-07	BDL 3.87E-02 BDL 2.25E-04	BDL 3.60E-07 BDL 6.26E-07	1		DUL	7.74L-00		8.20E-05		2.10E-06
119-90-4	3,3'-Dimethoxybenzidine	BDL	5.65E-03	BDL	4.82E-03	BDL 1.48E-03	BDL	3.43E-03	BDL 1.12E+00	BDL 4.54E-06				3.07E-05	BDL	8.20E-03		data rejected
60-11-7 57-97-6	Dimethylaminobenzene 7,12-Dimethybenz(a)anthracene	BDL	3.90E-04	BDL BDL				2.37E-04 4.73E-07	BDL 3.55E-02 BDL 2.25E-04	BDL 3.13E-07 BDL 6.26E-07	1			3.07E-05 3.07E-05		8.20E-03 3.30E-05		2.10E-04 2.10E-06
119-93-7	3,3'-Dimethylbenzidine	BDL	5.65E-03	BDL	4.82E-03			3.43E-03	BDL 2.25E-04 BDL 6.06E-01	BDL 4.54E-06	1			3.07E-05		8.80E-02		data rejected
122-09-8	a,a-Dimethylphenethylamine	BDL	2.34E-03	BDL	1.99E-03	BDL 1.48E-03	BDL	1.42E-03	BDL 2.81E-01	BDL 1.88E-06			BDL	3.07E-05	BDL	8.20E-03		data rejected
105-67-9 206-44-0	2,4-Dimethylphenol Fluoranthene		5.07E-04 6.72E-06	BDL	4.32E-04 1.00E-05	BDL 1.08E-03 3.82E-05	RDL	3.08E-04 4.89E-05	4.29E-01 1.58E-03	BDL 4.07E-07 9.79E-06	1			8.45E-04 3.07E-05	RDL	5.90E-03 3.60E-05		1.50E-04 2.10E-06
86-73-7	Fluorene		4.87E-06		1.75E-05		BDL	3.51E-05	BDL 1.12E-04	DLL 4.98E-05	1			3.99E-05	DLL	1.60E-05		3.41E-06
193-39-5	Indeno(1,2,3-cd)Pyrene	BDL	7.79E-07	BDL	9.40E-07	BDL 1.48E-05	BDL	4.73E-07	BDL 1.12E-04	BDL 5.58E-06			BDL	9.66E-05	DLL	1.60E-05	BDL .	2.10E-06
78-59-1 56-49-5	Isophorone	BDL	4.38E-04	BDL BDL				2.60E-04	BDL 4.20E-02	BDL 3.52E-07 BDL 6.26E-07	1					6.10E-03		1.60E-04
91-57-6	3-Methylcholanthrene 2-Methylnaphthalene		6.16E-05	DUL	6.64E-07 5.89E-04	BDL 1.48E-05 3.23E-05	DUL	4.73E-07 2.44E-05	BDL 2.25E-04 BDL 1.20E-04	7.41E-05	 			3.07E-05 5.06E-05		8.20E-05 3.40E-05	DUL	2.10E-06 6.98E-06
95-48-7	2-Methylphenol	BDL	4.09E-04				BDL	2.48E-04		DLL 4.26E-06								1.40E-04
	4-Methylphenol & 3-Methylphenol	BDL	1.10E-03		2 225 04	2 245 04	BDL	6.62E-04	2 525 04	BDL 1.27E-06			BDI	1 225 04		E 00E 04		1.20E-04
91-20-3 198-55-0	Naphthalene Perylene	BDL	1.62E-04 7.79E-07	BDL	3.22E-04 6.64E-07	3.24E-04 BDL 1.48E-05	BDI	7.93E-03 4.73E-07	2.52E-04 BDL 1.12E-04	2.80E-04 BDL 6.21E-07	1			1.33E-04 3.07E-05	DLI	5.90E-04 1.60E-05		9.98E-05 2.10E-06
85-01-8	Phenanthrene		4.23E-05		5.11E-05	BDL 3.62E-05		3.05E-04	2.33E-03	6.31E-05			BDL	1.21E-04		2.70E-05		2.53E-06
108-95-2	Phenol	BDL	1.26E-03	DD1	1.46E-03	BDL 5.79E-03	BDL	2.04E-03	6.07E+00	1.21E-06	lacksquare		DLL	1.31E-02	DLL	5.30E-03		1.12E-03
106-50-3	1,4-Phenylenediamine	BDL	3.51E-03	BDL	∠.ઝઝ⊏-∪ડ	BDL 1.48E-03	DUL	∠. I3E-U3	BDL 2.81E-01	BDL 2.82E-06	1		DUL	2.98E-05	DUL	8.20E-03		data rejected

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			0 - ExxonMobil		A0440 - BP		A3C0630 -		L2A0420 - Marathon		1530 - Hovensa		3B1250 - Valero		PA1A1030 - Sunoco		C0560 - Citgo		2B0720 - Flint Rosemount,		0380 - Chevron
		Detection	rrance CA		hiting, IN		iva Norco LA		obinson, IL		istiansted, USVI		Port Arthur, TX		iladelphia, PA		e Charles, LA		MN		Kapolei, HI
CAS#	Compound	Level (DL)		DL	lb/hr		lb/hr		lb/hr	DL	lb/hr		lb/hr	DL	lb/hr		lb/hr		lb/hr		lb/hr
129-00-0	Pyrene	BDL	6.83E-06 9.74E-04	BDL	1.06E-05		8.65E-05		2.49E-05	DDI	4.87E-03		2.26E-06 7.82E-07				3.68E-05 3.07E-05	DDI	7.30E-05 8.20E-03		2.10E-06 2.10E-04
95-53-4	o-Toluidine Total PAHs	DUL	9.74E-04	DUL	8.31E-04	DUL	1.48E-03		5.91E-04 8.72E-03	DUL	1.10E-01	DUL	7.02E-U7	+		DUL	3.07E-05	DUL	6.20E-03	DUL	2.10E-04
	Total FALIS							DDL	0.72L-03												
	METALS																				
	Antimony	BDL	2.86E-04		3.12E-04	DLL	3.47E-03	BDL	2.21E-03		2.00E-03	BDL	3.59E-05				3.43E-04				8.44E-05
	Arsenic	BDL	2.45E-04	BDL	2.10E-04		3.31E-04		1.94E-04	200	2.00E-04		1.44E-04				5.44E-04				6.80E-04
7440-41-7 7440-43-9	Beryllium Cadmium	BDL BDL	2.45E-04 2.45E-04	BDL	5.26E-05 1.19E-03	RDF	8.28E-05 8.30E-05		4.46E-05 2.68E-05	RDL	1.00E-05 2.00E-04	RDL	3.59E-05 8.35E-04	-			3.91E-06 5.37E-05				5.00E-06 4.40E-06
7440-43-3	Chromium	DDL	1.09E-03		2.44E-03		7.30E-04		1.29E-03		1.40E-03		4.21E-04	-			1.11E-03				4.07E-04
	Lead	DLL	4.64E-04		3.11E-03	BDL	1.66E-04	552	1.15E-03		1.90E-03		2.16E-04			DLL	6.27E-04				1.50E-04
7439-96-5	Manganese		7.54E-04		9.46E-04		3.84E-03		2.40E-03		6.30E-03		6.71E-04				7.70E-04				9.88E-04
7440-02-0	Nickel	DLL	6.08E-04	2001	3.33E-03	D. .	1.14E-02	DD1	4.61E-03		5.30E-03	DD:	1.11E-03			D	2.18E-03			D	1.63E-02
7782-22-4 7440-48-4	Selenium Cobalt	DLL	9.66E-04	BDL	5.26E-04 3.39E-04		1.02E-03 8.11E-04		7.29E-04 2.06E-04	1	1.40E-03 1.00E-03	RDL	3.59E-04 5.82E-05	-			9.53E-04 1.69E-04			DLL	3.80E-04 1.08E-03
	Hexavalent Chromium	BDL	1.13E-04	BDL	8.00E-03		1.64E-03		8.14E-05	DLL		BDI	3.24E-04		1.74E-04		2.04E-04	DLI	4.03E-05		1.00E-03
10040 20 0	Oxidized/organic Mercury	BDL	2.72E-04	DDL	6.78E-05	BDL	1.20E-05		7.24E-05	DEL	2.92E-05	000	1.90E-05		1.742 04		1.54E-06	DLL	1.002 00	DLL	1.50E-05
	Total Mercury	BDL	8.51E-04	BDL	1.98E-04		3.87E-05		1.91E-04				1.81E-04								
7439-97-6	Elemental Mercury	BDL	5.71E-04	BDL	1.19E-04		2.42E-05		1.04E-04		2.55E-04	BDL	1.52E-04		7.09E-04	DLL	3.86E-05	DLL	2.73E-05	DLL	3.00E-05
7664 41 7	Ammonio		5.49E+00	1	4.50E-01	יים	2.705.01		7.23E-01	-	0.05E+00	-	E 22E 01	יחם	0.00E+00	1	6 20E 01		5.50E+00		1 205 01
7664-41-7 630-08-0	Ammonia Carbon Monoxide		5.49E+00 7.86E+01	-	4.3UE-U1	DLL	2.70E-01 3.23E+00	-	1.23E-U1	1	9.85E+00 3.73E+01	-	5.22E-01 3.22E+00	DUL	0.00E+00 2.36E+01	1	6.39E-01 2.11E+01		J.5UE+UU		1.20E-01 1.26E+01
7782-50-5	Chlorine		7.00L 101	1	5.20E-02		5.25L · 00	BDL	1.73E-03		0.73L 101		J. ZZL - UU	1	2.50∟.01		2.112.01				1.202 101
67-56-1	Methanol	BDL	5.87E-01		4.86E+01	L		Ľ	7.67E+00	L	1.80E-01	<u> </u>	5.49E-01	L		DLL	5.86E-01	DLL	1.33E+00		2.80E-02
74-82-8	Methane		3.45E+01	BDL	7.00E-02		1.10E-01		8.00E-01		4.10E-01		4.73E-01		2.49E+00		7.77E-01		3.50E-01		8.15E-02
74-84-0	Ethane		1.21E+01	BDL	8.00E-02	BDL	2.60E-01	BDL	1.00E-01		7.68E-01	BDL	8.05E-01	-	1.26E+01		1.25E+00	BDL	3.40E-01	BDL	4.70E-01
75-69-4 74-83-9	Trichlorofluoromethane Bromomethane			-						1											
	Nitrogen Oxides		2.52E+01	-			1.59E+02			1	2.16E+01		9.53E+00		1.26E+01		1.01E+01				1.67E+01
10102 40 0	Sulfur Dioxide		2.84E+01				4.15E+01				2.84E+00	DLL	9.38E-01		2.70E+01		Reported a ned	ative (0.01		6.80E+00
	PARTICULATE MATTER																				
	Condensible Inorganic (aqueous) PM Condensible Organic Particulate Matter		1.99E+01 9.10E-01				2.05E+01 1.26E+00			1					3.29E+01 1.32E+00						1.59E+00 9.16E-02
	Condensible Organic Particulate Matter Condensible Particulate Matter		9.10E-01		9.49E+00		1.20E+00		8.53E+00	1	2.28E+01		2.29E+00		1.32E+00		2.61E+00				9.10E-02
	Filterable Particulate		1.26E+00		3.43E · 00		2.17E+01		2.27E+01		1.54E+01		6.22E+00		8.20E+01		Z.01L100				4.45E+00
	Filterable PM2.5				1.32E+01																2.42E+00
	Total PM2.5		2.10E+01		2.27E+01		4.055.04		0.405 - 0.4		0.005 - 04		0.545.00		1.105.00		4.005 - 00				4.10E+00
	Total PM						4.35E+01		3.12E+01	1	3.82E+01		8.51E+00	-	1.16E+02	-	4.23E+00				
	TOTAL PCBs																				
	Total PCBs				3.10E-07			BDL	2.17E-08			BDL	6.51E-09								
	PCB TEQs								1.65E-10												
	DIOVINI AND ELIDANIC																				
	DIOXIN AND FURANS	BDI	1.01E-09		2.73E-09					DDI	3.92E-10	DDI	6.92E-11			DDI	3.38E-10			DDI	3.00E-10
	2,3,3',4,4',5,5'-HpCB (PCB189) 2,3,3',4,4',5'-HxCB (PCB157)	BDL DLL	5.42E-10		2.73E-09 2.09E-09						2.37E-10		1.42E-10	+			3.54E-10				5.70E-10
	2,3,3,4,4,5-HxCB (PCB156)		1.82E-09	1	7.50E-09	l				011	6.27E-10	BDL	1.48E-10			202	1.08E-08				5.70E-10
	2,3,3',4,4'-PeCB (PCB105)		1.25E-08		6.14E-08						5.14E-09	DLL	6.77E-10				8.98E-08			BDL	3.57E-09
	2,3',4,4',5,5'-HxCB (PCB167)	DLL	8.42E-10		5.88E-09	<u> </u>					3.26E-10	BDL	1.67E-10				2.69E-08				3.30E-10
-	2,3,4,4',5-PeCB (PCB114) 2,3',4,4',5-PeCB (PCB118)	BDL	8.62E-10 3.22E-08	-	5.40E-09 1.71E-07	1		-		RDL	4.42E-10 1.19E-08		9.44E-11 1.78E-09	1		DLL	8.30E-09 3.01E-07				2.80E-10 1.02E-08
	2',3,4,4',5-PeCB (PCB118) 2',3,4,4',5-PeCB (PCB123)	DLL	1.40E-09	-	1.71E-07 1.68E-08	1				DH	6.17E-10	BDI	1.51E-10	+		1	2.85E-07			BDI	4.70E-10
	2,3,4,6,7,8-HxCDF			DLL	2.19E-09	l					1	DLL	1.74E-10	1			6.97E-10				1.80E-10
	2,3,7,8-TCDD	BDL	6.79E-10	DLL	6.30E-10		3.19E-10					BDL	1.83E-10			BDL	3.82E-10			BDL	6.80E-10
	2,3,7,8-TCDF	DDI	1.145.00	-	3.42E-09	BDL	4.77E-10	ļ		DC:	2.105.12		2.19E-10	1			5.44E-10				4.30E-10
-	3,3',4,4',5,5'-HxCB (PCB169) 3,3',4,4',5-PeCB (PCB126)	BDL BDL	1.14E-09 6.00E-10	-	9.42E-10 3.39E-09	1		-			3.19E-10 4.30E-10		2.80E-09 1.67E-10	1			3.91E-10 3.43E-10				3.40E-10 3.00E-10
-	3,3',4,4',5-PeCB (PCB126)	DUL	6.71E-09	1	2.90E-08	1			1		4.30E-10 5.90E-09		. 2.60E-10				7.39E-09				9.10E-10
	3,4,4',5-TCB (PCB81)	DLL	4.28E-10	1	3.69E-09	t					5.88E-10		1.06E-10	1			5.75E-09				3.10E-10
	OCDD				4.96E-09		1.16E-09										1.45E-08			DLL	1.88E-09
	OCDF	BDL	1.77E-09	DLL	7.00E-09	BDL	5.58E-10			1	-		2.66E-10	1			2.22E-09				4.06E-09
-		BDL BDL	3.45E-10 8.65E-10	-	2.77E-09	BDI	3.96E-10			-	-		1.44E-10 4.33E-10	-			6.42E-10 7.12E-10				2.00E-10 4.30E-10
		BDL	5.09E-10	DLL			4.77E-10			\vdash	+		. 3.76E-10	+			5.93E-10				2.20E-10
	1,2,3,4,6,7,8-HpCDF	DLL	5.59E-10	DLL			3.24E-10						2.64E-10								1.39E-09
	1,2,3,4,7,8,9-HpCDF	BDL	8.58E-10	DLL	7.57E-09	BDL	3.33E-10					DLL	1.45E-10				1.14E-09			DLL	4.50E-10
	1,2,3,4,7,8-HxCDD	BDL	6.11E-10	DLL	4.75E-10		3.15E-10					BDL	1.71E-10				9.40E-10				3.30E-10
	1,2,3,4,7,8-HxCDF	BDI	6 21E 10	DU			2.88E-10			-	-		1.32E-10	-	-		6.93E-10				2.80E-10
	1,2,3,6,7,8-HxCDD 1,2,3,7,8,9-HxCDD	BDL BDL	6.21E-10 6.72E-10	DLL			3.15E-10 2.88E-10	-		1	+		1.69E-10 1.67E-10	-	-		8.88E-10 9.16E-10				4.00E-10 3.30E-10
	1,2,3,7,8,9-HxCDF	BDL	4.50E-10	DLL	5.37E-09		3.60E-10						1.26E-10	1			8.26E-10				2.10E-10
	1,2,3,7,8-PeCDD	BDL	7.53E-10	DLL	9.59E-10	BDL	2.88E-10			L		BDL	3.49E-10	$oldsymbol{ol}}}}}}}}}}}}}}$		BDL	6.27E-10			BDL	3.10E-10
	1,2,3,7,8-PeCDF			DLL	6.28E-09	BDL	2.97E-10					BDL	3.01E-10			BDL	5.80E-10			BDL	2.80E-10
L	Total HpCDD				4.62E-09	BDL	3.96E-10		stion 7 Dags	<u> </u>	L		5.17E-10		<u> </u>	<u> </u>	1		ato: 1/24/20		4.30E-10

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		Toi	00 - ExxonMobil rrance CA		0440 - BP niting, IN		_A3C0630 - tiva Norco LA		IL2A0420 - Marathon Robinson, IL		A1530 - Hovensa istiansted, USVI		3B1250 - Valero ort Arthur, TX		PA1A1030 - Sunoco illadelphia, PA		3C0560 - Citgo ke Charles, LA		I2B0720 - Flint s Rosemount, MN		\0380 - Chevron Kapolei, Hl
CAS#	Compound	Detection Level (DL)	lb/hr	DL	lb/hr	DL	lb/hr	DL	lb/hr	DL	lb/hr	DL	lb/hr	DL	lb/hr	DL	lb/hr	DL	lb/hr	DL	lb/hr
- C. 10	Other HpCDF				1.27	+			1.571.1	 	127111		127111	+			127711				4.44E-10
	Total HpCDF			DLL	1.41E-08	BDL	3.51E-10					DLL	3.31E-10								2.23E-09
	Other HxCDD																			DLL	1.77E-09
	Total HxCDD				5.68E-09	BDL	3.15E-10					BDL	1.71E-10							DLL	2.84E-09
	Other HxCDF																			DLL	3.15E-10
	Total HxCDF				2.50E-08	BDL	3.06E-10					DLL	3.65E-10							DLL	7.90E-10
	Other PeCDD																				1.45E-10
	Total PeCDD				7.05E-09	BDL	5.67E-10					BDL	3.49E-10							DLL	4.41E-10
	Other PeCDF																				3.38E-10
	Total PeCDF			DLL	3.69E-08	BDL	5.76E-10					DLL	4.95E-10							DLL	7.90E-10
	Other TCDD					L														DLL	8.90E-12
	Total TCDD				8.89E-09	BDL	2.97E-10					DLL	4.50E-10							DLL	6.90E-10
	Other TCDF					L												ļ			
	Total TCDF				9.19E-08	BDL	8.46E-10					BDL	2.19E-10					ļ		BDL	4.30E-10
	Total Dioxins and Furans			DLL	2.52E-07	<u> </u>				-	1.41E-08	1	5.80E-09	_				<u> </u>			
	Total PCDD/F					RDL	5.77E-09		2.18E-08	-		1		_				<u> </u>			
	Total PCDD/F TEQ					1			3.69E-09	-		1		_				<u> </u>		L	
	Total Dioxins					1				-	7.20E-09	1		_				<u> </u>		DLL	6.29E-09
	Total Furans					1				-	6.89E-09	1		_				<u> </u>		DLL	8.29E-09
I	Total Hydrocarbon		1.01E+02												7.61E-01		3.19E+00			1	1

Flares

1/24/2022 & Revision #2

Table 13.5-1 (English Units). THC, NOx AND SOOT EMISSIONS FACTORS FOR FLARE OPERATIONS FOR CERTAIN CHEMICAL MANUFACTURING PROCESSES^a

Pollutant	SCC ^e	Emissions Factor Value	Emissions Factor Units	Grade or Representativeness
THC, elevated flares ^c	30190099;	0.14 ^{b,f}	1b/10 ⁶ Btu	В
THC, enclosed ground flares ^{g,h} Low Percent Load ⁱ	30119701; 30119705; 30119709; 30119741	8.37 ^j or 3.88e-3 ^f	lb/10 ⁶ scf gas burned lb/10 ⁶ Btu heat input	Moderately
THC, enclosed ground flares ^{g,h} Normal to High Percent Load ⁱ	30119741	2.56 ^j or 1.20e-3 ^f	lb/10 ⁶ scf gas burned lb/10 ⁶ Btu heat input	Moderately
Nitrogen oxides, elevated flares ^d		$0.068^{b,k}$	lb/10 ⁶ Btu	В
Soot, elevated flares ^d		$0 - 274^{b}$	μg/L	В

- ^a All of the emissions factors in this table represent the emissions exiting the flare. Since the flare is not the originating source of the THC emissions, but rather the device controlling these pollutants routed from a process at the facility, the emissions factors are representative of controlled emissions rates for THC. These values are not representative of the uncontrolled THC routed to the flare from the associated process, and as such, they may not be appropriate for estimating the uncontrolled THC emissions or potential to emit from the associated process.
- ^b Reference 1. Based on tests using crude propylene containing 80% propylene and 20% propane.
- ^c Measured as methane equivalent. The THC emissions factor may not be appropriate for reporting volatile organic compounds (VOC) emissions when a VOC emissions factor exists.
- d Soot in concentration values: nonsmoking flares, 0 micrograms per liter (μg/L); lightly smoking flares, 40 μg/L; average smoking flares, 177 μg/L; and heavily smoking flares, 274 μg/L.
- ^e See Table 13.5-4 for a description of these SCCs.
- ^f Factor developed using the lower (net) heating value of the vent gas.
- g THC measured as propane by US EPA Method 25A.
- h These factors apply to well operated ground flares achieving at least 98% destruction efficiency and operating in compliance with the current General Provisions requirements of 40 CFR Part 60, i.e. >200 btu/scf net heating value in the vent gas and less than the specified maximum exit velocity. The emissions factor data set had an average destruction efficiency of 99.99%. Based on tests using pure propylene fuel. References 12 through 33 and 39 through 45.
- The dataset for these tests were broken into four different test conditions: ramping back and forth between 0 and 30% of load; ramping back and forth between 30% and 70% of load; ramping back and forth between 70% and 100% of load; and a fixed rate maximum load condition. Analyses determined that only the first condition was statistically different. Low percent load is represented by a unit operating at approximately less than 30% of maximum load.
- Heat input is an appropriate basis for combustion emissions factor. However, based on available data, heat input data is not always known, but gas flowrate is generally available. Therefore, the emissions factor is presented in two different forms.
- ^k Factor developed using the higher (gross) heating value of the vent gas.

Table 13.5-2 (English Units). VOC and CO EMISSIONS FACTORS FOR ELEVATED FLARE OPERATIONS FOR CERTAIN REFINERY AND CHEMICAL MANUFACTURING PROCESSES^{a,b}

Pollutant	SCC ^e	Emissions Factor (lb/10 ⁶ Btu) ^f	Representativeness
Volatile organic compounds ^c	30190099; 30600904; 30119701; 30119705; 30119709; 30119741; 30119799; 30130115;	0.66	Poorly
Carbon monoxide ^d	30600201; 30600401; 30600508; 30600903; 30600999; 30601701; 30601801; 30688801; 40600240	0.31	Poorly

^a The emissions factors in this table represent the emissions exiting the flare. Since the flare is not the originating source of the VOC emissions, but rather the device controlling these pollutants routed from a process at the facility, the emissions factor is representative of controlled emissions rates for VOC. This values is not representative of the uncontrolled VOC routed to the flare from the associated process, and as such, it may not be appropriate for estimating the uncontrolled VOC emissions or potential to emit from the associated process.

- ^c References 4 through 9 and 11.
- ^d References 1, 4 through 8, and 11.
- ^e See Table 13.5-4 for a description of these SCCs.
- ^f Factor developed using the lower (net) heating value of the vent gas.

b These factors apply to well operated flares achieving at least 98% destruction efficiency and operating in compliance with the current General Provisions requirements of 40 CFR Part 60, i.e. >300 btu/scf net heating value in the vent gas and less than the specified maximum flare tip velocity. The VOC emissions factor data set had an average destruction efficiency of 98.9%, and the CO emissions factor data set had an average destruction efficiency of 99.1% (based on test reports where destruction efficiency was provided). These factors are based on steam-assisted and air-assisted flares burning a variety of vent gases.

Engines

1/24/2022 & Revision #2

Table 3.3-1. EMISSION FACTORS FOR UNCONTROLLED GASOLINE AND DIESEL INDUSTRIAL ENGINES^a

		ne Fuel 01, 2-03-003-01)		el Fuel 02, 2-03-001-01)	
Pollutant	Emission Factor (lb/hp-hr) (power output)	Emission Factor (lb/MMBtu) (fuel input)	Emission Factor (lb/hp-hr) (power output)	Emission Factor (lb/MMBtu) (fuel input)	EMISSION FACTOR RATING
NO _x	0.011	1.63	0.031	4.41	D
СО	6.96 E-03 ^d	0.99^{d}	6.68 E-03	0.95	D
SO_x	5.91 E-04	0.084	2.05 E-03	0.29	D
PM-10 ^b	7.21 E-04	0.10	2.20 E-03	0.31	D
CO ₂ ^c	1.08	154	1.15	164	В
Aldehydes	4.85 E-04	0.07	4.63 E-04	0.07	D
TOC					
Exhaust	0.015	2.10	2.47 E-03	0.35	D
Evaporative	6.61 E-04	0.09	0.00	0.00	E
Crankcase	4.85 E-03	0.69	4.41 E-05	0.01	E
Refueling	1.08 E-03	0.15	0.00	0.00	E

^a References 2,5-6,9-14. When necessary, an average brake-specific fuel consumption (BSFC) of 7,000 Btu/hp-hr was used to convert from lb/MMBtu to lb/hp-hr. To convert from lb/hp-hr to kg/kw-hr, multiply by 0.608. To convert from lb/MMBtu to ng/J, multiply by 430. SCC = Source Classification Code. TOC = total organic compounds.

PM-10 = particulate matter less than or equal to 10 μ m aerodynamic diameter. All particulate is

Assumed to be $\leq 1~\mu m$ in size. Assumes 99% conversion of carbon in fuel to CO₂ with 87 weight % carbon in diesel, 86 weight % carbon in gasoline, average BSFC of 7,000 Btu/hp-hr, diesel heating value of 19,300 Btu/lb, and gasoline heating value of 20,300 Btu/lb. Instead of 0.439 lb/hp-hr (power output) and 62.7 lb/mmBtu (fuel input), the correct emissions factors values are 6.96 E-03 lb/hp-hr (power output) and 0.99 lb/mmBtu (fuel input), respectively. This is an editorial correction. March 24, 2009

Table 3.3-2. SPECIATED ORGANIC COMPOUND EMISSION FACTORS FOR UNCONTROLLED DIESEL ENGINES^a

EMISSION FACTOR RATING: E

Pollutant	Emission Factor (Fuel Input) (lb/MMBtu)
Benzene ^b	9.33 E-04
Toluene ^b	4.09 E-04
Xylenes ^b	2.85 E-04
Propylene	2.58 E-03
1,3-Butadiene ^{b,c}	<3.91 E-05
Formaldehyde ^b	1.18 E-03
Acetaldehyde ^b	7.67 E-04
Acrolein ^b	<9.25 E-05
Polycyclic aromatic hydrocarbons (PAH)	
Naphthalene ^b	8.48 E-05
Acenaphthylene	<5.06 E-06
Acenaphthene	<1.42 E-06
Fluorene	2.92 E-05
Phenanthrene	2.94 E-05
Anthracene	1.87 E-06
Fluoranthene	7.61 E-06
Pyrene	4.78 E-06
Benzo(a)anthracene	1.68 E-06
Chrysene	3.53 E-07
Benzo(b)fluoranthene	<9.91 E-08
Benzo(k)fluoranthene	<1.55 E-07
Benzo(a)pyrene	<1.88 E-07
Indeno(1,2,3-cd)pyrene	<3.75 E-07
Dibenz(a,h)anthracene	<5.83 E-07
Benzo(g,h,l)perylene	<4.89 E-07
TOTAL PAH	1.68 E-04

a Based on the uncontrolled levels of 2 diesel engines from References 6-7. Source Classification Codes 2-02-001-02, 2-03-001-01. To convert from lb/MMBtu to ng/J, multiply by 430. b Hazardous air pollutant listed in the *Clean Air Act*. c Based on data from 1 engine.

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES^a (SCC 2-02-002-54)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Criteria Pollutants and Greenhouse	e Gases	
NO _x c 90 - 105% Load	4.08 E+00	В
NO _x c <90% Load	8.47 E-01	В
CO ^c 90 - 105% Load	3.17 E-01	C
CO ^c <90% Load	5.57 E-01	В
CO_2^{d}	1.10 E+02	A
SO ₂ ^e	5.88 E-04	A
TOC ^f	1.47 E+00	A
Methane ^g	1.25 E+00	C
VOCh	1.18 E-01	C
PM10 (filterable) ⁱ	7.71 E-05	D
PM2.5 (filterable) ⁱ	7.71 E-05	D
PM Condensable ^j	9.91 E-03	D
Trace Organic Compounds		
1,1,2,2-Tetrachloroethane ^k	<4.00 E-05	Е
1,1,2-Trichloroethane ^k	<3.18 E-05	Е
1,1-Dichloroethane	<2.36 E-05	E
1,2,3-Trimethylbenzene	2.30 E-05	D
1,2,4-Trimethylbenzene	1.43 E-05	C
1,2-Dichloroethane	<2.36 E-05	Е
1,2-Dichloropropane	<2.69 E-05	Е
1,3,5-Trimethylbenzene	3.38 E-05	D
1,3-Butadiene ^k	2.67E-04	D
1,3-Dichloropropene ^k	<2.64 E-05	Е
2-Methylnaphthalene ^k	3.32 E-05	C
2,2,4-Trimethylpentane ^k	2.50 E-04	C
Acenaphthenek	1.25 E-06	С

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES (Continued)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Acenaphthylene ^k	5.53 E-06	С
Acetaldehyde ^{k,l}	8.36 E-03	A
Acrolein ^{k,l}	5.14 E-03	A
Benzene ^k	4.40 E-04	A
Benzo(b)fluoranthene ^k	1.66 E-07	D
Benzo(e)pyrene ^k	4.15 E-07	D
Benzo(g,h,i)perylene ^k	4.14 E-07	D
Biphenyl ^k	2.12 E-04	D
Butane	5.41 E-04	D
Butyr/Isobutyraldehyde	1.01 E-04	С
Carbon Tetrachloride ^k	<3.67 E-05	Е
Chlorobenzene ^k	<3.04 E-05	Е
Chloroethane	1.87 E-06	D
Chloroform ^k	<2.85 E-05	Е
Chrysene ^k	6.93 E-07	C
Cyclopentane	2.27 E-04	С
Ethane	1.05 E-01	С
Ethylbenzene ^k	3.97 E-05	В
Ethylene Dibromide ^k	<4.43 E-05	Е
Fluoranthenek	1.11 E-06	С
Fluorene ^k	5.67 E-06	С
Formaldehyde ^{k,l}	5.28 E-02	A
Methanol ^k	2.50 E-03	В
Methylcyclohexane	1.23 E-03	С
Methylene Chloride ^k	2.00 E-05	С
n-Hexane ^k	1.11 E-03	С
n-Nonane	1.10 E-04	С

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES (Continued)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
n-Octane	3.51 E-04	С
n-Pentane	2.60 E-03	С
Naphthalenek	7.44 E-05	С
PAH^{k}	2.69 E-05	D
Phenanthrene ^k	1.04 E-05	D
Phenol ^k	2.40 E-05	D
Propane	4.19 E-02	С
Pyrene ^k	1.36 E-06	С
Styrene ^k	<2.36 E-05	Е
Tetrachloroethane ^k	2.48 E-06	D
Toluenek	4.08 E-04	В
Vinyl Chloride ^k	1.49 E-05	С
Xylene ^k	1.84 E-04	В

a Reference 7. Factors represent uncontrolled levels. For NO_x, CO, and PM10, "uncontrolled" means no combustion or add-on controls; however, the factor may include turbocharged units. For all other pollutants, "uncontrolled" means no oxidation control; the data set may include units with control techniques used for NOx control, such as PCC and SCR for lean burn engines, and PSC for rich burn engines. Factors are based on large population of engines. Factors are for engines at all loads, except as indicated. SCC = Source Classification Code. TOC = Total Organic Compounds. PM-10 = Particulate Matter ≤ 10 microns (μm) aerodynamic diameter. A "<" sign in front of a factor means that the corresponding emission factor is based on one-half of the method detection limit. Emission factors were calculated in units of (lb/MMBtu) based on procedures in EPA Method 19. To convert from (lb/MMBtu) to (lb/10⁶ scf), multiply by the heat content of the fuel. If the heat content is not available, use 1020 Btu/scf. To convert from (lb/MMBtu) to (lb/hp-hr) use the following equation:

lb/hp-hr = (lb/MMBtu) (heat input, MMBtu/hr) (1/operating HP, 1/hp)

Emission tests with unreported load conditions were not included in the data set. Based on 99.5% conversion of the fuel carbon to CO_2 . CO_2 [lb/MMBtu] = (3.67)(%CON)(C)(D)(1/h), where %CON = percent conversion of fuel carbon to CO_2 , C = carbon content of fuel by weight (0.75), D = density of fuel, $4.1 E+04 lb/10^6$ scf, and

- h = heating value of natural gas (assume 1020 Btu/scf at 60°F).
- ^e Based on 100% conversion of fuel sulfur to SO_2 . Assumes sulfur content in natural gas of $_2,000 \text{ gr/}10^6 \text{scf}$.
- Emission factor for TOC is based on measured emission levels from 22 source tests.
- g Emission factor for methane is determined by subtracting the VOC and ethane emission factors from the TOC emission factor. Measured emission factor for methane compares well with the calculated emission factor, 1.31 lb/MMBtu vs. 1.25 lb/MMBtu, respectively.
- h VOC emission factor is based on the sum of the emission factors for all speciated organic compounds less ethane and methane.
- Considered $\leq 1 \ \mu \text{m}$ in aerodynamic diameter. Therefore, for filterable PM emissions, PM10(filterable) = PM2.5(filterable).
- PM Condensable = PM Condensable Inorganic + PM-Condensable Organic
- ^k Hazardous Air Pollutant as defined by Section 112(b) of the Clean Air Act.
- For lean burn engines, aldehyde emissions quantification using CARB 430 may reflect interference with the sampling compounds due to the nitrogen concentration in the stack. The presented emission factor is based on FTIR measurements. Emissions data based on CARB 430 are available in the background report.

Cooling Towers

Table 5.1-3 (Metric And English Units). FUGITIVE EMISSION FACTORS FOR PETROLEUM REFINERIES^a

EMISSION FACTOR RATING: D

Emission Source	Emission Factor Units	Emission Factors		Applicable Control Technology
		Uncontrolled Emissions	Controlled Emissions	
Cooling towers ^b	kg/10 ⁶ L cooling water	0.7	0.08	Minimization of hydrocarbon leaks into cooling water system; monitoring of cooling water for hydrocarbons
	lb/10 ⁶ gal cooling water	6	0.7	Minimization of hydrocarbon leaks into cooling water system; monitoring of cooling water for hydrocarbons
Oil/water separators ^c	kg/10 ³ L waste water	0.6	0.024	Covered separators and/or vapor recovery systems
	lb/10 ³ gal waste water	5	0.2	Covered separators and/or vapor recovery systems
Storage		See Chap	ter 7 - Liquid	Storage Tanks
Loading	See Section	n 5.2 - Transpor	rtation And M	arketing Of Petroleum Liquids

^a References 2,4,12-13.

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^b If cooling water rate is unknown (in liters or gallons) assume it is 40 times the refinery feed rate (in liters or gallons). Refinery feed rate is defined as the crude oil feed rate to the atmospheric distillation column. 1 bbl (oil) = 42 gallons (gal), $1 \text{ m}^3 = 1000 \text{ L}$.

^c If waste water flow rate to oil/water separators is unknown (in liters or gallons) assume it is 0.95 times the refinery feed rate (in liters or gallons). Refinery feed rate is defined as the crude oil feed rate to the atmospheric distillation column. 1 bbl (oil) = 42 gal, 1 m³ = 1000 L.

Fugitives

EPA-453/R-95-017

1995 Protocol for Equipment Leak Emission Estimates

Emission Standards Division

U.S. ENVIRONMENTAL PROTECTION AGENCY
Office of Air and Radiation
Office of Air Quality Planning and Standards
Research Triangle Park, North Carolina 27711

November 1995

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TABLE 2-2. REFINERY AVERAGE EMISSION FACTORS^a

Equipment type	Service	Emission factor (kg/hr/source)b
Valves	Gas Light liquid Heavy liquid	0.0268 0.0109 0.00023
Pump seals ^C	Light liquid Heavy liquid	0.114 0.021
Compressor seals	Gas	0.636
Pressure relief valves	Gas	0.16
Connectors	All	0.00025
Open-ended lines	All	0.0023
Sampling connections	All	0.0150

aSource: Reference 2.

bThese factors are for non-methane organic compound emission rates.

^CThe light liquid pump seal factor can be used to estimate the leak rate from agitator seals.

TABLE 5-3. CONTROL EFFECTIVENESS FOR AN LDAR PROGRAM AT A REFINERY PROCESS UNIT

	Control effectiveness (%)			
Equipment type and service	Monthly monitoring 10,000 ppmv leak definition	Quarterly monitoring 10,000 ppmv leak definition	HON reg neg ^a	
Valves - gas	88	70	96	
Valves - light liquid	76	61	95	
Pumps - light liquid	68	45	88	
Connectors - all	b	b	81	

^a Control effectiveness attributable to the requirements of the proposed hazardous organic NESHAP equipment leak negotiated regulation are estimated based on equipment-specific leak definitions and performance levels.

b Data are not available to estimate control effectiveness.

Air Permit Technical Guidance for Chemical Sources

Fugitive Guidance

APDG 6422

Air Permits Division Texas Commission on Environmental Quality

June 2018

Table V: Control Efficiencies for LDAR

Equipment/Service	28M	28RCT	28VHP	28MID	28LAER	28CNTQ	28CNTA	28PI	28AVO ⁹
Valves ¹									97%
Gas/Vapor	75%	97%	97%	97%	97%			30%	
Light Liquid	75%	97%	97%	97%	97%			30%	
Heavy Liquid⁵	0% ⁶	0% ⁶	0% ⁶	0% ⁶	30% ^{6, 8}			30%8	
Pumps ¹									93%
Light Liquid	75%	75%	85%	93%	93%			30%	
Heavy Liquid⁵	0%	0%7	0%7	0%8, 10	30% ⁸			30%8	
Flanges/Connectors ¹	30%	30%	30%	30%				30%	97%
Gas/Vapor					97%	97%	75%		
Light Liquid					97%	97%	75%		
Heavy Liquid ⁸					30%	30%	30%		
Compressors ¹	75%	75%	85%	95%	95%			30%	95%
Relief Valves ^{1, 2} (Gas/Vapor)	75%	97%	97%	97%	97%			30%	97%
Sampling Connection ³ (pounds per hour per sample taken)	0%	0%	0%	0%	0%			0%	0%
Open Ended Lines ^{1, 4}									

It should be noted in the application and added to the permit conditions if any of the footnotes are applicable. For example, if components in heavy liquid service are monitored, then the application should include the monitored concentration and the concentration of saturation, in ppmv and such monitoring will be added as a separate condition.

Endnotes Table V

- Control efficiencies apply only to components that are actually monitored. Control efficiencies do not apply to components that are difficult or unsafe-to-monitor on the standard schedule. However, difficult-to-monitor gas or light liquid valves under the 28RCT, 28VHP, 28MID, or 28LAER programs that are monitored once per year may apply a 75% reduction credit.
- 100% control may be taken if a relief valve vents to an operating control device or if it is equipped with a rupture disc and a pressure-sensing device between the valve and disc to monitor for disc integrity. For new facilities, BACT guidelines generally require that all relief valves vent to a control device. When there are safety reasons that the relief valve cannot achieve 100% control, the relief valve can be monitored under the LDAR programs for the credit listed. This monitoring must be performed regardless of whether the relief valve is considered accessible, difficult-to-monitor or unsafe-to-monitor. Relief valves that do not achieve 100% control should not be built in locations that are unsafe-to-monitor.
- Sampling connection control efficiencies are covered under other equipment and services. Sampling emissions are based on the number of samples taken per year as opposed to the number of connections. Fugitives for a closed loop sampling system are based on the component count.
- Good design criteria for special chemicals handling and most LDAR programs require open-ended lines to be equipped with an appropriately sized cap, blind flange, plug, or a second valve. If so equipped, open-ended lines may be given a 100% control credit. Regardless of the lines given 100% credit, these lines should be mentioned in permit applications. Exceptions to the LDAR program criteria may be made for safety reasons with the approval of TCEQ management.

- Monitoring components in heavy liquid service using an instrument is not required by any of the 28 Series LDAR programs. If monitored with an instrument, the applicant must demonstrate that the VOC being monitored has sufficient vapor pressure to allow for reduction credit. Monitoring near or below background concentration is unreasonable and additional credit is not given for monitoring generic VOC below 500 ppmv. Credit will be given in cases where a specific compound is monitored below 500 ppmv when sufficient demonstration has been made of the ability to monitor at the specified concentration and there is no concern about the monitoring concentration being close to the background concentration. No credit may be taken if the concentration at saturation is below the leak definition of the monitoring program (i.e. (0.044 psia/14.7 psia) x 10⁶ = 2,993 ppmv versus leak definition = 10,000 ppmv).
- If the concentration at saturation is greater than the leak definition. Contact the TCEQ to determine whether valves in heavy liquid service may be given a 97% credit if monitored at 500 ppmv
- If the concentration at saturation is greater than the leak definition. Contact the TCEQ to determine whether pumps in heavy liquid service may be given a 85% reduction credit if monitored at 2.000 ppmy.
- Ultra heavy liquid with a vapor pressure < 0.0147 psia at operating temperature may receive higher emission reduction credit (matching the credit of 28AVO) provided a 28PI inspection program is performed on these components.
- Audio, Visual and Olfactory (AVO) AVO credit is based on the chemical constituent, not vapor pressure or service type. This program (28AVO) is approved for chlorine, ammonia, hydrogen sulfide, hydrogen fluoride, mercaptans, and hydrogen cyanide only.
- If the concentration at saturation is greater than the leak definition. Contact the TCEQ to determine whether pumps in heavy liquid service may be given a 93% credit if monitored at 500 ppmv.

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Saved Date: 8/31/2021

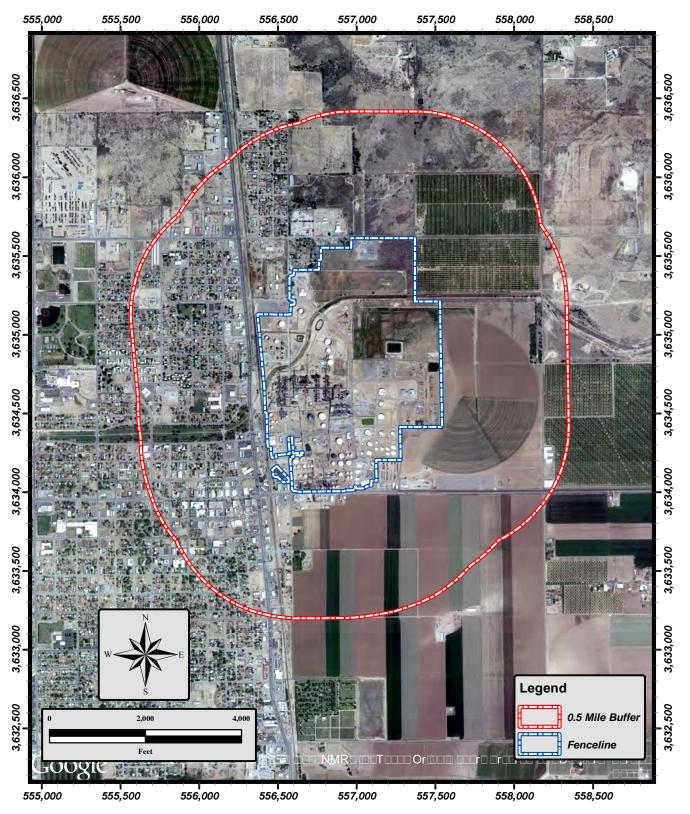
Section 8

Map(s)

A map such as a 7.5 minute topographic quadrangle showing the exact location of the source. The map shall also include the following:

The UTM or Longitudinal coordinate system on both axes	An indicator showing which direction is north	
A minimum radius around the plant of 0.8km (0.5 miles)	Access and haul roads	
Topographic features of the area	Facility property boundaries	
The name of the map	The area which will be restricted to public access	
A graphical scale		

Three maps are included in this section. Figure 1 is a map of the refinery and surrounding area. Figure 2 depicts the city limits of Artesia. Figure 3 shows the location of the refinery flares.



Grid Presented is UTM Zone 13, NAD 1983



FIGURE 1 AREA MAP Artesia Refinery Artesia, New Mexico

from USGS Quadrangle Artesia, New Mexico Ground Condition Depicted May 2014 Digital Data Courtesy of Google Earth

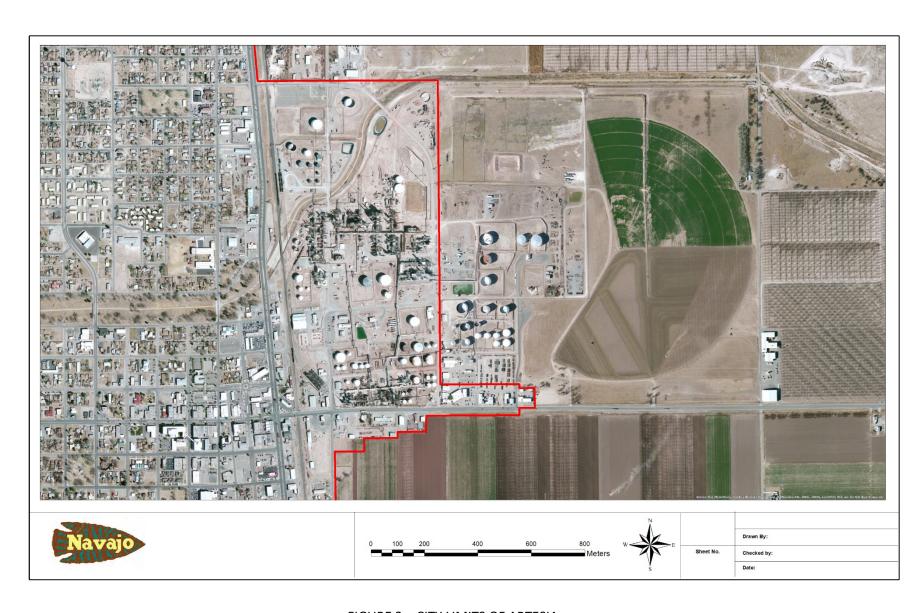


FIGURE 2 – CITY LIMITS OF ARTESIA

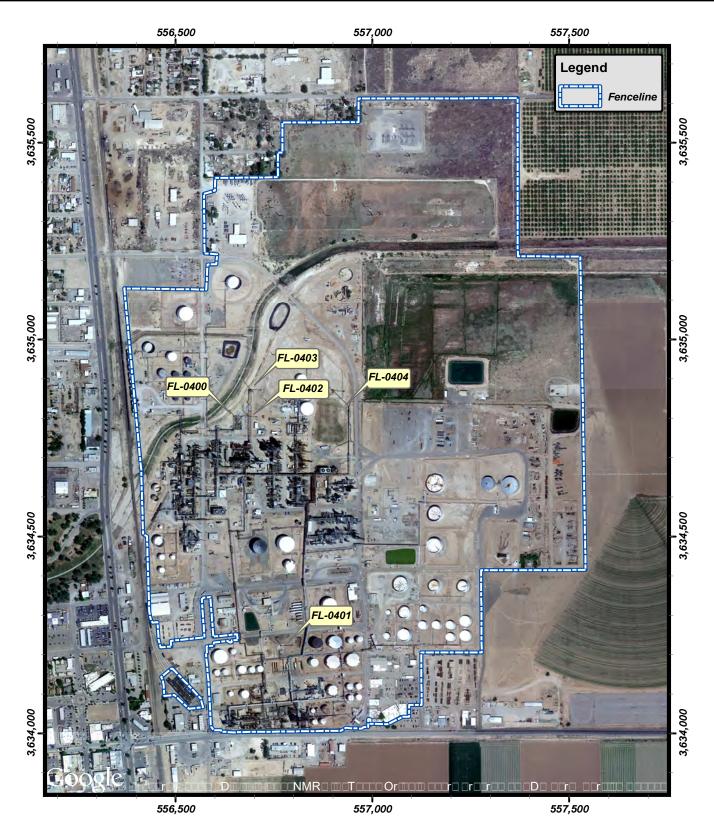




FIGURE 3 UNIT LOCATION MAP Artesia Refinery Artesia, New Mexico

from USGS Quadrangle Artesia, New Mexico Ground Condition Depicted May 2014 Digital Data Courtesy of Google Earth

Section 9

Proof of Public Notice

(for NSR applications submitting under 20.2.72 or 20.2.74 NMAC) (This proof is required by: 20.2.72.203.A.14 NMAC "Documentary Proof of applicant's public notice")

■ I have read the AQB "Guidelines for Public Notification for Air Quality Permit Applications"
This document provides detailed instructions about public notice requirements for various permitting actions.
It also provides public notice examples and certification forms. Material mistakes in the public notice will require a re-notice before issuance of the permit.

Unless otherwise allowed elsewhere in this document, the following items document proof of the applicant's Public Notification. Please include this page in your proof of public notice submittal with checkmarks indicating which documents are being submitted with the application.

New Permit and Significant Permit Revision public notices must include all items in this list.

Technical Revision public notices require only items 1, 5, 9, and 10.

Per the Guidelines for Public Notification document mentioned above, include:

- 1. A copy of the certified letter receipts with post marks (20.2.72.203.B NMAC)
- 2. A list of the places where the public notice has been posted in at least four publicly accessible and conspicuous places, including the proposed or existing facility entrance. (e.g. post office, library, grocery, etc.)
- 3. A copy of the property tax record (20.2.72.203.B NMAC).
- 4. A sample of the letters sent to the owners of record.
- 5. A sample of the letters sent to counties, municipalities, and Indian tribes.
- 6. A sample of the public notice posted and a verification of the local postings.
- 7. A table of the noticed citizens, counties, municipalities and tribes and to whom the notices were sent in each group.
- 8. A copy of the public service announcement (PSA) sent to a local radio station and documentary proof of submittal.
- 9. A copy of the <u>classified or legal</u> ad including the page header (date and newspaper title) or its affidavit of publication stating the ad date, and a copy of the ad. When appropriate, this ad shall be printed in both English and Spanish.
- 10. A copy of the <u>display</u> ad including the page header (date and newspaper title) or its affidavit of publication stating the ad date, and a copy of the ad. When appropriate, this ad shall be printed in both English and Spanish.
- 11. A map with a graphic scale showing the facility boundary and the surrounding area in which owners of record were notified by mail. This is necessary for verification that the correct facility boundary was used in determining distance for notifying land owners of record.

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Airgas USA LLC PO Box 1152 Tulsa, OK 74101-1152



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Corinne B Grace Trust Western Commerce Bank Trustees PO Box 1358 Carlsbad, NM 88221-1358





Saved Date: 8/31/2021

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DOC Properties LLC 813 N Washington Ave Roswell, NM 88201







Donald R & David Golemon 602 E Richey Ave Artesia, NM 88210



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JD Gilbert, Jr RC Hoelscher & Karen Schroeder 2139 Spring Creek Rd Lebanon, TN 37087



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Jesus M & Maria Mascorro 1416 N Freeman Ave Artesia, NM 88210



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Johnny W & Terry J Fowler PO Box 1223 Artesia, NM 88211-1223



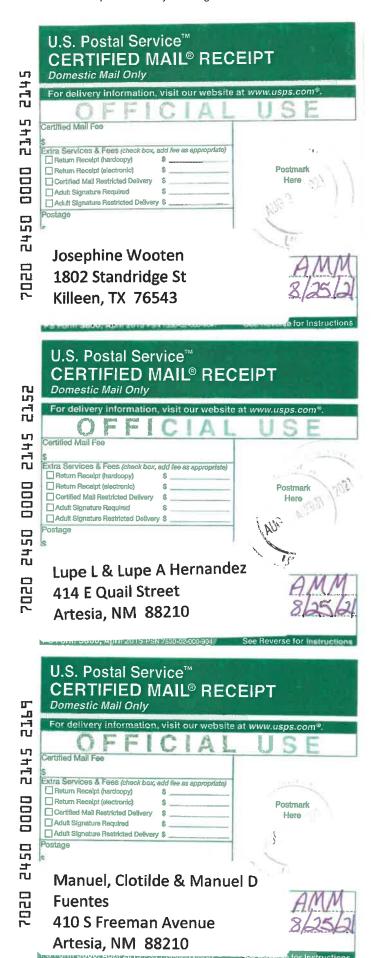
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Stephen Earl & Jana S Borland **PO Box 371** Artesia, NM 88211-0371



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Sybill Smith R252 N Haldeman Rural Rd Artesia, NM 88210





Timmy K & Teresa L Baize 210 S Roselawn Ave Artesia, NM 88210











General Posting of Notices – Certification

buzanne Garcia, the undersigned, certify that on August 25, 2021, posted a true and correct copy of the attached Public Notice in the following publicly accessible and conspicuous places in the City of Artesia in Eddy County, State of New Mexico on the following dates:

- 1. Artesia Refinery (August 25, 2021)
- 2. Artesia City Hall (August 25, 2021)
- 3. Artesia Public Library (August 25, 2021)
- 4. Artesia Post Office (August 25, 2021)

Signed this <u>25</u> day of <u>6</u>



August 23, 2021

Ms. Aubrey Hobson City of Artesia - City Clerk 511 W. Texas Avenue Artesia, NM 88210

Certified Mail/Return Receipt No. 7020 2450 0000 2145 1773

Saved Date: 8/31/2021

Re: Public Notice

Application for a PSD Major Air Permit Modification for Artesia Refinery HollyFrontier Navajo Refining LLC Artesia, Eddy County, New Mexico

Dear Ms. Hobson,

HollyFrontier Navajo Refining LLC ("Navajo") announces its application submittal to the New Mexico Environment Department ("NMED") for a significant permit revision of the Artesia Refinery permit PSD-NM-0195M39R3. The expected date of application submittal to the Air Quality Bureau is September 02, 2021.

The exact location for the facility known as, Artesia Refinery, is at 501 E. Main St., Artesia, NM 88210. The approximate location of this facility is less than 0.5 miles east of the intersection of E. Main St. and S. 1st St. in Eddy County.

Navajo is submitting this application for a significant permit revision of Permit No. PSD-NM-0195M39R3, in accordance with 20.2.72.219.D New Mexico Administrative Code. This revision is necessary to adequately represent the operational conditions at the refinery, to update the calculations' methodology where appropriate and according to latest guidance published, and to update representations from previous submittals.

The estimated maximum quantities of any regulated air contaminant will be as follows in pound per hour (pph) and tons per year (tpy) and may change slightly during the course of the Department's review:

Pollutant	pph	tpy
Nitrogen Oxides (NO _x)	456.40	798.60
Carbon Monoxide (CO)	2,067.40	1,448.90
Volatile Organic Compounds (VOC)	2,460.50	1,325.70
Sulfur Dioxide (SO ₂)	2,050.00	438.30
Particulate Matter (PM)	58.00	219.40
Particulate Matter 10 microns or less (PM ₁₀)	85.50	214.30
Particulate Matter 2.5microns or less (PM _{2.5})	84.20	208.80
Hydrogen Sulfide (H ₂ S)	20.40	5.90
Lead (Pb)	0.00	0.00
Total sum of all Hazardous Air Pollutants (HAPs)	74.50	228.00
Ammonia (NH ₃)	18.60	81.10
Sulfuric Acid (H ₂ SO ₄)	7.10	18.10
Green House Gas Emissions as Total CO2e	0.00	10,783,565.30

Ms. Aubrey Hobson City of Artesia - City Clerk August 23, 2021 Page 2 of 3

The standard operating schedule of the facility is and will continue to be continuous 24 hours per day, 7 days a week, and a maximum of 52 weeks per year.

The owner and/or operator of the Facility is: HollyFrontier Navajo Refining LLC, P.O. Box 159, Artesia, NM 88211-0159.

If you have any comments about the construction or operation of this facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to this address: Permit Programs Manager; New Mexico Environment Department; Air Quality Bureau; 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816; (505) 476-4300; 1 800 224-7009; https://www.env.nm.gov/aqb/permit/aqb_draft_permits.html. Other comments and questions may be submitted verbally.

Please refer to the company name and facility name, or send a copy of this notice along with your comments, since the Department may have not yet received the permit application. Please include a legible return mailing address with your comments. Once the Department has performed a preliminary review of the application and its air quality impacts, the Department's notice will be published in the legal section of a newspaper circulated near the facility location.

Atención

Este es un aviso de la oficina de Calidad del Aire del Departamento del Medio Ambiente de Nuevo México, relativo a las emisiones producidas por una industria en este área. Si usted desea información en español, por favor comuníquese con esta oficina en el teléfono 505-476-5557.

Sincerely,

Kawika Tupou

Environmental Manager

HollyFrontier Navajo Refining LLC

501 E. Main Street

Artesia, NM 88210

cc:

Eddy County, Darlene Rosprim, County Clerk

Chaves County, Cindy Fuller, County Clerk

NMED, Melinda Owens, via email to Melinda.Owens@state.nm.us

NMED, Joe Kimbrell, via email to Joseph.Kimbrell@state.nm.us

HollyFrontier, P. Miller, T. Wheeler, S. Gokhale, A. Miro

Ms. Aubrey Hobson City of Artesia - City Clerk August 23, 2021 Page 3 of 3

Notice of Non-Discrimination

NMED does not discriminate on the basis of race, color, national origin, disability, age or sex in the administration of its programs or activities, as required by applicable laws and regulations. NMED is responsible for coordination of compliance efforts and receipt of inquiries concerning non-discrimination requirements implemented by 40 C.F.R. Part 7, including Title VI of the Civil Rights Act of 1964, as amended; Section 504 of the Rehabilitation Act of 1973; the Age Discrimination Act of 1975, Title IX of the Education Amendments of 1972, and Section 13 of the Federal Water Pollution Control Act Amendments of 1972. If you have any questions about this notice or any of NMED's non-discrimination programs, policies or procedures, or if you believe that you have been discriminated against with respect to a NMED program or activity, you may contact: Kathryn Becker, Non-Discrimination Coordinator, NMED, 1190 St. Francis Dr., Suite N4050, P.O. Box 5469, Santa Fe, NM 87502, (505) 827-2855, nd.coordinator@state.nm.us. You may also visit our website at https://www.env.nm.gov/non-employee-discrimination-complaint-page/ to learn how and where to file a complaint of discrimination.



August 23, 2021

Ms. Cindy Fuller Chaves County, County Clerk #1 St. Mary's Place, Suite 110 Roswell, NM 88203

Certified Mail/Return Receipt No. 7020 2450 0000 2145 1780

Saved Date: 8/31/2021

Re:

Public Notice

Application for a PSD Major Air Permit Modification for Artesia Refinery HollyFrontier Navajo Refining LLC

Artesia, Eddy County, New Mexico

Dear Ms. Fuller,

HollyFrontier Navajo Refining LLC ("Navajo") announces its application submittal to the New Mexico Environment Department ("NMED") for a significant permit revision of the Artesia Refinery permit PSD-NM-0195M39R3. The expected date of application submittal to the Air Quality Bureau is September 2, 2021.

The exact location for the facility known as, Artesia Refinery, is at 501 E. Main St., Artesia, NM 88210. The approximate location of this facility is less than 0.5 miles east of the intersection of E. Main St. and S. 1st St. in Eddy County.

Navajo is submitting this application for a significant permit revision of Permit No. PSD-NM-0195M39R3, in accordance with 20.2.72.219.D New Mexico Administrative Code. This revision is necessary to adequately represent the operational conditions at the refinery, to update the calculations' methodology where appropriate and according to latest guidance published, and to update representations from previous submittals.

The estimated maximum quantities of any regulated air contaminant will be as follows in pound per hour (pph) and tons per year (tpy) and may change slightly during the course of the Department's review:

Pollutant	pph	tpy
Nitrogen Oxides (NO _x)	456.40	798.60
Carbon Monoxide (CO)	2,067.40	1,448.90
Volatile Organic Compounds (VOC)	2,460.50	1,325.70
Sulfur Dioxide (SO ₂)	2,050.00	438.30
Particulate Matter (PM)	58.00	219.40
Particulate Matter 10 microns or less (PM ₁₀)	85.50	214.30
Particulate Matter 2.5microns or less (PM _{2.5})	84.20	208.80
Hydrogen Sulfide (H ₂ S)	20.40	5.90
Lead (Pb)	0.00	0.00
Total sum of all Hazardous Air Pollutants (HAPs)	74.50	228.00
Ammonia (NH ₃)	18.60	81.10
Sulfuric Acid (H ₂ SO ₄)	7.10	18.10
Green House Gas Emissions as Total CO2e	0.00	10,783,565.30

Ms. Cindy Fuller Chaves County, County Clerk August 23, 2021 Page 2 of 3

Saved Date: 8/31/2021

The standard operating schedule of the facility is and will continue to be continuous 24 hours per day, 7 days a week, and a maximum of 52 weeks per year.

The owner and/or operator of the Facility is: HollyFrontier Navajo Refining LLC, P.O. Box 159, Artesia, NM 88211-0159.

If you have any comments about the construction or operation of this facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to this address: Permit Programs Manager; New Mexico Environment Department; Air Quality Bureau; 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816; (505) 476-4300; 1 800 224-7009; https://www.env.nm.gov/aqb/permit/aqb_draft_permits.html. Other comments and questions may be submitted verbally.

Please refer to the company name and facility name, or send a copy of this notice along with your comments, since the Department may have not yet received the permit application. Please include a legible return mailing address with your comments. Once the Department has performed a preliminary review of the application and its air quality impacts, the Department's notice will be published in the legal section of a newspaper circulated near the facility location.

Atención

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Sincerely,

Kawika Tupou

Environmental Manager

HollyFrontier Navajo Refining LLC

501 E. Main Street

Artesia, NM 88210

cc:

City of Artesia, Aubrey Hobson, City Clerk
Eddy County, Darlene Rosprim, County Clerk
NMED, Melinda Owens, via email to Melinda.Owens@state.nm.us
NMED, Joe Kimbrell, via email to Joseph.Kimbrell@state.nm.us
HollyFrontier, P. Miller, T. Wheeler, S. Gokhale, A. Miro

Ms. Cindy Fuller Chaves County, County Clerk August 23, 2021 Page 3 of 3

Saved Date: 8/31/2021

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August 23, 2021

Ms. Darlene Rosprim Eddy County, County Clerk 325 S. Main Street Carlsbad, NM 88220

Certified Mail/Return Receipt No. 7020 2450 0000 2145 1797

Re:

Public Notice

Application for a PSD Major Air Permit Modification for Artesia Refinery HollyFrontier Navajo Refining LLC Artesia, Eddy County, New Mexico

Dear Ms. Fuller,

HollyFrontier Navajo Refining LLC ("Navajo") announces its application submittal to the New Mexico Environment Department ("NMED") for a significant permit revision of the Artesia Refinery permit PSD-NM-0195M39R3. The expected date of application submittal to the Air Quality Bureau is September 02, 2021.

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Ms. Darlene Rosprim Eddy County, County Clerk August 23, 2021 Page 2 of 3

Saved Date: 8/31/2021

The standard operating schedule of the facility is and will continue to be continuous 24 hours per day, 7 days a week, and a maximum of 52 weeks per year.

The owner and/or operator of the Facility is: HollyFrontier Navajo Refining LLC, P.O. Box 159, Artesia, NM 88211-0159.

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Sincerely,

Kawika Tupou

Environmental Manager

HollyFrontier Navajo Refining LLC

501 E. Main Street

Artesia, NM 88210

cc:

City of Artesia, Aubrey Hobson, City Clerk

Chaves County, Cindy Fuller, County Clerk

NMED, Melinda Owens, via email to Melinda. Owens@state.nm.us

NMED, Joe Kimbrell, via email to Joseph.Kimbrell@state.nm.us

HollyFrontier, P. Miller, T. Wheeler, S. Gokhale, A. Miro

Ms. Darlene Rosprim Eddy County, County Clerk August 23, 2021 Page 3 of 3

Saved Date: 8/31/2021

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HollyFrontier Navajo Refining LLC 501 East Main • Artesia, NM 88210 (575) 748-3311 • http://www.hollyfrontier.com



August 23, 2021

Neighbor of Navajo Refinery Located @ 501 East Main Street Artesia, NM 88210

Re: Public Notice

Application for a PSD Major Air Permit Modification for Artesia Refinery

HollyFrontier Navajo Refining LLC Artesia, Eddy County, New Mexico

Dear Neighbor,

HollyFrontier Navajo Refining LLC ("Navajo") announces its application submittal to the New Mexico Environment Department ("NMED") for a significant permit revision of the Artesia Refinery permit PSD-NM-0195M39R3. The expected date of application submittal to the Air Quality Bureau is September 02, 2021.

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Sincerely,

Kawika Tupou

Environmental Manager

HollyFrontier Navajo Refining LLC

501 E. Main Street

Artesia, NM 88210

cc:

City of Artesia, Aubrey Hobson, City Clerk

Chaves County, Cindy Fuller, County Clerk

Eddy County, Darlene Rosprim, County Clerk

NMED, Melinda Owens, via email to Melinda. Owens@state.nm.us

NMED, Joe Kimbrell, via email to Joseph.Kimbrell@state.nm.us

HollyFrontier, P. Miller, T. Wheeler, S. Gokhale, A. Miro

August 23, 2021 Page 3 of 3

Notice of Non-Discrimination

NMED does not discriminate on the basis of race, color, national origin, disability, age or sex in the administration of its programs or activities, as required by applicable laws and regulations. NMED is responsible for coordination of compliance efforts and receipt of inquiries concerning non-discrimination requirements implemented by 40 C.F.R. Part 7, including Title VI of the Civil Rights Act of 1964, as amended; Section 504 of the Rehabilitation Act of 1973; the Age Discrimination Act of 1975, Title IX of the Education Amendments of 1972, and Section 13 of the Federal Water Pollution Control Act Amendments of 1972. If you have any questions about this notice or any of NMED's non-discrimination programs, policies or procedures, or if you believe that you have been discriminated against with respect to a NMED program or activity, you may contact: Kathryn Becker, Non-Discrimination Coordinator, NMED, 1190 St. Francis Dr., Suite N4050, P.O. Box 5469, Santa Fe, NM 87502, (505) 827-2855, nd.coordinator@state.nm.us. You may also visit our website at https://www.env.nm.gov/non-employee-discrimination-complaint-page/ to learn how and where to file a complaint of discrimination.

<u>Submittal of Public Service Announcement – Certification</u>

I, Alena Miro	, the undersigned, certify that on August 26, 2021,
	ent to Pecos Valley Broadcasting Company that serves
	w Mexico, in which the source is or is proposed to be
•	asting Company RESPONDED THAT IT WOULD
AIR THE ANNOUNCEMENT.	
Signed this 26 day of August	, 2021 ,
alem	8/26/2021
Signature	Date
Alena Miro	
Printed Name	
Environmental Engineer	
Title {APPLICANT OR RELATIONS	HIP TO APPLICANT}

Section 9, Page 24 Saved Date: 8/31/2021

Affidavit of Publication	Copy of Public		
State of New Mexico Publisher	HollyFrontier Navajo Refining LLG application submittal to the New M partment ("NMED") for a significa Artesia Refinery permit PSD-NN4- ed date of application submittal to September 2, 2021.	ice	
State of New Mexico	HollyFrontier Navajo Refining LLC	("Navajo") an	nounces
County of Eddy:	application submittal to the New M partment ("NMED") for a significa-	nt permit revis	ion of th
Danny Scott Leas Store Publisher	Artesia Refinery permit PSD-NM-0 ed date of application submittal to t	195M39R3. The Air Quality	he exped Bureau
guary arteria any system as as	September 2, 2021.		
he Artesia Daily Press, a daily newspaper of General	The exact location for the facility ki	nown as, Artes	ia Refine
culation, published in English at Artesia, said county	The exact location for the facility ki is at 501 E. Main St., Artesia, NM 8 location of this facility is less than 6	.5 miles east o	f the inte
ate, and that the hereto attached	section of E. Main St. and S. 1st St.	in Ludy Cours	1
Legal Ad	Navajo is submitting this application revision of Permit No. PSD-NM-01 with 20.2.72.219.D New Mexico Ad	n for a signific 95M39R3, in	ant perr
sublished in a regular and entire issue of the said	with 20.2.72.219.D New Mexico Ac	ministrative C	ode. The
a Daily Press, a daily newspaper duly qualified	conditions at the refinery, to update	the calculation	ns' meth
nat purpose within the meaning of Chapter 167 of	revision is necessary to adequately conditions at the refinery, to update odology where appropriate and acc published, and to update represent	itions from pre	vious su
937 Session Laws of the state of New Mexico for	mittais.		
1 Consecutive weeks/day on the same	The estimated maximum quantities taminant will be as follows in pour per year (tpy) and may change slighthe Department's review:	of any regulat	ed air co
as follows:	per year (tpy) and may change sligh	tly during the	course o
Publication August 26, 2021	the Department's review:		
nd Publication	Pollutant Nitrogen Oxides (NOx)	pph 456.40	tpy 798.6
1 Publication	Nitrogen Oxides (NOx) Carbon Monoxide (CO)	2,067.40	1,448
h Publication	Carbon Monoxide (CO) Volatile Organic Compounds (VO) Sulfur Dioxide (SO2) Particulate Matter (PM)	2,050.00	438.3
Publication	Particulate Matter (PM) Particulate Matter 10 microns	58.00	219.4
Publication	or less (PM10) Particulate Matter 2.5microns or less (PM2.5)	85.50.) bin.	214.3
th Publication	or less (PM2.5)	84.20 20.40	208.8 5.90
ribed and sworn before me this	Hydrogen Sulfide (H2S) Lead (Pb)	0.00	0.00
day of August 2021	Total sum of all Hazardous Air	74.50	228.0
	Pollutants (HAPs) Ammonia (NH3) Sulfuric Acid (H2SO4)	18.60 7.10	81.10 18.10
OFFICIAL SEAL Lottsha Romine	Green House Gas Emissions as Total CO2e		0,783,56
OFFICIAL SEAL Listsha Romine AUTHORY PUBLIC-STATE OF NEW MEXICO My commission expires: 511 3.12-223	PERSONAL COLUMN STATEMENT		
sty commission expires:	The standard operating schedule o tinue to be continuous 24 hours pe maximum of 52 weeks per year.	r day, 7 days a	week, an
THE REPORT OF THE PARTY OF	The owner and/or operator of the I Navajo Refining LLC, P.O. Box 159	acility is: Holl , Artesia, NM	Frontier 88211-01
Listisha Romine utisha Romine utisha Romine utisha Romine	If you have any comments about the tion of this facility, and you want yas part of the permit review process comments in writing to this address whesto Christoment D. Bureau, 32750-1800 of the Michael Comments of the Work	our comments s, you must sul ss: Permit Prog epartment; Air ez, Suite 1; Sani 00; 1 800 224-7 draft_permits. ubmitted verba	to be made omit you rams Ma Quality as Fe, Ne 1009; http. html. Other
	With your comments, please refer facility name, or send a copy of thi comments. This information is ne ment may have not yet received in include a legible return mailing adment has completed its preliminar and its air quality impacts, the De published in the legal section of a the facility location.	to the company s notice along of cessary since the e permit applic dress. Once the y review of the partment's notion mewspaper circ	y name a with you ne Depar ation. P e Depar applicat ce will be ulated n
	Atencid Este es un aviso de la oficina de Ci tamento del Medio Ambiente de N emisiones producidas por una indi desea información en español, por esta oficina en el teléfono 505-476	n didad del Aire Juevo México, ustria en este á favor comunio 5557.	del Depa relativo a rea. Si us quese cor
	Netice of Nen-Di NMED does not discriminate Di notal origin, disability, age or sec programs or activities, as required ulations. NMED is responsible to efforts and recipit of inquired origination of the Color of the Color Tille VI of the Cavil Rights and to 150 4 of the Rehabilitation Act of 15 1372, and Section 13 of the Feder Act Amendments of 1972. If you this notice or any of NMED's non policies or procedures, or if you b discriminated against with respec- activity, you may contact. Kally to continuous contacts or the color origination of the Color origination	icrimination the basis of ractin the administ by applicable I coordination (cerning non-d. C.F.R. Part 7, in 1964, as amend 7/3; the Age Diducation Amenal Water Polluti have any questi-discrimination elieve that you to a NMED p. Becker, Non-I. Francis Dr., S. (2, (505) 827-24 also visit our 2012 also visit our 2012 and 2012 also visit our 2012 and 2012 also visit our 2012 also visit	e, color, n tration of laws and of of compli iscrimina cluding led; Secti scrimina dments c on Contr ons abou n program to program o Discrimir uite N40: 355, nd. cc ebsite at
	Published in the Artesia Daily Pro 2021 Legal No. 25857.		

County of Eddy: Danny Scott being duly sourm suyes that he is the Publis of the Artesia Daily Press, a daily newspaper of General circulation, published in English at Artesia, said county and stare, and that the hereto attached Display Ad was published in a regular and entire issue of the said Artesia Daily Press, a daily newspaper duly qualified for that purpose within the meaning of Chapter 167 of the 1937 Session Lawa of the state of New Mexico for 1 Consecutive weeks/day on the same days as follows: First Publication Second Publication First Publication Second Publication Seventh Publication Seventh Publication Seventh Publication Subscribed and sworn before me this 26th day of August Any commence and Publication Subscribed and sworn before me this 26th day of August Latisha Romine Latisha Romine	County of Eddy: Danny Scott being daily swyern sayes that he is the Publist of the Artesia Daily Press, a daily newspaper of General circulation, published in English at Artesia, said county and state, and that the hereto attached Display Ad was published in a regular and entire issue of the said Artesia Daily Press, a daily newspaper duly qualified for that purpose within the meaning of Chapter 167 of the 1937 Session Laws of the state of New Mexico for Consecutive weeks/day on the same day as follows: First Publication August 26, 2021 Second Publication First Publication First Publication Sitch Publication Seventh Publication Sitch Publication Seventh Publication Subscribed and sworn before me this 26th day of August 2	County of Eddy: Danny Scott being duly swyern sayes that he is the of the Artesia Daily Press, a daily newspaper of General circulation, published in English at Artesia, said county and stare, and that the bereto attached Display Ad was published in a regular and entire issue of the said Artesia Daily Press, a daily newspaper duly qualifiled for that purpose within the meaning of Chapter 167 of the 1937 Session Laws of the state of New Mexico for 1 Consecutive weeks/day on the same days as follows: First Publication Second Publication First Publication Second Publication Seventh Publication Seventh Publication Seventh Publication Subscribed and sworn before me this 26th day of August 2 August 2 Latisha Romine Latisha Romine Latisha Romine	County of Eddy: Danny Scott being daily swyern sayes that he is the of the Artesia Daily Press, a daily newspaper of General circulation, published in English at Artesia, said county and state, and that the hereto attached Display Ad was published in a regular and entire issue of the said Artesia Daily Press, a daily newspaper duly qualifiled for that purpose within the meaning of Chapter 167 of the 1937 Session Lawa of the state of New Mexico for 1 Consecutive weeks/day on the same days as follows: First publication Second Publication First Publication Second Publication Seventh Publication Seventh Publication Seventh Publication Seventh Publication Subscribed and sworn before me this 26th day of August 2 OFFICIAL SEAL Not represent the publication Subscribed and sworn before me this 26th day of August 2 Latisha Romine Latisha Romine	County of Eddy: Danny Scott being duly sofern sayes that he is the Publish of the Artesia Daily Press, a daily newspaper of General circulation, published in English at Artesia, said county and stare, and that the hereto attached Display Ad was published in a regular and entire issue of the said Artesia Daily Press, a daily newspaper duly qualified for that purpose within the meaning of Chapter 167 of the 1937 Session Laws of the state of New Mexico for 1 Consecutive weeks/day on the same days as follows: First Publication Second Publication First Publication Second Publication First Publication Seventh Publication Seventh Publication Subscribed and sworn before me this 26th day of August 2 OFFICIAL EAA. Wornstein General Consecutive Relations and Publication Subscribed and sworn before me this 26th day of August 2 Latisha Romine	County of Eddy: Danny Scott being duly sofern sayes that he is the Publish of the Artesia Daily Press, a daily newspaper of General circulation, published in English at Artesia, said county and stare, and that the hereto attached Display Ad was published in a regular and entire issue of the said Artesia Daily Press, a daily newspaper duly qualified for that purpose within the meaning of Chapter 167 of the 1937 Session Laws of the state of New Mexico for 1 Consecutive weeks/day on the same days as follows: First Publication Second Publication First Publication Second Publication First Publication Seventh Publication Seventh Publication Subscribed and sworn before me this 26th day of August 2 OFFICIAL EAA. 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Copy of Publication:

HollyFrontier Navajo Refining LLC ("Navajo") announ application submittal to the New Mexico Environment partment ("Nabel") for a significant permit revision of Artesia Refinery permit PSD-NN-0195M39R3. The ex ed date of application submittal to the Air Quality Bure September 2, 2021.

The exact location for the facility known as, Artesia Ref is at 501 E. Main St., Artesia, NM 88210. The approximal location of this facility is less than 0.5 miles east of the is section of E. Main St. and S. 1st St. in Eddy County.

Navajo is submitting this application for a significant perevision of Permit No. PSD. NM. 0195MsPS, in accord with 20.27.2 19.0 New Mexico Administrative Code, revision is necessary to adequately represent the operation of the order of the conditions at the refinery, to update the calculations in odology where appropriate and according to latest guid published, and to update representations from previous submittals.

The estimated maximum quantities of any regulated air taminant will be as follows in pound per hour (pph) and per year (tpy) and may change slightly during the course the Department's review:

Pollutant	pph	tp
Nitrogen Oxides (NOx)	456.40	798
Carbon Monoxide (CO)	2,067.40	1.44
Volatile Organic Compounds (VOC)		1,32
Sulfur Dioxide (SO2)	2,050.00	438
Particulate Matter (PM)	58.00	219
Particulate Matter 10 microns		T-VALUE OF
or less (PM10) & committees	85.50	214
Particulate Matter 2.5microns	ani	201 27
or less (PM2.5)	84.20	208
Hydrogen Sulfide (H2S)	20.40	5.90
Lead (Pb)	0.00	0.00
Total sum of all Hazardous Air		
Pollutants (HAPs)	74.50	228
Ammonia (NH3)	18.60	81.1
Sulfuric Acid (H2SO4)	7.10	18.
Green House Gas Emissions		10.
as Total CO2e	0.00	10,783,5

The standard operating schedule of the facility is and will continue to be continuous 24 hours per day, 7 days a weet and a maximum of 52 weeks per year.

The owner and/or operator of the Facility is: HollyFronti Navajo Refining LLC, P.O. Box 159, Artesia, NM 88211-

If you have any comments about the construction or ope tion of this facility, and you want your comments to be a part of the permit review process, you must submit yo comments in writing to this address. Permit Programs M Bureaus 252 Campion de los Marcopartients: AR (2018) Mexicos 87505-1816; (593) 476-4300, 1 800 2247-7009. However, Transport of the Marcopartients of the Marcopartients of the Marcopartient of the Marcoparti

With your comments, please refer to the company name facility name, or send a copy of this notice along with yo comments. This information is necessary since the Department may have not yet received the permit applicati

Atención

Este es un aviso de la oficina de Calidad del Aire del Dej tamento del Medio Ambiente de Nuevo México, relativo emisiones producidas por una industria en este área. Si 1 desea información en español, por favor comuniquese o esta oficina en el telefono 505 476 55557.

sets officine en el tefenos 505-476-5357.

Notice of Non-Discrimination

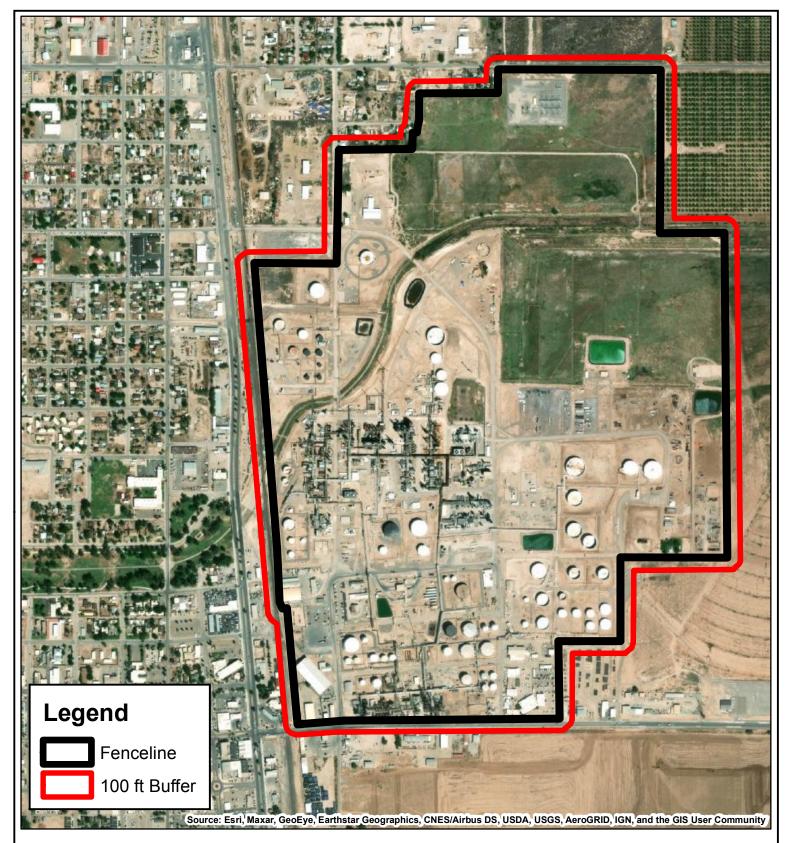
NMED does not discriminate on the basis of race, color, national origin, disability, age or see in the administratic of its programs or activities, as required by applicable la and regulations. NMED is responsible for coordination of compliance efforts and recept of inquiries concerning non-discrimination requirements implemented by 40 C. amended, Seng Tule V of the Colvil Rights Act of 1984, amended, Seng Tule V of the Colvil Rights Act of 1984, amended, Seng Tule V of the Colvil Rights Act of 1984, amended to 1984, and the Colvil Rights Act of 1984, amended, Seng Tule V of the Colvil Rights Associated and the Colvil Rights Act of 1984, amended to 1982, and Section 13 to 1987, and Seng Rights and the Colvil Rights Act of 1984, and the Colvil Rights Act of 1984, and the Colvil Rights Act of 1984, and the Colvil Rights and the Colvil Rights

NEWSPAPER ENGLISH

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of the Artesia Daily Press, a daily newspaper of General circulation, published in English at Artesia, said county			
and state, and that the hereto attached Legal Ad	La refineria, conocida como "Ar en 501 E. Main St., Artesia, NM las al este de la intersección entr condado de Eddy.	88210, a menos e E. Main S. y S	s de 0.5 mil- . 1st St., en e
was published in a regular and entire issue of the said Artesia Daily breas, a daily newspaper daily qualified for that purpose within the meaning of Chapter 167 of the 1937 Sessiol Last of the state of New Mexico for Consecutive weeks/sky on the same day as follows: Free Publication August 26, 2021	Navier solicita esta evalulón eje PSD-NM-1015MSPSI, de acuer istrativo de Naveo México 20.2: necesaria para representa escele de operación de la refineria, par odología de calculo de emisione con la companya de la hechas con anteriordida. Interior de la companya de la company	iadamente las ci a la actualizació s de acuerdo con lización de repri	ondiciones n de la met n las última esentacione
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Fourth Publication	Óxidos de Nitrógeno (NOx) Monoxido de Carbono (CO)	pph 456.40 2,067.40	798.60 1,448.9
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atisha Romine	Pata enviar concentarios sobre la esolicitada, y a úsera que sus composesos de evaluación de este pere recursos de la composición de la conferencia de la refinería, o induoy nan copia necesario puesta que el Departamento de la refinería de la refinería de la conferencia de la solicitad recolhada, y si impacto del designos de la solicitada (Conferencia).	onstrucción u o ntarios se incluy miso, por favor e ente dirección: incoment Depar se Marquez, Suite) 476-4300; 1 8% initiaço draft, p pueden resolver ios el nombre y de este aviso. E ento (NMED) per nás una direcció sodrá enviar la radicidad que na la adicidad que na viso en la calidad que na viso en la selection de la securio de la s	prontier Na- 111-0159. peración pan en el mvie sus Permit Pro- tment; Air el santa 00 224-7090 odrán recividad por inpostal respuesta a preliminar del aire, el sección legal
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NEWSPAPER SPANISH

Affidavit of Publication	Copy of Publication:
No.	NOTHICACION HollyFrontier Navalo kerhaing LLC ('Navajo') anuncia la solicitud presentada a la Olicina de Calilada del Aire (en sus sigias en inglés, ACB) del Departamento de Medio Ambierte de Nuero Meiros (en sus siglés an inglés, MAED), para la revisión del periore (na su siglés an inglés, MAED), para la revisión del periore (ha Navalos del Arrela, insimero (ha) NAVA (1935Ad5982, La í chia proyectada, para la procentación de esta solicitud es el 2 de septembre de 2021.
State of New Mexico Publisher	solicitud presentada a la Oficina de Calidad del Aire (en sus
County of Eddy:	de Nuevo México (en sus siglas en inglés, NMED), para la
Danny Scott / James 46	Artesia, número PSD-NM-0195M39R3. La fecha proyectada
being duly sworn sayes that he is the Publisher	para la presentación de esta soncitud es el 2 de septembre de 2021.
of the Artesia Daily Press, a daily newspaper of General	La refineria, conocida como "Artesia Refinery", está ubicada
circulation, published in English at Artesia, said county	La refinería, conocida como "Artesia Refinery", está ubicada en 501 E. Main St., Artesia, NM 88210, a menos de 0.5 mil- las al este de la intersección entre E. Main S. y S. 1st St., en el
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Display Ad	Navajo solicita esta revisión significativa del permiso número
as published in a regular and entire issue of the said	PSD-NM-0195M39R3, de acuerdo con el Codigo Admin- istrativo de Nuevo México 20.2.72.219.D. Esta revisión es
tesia Daily Press, a daily newspaper duly qualified	necesaria para representar adecuadamente las condiciones de operación de la refinería, para la actualización de la met-
r that purpose within the meaning of Chapter 167 of	odología de cálculo de emisiones de acuerdo con las últimas
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OFFICIAL SEAL Listable Routine NOTARY PURL-STATE OF NEW MEXICO INV commission graphs (1) 2 2 2	Cases de Efecto Invernadero como CO2. La operación de la refineria es y continuará siendo de 24 horas al día, 7 días a la semana, y por un máximo de 52 sema nas al año.
Attation Parmine atisha Romine otary Public, Eddy County, New Mexico	Pana emirar comentarios sobre la construcción u operación inolicitada, y al elecar que sua comitantios se incluyan en el proceso de evaluación de este permitos, por favor envie sua comentarios, por estros, a las aguiente dirección. Permit Por Comentarios por estros, a las aguiente dirección. Permit Por Country Branco, por estra de la Country Branco, 255 Camino de los Marquez. Sulle 1; Nante Porto, estre 155 Camino de los Marquez. Sulle 1; Nante Porto, estre 155 Camino de los Marquez. Sulle 1; Nante Porto, por la comitación de la constitución de la constituci
	Por lawor, incluyed as its associations of months' yidiocaton increasing puesto que el Departamento (NMED) podris recibir sus comentarios antes de recibir la solicitud enviada por la industria. Per fover inchay adensis una dirección postal donde el Departamento (NMED) podris envia is respuesta de la solicitud recibida y su impacto en la calidad del arc, el Departamento (NMED) publicará un aviso en la sección del del directo del directo del del directo del del directo del directo del del directo del direct
	Atención Este es un aviso de la oficina de Calidad del Aire del Depar- tamento del Medio Ambiente de Nuevo México, relativo a la emisiones producidas por una industria en este área. Si uste desea información en español, por favor comuniquese con esta oficina en el telefono 505-476-5557.
	Aviso Antidiscriminación BI Deparamento (NMED) no discrimina por razón de raza, color, nacionalidad de origen, impedimento fisico o men- ral, edad, o género, en la administración de sus programas o actividades, tal y como lo establece la legislación sigente. El Departamento (NMED) es responsible de la coordinación de las treas de cumplimiento (egal, así como de la recepción de catestiones sesculades con requerimientos de no discrimi- de catestiones sesculades con requerimientos de no discrimi- de catestiones sescolades con El 180 y 180 et la Receición de 181 Ley de Derechos Civiles de 1984, la Sección No. 504 de la Ley de Rebabilitación de 1987, la Receición No. 504 de la Ley de Rebabilitación 15 de las modificaciones de Educación de 1972 y 18 et titulo 15 de las modificaciones de Educación de 1972 y 18 et titulo 15 de 180 modificaciónes de Lorgoción de 1972 y 18 et titulo 15 de 180 modificación de 1972 de la Ley Federal de Control de Polución de Avis
	St time alguma progunta relativa a case anuncio, o los pro- gramas, politicas y procedimientos antidiscriminación del Departamento (NMED), o si usted cree que ha sido discrim- inado en relación a los programas a catividades del Depar- tamento (NMED), por fisoro contacte con: Kulturya Reckri- D. p. Suite NADO, D. O. 80, 546, 546, 546, 546, 546, 546, 546, 546





Prepared by: RTP Environmental Associates, Inc., Westbury, NY



Artesia Refinery: AREA MAP

Artesia Refinery 501 E. Main St Artesia, NM 88210

					Feet
0	500	1,000	2,000	3,000	4,000

Section 10

Written Description of the Routine Operations of the Facility

<u>A written description of the routine operations of the facility</u>. Include a description of how each piece of equipment will be operated, how controls will be used, and the fate of both the products and waste generated. For modifications and/or revisions, explain how the changes will affect the existing process. In a separate paragraph describe the major process bottlenecks that limit production. The purpose of this description is to provide sufficient information about plant operations for the permit writer to determine appropriate emission sources.

The Artesia Refinery operates one crude oil distillation unit and various downstream process units to produce various petroleum products. The Artesia Refinery processes crude oil, as well as intermediates, received from outside sources such as Navajo's Lovington Refinery and other third-party sources. The crude oil, and other intermediates, enter the Artesia Refinery via pipeline, truck, or rail. The Artesia Refinery produces liquefied petroleum gases ("LPG"), kerosene, diesel fuel, various grades of gasoline, carbon black oil, gas oils, fuel oils, asphalt, pitch, and molten sulfur. For its own use, the Artesia Refinery produces refinery fuel gas, hydrogen, nitrogen, and steam.

This permit application proposes reconciliation of several emission limits to reflect updated calculation methods and requests authorization of certain physical changes and changes in method of operation. These changes—to accommodate use of different refinery fuel gas streams in three process furnaces, to increase the maximum vapor pressure of some petroleum liquids stored in storage vessels and loaded at loading racks, to reflect addition of supplemental gas piping and increased gas flow to the flares; and to accommodate an increase in the VOC concentration in the wastewater entering the dissolved air flotation units—will not affect the routine operations of the Artesia Refinery as described above.

Section 11 Source Determination

Source submitting under 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC

Sources applying for a construction permit, PSD permit, or operating permit shall evaluate surrounding and/or associated sources (including those sources directly connected to this source for business reasons) and complete this section. Responses to the following questions shall be consistent with the Air Quality Bureau's permitting guidance, <u>Single Source Determination Guidance</u>, which may be found on the Applications Page in the Permitting Section of the Air Quality Bureau website.

Typically, buildings, structures, installations, or facilities that have the same SIC code, that are under common ownership or control, and that are contiguous or adjacent constitute a single stationary source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes. Submission of your analysis of these factors in support of the responses below is optional, unless requested by NMED.

A. Identify the emission sources evaluated in this section (list and describe):

The stationary source that is the subject of this permit application comprises all pollutant-emitting activities at the Artesia Refinery owned and operated by HollyFrontier Navajo Refining LLC's Artesia Refinery.

B. Apply the 3 criteria for determining a single source:

<u>SIC Code</u>: Surrounding or associated sources belong to the same 2-digit industrial grouping (2-digit SIC code) as this facility, <u>OR</u> surrounding or associated sources that belong to different 2-digit SIC codes are support facilities for this source.

	□ Yes	■ No
Common Ownership or Cownership or control as this		anding or associated sources are under common
	Yes	□ No
Contiguous or Adjacent: with this source.	Surrounding o	r associated sources are contiguous or adjacent
	■ Yes	□ No

C. Make a determination:

- The source, as described in this application, constitutes the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes. If in "A" above you evaluated only the source that is the subject of this application, all "YES" boxes should be checked. If in "A" above you evaluated other sources as well, you must check AT LEAST ONE of the boxes "NO" to conclude that the source, as described in the application, is the entire source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes.
- □ The source, as described in this application, **does not** constitute the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes (A permit may be issued for a portion of a source). The entire source consists of the following facilities or emissions sources (list and describe):

The stationary source that is the subject of this permit application comprises all pollutant-emitting activities at the Artesia Refinery owned and operated by HollyFrontier Navajo Refining LLC's Artesia Refinery. Also evaluated in this section is a separate but adjacent stationary source owned in part by Artesia Renewable Diesel Company LLC ("ARDC") and in part by Artesia PTU LLC ("APTU").

The Renewable Diesel Unit ("RDU") owned and operated by ARDC and the Pretreatment Unit ("PTU") owned and operated by APTU will carry a Standard Industrial Classification ("SIC") major group different from the SIC major group carried by Navajo Artesia Refinery, and thus are not in the same industrial grouping, and therefore constitute a stand-alone stationary source separate from the Refinery. The Navajo Artesia Refinery falls within SIC Major Group 29 (Petroleum Refining and Related Industries), and specifically, SIC code 2911 (Petroleum Refining). Unlike the Navajo Artesia Refinery, the RDU and the PTU will not be engaged in in petroleum refining and will not produce refined petroleum products through fractionation or straight distillation of crude oil, redistillation of unfinished petroleum derivatives, cracking, or other processes. As a result, the RDU and PTU will not fall within the petroleum refining SIC code of 2911.

Rather, because of the raw materials used and the resulting non-petroleum-based renewable diesel product, the RDU is properly classified in SIC Major Group 28 (Chemicals and Allied Products), with the specific SIC code of 2869 (Industrial Organic Chemicals, Not Elsewhere Classified). Regarding the PTU, this unit will serve as an auxiliary establishment to the RDU, because, based on current plans, it will be primarily engaged in producing goods or providing services for other establishments of the same company, rather than for the general public or for other business units. The SIC Manual prescribes that auxiliary establishments are classified on the basis of the primary activity of the operating establishment(s) they serve. The PTU is therefore properly assigned a SIC code based on the primary economic activity of the establishment that it supports, namely, SIC Major Group 28 and SIC code 2869, corresponding to the production of renewable diesel.

Section 12

Section 12.A PSD Applicability Determination for All Sources

(Submitting under 20.2.72, 20.2.74 NMAC)

<u>A PSD applicability determination for all sources</u>. For sources applying for a significant permit revision, apply the applicable requirements of 20.2.74.AG and 20.2.74.200 NMAC and to determine whether this facility is a major or minor PSD source, and whether this modification is a major or a minor PSD modification. It may be helpful to refer to the procedures for Determining the Net Emissions Change at a Source as specified by Table A-5 (Page A.45) of the <u>EPA New Source Review Workshop Manual</u> to determine if the revision is subject to PSD review.

A.	This fac	cility is:
		a minor PSD source before and after this modification (if so, delete C and D below).
		a major PSD source before this modification. This modification will make this a PSD minor
		source.
	_	the papers of the second of the programmer of th

- □ an existing PSD Major Source that has never had a major modification requiring a BACT analysis.
- an existing PSD Major Source that has had a major modification requiring a BACT analysis
- \square a new PSD Major Source after this modification.
- B. This facility is one of the listed 20.2.74.501 Table I PSD Source Categories. The "project" emissions for each of the four projects for which authorization is requested in this permit application are evaluated below. Each project is reviewed separately because the projects are not substantially related to one another as explained in detail in Section 3.

Loading Racks and Storage Tanks

The project involving fixed-roof and floating-roof storage tanks and loading racks involves only existing emission units; therefore, the emissions increase is calculated as the sum of the difference between the projected actual emissions and the baseline actual emissions, for each affected loading rack and tank according to 20.2.74.200.D(3) NMAC. The only regulated NSR pollutants emitted in appreciable quantities by these existing emissions units are VOC and H_2S . The baseline period selected for the VOC and H_2S emissions analysis is calendar years 2018-2019. The emissions increase from the project is summarized in the table below.

			VOC			H_2S			
Emissions Unit Description	BAE (tpy)	PAE (tpy)	Excludable Increase (tpy)	Project Related Increase (tpy)	BAE (tpy)	PAE (tpy)	Excludable Increase (tpy)	Project Related Increase (tpy)	
Loading Racks	5.34	46.80	9.61	31.85	-	0.04	-	0.04	
Fixed Roof Tanks*	208.33	182.54	1.55	-27.33	-	0.07	-	0.07	
External Floating Roof Tanks	50.46	65.94	0.21	15.27	0.39	0.58	0.002	0.19	
Internal Floating Roof Tanks	54.52	74.10	0.80	18.78	0.11	0.15	0.0002	0.04	
TOTAL	318.65	369.37	12.16	38.56	0.50	0.84	0.003	0.34	

^{*} T-0418 is included with the fixed roof tanks, but will be an internal floating roof tank following the retrofit described in this permit application.

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Accordingly, emissions increases for all regulated pollutants are less than the PSD significant levels:

Flares

The project involving the flares involves only existing emission units; therefore, the emissions increase is calculated as the sum of the difference between the projected actual emissions and the baseline actual emissions, for each affected flare according to 20.2.74.200.D(3) NMAC. The baseline period selected for all pollutants October 2016 through September 2018. For all pollutants other than CO, pursuant to 20.2.74.7.AR(4) NMAC, Navajo has elected to use potential to emit in lieu of making a projection of PAE. As summarized in the table below, the project is a major modification for VOC.

Pollutant	BAE (tpy)	PAE (tpy)	Project Related Increase (tpy)
NOx	24.66	63.83	39.17
СО	94.94	188.43	93.49
VOC	27.35	235.05	207.70
SO2	32.56	52.18	19.62
GHG	102,601	72,824	-29,777
TOTAL	324.47	364.80	16.45

Accordingly, emissions increase for all regulated pollutants are:

a. NOx: 39.17 TPY (< 40 TPY)
b. CO: 93.49 TPY (< 100 TPY)
c. VOC: 207.70 TPY (> 40 TPY)
d. SOx: 19.62 TPY (< 40 TPY)
e. PM: 0.0 TPY (< 25 TPY)
f. PM10: 0.0 TPY (< 15 TPY)

g. PM2.5: 0.0 TPY (< 10 TPY)
h. Fluorides: 0.0 TPY (< 3 TPY)
i. Lead: 0.0 TPY (< 0.6 TPY)
j. H2S: 0.0 TPY (< 10 TPY)
k. GHG: -29,777 TPY (< 75,000 TPY)

Hydrogen Reformer Furnaces (H-8801/8802 and H-9851)

The proposed changes to the hydrogen reformer furnaces (H-8801/8802 and H-9851) to accommodate combustion of amine-treated RFG will result in the following increases in emissions for regulated NSR pollutants, all of which are less than the PSD significant levels. The SO₂ increase is calculated as the difference between (i) the sum of the current allowable emissions from these furnaces in Permit No. PSD-NM-0195-M39R4 (3.00 tpy) and (ii) the sum of the requested allowable emissions from these units (15.96 tpy).

Dissolved Air Flotation Units

The requested revisions to the VOC emission limits for the dissolved air flotation units will result in the following increases in emissions for regulated NSR pollutants, all of which are less than the PSD significant levels. The VOC increase is calculated as the difference between (i) the sum of the current

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allowable emissions from T-0806 and T-0896 in Permit No. PSD-NM-0195-M39R4 (1.4 tpy) and (ii) the sum of the requested allowable emissions from these units (7.18 tpy).

a. NOx: 0.0 TPY (< 40 TPY)

b. CO: 0.0 TPY (< 100 TPY)

c. VOC: 5.78 TPY (< 40 TPY)

d. SOx: 0.0 TPY (< 40 TPY)

e. PM: 0.0 TPY (< 25 TPY)

f. PM10: 0.0 TPY (< 15 TPY)

g. PM2.5: 0.0 TPY (< 10 TPY)
h. Fluorides: 0.0 TPY (< 3 TPY)
i. Lead: 0.0 TPY (< 0.6 TPY)
j. H2S: 0.0 TPY (< 10 TPY)
k. GHG: 0.0 TPY (not regulated)

Netting is not required for any of the projects for which authorization is sought in this permit application. The project at the flares will cause a significant increase in emissions of VOC. Navajo is electing not to perform a netting analysis for VOC but rather to undergo PSD review as a major modification with a significant net emissions increase for VOC. The project at the flares will not cause a significant increase in emissions of any other regulated NSR pollutant. Other changes for which authorization is sought herein (i.e., the loading racks and storage tanks, the hydrogen reformer furnaces, and the dissolved air flotation unit) will not cause a significant increase in emissions of any regulated NSR pollutant.

- C. BACT is required for emissions of VOC from the refinery's five flares. Each flare is an emissions unit at which a net increase in emissions of VOC will occur as a result of the physical or operational change in the emissions unit performed as part of the major modification described above. BACT for VOC emissions from the flares is evaluated in Section 12.B below. BACT is not required for other projects and other emissions units because the changes to these units are stand-alone projects that are not by themselves major modifications and are separate and independent from the major modification involving the flares.
- D. If this is an existing PSD major source, or any facility with emissions greater than 250 TPY (or 100 TPY for 20.2.74.501 Table 1 PSD Source Categories), determine whether any permit modifications are related, or could be considered a single project with this action, and provide an explanation for your determination whether a PSD modification is triggered. With this permit application, as described in detail in Section 3, Navajo is requesting authorization for four projects. Each of these projects involves changes to a distinct set of emissions units: 1) loading racks and fixed-roof and floating-roof storage tanks; 2) flares; 3) hydrogen reformer furnaces; and 4) dissolved air floation units. Each of these actions represents stand-alone projects, separate and independent from and wholly unrelated to one another. As described in B-D above, the flares project is a major modification subject to PSD review for VOC emissions. Other changes to permit terms requested in this permit application are not a major modification subject to PSD review because they are reconciliations involving no physical changes in or changes in method of operation of the stationary source.

If this is **NOT** a PSD application, delete this sentence and the entire Section 12.B below.

Section 12.B Special Requirements for a PSD Application

(Submitting under 20.2.74 NMAC)

Prior to Submitting a PSD application, the permittee shall:

- Submit the BACT analysis for review prior to submittal of the application. No application will be ruled complete until the final determination regarding BACT is made, as this determination can ultimately affect information to be provided in the application. A pre-application meeting is recommended to discuss the requirements of the BACT analysis.
- Submit a modeling protocol prior to submitting the permit application. [Except for GHG]
- ☐ Submit the monitoring exemption analysis protocol prior to submitting the application. [Except for GHG]

For PSD applications, the permittee shall also include the following:

- Documentation containing an analysis on the impact on visibility. [Except for GHG]
- Documentation containing an analysis on the impact on soil. [Except for GHG]
- Documentation containing an analysis on the impact on vegetation, including state and federal threatened and endangered species. [Except for GHG]
- Documentation containing an analysis on the impact on water consumption and quality. [Except for GHG]
- Documentation that the federal land manager of a Class I area within 100 km of the site has been notified and provided a copy of the application, including the BACT and modeling results. The name of any Class I Federal area located within one hundred (100) kilometers of the facility.

Only PSD analyses for the major modification proposed in this permit application—requested revisions of permit

terms for the flares, which is a major modification with respect to emissions of VOC—are addressed in this Section 12.B. Section 20 of this permit application includes analyses of other requested permit revisions, including reconciliations.

BACT for VOC emissions from the five affected flares at the Navajo Artesia Refinery flares requires no additional controls beyond the work practices already required as demonstrated by the following analysis.

Step 1: Identify All Control Options

Identified control technologies and techniques for VOC emissions from refinery flares include use of flare gas recovery systems, which reduce the quantity of VOC-containing gas routed to the flares by capturing and compressing these gases into the refinery's fuel gas system for use in boilers and process heaters, and equipment design standards and work practices to ensure a high VOC destruction efficiency is achieved at the flare tip. These equipment design standards and work practices are maintaining a pilot flame at all times; maintaining adequate flare capacity to ensure the flare tip exit velocity does not exceed the level at which flame lift-off would occur; and maintaining the net heating value of the flare combustion zone gas (NHV_{CZ}) above the level required for flammability.

Step 2 – Eliminate Technically Infeasible Control Options

All of the identified control options are technically feasible for all five flares at the Artesia Refinery.

Step 3 – Characterize Control Effectiveness of Technically Feasible Control Options

All identified equipment design standards and work practices are already in place and enforceable for the five flares at the Artesia Refinery pursuant to 40 CFR § 63.670. These equipment design standards and work practices are

sufficient to achieve 98 percent VOC destruction efficiency on a continuous basis.⁵ Potential VOC emissions with these equipment design standards and work practices are 225 tpy (total for five flares, including routine and MSS emissions).

The only other identified control strategy for the five flares at the Artesia Refinery is to install and operate flare gas recovery systems (FGRS) in addition to the required equipment design standards and work practices. It is conservatively assumed for purposes of this BACT evaluation for the flares at the Artesia Refinery that this control strategy would achieve a further reduction in VOC emissions of 100 percent of the routine (non-MSS) emissions, assuming a two-compressor configuration. Actual VOC reduction efficiency would be somewhat less because achievable compressor reliability (i.e., uptime) is less than 100 percent and because flaring is avoided only when fuel demands at the refinery's fuel gas-fired boilers and process heaters exceed the supply of available fuel gas, including recovered gas from the flare headers.

Step 4 – Evaluate More Effective Control Options

The most cost-effective possible FGRS at the Artesia Refinery is a two-compressor system with a design capacity of approximately 100,000 standard cubic feet per hour, sized to accommodate the combined flow to the FL-0400 North Plant Flare and the FL-0404 GOHT Flare. This design provides for re-routing the flow of excess hydrogen product from the refinery's hydrogen production (pressure swing adsorption) units to bypass the FGRS. As shown in the table below, this control strategy is not economically reasonable and should not be required as BACT. FGRS in any other configuration, or for any of the other flares at the Artesia Refinery, would be less cost effective.

Parameter	Value	Notes
Installed cost	\$ 45,000,000	Site-specific engineering study
Capital recovery factor	9.44%	20 years, 7% interest
Annualized capital recovery cost	\$ 4,250,000	
Annual O&M cost	\$ -	Conservatively assumed to be zero
VOC emissions reduction (tpy)	100	Conservatively assumed to be 100% of routine (non-MSS) flow
Cost effectiveness of VOC emissions reduction (\$/ton)	\$ 42,500	

Table 12.B-1 Cost Effectiveness of FGRS for FL-400 and FL-404

Step 5 – Establish BACT

Navajo proposes that the emission limits representing BACT for VOC emissions from the affected flares are the emission rates in Table 2-E of this permit application.

An analysis of the impacts on air quality due to the requested increases in allowable VOC emissions from flares is presented in the air dispersion modeling report in Section 16 of this permit application.

The requested increases in allowable VOC emissions from flares will have no adverse impact on visibility. See, for example, *Workbook for Plume Visual Impact Screening and Analysis (Revised)*, EPA-454/R-92-023, U.S. EPA, Oct. 1992, identifying that only particulate matter, NO_X, and sulfates are expected to impair near-field visibility. These increases also will have no adverse impacts on soil or vegetation. See, for example, *A Screening Procedure for the Impacts of Air Pollution Sources on Plants, Soils, and Animals*, EPA-450/2-81-078, U.S. EPA, Dec. 1980, indicating that ethylene is the only hydrocarbon causing adverse effects on vegetation at ambient concentrations of 1 part per million by volume ("ppmv") or less. See, also, U.S. EPA's final rule revoking the National Ambient Air

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⁵ See, generally, *Petroleum Refinery Sector Risk and Technology Review and New Source Performance Standards*, 80 Fed. Reg. 75178 (Dec. 1, 2015); see, also, *National Emission Standards for Hazardous Air Pollutants for Petroleum Refineries—Background Information for Final Rule—Summary of Public Comments and Responses*, U.S. EPA, Office of Air Quality Planning and Standards, Research Triangle Park, NC (Sept. 2015)(available at www.epa.gov/sites/production/files/2018-07/documents/epa-hq-oar-2010-0682-0802.pdf).

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Quality Standard ("NAAQS") for hydrocarbons, 48 *Fed. Reg.* 628, indicating "hydrocarbons, as a class, do not appear to cause adverse health or welfare effects at the present ambient air levels." The requested increases in allowable VOC emissions from the flares also will have no impact on water consumption or quality.

Section 13

Determination of State & Federal Air Quality Regulations

This section lists each state and federal air quality regulation that may apply to your facility and/or equipment that are stationary sources of regulated air pollutants.

Not all state and federal air quality regulations are included in this list. Go to the Code of Federal Regulations (CFR) or to the Air Quality Bureau's regulation page to see the full set of air quality regulations.

Required Information for Specific Equipment:

For regulations that apply to specific source types, in the 'Justification' column **provide any information needed to determine if the regulation does or does not apply**. **For example**, to determine if emissions standards at 40 CFR 60, Subpart IIII apply to your three identical stationary engines, we need to know the construction date as defined in that regulation; the manufacturer date; the date of reconstruction or modification, if any; if they are or are not fire pump engines; if they are or are not emergency engines as defined in that regulation; their site ratings; and the cylinder displacement.

Required Information for Regulations that Apply to the Entire Facility:

See instructions in the 'Justification' column for the information that is needed to determine if an 'Entire Facility' type of regulation applies (e.g. 20.2.70 or 20.2.73 NMAC).

Regulatory Citations for Regulations That Do Not, but Could Apply:

If there is a state or federal air quality regulation that does not apply, but you have a piece of equipment in a source category for which a regulation has been promulgated, you must **provide the low level regulatory citation showing why your piece of equipment is not subject to or exempt from the regulation.** For example if you have a stationary internal combustion engine that is not subject to 40 CFR 63, Subpart ZZZZ because it is an existing 2 stroke lean burn stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, your citation would be 40 CFR 63.6590(b)(3)(i). We don't want a discussion of every non-applicable regulation, but if it is possible a regulation could apply, explain why it does not. For example, if your facility is a power plant, you do not need to include a citation to show that 40 CFR 60, Subpart OOO does not apply to your non-existent rock crusher.

Regulatory Citations for Emission Standards:

For each unit that is subject to an emission standard in a source specific regulation, such as 40 CFR 60, Subpart OOO or 40 CFR 63, Subpart HH, include the low level regulatory citation of that emission standard. Emission standards can be numerical emission limits, work practice standards, or other requirements such as maintenance. Here are examples: a glycol dehydrator is subject to the general standards at 63.764C(1)(i) through (iii); an engine is subject to 63.6601, Tables 2a and 2b; a crusher is subject to 60.672(b), Table 3 and all transfer points are subject to 60.672(e)(1)

Federally Enforceable Conditions:

All federal regulations are federally enforceable. All Air Quality Bureau State regulations are federally enforceable except for the following: affirmative defense portions at 20.2.7.6.B, 20.2.7.110(B)(15), 20.2.7.11 through 20.2.7.113, 20.2.7.115, and 20.2.7.116; 20.2.37; 20.2.42; 20.2.43; 20.2.62; 20.2.63; 20.2.86; 20.2.89; and 20.2.90 NMAC. Federally enforceable means that EPA can enforce the regulation as well as the Air Quality Bureau and federally enforceable regulations can count toward determining a facility's potential to emit (PTE) for the Title V, PSD, and nonattainment permit regulations.

INCLUDE ANY OTHER INFORMATION NEEDED TO COMPLETE AN APPLICABILITY DETERMINATION OR THAT IS RELEVENT TO YOUR FACILITY'S NOTICE OF INTENT OR PERMIT.

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EPA Applicability Determination Index for 40 CFR 60, 61, 63, etc: http://cfpub.epa.gov/adi/

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Table 13-1 - State Regulations

STATE REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
20.2.1 NMAC	General Provisions	Yes	Facility	General Provisions apply Construction permit applications.
20.2.3 NMAC	Ambient Air Quality Standards NMAAQS	Yes	Facility	The Artesia Refinery is subject to 20.2.3 NMAC State Implementation Plan ("SIP") approved regulation that limits the maximum allowable concentration of, Sulfur Compounds, Carbon Monoxide and Nitrogen Dioxide.
20.2.7 NMAC	Excess Emissions	Yes	Facility	The Artesia Refinery is subject to permit emissions limits, and federal or state regulation's numerical emissions standards. Thus, it is subject to 20.2.7 NMAC requirements.
20.2.23 NMAC	Fugitive Dust Control	No	Facility	The Artesia Refinery is not a fugitive dust source listed at 20.2.23.108.A NMAC, and is not located in an area subject to a mitigation plan pursuant to 40 CFR 51.930. As of January 2019, the only areas of the State subject to a mitigation plan per 40 CFR 51.930 are in Doña Ana and Luna Counties.
20.2.33 NMAC	Gas Burning Equipment - Nitrogen Dioxide	Yes	See Table 13-3	The Artesia Refinery has new (equipment which commenced construction or modification after February 17, 1972) and existing gas burning equipment (i.e., gas fired boilers and heaters) with a heat input of greater than 1,000,000 million British Thermal Units per year per unit. Table 13-3 at the end of this section, summarizes the applicable regulations to the Artesia Refinery boilers and heaters.
20.2.34 NMAC	Oil Burning Equipment: NO ₂	No	N/A	The Artesia Refinery does not have oil burning equipment (i.e., external combustion emission sources, such as oil-fired boilers and heaters) having a heat input of greater than 1,000,000 million British Thermal Units per year per unit.
20.2.35 NMAC	Natural Gas Processing Plant – Sulfur	No	N/A	The Artesia Refinery is not a natural gas processing plant as the term is defined in 20.2.35.7.A and B.
20.2.37 and 20.2.36 NMAC	Petroleum Processing Facilities and Petroleum Refineries	N/A	N/A	The Artesia Refinery had equipment subject to 20.2.36 and 20.2.37 NMAC before the repeal of these rules. Therefore, the affected combustion emission sources are now subject to 20.2.61 NMAC.
20.2.38 NMAC	Hydrocarbon Storage Facility	Yes	See Table 13-12	Section 111 of this rule does not apply because the Artesia Refinery is not located within five miles of the corporate limits of a municipality that has a population of 20,000 or greater. Section 112 of this rule does not apply because the Artesia Refinery is not a petroleum production facility. Table 13-12, included at the end of this section, summarizes the Artesia Refinery petroleum storage tanks subject to certain other 20.2.38 NMAC requirements.
20.2.39 NMAC	Sulfur Recovery Plant - Sulfur	No	N/A	The Artesia Refinery SRUs are part of a petroleum processing facility, therefore, per 20.2.39.6 NMAC this regulation is not applicable.
20.2.61.109 NMAC	Smoke & Visible Emissions	Yes	See Tables 13-3, 13-4, 13-6, and 13-7	The Artesia Refinery boilers, heaters, SRU tail gas incinerators, flares, and engines are subject to the 20% opacity limit for Stationary Combustion Equipment in 20.2.61.109 NMAC as summarized in Tables 13-3 through 13-6 included at the end of this section.

STATE REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
20.2.70 NMAC	Operating Permits	Yes	Facility	The Artesia Refinery is a major source with a potential to emit ("PTE") of 100 tpy or more for NO _X , CO, VOC, SO ₂ and PM/PM ₁₀ /PM _{2.5} , and a HAPs PTE of 10 tpy or more for a single HAP or 25 or more tpy for combined HAPs. The Artesia Refinery operates under Operating Permit P051-R3.
20.2.71 NMAC	Operating Permit Fees	Yes	Facility	The Artesia Refinery is subject to 20.2.70 NMAC. The Artesia Refinery Operating Permit P051-R3 includes numerical ton per year emission limits. Therefore, it is subject to 20.2.71 NMAC
20.2.72 NMAC	Construction Permits	Yes	Facility	The Artesia Refinery is subject to 20.2.72 NMAC and NSR Permit number: PSD-NM-0195-M39R4.
20.2.73 NMAC	NOI & Emissions Inventory Requirements	Yes	Facility	Notice of Intent ("NOI"): N/A. All facilities that are a Title V Major Source as defined at 20.2.70.7.R NMAC, are subject to Emissions Inventory Reporting.
20.2.74 NMAC	Permits – Prevention of Significant Deterioration (PSD)	Yes	Units	Per 20.2.74.7.AG(1) NMAC, the Artesia Refinery is a major stationary source as it is a stationary source listed in Table 1 (20.2.74.501 NMAC) which emits, or has the potential to emit, emissions equal to or greater than one hundred (100) tons per year of any regulated NSR air pollutant. Certain units at the Artesia Refinery are subject to PSD requirements in NSR Permit No. PSD-NM-0195-M39R4.
20.2.75 NMAC	Construction Permit Fees	Yes	Facility	The Artesia Refinery is not subject to the 20.2.75.11.E annual fees because it is subject to 20.2.71 NMAC.
20.2.77 NMAC	New Source Performance	Yes	See Tables 13-3 thru 13-12	Tables 13-3 through 13-12, included at the end of this section. summarize 40 CFR Part 60 applicability for the Artesia Refinery NSPS affected facilities.
20.2.78 NMAC	Emission Standards for HAPS	Yes	Facility	The Artesia Refinery is subject to 40 CFR 61, Subpart FF but is exempt from control requirements (40 CFR §§ 61.340(a) and 61.342(a))
20.2.79 NMAC	Permits – Nonattainment Areas	No	Facility	The Artesia Refinery is located in Eddy County, an area that is designated as unclassifiable or attainment with respect to all National Ambient Air Quality Standards.
20.2.80 NMAC	Stack Heights	No	Facility	Rule restricts NMED, not stationary sources.
20.2.82 NMAC	MACT Standards for source categories of HAPS	Yes	See Tables 13-3 thru 13-12	Tables 13-3 through 13-12, included at the end of this section. summarize 40 CFR Part 63 applicability for the Artesia Refinery affected HAPs emission sources.

Table 13-2 - Federal Regulations

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
40 CFR 50	NAAQS	Yes	Facility	The Artesia Refinery is subject to 20.2.70, 20.2.72, and 20.2.74 NMAC. Per 20.2.70.7.E.11
40 CFR 60 Subpart A	General Provisions	Yes	See Tables 13-3 thru 13-12	Tables 13-3 through 13-12, included at the end of this section. summarize 40 CFR Part 60 applicability for the Artesia Refinery NSPS affected facilities.
40 CFR 60 Subpart D	Standards of Performance for Fossil-Fuel-Fired Steam Generators	No	N/A	The Artesia Refinery boilers design capacities are less than Subpart D applicability threshold of 250 MMBtu/hr, and the process heaters are not fossil-fuel-fired steam generating units, as the term is defined in 40 CFR § 60.41.
40 CFR 60 Subpart Da	Standards of Performance for Electric Utility Steam Generating Units	No	N/A	The Artesia Refinery does not own or operate an electric utility steam generating unit, as the term is defined in 40 CFR \$60.41Da.
40 CFR 60 Subpart Db	Standards of Performance for Industrial-Commercial- Institutional Steam Generating Units	Yes	See Table 13-3	The Artesia Refinery boilers B-0007, B-0008, and B-0009 and hot oil heater H-2501 commenced construction after June 19, 1984, have design heat input capacities great than 100 MMBtu/hr (HHV), fire solely fuel gas, and are "steam generating units" as this term is defined in 40 CFR §60.41b. Subpart Db standards for PM and SO ₂ are not applicable to refinery fuel gas firing units.
40 CFR 60 Subpart Dc	Standards of Performance for Small Industrial- Commercial-Institutional Steam Generating Units	Yes	See Table 13-3	The SRU Hot Oil Heaters H-0464 and H-3101 each commenced construction after June 9, 1989, has design heat input capacity greater than 10 MMBtu/hr (HHV) and less than 100 MMBtu/hr (HHV), fires solely fuel gas, and is a "steam generating unit" as this term is defined in 40 CFR §60.41c. Subpart Dc standards for SO ₂ and PM are not applicable to refinery fuel gas firing units.
40 CFR 60 Subpart J	Standards of Performance for Petroleum Refineries	Yes	See Tables 13-3 and 13-5	Tables 13-3 and 13-5, included at the end of this section. summarize 40 CFR Part 60, Subpart J applicability for potentially affected Artesia Refinery boilers, heaters, FCCU, and SRU2.
40 CFR 60 Subpart Ja	Standards of Performance for Petroleum Refineries for which Construction, Reconstruction, or Modification Commenced After May 14, 2007	Yes	See Tables 13-3, 13-4, 13-6	Tables 13-3, 13-4, and 13-6, included at the end of this section. summarize 40 CFR Part 60, Subpart Ja applicability for potentially affected Artesia Refinery boilers, heaters, SRU3, and flares.

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
40 CFR 60 Subpart K	Standards of Performance for Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	Yes	See Table 13-12	Table 13-12, included at the end of this section, summarizes 40 CFR Part 60, Subpart K applicability for potentially affected Artesia Refinery storage tanks.
40 CFR 60 Subpart Ka	Standards of Performance for Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	Yes	See Table 13-12	Table 13-12 included at the end of this section, summarizes 40 CFR Part 60, Subpart Ka applicability for potentially affected Artesia Refinery storage tanks.
40 CFR 60 Subpart Kb	Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	Yes	See Table 13-12	Table 13-12, included at the end of this section, summarizes 40 CFR Part 60, Subpart Kb applicability for potentially affected Artesia Refinery storage tanks.
40 CFR 60 Subpart GG	Standards of Performance for Stationary Gas Turbines	No	N/A	The Artesia Refinery does not include stationary gas turbines.
40 CFR 60 Subpart XX	Standards of Performance for Bulk Gasoline Terminals	No	See Table 13-10	Table 13-10, included at the end of this section, summarizes 40 CFR Part 60, Subpart XX applicability for potentially affected Artesia Refinery loading racks.
40 CFR 60 Subpart GGG	Standards of Performance for Equipment Leaks of VOC in Petroleum Refineries for which Construction, Reconstruction, or Modification Commenced after January 4, 1983, and on or before November 7, 2006	No	N/A	The Artesia Refinery affected facilities were constructed, reconstructed, or modified after November 7, 2006, and are therefore subject to 40 CFR 60, Subpart GGGa, rather than Subpart GGG.

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
40 CFR 60 Subpart GGGa	Standards of Performance for Equipment Leaks of VOC in Petroleum Refineries for Which Construction, Reconstruction, or Modification Commenced after November 7, 2006	Yes	See Table 13-11	Table 13-11, included at the end of this section, summarizes 40 CFR Part 60, Subpart GGGa applicability for the affected facilities in the Artesia Refinery.
40 CFR 60 Subpart KKK	Standards of Performance for Equipment Leaks of VOC From Onshore Natural Gas Processing Plants for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011	No	N/A	The Artesia Refinery is not a natural gas processing plant as this term is defined in 40 CFR § 60.631.
40 CFR 60 Subpart LLL	Standards of Performance for SO ₂ Emissions from Onshore Natural Gas Processing for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011	No	N/A	The Artesia Refinery does not include any sweetening units as this term is defined in 40 CFR § 60.641.
40 CFR 60 Subpart NNN	Standards of Performance for Volatile Organic Compound (VOC) Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Distillation Operations	Yes	W-623,	The depropanizer column in the Alkylation Unit is subject to this rule because it produces, among other things, propane as a product. (See, 40 CFR §§ 60.660(b) and 60.667.)
40 CFR 60 Subpart QQQ	Standards of Performance for VOC Emissions from Petroleum Refinery Wastewater Systems	Yes	See Tables 13-9 and 13-11	Tables 13-9 and 13-11, included at the end of this section, summarize 40 CFR Part 60, Subpart QQQ applicability for the affected facilities in the Artesia Refinery.
40 CFR 60 Subpart RRR	Standards of Performance for Volatile Organic Compound (VOC) Emissions from Synthetic Organic Chemical Manufacturing Industry (SOCMI) Reactor Processes	Yes	Alky Reactor	The reactor in the Alkylation Unit is subject to this rule because it produces, among other things, propane as a product. (See, 40 CFR §§ 60.700(b) and 60.707.)

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
40 CFR 60 Subpart IIII	Standards of performance for Stationary Compression Ignition Internal Combustion Engines	Yes	See Table 13-7	Table 13-7 included at the end of this section, summarizes 40 CFR Part 60, Subpart IIII applicability for the Artesia Refinery stationary compression ignition ("CI") internal combustion engines ("ICE.")
40 CFR 60 Subpart JJJJ	Standards of Performance for Stationary Spark Ignition Internal Combustion Engines	No	N/A	The Artesia Refinery does not own or operate any stationary spark ignition internal combustion engines.
40 CFR 60 Subpart OOOO	Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution for which construction, modification or reconstruction commenced after August 23, 2011 and before September 18, 2015	No	N/A	The Artesia Refinery is not in the Crude Oil and Natural Gas Production source category, as defined in §60.5430.
40 CFR 60 Subpart OOOOa	Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015	No	N/A	The Artesia Refinery is not in the Crude Oil and Natural Gas Production source category, as defined in §60.5430a.
40 CFR 60 Subpart TTTT	Standards of Performance for Greenhouse Gas Emissions for Electric Generating Units	No	N/A	The Artesia Refinery does not own or operate any steam generating unit, IGCC, or stationary combustion turbine as these terms are defined in 40 CFR § 60.5580 that commenced construction after January 8, 2014 and have a base load rating greater than 250 MMBtu/hr of fossil fuel.
40 CFR 60 Subpart UUUUa	Emission Guidelines for Greenhouse Gas Emissions from Existing Electric Utility Generating Units	No	N/A	Rule applies to NMED, not stationary sources.
40 CFR 60 Subparts WWW, XXX, Cc, and Cf	Standards of performance for Municipal Solid Waste (MSW) Landfills	No	N/A	The Artesia Refinery is not a municipal solid waste landfill.
40 CFR 61 Subpart A	General Provisions	Yes	Units Subject to 40 CFR 61	Applies if any other Subpart in 40 CFR 61 applies.
40 CFR 61 Subparts J & V	National Emission Standard for Equipment Leaks (Fugitive Emission Sources) of Benzene	No	N/A	The Artesia Refinery does not operate any piece of equipment in benzene service (i.e., fluid that is at least 10 percent benzene by weight) as this term is defined in 40 CFR § 61.111.
40 CFR 61 Subpart M	National Emission Standard for Asbestos	Yes	Facility	The Artesia Refinery complies with the requirements of 40 CFR §61.145 as applicable.

Artesia Refinery

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
40 CFR 61 Subpart FF	National Emission Standard for Benzene Waste Operations	Yes	See Tables 13-9 and 13-12	Tables 13-9 and 13-12, included at the end of this section. summarize 40 CFR Part 61, Subpart FF applicability for the Artesia Refinery storage tanks and wastewater emission sources.
MACT 40 CFR 63.1, Subpart A	General Provisions	Yes	Units Subject to 40 CFR 63	Applies if any other Subpart in 40 CFR 63 applies.
NESHAP 40 CFR 63.400, Subpart Q	National Emission Standards for Hazardous Air Pollutants for Industrial Process Cooling Towers	No	See Table 13-8	The Artesia Refinery no longer owns or operates any industrial process cooling tower operated with chromium-based water treatment chemicals.
NESHAP 40 CFR 63.640, Subpart R	National Emission Standards for Gasoline Distribution Facilities (Bulk Gasoline Terminals and Pipeline Breakout Stations)	No	See Table 13-10	Table 13-10, included at the end of this section, summarizes 40 CFR Part 63, Subpart R applicability for potentially affected Artesia Refinery loading rack.
NESHAP 40 CFR 63.640, Subpart CC	National Emission Standards for Hazardous Air Pollutants from Petroleum Refineries	Yes	See Tables 13-3 through 13-12	Tables 13-3 through 13-12, included at the end of this section. summarize 40 CFR Part 63, Subpart CC applicability for the Artesia Refinery NESHAP affected sources.
MACT 40 CFR 63.760 Subpart HH	Oil and Natural Gas Production Facilities	No	N/A	The Artesia Refinery is not an oil and natural gas production facility.
MACT 40 CFR 63.1270 Subpart HHH	National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities	No	N/A	The Artesia Refinery is not a natural gas transmission and storage facility.
MACT 40 CFR 63.1561 Subpart UUU	National Emission Standards for Hazardous Air Pollutants for Petroleum Refineries: Catalytic Cracking Units, Catalytic Reforming Units, and Sulfur Recovery Units	Yes	See Tables 13-4 and 13-5	Tables 13-4 and 13-5, included at the end of this section. summarize 40 CFR Part 63, Subpart UUU applicability for the Artesia Refinery FCC regenerator, Continuous Catalyst Regenerator ("CCR"), and SRUs.

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
MACT 40 CFR 63.6580 Subpart ZZZZ	National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines (RICE MACT)	Yes	See Table 13-7	Table 13-7, included at the end of this section, summarizes 40 CFR Part 60, Subpart ZZZZ applicability for the Artesia Refinery stationary reciprocating internal combustion engines ("RICE.")
MACT 40 CFR 63.7485 Subpart DDDDD	National Emission Standards for Hazardous Air Pollutants for Major Industrial, Commercial, and Institutional Boilers & Process Heaters	Yes	See Table 13-3	Table 13-3, included at the end of this section, summarizes 40 CFR Part 60, Subpart DDDDD applicability for the Artesia Refinery boilers and process heaters as defined in §63.7575.
40 CFR 63 Subpart UUUUU	National Emission Standards for Hazardous Air Pollutants Coal & Oil Fire Electric Utility Steam Generating Unit	No	N/A	The Artesia Refinery does not own or operate a coal-fired electric generating unit ("EGU") or an oil-fired EGU as defined in §63.10042.
40 CFR 63 Subpart BBBBBB	National Emission Standards for Hazardous Air Pollutants for Source Category: Gasoline Distribution Bulk Terminals, Bulk Plants, and Pipeline Facilities	No	N/A	The Artesia Refinery is not an area source of HAPs.
40 CFR 63 Subpart CCCCCC	National Emission Standards for Hazardous Air Pollutants for Source Category: Gasoline Dispensing Facilities	No	N/A	The Artesia Refinery is not an area source of HAPs.
40 CFR 64	Compliance Assurance Monitoring	No	N/A	The Artesia Refinery FCC Regenerator and SRUs are subject to 40 CFR 63, Subpart UUU emission standards proposed after November 15, 1990, and are therefore exempt from the requirements of 40 CFR Part 64 per §64.2(b)(1)(i). The Artesia Refinery fuels truck loading rack, TL-4, is subject to 40 CFR 63, Subpart CC emission standards proposed after November 15, 1990, and are therefore exempt from the requirements of 40 CFR Part 64 per §64.2(b)(1)(i).
40 CFR 68	Chemical Accident Prevention	Yes	Facility	The Artesia Refinery is a stationary source that processes more than the threshold quantity of a regulated substance, as determined under 40 CFR §68.115.
Title IV – Acid Rain 40 CFR 72.6	Acid Rain	No	N/A	The Artesia Refinery does not generate commercial electric power or electric power for sale.
Title IV – Acid Rain 40 CFR 73.2	Sulfur Dioxide Allowance Emissions	No	N/A	The Artesia Refinery does not generate commercial electric power or electric power for sale.

FEDERAL REGU- LATIONS CITATION	11116		Unit(s) or Facility	JUSTIFICATION:		
Title IV- Acid Rain 40 CFR 75.2	Continuous Emissions Monitoring	No	N/A	The Artesia Refinery does not generate commercial electric power or electric power for sale.		
Title IV – Acid Rain 40 CFR 76.1	Acid Rain Nitrogen Oxides Emission Reduction Program	Oxides Emission No N/A The Artesia Refinery doc		The Artesia Refinery does not generate commercial electric power or electric power for sale.		
Title VI – 40 CFR 82	Protection of Stratospheric Ozone	Yes	N/A	The Artesia Refinery maintains and services building air conditioning units that may contain affected refrigerants. Therefore, the Artesia Refinery is subject to Subpart F to Part 82, which regulates activities to maintaining, servicing, or repairing appliances containing class I, class II or non-exempt substitute refrigerants.		

Table 13-3 Boilers and Heaters Summary of Applicable Regulations

Unit ID	Description	NSPS D	NSPS Db	NSPS Dc	NSPS J a	NSPS Ja ^b	MACT DDDDD	20.2.33.108 NMAC	20.2.61 NMAC	CAM
B-0007	Boiler 7	NO	YES	NO	YES	NO	YES	YES	YES	NO
B-0008	Boiler 8	NO	YES	NO	YES	NO	YES	YES	YES	NO
B-0009	Boiler 9	NO	YES	NO	NO	YES c	YES	YES	YES	NO
H-0009	Unit 13 Naphtha Splitter Reboiler	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0011	Unit 21 Vacuum Unit Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0018	Unit 06 HDS Reboiler	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0019	South Crude Charge Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0020	South Crude Charge Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0028	Unit 21 Heater H-28	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0030	Unit 06 Charge Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0040	Unit 13 Charge Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0303	Unit 05 Charge Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0312	Unit 10 FCC Feed Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0352	Unit 70 CCR Reformer Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0353	Unit 70 CCR Reformer Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0354	Unit 70 CCR Reformer Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0355	Unit 70 Stabilizer Reboiler Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0362	Unit 70 CCR Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0363	Unit 70 CCR Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0364	Unit 70 CCR Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0421	Unit 44 Charge Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0464	SRU Hot Oil Heater	NO	NO	YES	YES	NO	YES	NO	YES	NO
H-0473	SRU2 Tail Gas Incinerator	NO	NO	NO	YES	NO	NO	NO	YES	NO
H-0600	Unit 09 Depropanizer Reboiler Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-0601	Unit 33 Charge Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-2421	Unit 45 Charge Heater	NO	NO	NO	YES	NO	YES	NO	YES	NO
H-8801/ H-8802	Unit 63 Hydrogen Plant Reformer	NO	NO	NO	YES	NO	YES	YES	YES	NO
H-3402	Unit 34 Hydrocracker Reboiler 1	NO	NO	NO	NO	YES	YES	NO	YES	NO
H-3403	Hydrocracker Reactor Charge Heater	NO	NO	NO	NO	YES	YES	NO	YES	NO
H-5401	Unit 54 HDS Reactor Heater	NO	NO	NO	NO	YES	YES	NO	YES	NO
H-9851	Unit 64 Hydrogen Plant Reformer	NO	NO	NO	NO	YES	YES	YES	YES	NO

Unit ID	Description	NSPS D	NSPS Db	NSPS Dc	NSPS J ^a	NSPS Ja ^b	MACT DDDDD	20.2.33.108 NMAC	20.2.61 NMAC	CAM
H-2501	Unit 25 ROSE® Unit No.2 Hot Oil Heater	NO	YES	NO	NO	YES c	YES	YES	YES	NO
H-3101	SRU3 Hot Oil Heater	NO	NO	YES	NO	YES d	YES	NO	YES	NO
H-3103	SRU3 Tail Gas Incinerator	NO	NO	NO	NO	YES	NO	NO	YES	NO

- a. For all fuel gas combustion devices that are affected facilities under NSPS subpart J, Navajo has elected to comply with the fuel gas H_2S concentration standard under $40 \text{ CFR} \ 860.102a(g)(1)(ii)$ and associated monitoring, recordkeeping, and reporting requirements in NSPS subpart Ja, as provided by $40 \text{ CFR} \ 860.100(e)$ and 60.100a(b).
- b. Except as noted, affected facilities under NSPS subpart Ja are process heaters subject to both the fuel gas H_2S concentration standard under 40 CFR § 60.102a(g)(1)(ii) and, if applicable based on heat input capacity, emission standards for NO_X under § 60.102a(g)(2).
- c. Steam generating unit, not subject to NO_X emission standards under NSPS subpart Ja pursuant to 40 CFR § 60.40b(c).
- d. Steam generating unit, not subject to NO_X emission standards under NSPS subpart Ja pursuant to 40 CFR § 60.40c(h).

Table 13-4 SRU Summary of Applicable Regulations

Source ID	Emission Point ID	Description	NSPS J	NSPS Ja	MACT UUU	20.2.61 NMAC	20.2.39 NMAC	CAM
SRU2	H-0473	SRU2 Tail Gas Incinerator	YES	NO	YES	YES	NO	YES Satisfied by MACT UUU
SRU3	H-3103	SRU3 Tail Gas Incinerator	NO	YES	YES	YES	NO	YES Satisfied by MACT UUU

Table 13-5 FCCU and CCR Summary of Applicable Regulations

Unit ID	NSPS J	NSPS Ja	MACT UUU	CAM
FCCREGEN	YES	NO	YES	YES Satisfied by MACT UUU
CCR	N/A	N/A	YES	NO

Table 13-6 Flares Summary of Applicable Regulations

Unit ID	Description ^a	NSPS J	NSPS Ja	MACT CC	20.2.61 NMAC
FL-400	North Plant Flare	NO	YES	YES	YES
FL-401	South Plant Flare	NO	YES	YES	YES
FL-402	FCCU Flare	NO	YES	YES	YES
FL-403	Alky Flare	NO	YES	YES	YES
FL-404	GOHT Flare	NO	YES	YES	YES
FL-HEP- PORT	Portable Flare for Holly Energy Partners (HEP) Pipeline Pigging Operations	NOb	NOb	NO ^c	NO ^d

a. FL-400 through FL-404 flares are steam assisted.

Table 13-7 Engines Summary of Applicable Regulations

Source ID	Description	NSPS IIII			20.2.61.109 NMAC	CAM
MG-0001	Portable Air Compressor	YES	NO	YES	YES	NO
MG-0002	Portable Air Compressor	YES	NO	YES	YES	NO
MG-0003	Portable Air Compressor	YES	NO	YES	YES	NO
MG-0004	Portable Fire Water Pump Engine	YES	NO	YES	YES	NO
SG-0100	UPS backup generator	NO	NO	YES	YES	NO
SG-0101	UPS backup generator	NO	NO	YES	YES	NO
SG-0102	Server Backup Generator	YES	NO	YES	YES	NO
FWG-0600	Fire Water Pump Engine	YES	NO	YES	YES	NO
FWG-0601	Fire Water Pump Engine	YES	NO	YES	YES	NO
FWG-0602	Fire Water Pump Engine	YES	NO	YES	YES	NO
FWG-0603	Fire Water Pump Engine	YES	NO	YES	YES	NO

b. Flare is not in a petroleum refinery.

c. Flare is not used as a control device for any emission points listed in 40 CFR § 63.640(c).

d. Flare is portable, not stationary.

Table 13-8 Cooling Towers Summary of Applicable Regulations

Cooling Tower	Description	MACT Q	MACT CC ^a	CAM
Y-0001	TCC Cooling Tower	NO	YES	NO
Y-0002	S. Alky Cooling Tower (Marley Cooling Tower)	NO	YES	NO
Y-0008	North Alky Cooling Tower	NO	YES	NO
Y-0011	FCC & NP Cooling Tower	NO	YES	NO
Y-0012	Hydrogen Plants Cooling Tower	NO	YES	NO
CT TT-0006	Unit 07 Amine W-0745 Cooling Tower	NO	NO	NO

a For MACT CC, the "heat exchange system" is included in the existing affected source. "YES" indicates the listed cooling tower is part of a heat exchange systems that is part of the affected source.

Table 13-9 Wastewater Units Summary of Applicable Regulations

Equipment ID	Emission Point ID	NESHAP FF	NSPS QQQ	MACT CC	CAM	
Collector Sump						
T-0845 Weir Box	D-8000/D-	MEG	MEG	YES	NO	
T-0844 Stilling Well	8001	YES	YES	YES	NO	
T-0846 Stormwater Lift Station (SWLS)						
T-0830 Stormwater Surge Tank	T-0830	YES	YES	YES	NO	
S-1/T-1 Barscreen and Junction Box						
API-894	D-0829/0830	YES	YES	YES	NO	
API-895						
Equalization T-801	T-801	YES	NO	YES	NO	
Equalization T-836	T-836	YES	NO	YES	NO	
Flocculator T-0805	T-805	YES	NO	YES	NO	
DAF-896	DAE 906/906	VEC	NO	MEG	NO	
DAF-806	DAF-896/ 806	YES	NO	YES	NO	
Open Sump T-897	T-0897	YES	NO	YES	NO	
Walnut Hull Filters D-810/811 and Mechanical Filter D-808/809	D-810/811 D-808/809	YES	NO	YES	NO	
DAF Surge Tank T-809	T-0809	YES	NO	YES	NO	

Table 13-10 Truck and Rail Loading Racks Summary of Applicable Regulations

Unit ID	Description	NSPS XX	MACT R	MACT CC	CAM
TLO-1	Asphalt Truck Loading and Off- Loading Rack #1	NO	NO	NO	NO
TL-2	Asphalt Truck Loading Rack #2	NO	NO	NO	NO
TL-4	Fuels Truck Loading Rack	NO*	NO**	YES	NO
TL-7	CBO/LCO Truck Loading Rack	NO	NO	NO	NO
RLO-8	Railcar Loading & Off-Loading	NO	NO	NO	NO
RLO-19	Railcar Loading & Off-Loading	NO	NO	NO	NO
TLO-20	Asphalt/Pitch Truck Loading	NO	NO	NO	NO
TRLO-9	Molten Sulfur Truck/Railcar Loading	NO	NO	NO	NO

^{*}Compliance is not required pursuant to 40 CFR § 63.640(r).

Table 13-11 Fugitives Summary of Applicable Regulations

Title V Permit Unit ID	Description	MACT CC	NSPS GGGa	NSPS QQQ ^a	NESHAP J ^b	NESHAP V ^c
FUG-02-SP CRUDE	South Division Crude Unit	NOd	YES	YES	NO	NO
FUG-06-NHDU	Naphtha HDS Unit 06	NO ^d	YES	YES	NO	NO
FUG-07-N AMINE	Amine Unit-Treating/Regen.	NOd	YES	YES	NO	NO
FUG-07-SWS1	Sour Water Stripper	NOd	YES	YES	NO	NO
FUG-08-TRUCK RK	Loading Racks	NOd	YES	YES	NO	NO
FUG-09-N ALKY	North Alkylation Unit (New-Inside battery limits)	NOd	YES	YES	NO	NO
FUG-10-FCC	FCC w/CVS	NOd	YES	YES	NO	NO
FUG-13-NHDU	Naphtha HDS Unit 13	NOd	YES	YES	NO	NO
FUG-18-LSR MEROX TRT	Merox/Merichem Treating Units	NOd	NO	YES	NO	NO
FUG-19-NAPH	Naphtha Merox	NOd	NO	YES	NO	NO
FUG-20-ISOM	BenFree Unit	NOd	YES	YES	NO	NO
FUG-21-SP VACUUM	Flasher/Vacuum Unit	NOd	YES	YES	NO	NO
FUG-25-ROSE-2	ROSE Unit	NOd	YES	YES	NO	NO

^{**}Compliance is not required pursuant to 40 CFR § 63.420(i).

Title V Permit Unit ID	Description	MACT CC	NSPS GGGa	NSPS QQQ ^a	NESHAP J ^b	NESHAP V ^c
FUG-29-BLENDER/TK FARM	Light Oil Tankage	NO ^d	YES	YES	NO	NO
FUG-30-SRU2/TGTU	SRU2/SWS w/CVS	NOd	YES	YES	NO	NO
FUG-31- SRU3/TGTU3/TGI3	SRU3 Unit	NOd	YES	YES	NO	NO
FUG-33-DIST HDU	Relocated Diesel HDS Unit w/CVS	NO ^d	YES	YES	NO	NO
FUG-34- HYDROCRACKER	WX Hydrocracker	NO ^d	YES	YES	NO	NO
FUG-35-SAT GAS	Saturates Gas Plant	NOd	YES	YES	NO	NO
FUG-36-RO	Reverse Osmosis	NO	NO	YES	NO	NO
FUG-37-NP-UT	North Plant Utilities	NO	NO	YES	NO	NO
FUG-41-PBC	PBC Unit	NOd	YES	YES	NO	NO
FUG-43-S ALKY	South Alky Unit (W-76)	NOd	NO	YES	NO	NO
FUG-44-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	NOd	YES	YES	NO	NO
FUG-45-DIST-HDU	Gas Oil Hydrotreater (incl. CVS)	NOd	YES	YES	NO	NO
FUG-54-PRIMEG	Prime G Unit	NOd	YES	YES	NO	NO
FUG-63-H2 PLANT-1	Hydrogen Plant	NO	YES	YES	NO	NO
FUG-64-H2 PLANT-2	Hydrogen Plant	NO	YES	YES	NO	NO
FUG-70-CCR	CCR Reformer (w/in battery limits)	NOd	YES	YES	NO	NO
FUG-73-SP UTIL	Utilities	NO	NO	YES	NO	NO
FUG-80-WWTP CVS	Oil/Water Separator	NOd	YES	YES	NO	NO
FUG-LPG	LPG Storage System	NOd	YES	YES	NO	NO

<sup>a. All wastewater sources are subject to NSPS QQQ (0195-M17(5)(J), December 15, 2004).
b. No refinery streams contain benzene at concentration of 10% wt or greater.
c. NESHAP V is only applicable if subject to NESHAP J.</sup>

d. Exempt from MACT CC pursuant to 40 CFR §63.640(p)(2)

Table 13-12 Storage Tanks Summary of Applicable Regulations

Tank No.	NSPS K	NSPS Ka	NSPS Kb	MACT CC Storage	MACT CC Wastewater	NESHAP FF	NSPS QQQ	20.2.38.109 NMAC	20.2.38.110 NMAC	20.2.38.113 NMAC	CAM
T-0001	NO	NO	NO	NO	YES	YES	NO	NO	NO	NO	NO
T-0002	NO	NO	NO	NO	YES	YES	NO	NO	NO	NO	NO
T-0003	NO	NO	NO	NO	YES	YES	NO	NO	NO	NO	NO
T-0004	NO	NO	NO	NO	YES	NO	NO	NO	NO	NO	NO
T-0011	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0012	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0020	NO	NO	YES	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0021	NO	NO	YES	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0022	NO	NO	YES	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0023	NO	NO	YES	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0026	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0028	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0031	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0040	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0041	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0042	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0045	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0046	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0049	NO	NO	NO	YES	N/A	YES	YES	YES	YES	NO	NO
T-0055	NO	YES	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0056	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0059	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0061	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0063	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0064	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0065	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0071	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0072	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0073	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0074	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0075	NO	NO	YES	YES	N/A	N/A	N/A	NO	NO	NO	NO

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Tank No.	NSPS K	NSPS Ka	NSPS Kb	MACT CC Storage	MACT CC Wastewater	NESHAP FF	NSPS QQQ	20.2.38.109 NMAC	20.2.38.110 NMAC	20.2.38.113 NMAC	CAM
T-0076	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0079	NO	NO	YES	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0081	NO	NO	NO	YES	N/A	N/A	N/A	YES	NO	NO	NO
T-0082	NO	NO	NO	YES	N/A	N/A	N/A	YES	NO	NO	NO
T-0106	NO	NO	NO	YES	N/A	N/A	N/A	YES	YES	NO	NO
T-0107	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0108	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0109	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0110	NO	NO	NO	YES	N/A	N/A	N/A	YES	YES	NO	NO
T-0111	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0112	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0114	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0115	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0116	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0117	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0119	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0124	NO	YES	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0400	NO	YES	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0401	NO	YES	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0402	NO	YES	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0410	NO	NO	NO	YES	N/A	N/A	N/A	YES	YES	NO	NO
T-0411	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0412	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0413	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0415	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0417	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0418	NO	NO	YES	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0419	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0420	NO	NO	NO	YES	N/A	N/A	N/A	YES	YES	NO	NO
T-0422	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0423	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0431	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0432	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO

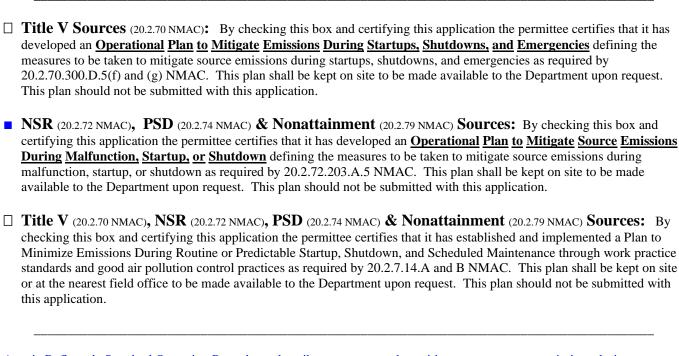
Tank No.	NSPS K	NSPS Ka	NSPS Kb	MACT CC Storage	MACT CC Wastewater	NESHAP FF	NSPS QQQ	20.2.38.109 NMAC	20.2.38.110 NMAC	20.2.38.113 NMAC	CAM
T-0433	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0434	NO	YES	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0435	NO	NO	YES	YES	N/A	N/A	N/A	YES	YES	YES	NO
T-0437	YES	NO	NO	YES	N/A	N/A	N/A	YES	NO	NO	NO
T-0438	NO	YES	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0439	NO	YES	NO	YES	N/A	N/A	N/A	YES	YES	YES	NO
T-0446	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0447	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0448	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0449	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0450	NO	NO	YES	YES	N/A	N/A	N/A	YES	NO	NO	NO
T-0451	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0452	NO	NO	YES	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0453	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0460	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0465	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0466	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0467	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0468	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0600	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0737	NO	NO	YES	YES	N/A	N/A	N/A	YES	YES	YES	NO
T-0802	NO	NO	YES	YES	N/A	N/A	N/A	YES	YES	YES	NO
T-0803	NO	NO	NO	NO	YES	YES	NO	NO	NO	NO	NO
T-0804	NO	NO	NO	NO	YES	YES	NO	NO	NO	NO	NO
T-0807	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0809	NO	NO	NO	NO	YES	YES	NO	NO	NO	NO	NO
T-0814	NO	NO	NO	YES	N/A	N/A	N/A	YES	YES	YES	NO
T-0815	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0816	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0821	NO	NO	YES	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0829	NO	NO	NO	NO	YES	YES	NO	NO	NO	NO	NO
T-0834	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0835	NO	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO

Tank No.	NSPS K	NSPS Ka	NSPS Kb	MACT CC Storage	MACT CC Wastewater	NESHAP FF	NSPS QQQ	20.2.38.109 NMAC	20.2.38.110 NMAC	20.2.38.113 NMAC	CAM
T-0838	YES	NO	NO	YES	N/A	N/A	N/A	NO	NO	NO	NO
T-0839	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0840	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0841	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0891	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-0892	NO	NO	NO	NO	N/A	N/A	N/A	NO	NO	NO	NO
T-1224	NO	NO	NO	NO	NO	NO	NO	NO	NO	NO	NO
T-1225	NO	NO	YES	YES	N/A	N/A	N/A	YES	NO	NO	NO
T-1227	NO	NO	YES	YES	N/A	N/A	N/A	YES	YES	YES	NO

Section 14

Operational Plan to Mitigate Emissions

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)



Artesia Refinery's Standard Operating Procedures describe measures used to mitigate source excess emissions during startup, shutdown, or malfunction. The Artesia Refinery will comply with the startup, shutdown, and malfunction requirements in 40 CFR 63, Subparts CC and UUU and maintain records to demonstrate compliance. Changes proposed in this application will not affect the current procedures.

Section 15

Alternative Operating Scenarios

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

Alternative Operating Scenarios: Provide all information required by the department to define alternative operating scenarios. This includes process, material and product changes; facility emissions information; air pollution control equipment requirements; any applicable requirements; monitoring, recordkeeping, and reporting requirements; and compliance certification requirements. Please ensure applicable Tables in this application are clearly marked to show alternative operating scenario.

Construction Scenarios: When a permit is modified authorizing new construction to an existing facility, NMED includes a condition to clearly address which permit condition(s) (from the previous permit and the new permit) govern during the interval between the date of issuance of the modification permit and the completion of construction of the modification(s). There are many possible variables that need to be addressed such as: Is simultaneous operation of the old and new units permitted and, if so for example, for how long and under what restraints? In general, these types of requirements will be addressed in Section A100 of the permit, but additional requirements may be added elsewhere. Look in A100 of our NSR and/or TV permit template for sample language dealing with these requirements. Find these permit templates at: https://www.env.nm.gov/aqb/permit/aqb_pol.html. Compliance with standards must be maintained during construction, which should not usually be a problem unless simultaneous operation of old and new equipment is requested.

In this section, under the bolded title "Construction Scenarios", specify any information necessary to write these conditions, such as: conservative-realistic estimated time for completion of construction of the various units, whether simultaneous operation of old and new units is being requested (and, if so, modeled), whether the old units will be removed or decommissioned, any PSD ramifications, any temporary limits requested during phased construction, whether any increase in emissions is being requested as SSM emissions or will instead be handled as a separate Construction Scenario (with corresponding emission limits and conditions, etc.

The Artesia Refinery operates as described in Section 10 of this application. No alternative operating scenarios are proposed.

waiver approval documentation.

Saved Date: 8/31/2021

Section 16

Air Dispersion Modeling

- 1) Minor Source Construction (20.2.72 NMAC) and Prevention of Significant Deterioration (PSD) (20.2.74 NMAC) ambient impact analysis (modeling): Provide an ambient impact analysis as required at 20.2.72.203.A(4) and/or 20.2.74.303 NMAC and as outlined in the Air Quality Bureau's Dispersion Modeling Guidelines found on the Planning Section's modeling website. If air dispersion modeling has been waived for one or more pollutants, attach the AQB Modeling Section modeling
- 2) SSM Modeling: Applicants must conduct dispersion modeling for the total short term emissions during routine or predictable startup, shutdown, or maintenance (SSM) using realistic worst case scenarios following guidance from the Air Quality Bureau's dispersion modeling section. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app form.html) for more detailed instructions on SSM emissions modeling requirements.
- 3) Title V (20.2.70 NMAC) ambient impact analysis: Title V applications must specify the construction permit and/or Title V Permit number(s) for which air quality dispersion modeling was last approved. Facilities that have only a Title V permit, such as landfills and air curtain incinerators, are subject to the same modeling required for preconstruction permits required by 20.2.72 and 20.2.74 NMAC.

What is the purpose of this application?	Enter an X for each purpose that applies
New PSD major source or PSD major modification (20.2.74 NMAC). See #1 above.	Į.
New Minor Source or significant permit revision under 20.2.72 NMAC (20.2.72.219.D NMAC). See #1 above. Note: Neither modeling nor a modeling waiver is required for VOC emissions.	X
Reporting existing pollutants that were not previously reported.	
Reporting existing pollutants where the ambient impact is being addressed for the first time.	
Title V application (new, renewal, significant, or minor modification. 20.2.70 NMAC). See #3	
above.	
Relocation (20.2.72.202.B.4 or 72.202.D.3.c NMAC)	
Minor Source Technical Permit Revision 20.2.72.219.B.1.d.vi NMAC for like-kind unit replacements.	
Other: i.e. SSM modeling. See #2 above.	
This application does not require modeling since this is a No Permit Required (NPR) application.	
This application does not require modeling since this is a Notice of Intent (NOI) application (20.2.73 NMAC).	
This application does not require modeling according to 20.2.70.7.E(11), 20.2.72.203.A(4), 20.2.74.303, 20.2.79.109.D NMAC and in accordance with the Air Quality Bureau's Modeling Guidelines.	

Check each box that applies:

Ш	See attached, approved modeling waiver for all pollutants from the facility.
	See attached, approved modeling waiver for some pollutants from the facility.
	Attached in Universal Application Form 4 (UA4) is a modeling report for all pollutants from the facility.
	Attached in UA4 is a modeling report for some pollutants from the facility.
	No modeling is required.

Section 17

Compliance Test History

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

TT 's NT	m (D)	E (D)
Unit No.	Test Description	Test Date
FL-0404 TS CMS	Annual CMS RATA and 3-year linearity	02/23/2021
FL-0402 TS CMS	Annual CMS RATA and 3-year linearity	02/25/2021
FL-0401 TS CMS	Annual CMS RATA and 3-year linearity	02/22/2021
FL-0400 TS CMS	Annual CMS RATA and 3-year linearity	02/24/2021
FL-0404 H2S CMS	Annual CMS RATA and 3-year linearity	02/23/2021
FL-0402 H2S CMS	Annual CMS RATA and 3-year linearity	02/25/2021
FL-0401 H2S CMS	Annual CMS RATA and 3-year linearity	02/22/2021
FL-0400 H2S CMS	Annual CMS RATA and 3-year linearity	02/24/2021
FL-0404 H2S CMS	Annual CMS RATA	03/03/2020
FL-0402 H2S CMS	Annual CMS RATA	02/27/2020
FL-0401 H2S CMS	Annual CMS RATA	02/26/2020
FL-0400 H2S CMS	Annual CMS RATA	03/02/2020
FL-0404 H2S CMS	Annual CMS RATA	03/27/2019
FL-0402 H2S CMS	Annual CMS RATA	02/19/2019
FL-0401 H2S CMS	Annual CMS RATA	02/21/2019
FL-0400 H2S CMS	Annual CMS RATA	02/20/2019
FL-0404 H2S CMS	Annual CMS RATA	02/14/2018
FL-0402 H2S CMS	Annual CMS RATA	01/23/2018
FL-0401 H2S CMS	Annual CMS RATA	01/26/2018
FL-0400 H2S CMS	Annual CMS RATA	01/24/2018
FL-0404 H2S CMS	Annual CMS RATA	01/19/2017
FL-0402 H2S CMS	Annual CMS RATA	01/20/2017
FL-0401 H2S CMS	Annual CMS RATA	01/17/2017
FL-0400 H2S CMS	Annual CMS RATA	01/24/2017
FL-0404 H2S CMS	Initial CMS RATA	02/03/2016
FL-0402 H2S CMS	Initial CMS RATA	01/31/2016
FL-0401 H2S CMS	Initial CMS RATA	01/26/2016
FL-0400 H2S CMS	Initial CMS RATA	01/23/2016
FCC REGEN		01, 20, 2010
DynaWave Scrubber	Annual CEMS RATA	03/05/2021
CEMS		03/ 02/ 2021
FCC REGEN		
DynaWave Scrubber	Annual CEMS RATA	02/05/2020
CEMS		
FCC REGEN		
DynaWave Scrubber	Annual CEMS RATA	02/13/2019
CEMS		02, 32, 232
FCC REGEN		
DynaWave Scrubber	Annual CEMS RATA	01/09/2018
CEMS		
FCC REGEN		
DynaWave Scrubber	Annual CEMS RATA	01/04/2017
CEMS		
FCC REGEN	Annual Devicemence Test for CD Alternative Manitorie - Dis-	01/042017
DynaWave Scrubber	Annual Performance Test for CD Alternative Monitoring Plan	01/042017
SRU3-TGI	Annual CEMS RATA	03/04/2021
SRU3-TGI	Annual CEMS RATA	03/18/2020
SRU3-TGI	Annual CEMS RATA	04/18/2019

Unit No.	Test Description	Test Date
SRU3-TGI	Annual CEMS RATA	03/21/2018
SRU3-TGI	Annual CEMS RATA	07/26/2017
SRU2-TGI	Annual CEMS RATA	03/03/2021
SRU2-TGI	Annual CEMS RATA	03/19/2020
SRU2-TGI	Annual CEMS RATA	04/10/2019
SRU2-TGI	Annual CEMS RATA	03/22/2018
SRU2-TGI	Annual CEMS RATA	04/27/2017
SRU2-TGI	Annual CEMS RATA	05/05/2016
B-9	Annual CEMS RATA	03/01/2021
B-9	Annual CEMS RATA	03/11/2020
B-9	Annual CEMS RATA	03/20/2019
B-9	Annual CEMS RATA	03/07/2018
B-9	Annual CEMS RATA	07/24/2017
B-8	Annual CEMS RATA	03/02/2021
B-8	Annual CEMS RATA	03/11/2020
B-8	Annual CEMS RATA	03/19/2019
B-8	Annual CEMS RATA	03/07/2018
B-8	Annual CEMS RATA	06/22/2017
B-8	Annual CEMS RATA	07/14/2016
B-7	Annual CEMS RATA	03/11/2021
B-7	Annual CEMS RATA	03/10/2020
B-7	Annual CEMS RATA	03/19/2019
B-7	Annual CEMS RATA	03/06/2018
B-7	Annual CEMS RATA	06/21/2017
B-7	Annual CEMS RATA	07/13/2016
H-362,363,364 Unit 70	Annual Performance Test	02/03/2021
H-362,363,364 Unit 70	Annual Performance Test	02/07/2020
H-362,363,364 Unit 70	Annual Performance Test	02/14/2019
H-362,363,364 Unit 70	Annual Performance Test	01/31/2018
H-362,363,364 Unit 70	Annual Performance Test	01/10/2017
H-362,363,364 Unit 70	Annual Performance Test	07/11/2016
H-9851	Annual CEMS RATA	03/08/2021
H-9851	Annual CEMS RATA	02/07/2020
H-9851	Annual CEMS RATA	03/21/2019
H-9851	Annual CEMS RATA	03/20/2018
H-9851	Annual CEMS RATA	06/20/2017
H-9851	Annual CEMS RATA	07/14/2016
H-8801, H-8802	Annual CEMS RATA	02/12/2020
H-8801, H-8802	Annual CEMS RATA	02/18/2019
H-8801, H-8802	Annual CEMS RATA	01/30/2018
H-8801, H-8802	Annual CEMS RATA	01/08/2017
H-5401 (Prime G)	Annual Performance Test	02/05/2021
H-5401 (Prime G)	Annual Performance Test	03/16/2020
H-5401 (Prime G)	Annual Performance Test	04/08/2019
H-5401 (Prime G)	Annual Performance Test	03/08/2018
H-5401 (Prime G)	Initial Performance Test	10/25/2017
H-3402	Annual Performance Test for NO _X , CO and O ₂ CMS RATA (AMP Req	02/00/2021
(HCKR-BOIL1)	is bi-annual)	03/09/2021
H-3402	Annual Performance Test for NO _X , CO and O ₂ CMS RATA (AMP Req	02/11/2020
(HCKR-BOIL1)	is bi-annual)	02/11/2020
H-3402	Annual Performance Test for NO _X , CO and O ₂ CMS RATA (AMP Req	02/15/2019
(HCKR-BOIL1)	is bi-annual)	02/13/2017
H-3402	Annual Performance Test for NO _X , CO and O ₂ CMS RATA (AMP Req	02/22/2018
(HCKR-BOIL1)	is bi-annual)	02/22/2010
H-3402	Annual Performance Test for NO _X , CO and O ₂ CMS RATA (AMP Req	01/11/2017
(HCKR-BOIL1)	is bi-annual)	01/11/2017

Unit No.	Test Description	Test Date
H-3402	Annual Performance Test for NO _X , CO and O ₂ CMS RATA (AMP Req	07/11/2016
(HCKR-BOIL1)	is bi-annual)	07/11/2010
H-3403 (HCKR) Unit 34	Annual Performance Test	03/09/2021
H-3403 (HCKR) Unit 34	Annual Performance Test	02/10/2020
H-3403 (HCKR) Unit 34	Annual Performance Test	02/14/2019
H-3403 (HCKR) Unit 34	Annual Performance Test	02/01/2018
H-3403 (HCKR) Unit 34	Annual Performance Test	01/23/2017
H-3403 (HCKR) Unit 34	Annual Performance Test	07/12/2016
H-2501 (ROSE2-HOH) Unit 25	Annual CEMS RATA	03/10/2021
H-2501 (ROSE2-HOH) Unit 25	Annual CEMS RATA	02/13/2020
H-2501 (ROSE2-HOH) Unit 25	Annual CEMS RATA	02/10/2019
H-2501 (ROSE2-HOH) Unit 25	Annual CEMS RATA	01/10/2018
H-2501 (ROSE2-HOH) Unit 25	Annual CEMS RATA	01/09/2017
H-2501 (ROSE2-HOH) Unit 25	Annual CEMS RATA	01/09/2017
H-2501 (ROSE2-HOH) Unit 25	Annual CEMS RATA	05/05/2016
H-2421	Annual Performance Test	02/02/2021
H-2421	Annual Performance Test	03/13/2020
H-2421	Annual Performance Test	04/18/2019
H-2421	Annual Performance Test	03/20/2018
H-2421	Annual Performance Test	01/05/2017
H-2421	Annual Performance Test	07/25/2017
H-0020	Annual Performance Test	02/01/2021
H-0020	Annual Performance Test	02/07/2020
H-0020	Annual Performance Test	02/20/2019
H-0020	Annual Performance Test	01/11/2018
H-0020	Annual Performance Test	01/05/2017
H-0019	Annual Performance Test	02/01/2021
H-0019	Annual Performance Test	02/06/2020
H-0019	Annual Performance Test	02/20/2019
H-0019	Annual Performance Test	01/11/2018
H-0019	Annual Performance Test	01/05/2017
LP (D-19) Fuel Gas H2S	Annual CMS RATA	03/03/2021
LP (D-19) Fuel Gas H2S	Annual CMS RATA	03/17/2020
LP (D-19) Fuel Gas H2S	Annual CMS RATA	03/07/2019
LP (D-19) Fuel Gas H2S	Annual CMS RATA	02/15/2018
LP (D-19) Fuel Gas H2S	Annual CMS RATA	01/03/2017
HP (D-770) Fuel Gas H2S (Permanent)	Annual CMS RATA	03/02/2021

Unit No.	Test Description	Test Date
HP (D-770) Fuel Gas H2S (Permanent)	Annual CMS RATA	03/17/2020
HP (D-770) Fuel Gas H2S (Permanent)	Annual CMS RATA	04/04/2019
HP (D-770) Fuel Gas H2S (Permanent)	Annual CMS RATA	02/27/2018
HP (D-770) Fuel Gas H2S (Permanent)	Annual CMS RATA	06/22/2017
HP (D-770) Fuel Gas H2S (Permanent)	Annual CMS RATA	07/14/2016
2 Backup Analyzers (Horiba brand with data logger)	Annual CEMS RATA	12/19/2019-sent to factory for rebuild and recertification.
2 Backup Analyzers (Horiba brand with data logger)	Annual CEMS RATA	03/07/2019
2 Backup Analyzers (Horiba brand with data logger)	Annual CEMS RATA	03/06/2018
2 Backup Analyzers (Horiba brand with data logger)	Annual CEMS RATA	06/20/2017
2 Backup Analyzers (Horiba brand with data logger)	Annual CEMS RATA	08/16/2016
TL-4	CEMS RATA	11/06/2019
TL-4	CEMS RATA	09/28/2018
TL-4	CEMS RATA	09/12/2017
TL-4	CEMS RATA	04/07/2016
Fuel Gas H ₂ S (Portable Back-up Analyzer)	Annual CMS RATA	07/13/2016

Section 20

Other Relevant Information

<u>Other relevant information</u>. Use this attachment to clarify any part in the application that you think needs explaining. Reference the section, table, column, and/or field. Include any additional text, tables, calculations or clarifying information.

Additionally, the applicant may propose specific permit language for AQB consideration. In the case of a revision to an existing permit, the applicant should provide the old language and the new language in track changes format to highlight the proposed changes. If proposing language for a new facility or language for a new unit, submit the proposed operating condition(s), along with the associated monitoring, recordkeeping, and reporting conditions. In either case, please limit the proposed language to the affected portion of the permit.

Historical PSD Review

As discussed in Sections 3 and 12 herein, with this permit application Navajo is seeking authorization for four separate and independent projects—one involving revisions to permit terms for certain loading racks and storage tanks; another involving changes to the flares; a third involving changes in fuel composition for three process heaters; and a fourth involving increases in the VOC concentration in the wastewater entering the dissolved air flotation units—as well as numerous permit revisions that are reconciliations involving no physical changes in or changes in method of operation of the stationary source. In this Section 20, Navajo is providing a summary of its review and evaluation of these revisions on historical PSD analyses for the Artesia Refinery.

<u>FCCU Catalyst Regenerator</u>. For the FCCU catalyst regenerator, Navajo is representing emissions of VOC for the first time and is representing higher PM_{10} and $PM_{2.5}$ emission rates.

The VOC emissions represented in the present application reflect new data gathered by U.S. EPA in the context of the Refinery Sector Rule. See April 2015 Emissions Estimation Protocol for Petroleum Refineries, Version 3, and ICR reported FCCU data and NPRA capacities. This is a reconciliation, not an emissions increase, and it has no implications for historical PSD applicability as discussed below.

The FCCU was constructed in 1979 as a replacement of a then-existing Thermofor Catalytic Cracking Unit ("TCCU"). Construction was authorized pursuant to a determination issued by NMED in May 1979, identified as Permit No. 236, that no permit was required because there was no increase in allowable emissions. Construction also was authorized by Permit No. PSD-NM-208 issued by U.S. EPA in July 1979. The PSD permit was rescinded in December 1981 because Navajo met the non-applicability and rescission criteria at 40 CFR §§ 52.21(i)(v) and 52.21(w)(3). See, 45 Fed. Reg. 52676 (Aug. 7, 1980) and 49 Fed. Reg. 11708 (Mar. 27, 1984). Specifically, under these provisions, and pursuant to the administrative stay of the PSD rules issued following the decision of the U.S. Court of Appeals in Ala. Power Co. v. Costle, 636 F.2d 323 (D.C. Cir. 1979), the applicability criteria in the proposed 1979 PSD rule revisions were applicable. See, 45 Fed. Reg. 7800 (Feb. 5, 1980). The emissions increase test for a major modification under the proposed 1979 PSD rule was a "significant net increase in that source's potential to emit," where significant for VOC emissions was defined as an increase of 10 tons per year. See, 44 Fed. Reg. 51924 (Sept. 5, 1979). Because the replacement of the TCCU with an FCCU did not increase the refinery's potential to emit of any pollutant, including VOC, PSD was not applicable.

The increase in the represented PM_{10} and $PM_{2.5}$ emission rates is a reconciliation, to account for condensable particulate matter for the first time. This is not an emissions increase and it has no implications for historical PSD applicability, as discussed below.

The GOHT project in 2001 involved changes to the FCCU and the permit record for that project (Permit 0195-M15) includes a PM_{10} emissions increase analysis. The pre-project actual filterable PM_{10} emissions were estimated to be 164.2 tpy, based on a 44.1 lb/hr filterable PM emission rate measured in a 1998 stack test and a 1999 stack test showing filterable $PM_{10} = 85\%$ of filterable PM. The unit was subject to a filterable PM/PM_{10} limit of 113.4 tpy in the M14 permit (and prior permits), which was less than the calculated actual emissions, so that allowable emissions rate is the pre-project actual filterable PM_{10} emission rate for the M15 PSD applicability analysis. The post-project allowable filterable PM_{10} emission rate was set to remain constant (i.e., no increase or decrease) at 113.4 tpy. The current representation is 90.9 tpy filterable PM_{10} plus 4.7 tpy condensable PM_{10} . This is not a relaxation of any limit relied upon in the M15 permitting and has no implications for that PSD analysis.

Beginning with the application for Permit No. PSD-NM-0195-M25 submitted in 2006, Navajo represented a filterable $PM_{10}/PM_{2.5}$ emission rate of 109.5 tpy. This value, which represents a slight decrease from the prior 113.4 tpy limit, is based on the Consent Decree filterable PM limit of 2.0 lb per ton of coke burned. The current representation is 90.9 tpy filterable PM_{10} plus 4.7 tpy condensable PM_{10} . This is not a relaxation of any limit relied upon in the M25 permitting—the FCCU catalyst regenerator was not among the emissions units affected by that project—and it has no implications for that PSD analysis.

<u>Sulfur Recovery Unit #2 Tail Gas Incinerator (H-0473)</u>. Navajo is representing higher PM_{10} and $PM_{2.5}$ emission rates than previously represented. This is a reconciliation, to account for condensable particulate matter for the first time. This is not an emissions increase and it has no implications for historical PSD applicability, as discussed below.

H-0473 was installed in 2001 pursuant to Permit No. 0195-M12 and the PM_{10} emissions increase from that project included only the emissions from H-0473. The original permitted filterable PM emissions from H-0473 were 1.1 tpy. The filterable PM emission limit and the represented filterable PM_{10} emission rate increased to 2.2 tpy upon issuance of Permit No. 0195-M20 in 2006. No changes to represented emission rates from H-0473 have occurred since 2006.

The current representation is 2.1 tpy filterable $PM_{10}/PM_{2.5}$ plus 6.3 tpy condensable $PM_{10}/PM_{2.5}$. This is not a relaxation of any limit relied upon in the M12 or M20 permitting and it has no implications for those PSD applicability analyses.

<u>Sulfur Recovery Unit #3 Tail Gas Incinerator (H-3103)</u>. Navajo is representing higher PM_{10} and $PM_{2.5}$ emission rates than previously represented. This is a reconciliation, to account for condensable particulate matter for the first time. This is not an emissions increase and it has no implications for historical PSD applicability, as discussed below.

H-3103 was initially constructed in 2009 as part of the 2007 refinery expansion project authorized pursuant to Permit No. PSD-NM-0195-M25. The requested reconciliation has no implications for the PSD applicability analysis performed in conjunction with Permit No. PSD-NM-0195-M25. The requested reconciliation also has no implications for the BACT determination made by NMED in conjunction with Permit No. PSD-NM-0195-M25. As indicated at pages 29-31 of the permit issued by NMED on Dec. 14, 2007, BACT for this unit is a set of work practices; these practices remain in place, unaffected by the consideration of condensable particulate matter. The original permitted filterable PM emissions from H-3103 were 2.2 tpy. No changes to represented emission rates from H-3103 have occurred since 2007.

The lower $PM_{10}/PM_{2.5}$ emission rates from H-3103 were considered in the PSD impact analyses performed in conjunction with issuance of Permit No. PSD-NM-0195-M25. Updated impact analyses for the 2007 refinery expansion project are discussed separately below.

<u>Unit 63 hydrogen reformer furnaces (H-8801 and H-8802)</u>. Navajo is requesting an increase in allowable emissions of SO₂ from these furnaces from the current limit of 0.8 tpy to a new limit of 4.96 tpy. These furnaces were initially constructed in 2006 pursuant to Permit No. 0195-M22. These were the only SO₂-emitting units affected by this project. The allowable SO₂ emissions from these furnaces in Permit 0195-M22 were 5.0 tpy. The requested relaxation has no implications for the PSD applicability analysis performed in conjunction with issuance of Permit No. 0195-M22.

The allowable SO₂ emissions from the H-8801 and H-8802 furnaces decreased to the current limit of 0.8 tpy at the time of issuance of Permit No. PSD-NM-0195-M25 in 2007. This was not a BACT limit, as these furnaces were not modified as part of the 2007 refinery expansion project.

The lower emission rate was considered in the PSD impact analyses performed in conjunction with issuance of Permit No. PSD-NM-0195-M25. Updated impact analyses for the 2007 refinery expansion project are discussed separately below.

<u>Unit 64 hydrogen reformer furnace (H-9851)</u>. Navajo is requesting an increase in allowable emissions of SO₂ from this furnace from the current limit of 2.2 tpy to a new limit of 11.0 tpy. This furnace was initially constructed as part of the 2007 refinery expansion project authorized pursuant to, and the current SO₂ emission limits were established in, Permit No. PSD-NM-0195-M25. The requested relaxation has no implications for the PSD applicability analysis performed in conjunction with Permit No. PSD-NM-0195-M25 as the project was a major modification for SO₂. The requested relaxation also has no implications for the BACT determination made by NMED in conjunction with Permit No. PSD-NM-0195-M25. As indicated at pages 29-30 of the permit issued by NMED on Dec. 14, 2007, and at page 2 of the Statement of Basis document issued by NMED on the same date, BACT for refinery fuel gas-fired combustion units is a fuel sulfur limit of 60 ppmv as H₂S on a 365-day rolling average basis. The revised limits proposed in this permit application are more stringent than the 2007 BACT determination.

The lower SO₂ emission rate was considered in the PSD impact analyses performed in conjunction with issuance of Permit No. PSD-NM-0195-M25. Updated impact analyses for the 2007 refinery expansion project are discussed separately below.

Boiler 9 (B-0009). Navajo is requesting increases in allowable emissions of all pollutants from this boiler because the actual heat input capacity of the installed boiler (244.4 MMBtu/hr HHV basis) is greater than the nominal capacity used at the time of its initial permitting (220 MMBtu/hr HHV). This boiler was initially constructed in 2012 pursuant to Permit No. PSD-NM-0195-M33. This was the only emissions unit affected by this project. The requested relaxation has no implications for the PSD applicability analysis performed in conjunction with issuance of Permit No. PSD-NM-0195-M33 because the allowable emissions requested in this permit application are less than the PSD significant levels for all pollutants.

<u>Dissolved Air Flotation (DAF) Units (T-0806 and T-0896)</u>. Navajo is requesting an increase in allowable emissions of VOC from these two units by 5.8 tpy, from the current level of 1.4 tpy to a new limit of 7.2 tpy. This relaxation has no implications for historical PSD applicability as discussed below.

T-0806 was initially permitted in 2007 as part of the 2007 refinery expansion project authorized pursuant to Permit No. PSD-NM-0195-M25, although it existed before that time. Initial construction of T-0896 was authorized under the same permit. The requested relaxation has no implications for the PSD applicability analysis performed in conjunction with Permit No. PSD-NM-0195-M25 as the project was a major modification for VOC.

The original permitted allowable VOC emissions from T-0806 and T-0896 were 5.3 tpy in total (2.65 tpy for each DAF). Total allowable emissions increased to 6.8 tpy in Permit No. PSD-NM-0195-M26 issued in 2009, decreased to 0.2 tpy in Permit No. PSD-NM-0195-M28 issued in 2011, and increased to the current 1.4 tpy level in Permit No. PSD-NM-0195-M36 issued in 2016. No changes to allowable emissions from T-0806 and T-0896 have occurred since 2016.

The requested relaxation has no implications for the BACT determination made by NMED in conjunction with Permit No. PSD-NM-0195-M25. As indicated at pages 29-31 of the permit issued by NMED on Dec. 14, 2007, BACT for the wastewater treatment facility included control requirements only for the new oil-water separator.

The requested relaxation has no implications for the PSD applicability analysis performed for the Prime G project in conjunction with Permit No. PSD-NM-0195-M36. The total project VOC increase calculated for that project was 25.9 tpy. Even if the present increase of 5.8 tpy is conservatively assumed to be entirely attributable to the Prime G project, and even if no consideration is given to the decrease in allowable emissions from fugitive emissions in the Prime G unit requested in this permit application, the increase from the Prime G project would remain well below the PSD significant level of 40 tpy.

<u>Alky Flare (FL-0403)</u>. For the Alky Flare, Navajo is requesting increases in allowable emissions of NO_X, CO, and VOC emission rates relative to Permit No. PSD-NM-0195M39R4.

The initial installation of this flare occurred in 1991 as part of the North Alkylation Unit project authorized under Permit No. 0195-M3, with changes to allowable emissions in Permit No. 0195-M4, both issued in 1991. The SO₂, NO_X, and CO emission rates represented in the present permit application for routine operation are less than the rates authorized in 1991 (0.8 tpy vs. 10.3 tpy for SO₂, 2.5 tpy vs. 15.8 tpy for NO_X, and 10.4 tpy vs. 59.0 tpy for CO), so the proposed increases have no implications with respect to the 1991 PSD applicability analyses for these pollutants. No VOC emissions were listed in the permits issued in 1991, and Navajo has not been able to locate a copy of the PSD applicability analyses performed with respect to VOC emissions in conjunction with issuance of the 1991 permits, but the allowable fugitive VOC emissions from equipment leaks in the North Alkylation Unit (FUG-09-N ALKY) in the 1991 permit (44.9 tpy) were greater than the sum of the represented VOC emissions from both equipment leaks (27.8 tpy) and FL-0403 (13.6 tpy) in the present permit application. The requested permit changes therefore have no implications for PSD applicability for the North Alkylation Unit project in 1991.

Allowable emissions from FL-0403 decreased from the initially permitted levels at the time of issuance of Administrative Permit Revision No. PSD-NM-0195-M26R1 in 2009. There were no physical changes or changes in method of operation and there can be no PSD implications associated with this permitting action.

GOHT Flare (FL-0404). For the GOHT Flare, Navajo is requesting increases in allowable emissions of SO₂, NO_X, CO, and VOC emission rates relative to Permit No. PSD-NM-0195M39R4.

These revisions to the permitted emission rates for the GOHT Flare will affect the PSD applicability analysis performed in conjunction with issuance of Permit No. 0195-M15 in 2001 authorizing the GOHT project and PSD impact analyses performed in conjunction with issuance of Permit No. PSD-NM-0195-M25 for the refinery expansion project in 2007. Updated analyses for the 2001 GOHT project and the 2007 refinery expansion project are discussed separately below.

<u>North Plant Flare (FL-0400)</u>, <u>South Plant Flare (FL-0401)</u>, <u>and FCCU Flare (FL-0402)</u>. For these flares, Navajo is requesting increases in allowable emissions of several pollutants.

Saved Date: 1/24/2022

FL-0400 and FL-0401 were in existence prior to enactment of the PSD permitting program, so the requested changes to permitted emission rates for these flares have no implications on historical PSD applicability for any project. Similarly, FL-0402 was constructed as part of the FCCU project authorized pursuant to a determination issued by NMED in May 1979, identified as Permit No. 236, that no permit was required because there was no increase in allowable emissions. Even if FL-0402 is conservatively assumed not to have been considered in that determination, the emission rates represented in the present permit application are less than the applicability thresholds in the then-effective PSD rule $(5.6 \text{ tpy SO}_2 \text{ vs. } 10 \text{ tpy threshold}, 2.2 \text{ tpy NO}_X \text{ vs. } 10 \text{ tpy threshold}, 9.1 \text{ tpy CO vs. } 100 \text{ tpy threshold}, and 7.7 \text{ tpy VOC vs. } 10 \text{ tpy threshold}.$

Refinery Expansion Project authorized by Permit No. PSD-NM-0195-M25. As noted above, several of the requested relaxations and reconciliations of emission rates requested in this permit application result in emission rates in excess of those used in the impact analyses performed in conjunction with issuance of this PSD permit in 2007. The air dispersion modeling report provided in Section 16 of this permit application includes updated impact analyses demonstrating that, even with the higher emission rates represented herein, the 2007 refinery expansion project does not cause or contribute to violations of any PSD increment; does not cause or contribute to exceedances of any NAAQS; does not adversely impact air quality related values in any Class I area; and does not cause adverse impacts on soils, vegetation, or visibility.

GOHT Project authorized by Permit No. 0195-M15. The GOHT Flare (FL-404) was initially installed pursuant to this construction permit issued in 2001 and the permitted potential emissions from FL-404 were considered in determining that this project was not a major modification under PSD. As previously reported to NMED in the permit application for Permit No. PSD-NM-0195-M39, increases in the emission limits for FL-404 results in the conclusion that the 2001 GOHT Project may have triggered PSD review for CO and NO_X emissions. The technical analysis submitted by Navajo in 2018, in conjunction with the permit application for Permit No. PSD-NM-0195-M39, demonstrated, among other things, that the GOHT Project does not trigger PSD review for any other pollutant; that the work practices in place at FL-404 represent BACT for CO and NO_X emissions; and that the 2001 GOHT Project does not cause or contribute to any PSD increment violation or NAAQS exceedance. The further increase in permitted emissions from FL-404 requested herein does not adversely affect any of these conclusions as discussed below.

The SO₂ and VOC net emissions changes from the 2001 GOHT Project as recalculated in Navajo's 2018 technical analysis were net decreases of 261 tpy and 320 tpy, respectively. The further increases associated with the present application are 1 tpy and 41 tpy, respectively. The prior conclusion that the 2001 GOHT Project did not cause significant net increases in emissions of these pollutants remains valid.

The work practices currently in place at FL-404 continue to represent BACT for CO and NO_X emissions. Table 20-1 presents additional analysis demonstrating that a flare gas recovery system is not required as BACT for FL-404:

Table 20-1 Cost Effectiveness of Flare Gas Recovery for FL-404

Parameter	Value	Notes
Installed cost	\$ 22,500,000	Conservative estimate, assumed to be 50% of total cost of 2-flare system
Capital recovery factor	9.44%	20 years, 7% interest
Annualized capital recovery cost	\$ 2,120,000	
Annual O&M cost	\$ -	Conservatively assumed to be zero
CO emissions reduction (tpy)	114.7	Conservatively assumed to be 100%
NO _X emissions reduction (tpy)	21.1	Conservatively assumed to be 100%
Cost effectiveness of CO emissions reduction (\$/ton)	\$ 18,500	
Cost effectiveness of NO _X emissions reduction (\$/ton)	\$ 101,000	

The air dispersion modeling report provided in Section 16 of this permit application includes updated impact analyses demonstrating that, even with the higher emission rates represented herein, the 2001 GOHT Project, conservatively considered in combination with the separate increases from the 2007 Refinery Expansion Project, does not cause or contribute to violations of the PSD increment for NO_X or exceedances of any NAAQS for CO or NO_X .

Saved Date: 1/24/2022

Units ID Updates

Through this permit application, Navajo requests the following updates to unit's IDs. These changes are requested to reconcile plant IDs with permit IDs, and involve no physical change in or changes in the method of operation of the stationary source.

Former Unit Number	Updated Unit Number	Source Description
H-0473 (SRU1/SRU2 TGI)	H-0473 (SRU2 TGI)	SRU2 Tail Gas Incinerator
SRU3-TGI	H-3103 (SRU3 TGI)	SRU3 Tail Gas Incinerator
V0543	MG-0001	Portable Air Compressor
V0545	MG-0002	Portable Air Compressor
V0546	MG-0003	Portable Air Compressor
V0511	MG-0004	Portable Fire Water Pump Engine
G0100	SG-0100	UPS Backup Generator
G0101	SG-0101	UPS Backup Generator
G0102	SG-0102	Sever Backup Generator
E0600W	FWG-0600	Fire Water Pump Engine
E0601M	FWG-0601	Fire Water Pump Engine
E0602E	FWG-0602	Fire Water Pump Engine
E0603	FWG-0603	Fire Water Pump Engine

Section 22: Certification

Company Name: Holly Frother Navajo Refini	ng, LLC						
I, Parrish Miller, hereby certify that the information	ion and data submitted in this application are true						
and as accurate as possible, to the best of my knowledge and professional expertise and experience.							
Signed this 2 day of September, 2011, upon my oath or affirm	nation, before a notary of the State of						
New Mexico.							
*Signature	9/2/21 Date						
Parrish Miller Printed Name	VP+ Refinery Managere Title						
Scribed and sworn before me on this 2 day of September	. 2021.						
My authorization as a notary of the State of New Mexico	expires on the						
27 day of April , 2024.							
Notary's Signature Notary's Printed Name	Date OFFICIAL SEAL SUZANNE GARCIA NOTARY PUBLIC STATE OF NEW MENICO My Comm. Expires 127						

*For Title V applications, the signature must be of the Responsible Official as defined in 20.2.70.7.AE NMAC.

Universal Application 4

Air Dispersion Modeling Report

Refer to and complete Section 16 of the Universal Application form (UA3) to assist your determination as to whether modeling is required. If, after filling out Section 16, you are still unsure if modeling is required, e-mail the completed Section 16 to the AQB Modeling Manager for assistance in making this determination. If modeling is required, a modeling protocol would be submitted and approved prior to an application submittal. The protocol should be emailed to the modeling manager. A protocol is recommended but optional for minor sources and is required for new PSD sources or PSD major modifications. Fill out and submit this portion of the Universal Application form (UA4), the "Air Dispersion Modeling Report", only if air dispersion modeling is required for this application submittal. This serves as your modeling report submittal and should contain all the information needed to describe the modeling. No other modeling report or modeling protocol should be submitted with this permit application.

16-A: Identification Name of facility: Artesia Refinery 2 Name of company: HollyFrontier Navajo Refining LLC 3 Current Permit number: PSD-NM-0195-M39R4; TV Operating Permit No. P-051R3 4 Name of applicant's modeler: David Keen, RTP Environmental Associates, Inc. 5 Phone number of modeler: 919-845-1422 x41 6 E-mail of modeler: keen@rtpenv.com

16	-B: Brief						
1	Was a modeling protocol submitted and approved? Yes⊠ No□						
2	Why is the modeling being done? PSD permit application and NAAQS/NMAAQS demonstration.	Other (describ	e below)				
3	Describe the permit changes relevant to the modeling.						
	Application to correct historical permitting errors and to permit unpermitted equipment.						
4	What geodetic datum was used in the modeling?	NAD83					
5	How long will the facility be at this location?	>25 yrs					
6	Is the facility a major source with respect to Prevention of Significant Deterioration (PSD)?	Yes⊠	No□				
7	Identify the Air Quality Control Region (AQCR) in which the facility is located	155					

	List the PSD baseline da	tes for this region (min	or or maior	, as appro	priate).				
-	NO ₂				3/16/1988				
8	SO_2			7/2	8/1978				
-	PM_{10}			2/20/1979					
-	PM _{2.5}			11/	13/2013				
	Provide the name and dis	stance to Class I areas	within 50 ki			00 km for 1	PSD permits).		
9	Bosque del Apache (245 White Mountains (134kr	km), Carlsbad Caverns						ldern	ess (79km),
10	1 Is the facility located in a non-attainment area? If so describe below Yes□ No⊠						No⊠		
11	Describe any special modeling requirements, such as streamline permit requirements.								
16.	·C: Modeling H	listory of Faci	ilit v						
10-	Describe the modeling hair Quality Standards (I waivers).	nistory of the facility, in	ncluding the AAQS (N						
	Pollutant	number that modeled pollutant facility-wide	Date of Permit Co		Comments				
	CO	n/a							
	NO ₂	PSD-NM-0195-M33	М33		Jan. 18, 2013		Cumulative analysis performed for 1-hr NAAQS, others below SILs		
1	SO ₂	PSD-NM-0195-M33		Jan. 18	, 2013		ve analysis perf others below S		ed for 1-hr
	H ₂ S	n/a							
	PM2.5	PSD-NM-0195-M33		Jan. 18	, 2013		ve analysis perf and increment,		
	PM10	PSD-NM-195-M25		Dec. 14	1, 2007				
	Lead	n/a							
	Ozone (PSD only) NM Toxic Air Pollutants (20.2.72.402 NMAC)	n/a n/a							
16-	D: Modeling p	erformed for	this ap	plicat	tion				
	For each pollutant, indic Choose the most complianalysis were also perfo	cate the modeling perfo	ormed and s	ubmitted	with this			ROI a	and cumulative
1	Pollutant	ROI	Cumulati analysis	ve	Culpabi analysis	•	Waiver approv	ved	Pollutant not emitted or not changed.
	СО								
	NO ₂		\boxtimes						
	SO_2		\boxtimes						
	H_2S		\boxtimes						

	PM2.5			\boxtimes					
	PM10		\boxtimes						
	Lead							X	
	Ozone		\boxtimes						
	State air toxic(s		\blacksquare						
	(20.2.72.402 NI	MAC)							
16-	16-E: New Mexico toxic air pollutants modeling								
1		lexico toxic ai	ir pollutants (NM				502 NMAC t	hat are mod	eled for this
	List any NMTA below, if require		nitted but not mod	leled becau	se stack height	correction fac	ctor. Add add	litional rows	s to the table
2	Pollutant	ission Rate unds/hour)	Emission Rate Level (pounds/		Stack Height (meters)	Correction	on Factor	Emissio	n Rate/ ion Factor
	фо	unus/nour)	Level (poullus/	iioui)	(meters)			Correct	ion ractor
16-	16-F: Modeling options								
1		ersion of AEF	RMOD used with	regulatory	default options	? If not explai	in Y	∕es⊠	No□
	below.								
16.	-G: Surrou	ındina ç	ource mod	eling					
1									
1	Date of surroun				pril 29, 2021				
		d differ from t	entory provided b the inventory prov rows as needed						
2	AQB Source ID		on of Corrections						
2	359@1 (Southeast Readi-Mix)	4.08 lb/hr	Thr PM10 and PM (17.875 TPY) for nited to 95 TPY.						
16-	·H: Buildir	ng and st	tructure d	<u>ownw</u> a	sh				
1	How many build	dings are pres	ent at the facility	? 63	3				
2	How many above the facility?	e ground stor	rage tanks are pre	sent at 9	8				
3	Was building do	ownwash mod	leled for all buildi	ngs and tar	iks? If not expl	ain why belov	v. Y	∕es⊠	No□
	All significant s	tructures (hei	ght above 10ft) w	ere include	d.				
4	Building comm	ents							

16-	I: Recent	ors and	modeled	property bou	ındarv			
1	"Restricted Arc continuous wal grade that wou within the prop is required in o receptors shall	ea" is an area alls, or other coll require spectorty may be interested to exclude the placed with the corother process.	to which puble ontinuous barrecial equipmendentified with le receptors from the proper	ic entry is effectively priers approved by the Det to traverse. If a large priesignage only. Public room the facility property ty boundaries of the factor at the facility that define	recluded. Effective bath partment, such as rugoroperty is completely ads cannot be part of a lift the facility does notifity.	ged physy enclosed a Restric ot have a	sical terrain w d by fencing, ted Area. A I	rith a steep a restricted area Restricted Area
2				ccessible roads in the re-	estricted area.		Yes□	No⊠
3	Are restricted a	rea boundary	coordinates in	ncluded in the modeling	g files?		Yes⊠	No□
	Describe the re	ceptor grids a	nd their spaci	ng. The table below ma	y be used, adding row	s as need	led.	1
4	Grid Type	Shape	Spacing	Start distance from restricted area or center of facility	End distance from restricted area or center of facility	Commo	ents	
	Cartesian	Fence following	100m	Starting at fence	2,500m from fence			
	Cartesian	Fence following	250m	2,500m from fence	7,500m from fence			
	Cartesian	Fence following	500m	7,500m from fence	10,000m from fence			
5	Describe receptor spacing along the fence line.							
	25m spacing al							
6	Describe the P		_	4-i	1 Davila Camailaa			
	Receptor locati	ons and eleva	nons were ob	tained from the Nationa	II Park Service.			
16.	J: Sensiti	ve areas						
1	Are there school	ols or hospital on is optional	s or other sen	sitive areas near the fac y undefined) but may h			Yes□	No⊠
3				be accelerated if there permit application?	is a public hearing. A	re there	Yes⊠	No□
16	-K: Mode	ling Scei	narios					
1	Identify, define, and describe all modeling scenarios. Examples of modeling scenarios include using different production rates, times of day, times of year, simultaneous or alternate operation of old and new equipment during transition periods, etc. Alternative operating scenarios should correspond to all parts of the Universal Application and should be fully described in Section 15 of the Universal Application (UA3).							
	Only one, wors	t-case scenari	o was modele	d which included startu	p and shutdown emiss	sions.		
2	Which scenario	produces the	highest conce	entrations? Why?				
	Not applicable.	Only a single	e, worst-case	scenario was modeled.				

	W/	-:		4- 1::4	.::	1	C :	9			1	
3	Were emis								or sets not	_		
)	to the factor							ciated fact	or sets, not	Yes□		No⊠
4									re the factor			
7		duplicate	table as ne	ecessary. I	t's ok to p	ut the table	e below sec	tion 16-K	if it makes fo	ormatting	easier.)	
	Sources: Hour of		Hour									
	Day	Factor	of Day	Factor								
	1		13									
	2		14									
	3		15									
	4		16									
	5		17									
_	6		18									
5	7		19									
	9		20									
	10		22									
	11		23			1		1				
	12		24									
		variable en	· I	oc were uc	ed that we	re not desc	ribed abov	e describe	them below			l l
	ii iiouiiy, v	arrabic cir	inssion race	25 Were use	ou that we	ic not desc	Tioca abov	c, describe	them below	•		
6	Were diffe	rent emiss	ion rates II	sed for sho	ort_term_ar	nd annual r	modeling?]	If so descri	he helow	Yes⊠		No□
	emissions v							ıy, 3-nr, 8-	hr and 24-hr	standards	. Annu	iai potentiai
	CIIISSIOIIS	were useu	to assess c	omphanec	with ann	uai staildai	us.					
16-	L: NO	Mode	eling									
	Which type			were used	?							
	Check all t											
		-										
		ARM2										
1		100%]	NO _X to NC	₂ conversi	on							
		PVMR	M									
		OLM										
	П	Other:										

16	-M: Particula	ate Matter Modelii	ng						
		s for which plume depletion mo							
1	□ PM2.	<u> </u>							
1	□ PM10)							
	None								
2	Describe the particl	e size distributions used. Include	de the source of information.						
2	Not applicable.								
3	Does the facility emit at least 40 tons per year of NO_X or at least 40 tons per year of SO_2 ? Sources that emit at least 40 tons per year of NO_X or at least 40 tons per year of SO_2 are considered to emit significant amounts of precursors and must account for secondary formation of PM2.5.								
4	Was secondary PM modeled for PM2.5? Yes⊠								
	If MERPs were use below.	d to account for secondary PM	2.5 fill out the information below. If an	nother method was u	used describe				
5	NO _X (ton/yr)	SO ₂ (ton/yr)	[PM2.5] _{annual}	[PM2.5] _{24-ho}	our				
	239.8	446.2	0.114 ug/m3	2.59 ug/m3	2.59 ug/m3				
16	-N: Setback l	Distances							
1	between the emission		their site configuration requires that see ea boundary (e.g. fence line) for both t itial location.						
	Not applicable.								
2		ited, modeled, setback distances in the relocation modeling.	s for future locations, if this permit is f	for a portable station	nary source.				
	Not applicable.								

16	-O: PSD Increment and Source IDs			
1	The unit numbers in the Tables 2-A, 2-B, 2-C, 2-E, 2-F, and 2-modeling files. Do these match? If not, provide a cross-referent if they do not match below.		Yes□	No⊠
	Unit Number in UA-2	Unit Number in Modeling File	S	
	Please see the attached Cross Reference Table.			
2	The emission rates in the Tables 2-E and 2-F should match the these match? If not, explain why below.	ones in the modeling files. Do	Yes⊠	No□
3	Have the minor NSR exempt sources or Title V Insignificant A been modeled?	Activities" (Table 2-B) sources	Yes□	No⊠

4	Which units consume ir increment at their poten	ncrement for which pollutation to emit rates.	ants? All sou	rces at the re	finery were conserva	atively assumed	to consume
7	Unit ID	NO ₂	SO ₂		PM10	PM2.5	
5	PSD increment descript (for unusual cases, i.e., after baseline date).	ion for sources. baseline unit expanded en	nissions	PM2.5 since permitting	t does not trigger inc ce it is an application errors which were co e. Increment compli- ollutants.	to correct histo ommitted prior	orical to the PM2.5
6	Are all the actual installation dates included in Table 2A of the application form, as required? This is necessary to verify the accuracy of PSD increment modeling. If not please explain. Yes No.						No□

16	16-P: Flare Modeling									
1	For each flare or flaring scenario, complete the following									
	Flare ID (and scenario)	Average Molecular Weight	Gross Heat Release (cal/s)	Effective Flare Diameter (m)						
	FL0400		5.91E+08	16.11						
	FL0401		2.10E+08	9.60						
	FL0402		1.96E+08	9.28						
	FL0403		8.61E+08	19.45						
	FL0404		1.54E+09	26.01						
	TL4VCU		3.50E+07	3.92						
	FLHEP		1.19E+07	2.29						
	TVCU		8.82E+04	0.20						

16-	Q: Volume and Related Sources		
1	Were the dimensions of volume sources different from standard dimensions in the Air Quality Bureau (AQB) Modeling Guidelines? If not please explain how increment consumption status is determined for the missing installation dates below.	Yes□	No⊠
	Describe the determination of sigma-Y and sigma-Z for fugitive sources.		
2	Sigma Y values calculated as the square root of the area, or average length of side, divided by 4 Manual for Single Volume Source). Area for tanks calculated from diameter. Sigma Z values for adjacent to a building calculated as the building height divided by 2.15 (Table 3-1 of AERMOD on or Adjacent to Building). Release height equal to center of volume except for storage tanks the top of the tank. In this case, the tank height was modeled as the release height.	for elevated sou Manual for Ele	rces on or evated Source

3	Describe how the volume sources are related to unit numbers. Or say they are the same.							
	They are the same (as specified in the attached cross reference table).							
4	Describe any open pits.							
	Not applicable.							
5	Describe emission units included in each open pit.							
3	Not applicable.							
16-	R: Background Concentrations							
	Were NMED provided background concentrations used? Identify the background station used below. If non-NMED provided background concentrations were used describe the data that was used.	Yes⊠	No□					
	CO: N/A							
1	NO ₂ : Outside Carlsbad (350151005)							
1	PM2.5: Hobbs-Jefferson (350450019) PM10: N/A							
	SO ₂ : Bloomfield(350450009)							
	Other:							
	Comments:							
2	Were background concentrations refined to monthly or hourly values? If so describe below.	Yes⊠	No□					
	98% hourly NO ₂ values by season and hour of day from Carlsbad were employed.							
16-	S: Meteorological Data							
1	Was NMED provided meteorological data used? If so select the station used.	Yes□	No⊠					
	If NMED provided meteorological data was not used describe the data set(s) used below. Discuss how missing data w handled, how stability class was determined, and how the data were processed.							
2								
16-	T: Terrain							
1	Was complex terrain used in the modeling? If not, describe why below.	Yes⊠	No□					
2	What was the source of the terrain data?							
2	National Elevation Data (NED)							

16-U: Modeling Files						
	Describe the modeling files:					
1	File name (or folder and file name)	Pollutant(s)	Purpose (ROI/SIA, cumulative, culpability analysis, other)			
	Artesia SIL_(MET Year)_(Pollutant)	PM25, PM10, H2S, SO2, NO2, CO	ROI and SIL			
	Artesia NAAQS_(MET Year)_(Pollutant)	PM25, H2S, SO2, NO2	Cumulative NAAQS			
	Artesia Increment_(MET Year)_(Pollutant)	NO2, SO2	Cumulative increment			
	Artesia TAP_(MET Year)_(Pollutant)	H2SO4, NH3	State toxics			

16-	16-V: PSD New or Major Modification Applications						
1	A new PSD major source or a major modification to an existing PSD major source requires additional analysis. Was preconstruction monitoring done (see 20.2.74.306 NMAC and PSD Preapplication Guidance on the AQB website)?	Yes□	No⊠				
2	If not, did AQB approve an exemption from preconstruction monitoring?	Yes⊠	No□				
3	Describe how preconstruction monitoring has been addressed or attach the approved preconstruction monitoring or monitoring exemption.						
3	Pursuant to 20.2.74.306.A NMAC and 40 CFR § 52.21(m)(1), HollyFrontier proposed to use the AQB's recommended background values in lieu of site-specific preconstruction data (see protocol page 5-2). The AQB approved the protocol, with the exception of the treatment of intermittent sources, on August 2, 2021.						
1	Describe the additional impacts analysis required at 20.2.74.304 NMAC.						
4	An analysis was conducted to assess the project's impacts to local soils, vegetation and visibility. Please see the attached application for more details.						
5	If required, have ozone and secondary PM2.5 ambient impacts analyses been completed? If so describe below.	Yes⊠	No□				
	Ozone and secondary PM2.5 impacts were calculated using the MERPs approach as discussed 16-M above.						

16-W: N	Modeling 1	Results								
1	If ambie required significa	If ambient standards are exceeded because of surrounding sources, a culpability analysis is required for the source to show that the contribution from this source is less than the significance levels for the specific pollutant. Was culpability analysis performed? If so describe below.			Yes□ No⊠					
2	Identify as neces	the maximum consary.	ncentrations f	rom the modeling	g analysis. Rows	may be mod	lified, add	ed and remove	d from the ta	ble below
Pollutant, Time	Facility	Modeled Concentration with	Secondary PM	Concentration	Cumulative Concentration (µg/m3)	Value of Standard (µg/m3)	Percent	Location		
Period and Standard		Surrounding Sources (µg/m3)	(μg/m3)				of Standard	d UTM E (m)	UTM N (m)	Elevatio n (ft)
H2S, 1-hr, NMAAQS	27.85	28.68	NA	NA	28.68	41.8	69	556415.70	3634620.21	3363.51
NO2, annual, NMAAQS	17.3	17.3	NA	5.0	22.3	94.02	24	556460.99	3635129.21	3365.12
NO2, 1-hr, NAAQS	174.0	174.0	NA	Varies	174.0	188.03	93	556460.99	3635129.21	3365.12
PM25, annual, NAAQS	4.4	5.6	0.11	5.9	11.6	12	96	556505.52	3635129.20	3364.43
PM25, 24-hr, NAAQS	17.9	18.4	2.59	13.4	34.4	35	98	556505.52	3635129.20	3364.43
SO2, 1-hr, NAAQS	157.0	157.0	NA	5.3	162.3	196.4	83	556300.00	3634300.00	3367.84
NO2, Annual, Increment	17.2	24.7	NA	NA	24.7	25	99	556505.52	3635129.20	3364.43
SO2, 24-hr, Increment	63.5	67.1	NA	NA	67.1	91	74	556375.48	3635087.04	3366.43
NH3, 8-hr, Toxics	32.3	32.3	NA	NA	32.3	180	18	556380.79	3635023.79	3365.84
H2SO4, 8-hr, Toxics	4.9	4.9	NA	NA	4.9	10	49	556300	3634900	3366.62

16-X: Summary/conclusions

A statement that modeling requirements have been satisfied and that the permit can be issued.

A dispersion modeling analysis was conducted for the HollyFrontier Navajo Artesia refinery. The model was conducted according to NMED and EPA policies and practices using the latest EPA-approved models. The models demonstrate compliance with all applicable ambient air quality standards.

AIR DISPERSION MODELING FOR HOLLYFRONTIER NAVAJO REFINING LLC IN ARTESIA, NEW MEXICO



Prepared for: HollyFrontier Navajo Refining LLC 501 E. Main St, Artesia, NM 88210

Prepared by: RTP Environmental Associates, Inc. 304A West Millbrook Road Raleigh, North Carolina 27609

Original Submittal September 2021 Updated January 2022



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1.0 INTRODUCTION

This document presents the results of the air quality dispersion modeling analysis conducted for HollyFrontier Navajo Refining LLC ("HollyFrontier") for its petroleum refinery in Artesia, New Mexico. This analysis was conducted in support of an air quality constructon permit application submitted to correct several permit conditions and to authorize changes to several emissions units. This analysis has been conducted by RTP Environmental Associates, Inc. ("RTP") on behalf of HollyFrontier.

The analysis evaluated emissions of the criteria and toxic air pollutants regulated under the applicable provisions of the New Mexico Administrative Code ("NMAC"). The New Mexico Air Quality Bureau ("AQB") requires an analysis of air quality standards with any construction permit application. The ambient standards that evaluated include the National Ambient Air Quality Standards ("NAAQS"), New Mexico Ambient Air Quality Standards ("NMAAQS"), Prevention of Significant Deterioration ("PSD") increments, and toxic air pollutants subject to 20.2.72.403.A(2).

This analysis conforms with the modeling procedures outlined in the Environmental Protection Agency's <u>Guideline on Air Quality Models</u>¹ ("Guideline" or "Appendix W"), the AQB's <u>Air Dispersion Modeling Guidelines</u>², and associated EPA modeling policy and guidance. The analysis also conforms with the modeling protocol submitted to the AQB and Federal Land Managers ("FLMs") on May 26, 2021 and approved, with a requested revision to the proposed treatment of intermittent emissions, by the AQB on August 2, 2021. No comments on the protocol were received from the FLMs.

RTP had proposed to exclude emergency engines and firewater pumps that emit intermittently from the demonstration of compliance with the 1-hr standards. The AQB stated that these sources should be included unless they were exempt from permitting. HollyFrontier has therefore elected to request an exemption from permitting for the emergency engines. The firewater pumps have been included in the 1-hr modeling demonstrations.



2.0 PROJECT DESCRIPTION

The Artesia Refinery occupies approximately 466 acres and has a crude oil capacity of 100,000 barrels per day. The Refinery has been in operation since the mid-1920s when oil wells were first drilled in southeastern New Mexico. The Refinery can process heavy, sour and light, sweet crude oils and runs a predominant slate of Permian Basin crudes that are gathered in West Texas and Southeast New Mexico. The refinery can also source a variety of crude oils from Cushing, Oklahoma including Canadian crudes.

With the permit application, HollyFrontier is requesting revisions to existing emission limits and other permit terms for several permitted emissions units; to add existing, unpermitted emissions units to the permit; to add permitted emission rates to the permit for certain emissions units from which not all emitted pollutants have previously been permitted; to authorize changes to the refinery's flares, including increases in emission limits; and to authorize changes in changes in fuel composition for three process heaters. The flare project is a major modification for VOC. None of the requested changes are major modifications under the PSD program for any pollutant other than VOC. However, several of the emission limits for which HollyFrontier is requesting revisions were considered in the impact analyses for two historical major modifications at the Artesia Refinery: The GOHT Project authorized by Permit No. 0195-M15, which was a major modification for emissions of CO and NOx, and the Refinery Expansion Project authorized by Permit No. PSD-NM-0195-M25, which was a major modification for emissions of CO, VOC, NOx, SO₂, PM10, and PM. The air dispersion modeling analysis discussed herein therefore includes updates to the impact analyses for those two major modifications.



3.0 SITE DESCRIPTION

The Artesia Refinery is located in Eddy County, in southeastern NM, approximately 62km south of Roswell and 225km northeast of El Paso. The approximate Universal Transverse Mercator ("UTM") coordinates of the refinery are 556,690 meters east and 3,634,600 meters north (NAD 83, UTM Zone 13) at an elevation of 3400 feet above sea level. Figure 1 shows the general location of the refinery. Figure 2 shows the specific refinery location on a 7.5-minute U.S. Geological Survey ("USGS") topographic map.

Eddy County is classified as attainment or unclassified for all regulated pollutants.

The refinery is classified under the regulations governing PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC) as a major stationary source.



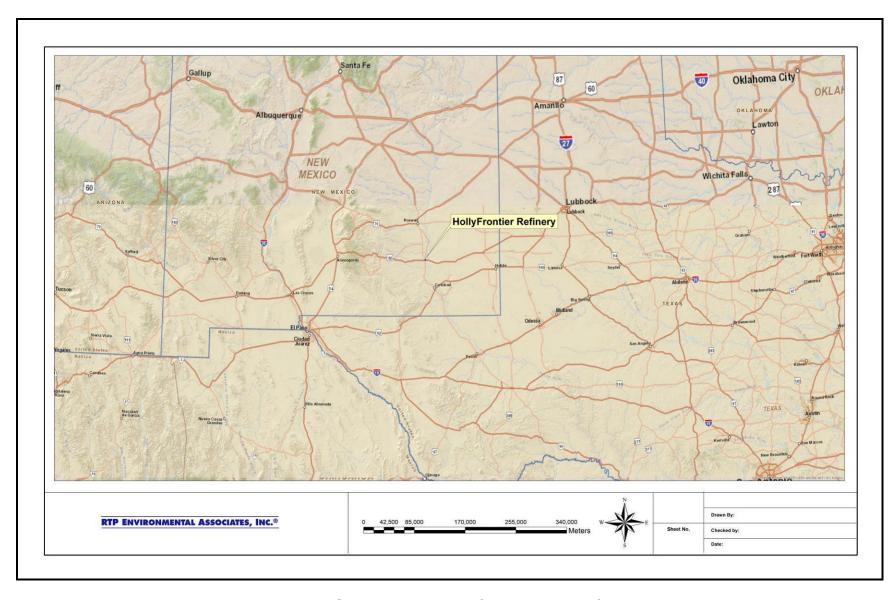


Figure 1. General Location of the Artesia Refinery



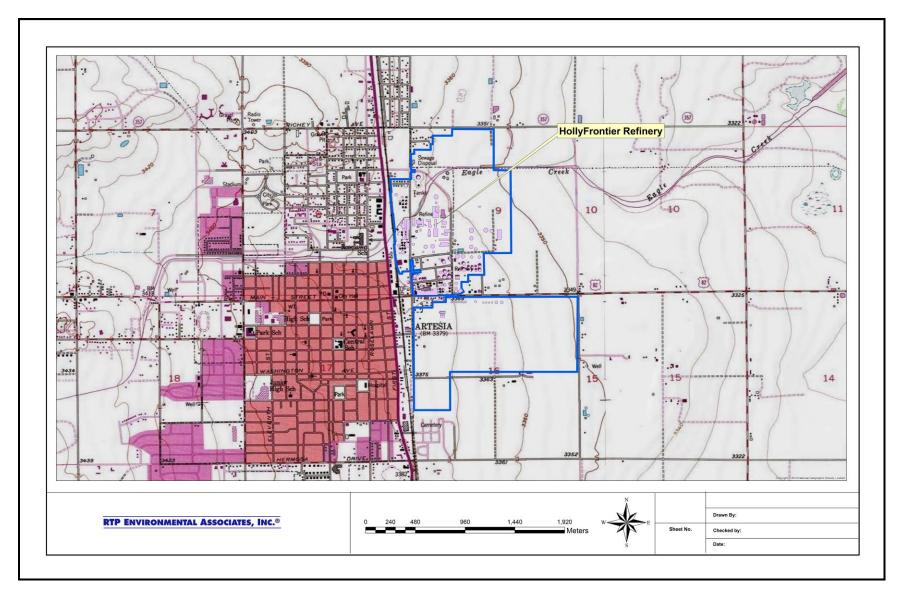


Figure 2. Specific Location of the Artesia Refinery



4.0 CLASS II AREA MODEL SELECTION AND MODEL INPUT

4.1 Model Selection

The latest version of the AMS/EPA Regulatory Model (AERMOD, Version 21112) was used to conduct the near-field dispersion modeling analysis. The modeling protocol stated that AERMOD Version 19191 would be used. However, EPA released an updated version of the model after the protocol was submitted. RTP has elected to use the most recent version of AERMOD in the analysis.

AERMOD is a Gaussian plume dispersion model that is based on planetary boundary layer principles for characterizing atmospheric stability. The model evaluates the non-Gaussian vertical behavior of plumes during convective conditions with the probability density function and the superposition of several Gaussian plumes. AERMOD is a modeling system with three components: AERMAP is the terrain preprocessor program, AERMET is the meteorological data preprocessor and AERMOD includes the dispersion modeling algorithms.

AERMOD is an appropriate model for calculating ambient concentrations near the Artesia Refinery based on the model's ability to incorporate multiple sources and source types. The model can also account for convective updrafts and downdrafts and meteorological data throughout the plume depth. The model also provides parameters required for use with up to date planetary boundary layer parameterization. The model also has the ability to incorporate building wake effects and to calculate concentrations within the cavity recirculation zone. All model options were selected as recommended in the EPA Guideline on Air Quality Models.

Oris Solution's BEEST Graphical User Interface ("GUI") was used to run AERMOD.

The GUI uses an altered version of the AERMOD code to allow for flexibility in the file naming convention. The dispersion algorithms of AERMOD are not altered. Therefore,



a model equivalency evaluation pursuant to Section 3.2 of Appendix W was not warranted.

The VISCREEN model is designed to assist in the evaluation of plume visual impacts as required under PSD. The model implements the visibility calculation procedures as outlined in the EPA's Workbook for Visual Impact Screening and Analysis.³ VISCREEN was used to assess the potential for the 2001 and 2007 major modifications to cause a visual plume within 50km of the proposed facility.

For more distant locations (i.e., areas located in excess of 50km from the proposed site), the AERMOD and VISCREEN models are not appropriate as the steady state assumptions in the models tend to degrade. Therefore, the EPA-approved version of the CALPUFF model (Version 5.8.5) was used to assess pollutant concentrations, deposition rates, and the potential for visibility impacts at these distant locations, namely PSD Class I areas. The CALPUFF modeling methodology is discussed in Section 6 of this report.

4.2 <u>Model Control Options and Land Use</u>

AERMOD was run in the regulatory default mode for all pollutants with the default rural dispersion coefficients. The use of rural dispersion coefficients is supported by the Land Use Procedure consistent with subsection 7.2.1.1.b.i of the Guideline and Section 5.1 of the AERMOD Implementation Guide. The USGS 2016 National Land Cover Data ("NLCD") within 3km of the site were converted to Auer 1978 land use types and evaluated.⁴ It was determined that the land use in the vicinity of the refinery is predominantly rural as defined by Auer (less than 50% of the area is classified as urban - Figure 3). Only the red and dark red regions in Figure 3 (NLCD categories 23 and 24) are considered urban.



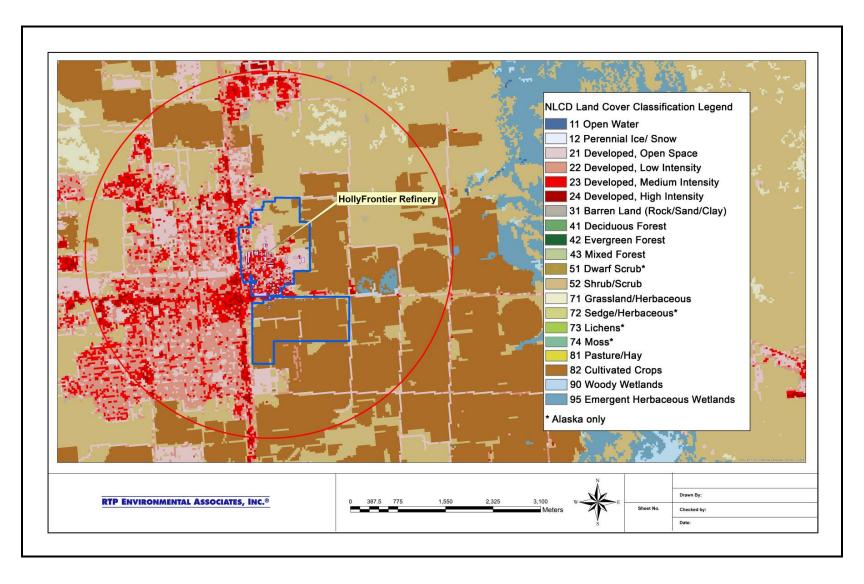


Figure 3. Land Use within Three Kilometers (Three Kilometer Radius Shown as Red Circle)



4.3 Source Data

Source Characterization

Point Sources

Most emission sources at the refinery vent to stacks with well-defined openings. These sources were modeled as point sources in AERMOD. Several other types of sources such as fugitive emissions from storage tanks and equipment leaks also required evaluation.

Fugitive Emissions

Fugitive emissions are those that are not emitted from a well-defined opening. These were modeled as volume sources. The initial dispersion coefficients (sigma y and sigma z) were calculated based upon the dimensions of the area of release and the equations contained in Table 3-1 of the AERMOD <u>User's Guide</u>.

All source locations were based upon a NAD83, UTM Zone 13 projection.

Flares

There are eight flares at the refinery for which emissions during periods of malfunction may exceed those during routine operation, including startup and shutdown periods. Malfunction emissions are not required to be modeled per 40 CFR Part 51 Appendix W. Emissions during startup or shutdown (i.e., non-emergency flaring) and other foreseeable operations were modeled using the proceedures outlined in the EPA's AERSCREEN manual⁵. These proceedures are slightly different than those contained in the AQB's Modeling Guidelines; however, the AQB approved of the AERSCREEN method on May 20, 2021. The effective stack height (H, in meters) was calculated as a function of heat release rate according to the following equation, where Q is the heat release rate of the flare in calories per second:

$$H_{\text{equivalent}} = H_{\text{actual}} + 4.56 \times 10^{-3} \times (Q)^{0.478}$$



The effective flare diameter (d, in meters) was calculated as a function of heat release rate according to the following equation, where Q is the heat release rate of the flare in calories per second:

$$d_{equivalent} = 9.88 \times 10^{-4} \times ((Q \times (1-0.55))^{0.5})$$

An exit temperature of 1273K and velocity of 20 m/sec was assumed.

All modeling input data, including the volume source and flare parameter calculations can be found in Attachment A to this report.

Good Engineering Practice Stack Height Analysis

A Good Engineering Practice ("GEP") stack height evaluation was conducted to determine appropriate building dimensions to include in the model. Procedures used were in accordance with those described in the EPA <u>Guidelines for Determination of Good Engineering Practice Stack Height (Technical Support Document for the Stack Height Regulations-Revised)</u>⁶. GEP formula stack height, as defined in 20.2.72.300 NMAC and in 40 CFR 51, is expressed as GEP = H_b + 1.5L, where H_b is the building height and L is the lesser of the building height or maximum projected width. Building/structure locations were determined from refinery construction drawings and prior modeling submissions. The structure locations and heights were input to the EPA's Building Profile Input Program ("BPIP-PRIME") computer program to calculate the direction-specific building dimensions needed for AERMOD. The Artesia Refinery plot plan and the ambient air boundaries are shown in Figure 4. A three dimensional rendering of the refinery is shown in Figure 5. All stacks and significant structures were included in the BPIP runs.



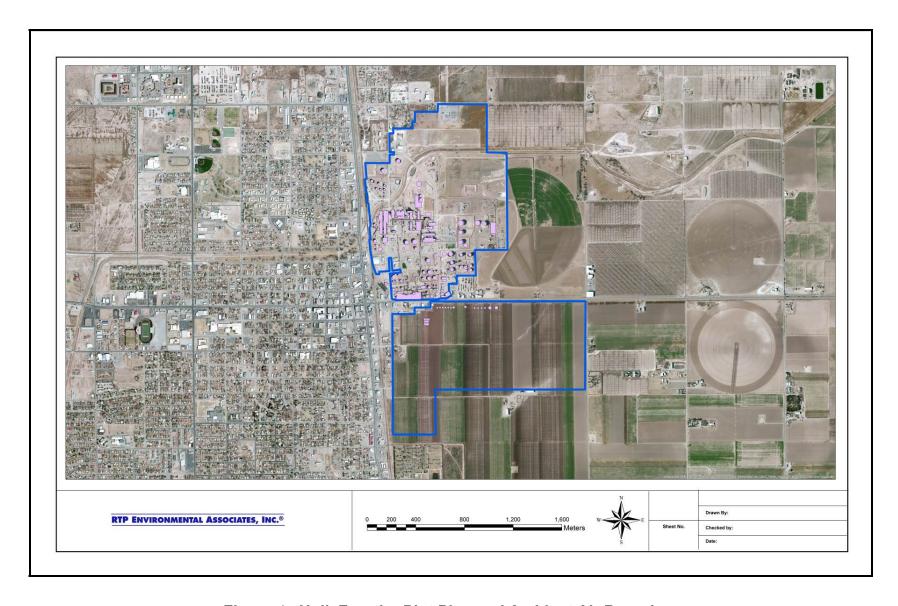


Figure 4. HollyFrontier Plot Plan and Ambient Air Boundary



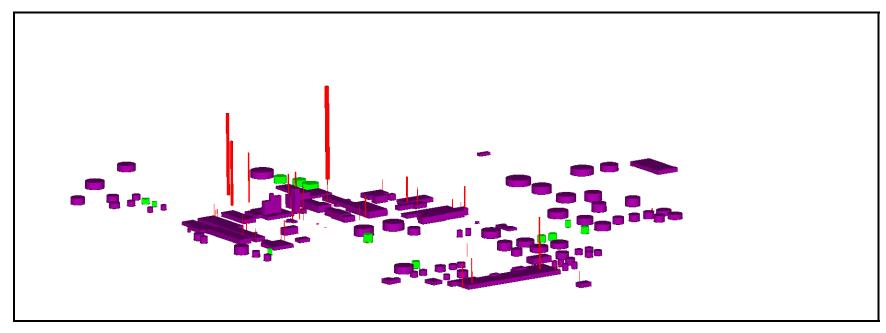


Figure 5. Artesia Refinery Three-Dimensional Plot Plan (View from SW)



4.4 Monitored Background Data

Ambient, background pollutant concentrations are needed to establish a representative background concentration to complete the NAAQS portion of the *Source Impact Analysis* of 20.2.74.303.B NMAC and 40 CFR § 52.21(k). The background concentrations are added to the modeled concentrations to assess NAAQS compliance. Ambient pollutant concentrations are also needed to fulfill the *Air Quality Analysis* requirement of 20.2.74.306.A NMAC and 40 CFR § 52.21(m), as discussed in Section 5.3 herein.

The AQB has recommended background concentrations established for New Mexico. These values are provided in the <u>Air Dispersion Modeling Guidelines</u> and were used in this analysis. These data satisfy the criteria provided in EPA's <u>Ambient Monitoring</u> Guidelines⁷ as being representative of the HollyFrontier site.

The background data employed are presented in Table 1.

Table 1. Background Concentrations

Pollutant	Averaging Time	Value (µg/m³)	Monitor Location
СО	8-hr	1524	Del Norte High School
	1-hr	2203	301001
NO ₂	Annual	5.0	Outside
1,02	1-hr	See Table 2	Carlsbad
PM ₁₀	24-hour	100.7	Eastern NM,
PM ₂₅	24-hour	13.4	Hobbs
	Annual	5.9	
О3	1-hour	150.5	

A range of monitored background NO₂ values that consider seasonal and diurnal variation was used to assess compliance with the 1-hr NO₂ NAAQS. These seasonal



values reflect the three year average of the 98th percentile value by hour of day and by season. Data from the Carlsbad monitor (AQS No. 35-015-1005) were used. Since the 2020 monitor values were not available, the lastest three years (2017-2019) were used. These seasonal NO₂ values (Table 2) were added to the modeled value within AERMOD.

Table 2. Carlsbad 98% Hourly NO₂ (ppb) By Season and Hour of Day

Model Ending				
Hour	Winter	Spring	Summer	Fall
01	24.67	13.67	10.67	19.00
02	23.00	15.33	13.33	17.33
03	21.67	15.67	14.33	20.67
04	25.33	16.33	14.67	22.67
05	23.33	19.00	15.33	22.00
06	24.67	20.67	16.67	21.67
07	24.67	21.33	17.67	19.67
08	21.33	18.33	14.33	19.00
09	20.00	14.67	14.33	18.67
10	20.00	12.00	10.67	16.00
11	18.00	10.33	7.67	14.00
12	16.33	8.00	5.33	12.00
13	15.67	7.33	5.00	11.00
14	12.00	5.67	4.33	10.33
15	12.33	5.33	4.00	9.33
16	14.67	5.00	3.33	8.67
17	18.00	4.67	3.33	11.00
18	20.00	6.33	4.00	12.33
19	18.33	10.33	6.67	12.00
20	16.00	11.67	9.67	12.00
21	15.67	10.33	10.67	12.67
22	19.00	10.00	11.00	14.33
23	21.33	10.00	10.00	14.67
24	23.33	10.33	10.33	19.00

4.5 Receptor Data

Modeled receptors were placed in all areas considered as "ambient air" pursuant to 40 CFR § 50.1(e). Ambient air is defined as that portion of the atmosphere, external to



buildings, to which the general public has access. Approximately 8,200 receptors were employed. The receptor grid consisted of three cartesian grids and receptors spaced at 25m intervals along the ambient boundary. The first cartesian grid extended to approximately 2.5km from the boundary in all directions. Receptors in this region were spaced at 100m intervals. The second grid extended to 7.5km. Receptor spacing in this region was 250m. The third grid extended to 10km with a spacing of 500m. The receptor grid was designed such that maximum impacts fall within the 100m spacing of receptors. The receptor grid spacing is presented in Table 3.

Table 3. Receptor Grid Spacing

Receptor Spacing (m)	Distance from Fence (m)
100	2,500
250	7,500
500	10,000

The Artesia Refinery is located in southeastern New Mexico. The terrain in the area is generally flat. Receptor elevations and hill height scale factors were calculated with AERMAP (18081). The elevation data were obtained from one arc-second National Elevation Data ("NED") obtained from the USGS. Locations were based upon a NAD83, UTM Zone 13 projection. The near-field receptor grid is presented in Figure 6.

4.6 Meteorological Data

Data Selection and Processing

The 2016-2020, 5-year sequential hourly surface meteorological data collected at the National Weather Service ("NWS") station in Artesia, NM (WBAN No. 03035) and upper air data from Midland, TX (WBAN No. 23023) were used in the near-field modeling analysis performed using AERMOD. These data were processed into a "model-ready" format using the latest version of AERMET (version 21112).



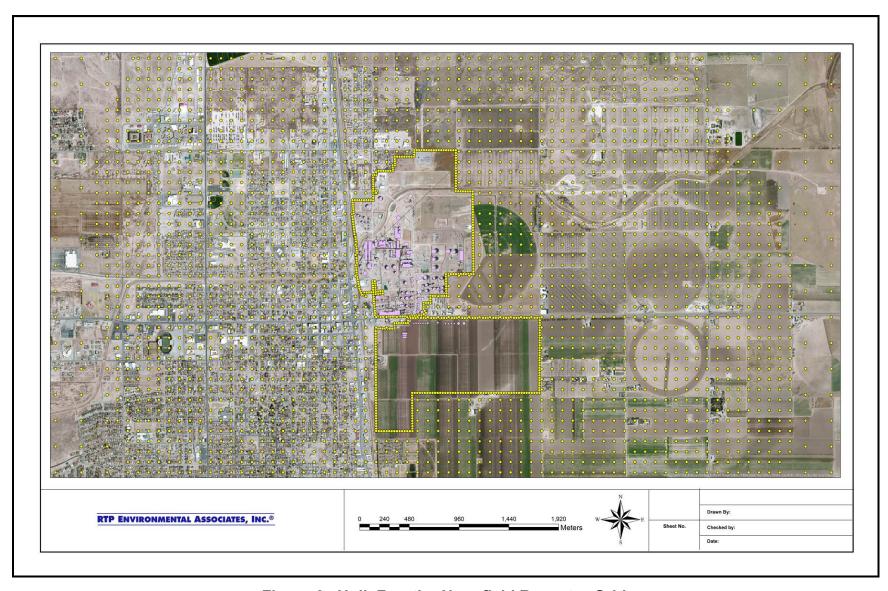


Figure 6. HollyFrontier Near-field Receptor Grid



In AERMET Stage 1, the Artesia surface meteorological data in the Integrated Surface Data ("ISD") format were extracted. Midland upper air meteorological data in the Forecast Systems Laboratory ("FSL") format were also extracted.

The AERMET meteorological processor requires estimates of the following surface characteristics: surface roughness length, albedo, and Bowen ratio. The surface roughness length is related to the height of obstacles to the wind flow. It is the height above the surface where the average wind speed is zero. The smoother the surface, the lower the roughness length. The surface roughness length influences the surface shear stress and is an important factor in calculating mechanical turbulence and stability. The albedo is the fraction of the total incident solar radiation reflected by the surface back to space without absorption. The Bowen ratio is an indicator of surface moisture and is the ratio of the sensible heat flux to the latent heat flux. The albedo and Bowen ratio are used for determining the planetary boundary layer parameters for convective conditions due to the surface sensible heat flux. RTP developed estimates of the surface characteristics using EPA's AERSURFACE program (Version 20060). A 1km search radius was employed at the location of the meteorological tower. Twelve sectors of 30 degrees each and seasonal resolution were used in the AERSURFACE analysis. The default season definitions were used with no continuous snow cover for one or more months during the winter and dry moisture. The "ADJ U*" option to allow for adjustments to the friction velocity under low wind speeds was employed. The 2016-2020 wind rose is shown in Figure 7.



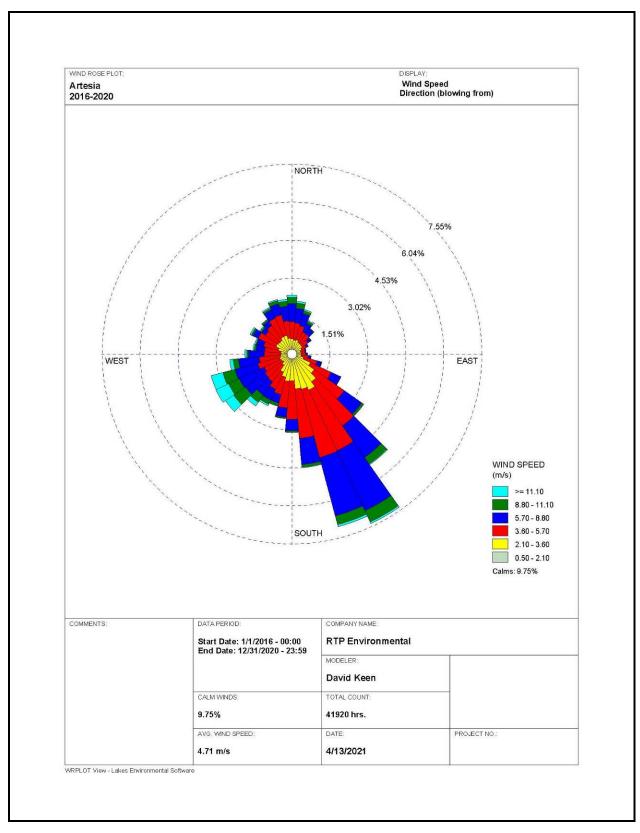


Figure 7. 2016-2020 Artesia Windrose



5.0 CLASS II AREA MODELING METHODOLOGY

5.1 Pollutants Subject to Review

The proposed permitting action will potentially allow for an increase in emissions of all criteria pollutants, with the exception of lead, as well as H₂S and two air toxics: ammonia and sulfuric acid mist. HollyFrontier has therefore elected to conduct a facility wide model for all pollutants using the requested permit to emit rates. Since precursor VOC emissions will also increase, ozone impacts were addressed.

5.2 Significant Impact Analysis

The criteria pollutant air quality analysis was conducted in two phases: an initial or significant impact analysis, and a refined phase including an increment analysis and a NAAQS/NMAAQS analysis. In the significant impacts analysis, the calculated maximum impacts associated with the project were determined for each pollutant. These impacts determined the net change in air quality resulting from the proposed modification. Five years of meteorological data were used in the significant impact analysis. Maximum modeled concentrations were compared to the pollutant-specific significance levels for all pollutants and averaging times except for the 1-hour NO₂, SO₂ and 24-hr PM2.5 impacts. For these pollutants and averaging times, the five-year average of the maximum impact at each receptor were used to assess significance. The PSD Class II and AQB Significant Impact Levels are listed in Table 4.



Table 4. PSD Class II and AQB Significant Impact Levels

Pollutant	Averaging Time	PSD Class II Significant Impact Levels (µg/m³)
CO	1-hour	2,000
	8-hour	500
H ₂ S	1-hour	5.0
PM10	24-hour	5.0
	Annual	1.0
PM2.5 ^a	24-hour	1.2
	Annual	0.3
NO ₂	1-hour	7.52 ^b
	Annual	1.0
SO ₂	1-hour	7.8 ^b
	3-hour	25.0
	24-hour	5.0
	Annual	1.0
O ₃	8-hour	1.96

^aPlease note that on January 22, 2013, the US Court of Appeals for the District of Columbia Circuit Court granted a request from the EPA to vacate and remand the PM_{2.5} SILs codified in the federal PSD rule. EPA modeling guidance (August 1, 2016), issued subsequent to the remand, continues to recommend use of the SILs listed above to justify permitting decisions for PM2.5 NAAQS and increment evaluations.

Pollutants with impacts that exceeded the ambient air significance levels, as defined in 40 CFR 51.165, were included in both the NAAQS/NMAAQS and increment analyses. In these latter analyses, impacts from the Artesia Refinery were added to concentrations calculated from other nearby PM10, PM2.5, SO₂ and H₂S sources, plus a regional background concentration (for the NAAQS/NMAAQS analysis only). The resultant total concentration was compared to the NAAQS/NMAAQS and increments to determine compliance.

5.3 <u>Preconstruction Monitoring</u>

In order to satisfy the requirement for an air quality analysis pursuant to 20.2.74.306.A NMAC and 40 CFR § 52.21(m)(1), HollyFrontier used the AQB's recommended background values discussed in Section 4.4 herein. HollyFrontier requested that the

^bThere are no 1-hr NO₂ or SO₂ SILs promulgated at 40 CFR 51.165. The EPA proposed interim SILs for NO₂ of 4ppb and SO₂ of 3ppb will be used.



existing ambient monitoring data be allowed for use in lieu of site-specific preconstruction data.

5.4 Nearby Source Inventories

Off-site sources were included in the H₂S, SO₂, PM2.5, PM10 NAAQS/NMAAQS analyses as well as the increment analyses. Modeled impacts from the nearby sources were added to impacts from HollyFrontier in assessing compliance. Prior to the most recent 2017 Appendix W (40 CFR Part 51) revisions, the maximum distance to a significant impact plus 50km was historically used as a radius to define the screening area. The most recent Appendix W modeling guideline now states that professional judgment must be exercised in assessing sources to be included in the modeling analysis. Appendix W as well as the NM Modeling Guidelines further state that the number of nearby sources explicitly modeled in the air quality analysis is expected to be few, except in unusual situations, and that these sources will typically be located within the first 10-20 kilometers from the proposed source (see January 17, 2017, 82 Federal Register 5182 at page 5221).

The AQB provided RTP Environmental with the offsite source inventories required to conduct the analyses. HollyFrontier modeled all SO₂, PM10, and PM2.5 sources located within 10km of the refinery. Background concentrations adequately represent any PM10/PM2.5 sources beyond 10km. No nearby sources were modeled in the NAAQS/NMAAQS for the remaining pollutants as the background values also adequately represent impacts. For the H₂S and increment analysis where backgound concentrations are not considered, all sources located within 25km of the refinery as well as any large sources (1,000 lb/hr) located within 50km of the refinery were modeled.

5.5 NAAQS/NMAAQS Analysis

A refined air quality analysis to determine compliance with the NAAQS/NMAAQS was conducted. As stated, this analysis was conducted to determine compliance with the



NAAQS/NMAAQS for all regulated pollutants with impacts that exceeded the significant impact levels. Lead emissions were not evaluated because the facility does not have appreciable lead emissions. Each new or modified source's potential emission rate was used. Average emissions were used for the existing FCC regenerator, which is not part of the project, in assessing NAAQS compliance. Average emissions are allowed to be modeled for non-modified units pursuant to Table 8-2 of the EPA's Modeling Guideline (Appendix W).

Only those receptors showing a significant impact were modeled for NAAQS/NMAAQS compliance. In assessing NAAQS/NMAAQS compliance for most pollutants, the AQB allows for applicants either to model nearby sources or to use a background concentration to represent impacts from the nearby sources. The AQB, however, recommends inclusion of both nearby sources located within 10km of the refinery and background in assessing PM2.5 and PM10 compliance. The form of the modeled values and whether nearby sources or background were included to assess NAAQS/NMAAQS compliance are shown in Table 5. The more stringent of either the NAAQS or NMAAQS are shown in Table 6. These are the standards HollyFrontier used to assess compliance. Modeling was not conducted for the SO₂ 24-hour NAAQS eventhough significant impacts were calculated because the AQB considers a compliance demonstration using the 1-hr standard as a surrogate for compliance with the 24-hr standard.



Table 5. Form of Modeled Values Used to Assess NAAQS/NMAAQS Compliance

Pollutant	Averaging Time	Add Background Concentration or Include Nearby Sources	Modeled Value
CO	8-hour	Background	Maximum
	1-hour	Background	Maximum
H ₂ S	1-hour	Nearby Sources	Maximum
NO ₂	Annual	Background	Average
	1-hour	Background	98 th percentile max daily 1-hour
PM2.5	Annual	Both	Average
	24-hour	Both	98 th percentile
PM10	24-hour	Both	High 6 th high
SO ₂	1-hour	Background	99 th percentile max daily 1-hour

Table 6. National and New Mexico Ambient Air Quality Standards

Pollutant	Averaging Time	Ambient Air Quality Standards (µg/m³)
CO	8-hour	9,960.1
	1-hour	14,997.5
H ₂ S	1-hour	41.8
NO ₂	Annual	94.02
	1-hour	188.03
O ₃	8-hour	137.3
PM2.5	Annual	12
	24-hour	35
PM10	24-hour	150
SO ₂ ^a	1-hour	196.4

^aModeling not required for the other SO2 averaging periods if compliance can be demonstrated with the 1-hour standard.



5.6 **PSD Increment Analysis**

The Artesia Refinery is located in Air Quality Control Region No. 155. The PSD Minor Source Baseline dates have been triggered in this baseline area for all pollutants. NO₂ was triggered 3/16/1988, SO₂ was triggered 7/28/1978, PM10 was triggered 8/4/1978, and PM2.5 was triggered 11/13/2013. The Artesia Refinery was constructed in the mid-1920's and modifications have been made since the increment trigger dates for all pollutants except PM2.5. Increment compliance was therefore evaluated for all pollutants except PM2.5. As a conservative means of assessing increment compliance, HollyFrontier modeled potential emissions from all sources at the refinery. Only those receptors showing a significant impact were modeled for increment compliance.

Compliance with the PSD increments was based on the cumulative impacts of the Artesia Refinery and other increment consuming sources identified in the nearby source emissions inventory. All nearby sources located within 25km of the refinery and any large (>1000 lb/hr) sources within 50km of the refinery were included in the Class II increment demonstration. The resultant cumulative impacts were compared to the PSD Class II increment levels. The highest modeled annual averages was used for evaluating compliance with the annual increments and the <a href="https://example.com/high-second-hi

The PSD Class I and Class II increments are shown in Table 7.



Table 7. PSD Class I and II Increments

Pollutant	Averaging Time	PSD Class I Increment (µg/m³)	PSD Class II Increment (µg/m³)
NO ₂	Annual	2.5	25
PM2.5	Annual	1	4
	24-hour	2	9
PM10	Annual	4	17
	24-hour	8	30
SO ₂	Annual	2	20
	24-hour	5	91
	3-hour	25	512

5.7 <u>Secondary PM2.5 Analyses</u>

On February 10, 2020, the USEPA issued draft guidance for assessing ozone and fine particulate matter modeling.⁸ The guidance addresses both primary and secondary PM2.5 impacts. Primary PM2.5 impacts refer to the impacts due to direct emissions of PM2.5. Secondary impacts refer to the PM2.5 impacts attributable to nitrates and sulfates formed due to precursor NO₂ and SO₂ emissions. The AQB's Guidelines, which follow EPA's, were followed in assessing secondary PM2.5 impacts. Specifically, the following Modeled Emission Rates for Precursors ("MERPs") values and equations was used:

PM2.5 Annual (
$$\mu$$
g/m³) = ((NOx (tpy)/3184) + (SO₂ (tpy)/2289)) x 0.2 PM2.5 24-hr (μ g/m³) = ((NOx (tpy)/1155) + (SO₂ (tpy)/225)) x 1.2

The calculated secondary PM2.5 impacts were added to the modeled concentrations to assess significant impacts as well as compliance with the NAAQS/NMAAQS and increments.

5.8 O₃ Analyses

Ozone impacts were calculated using the AQB's Guidelines, which follow the EPA's MERPS guidance. Specifically, the following values and equations was used:

Ozone 8-hour (μ g/m3) = ((NOx (tpy)/184) + (VOC (tpy)/1049)) x 1.96



The calculated secondary O_3 impacts were compared to the O_3 significant impact level of 1.96 $\mu g/m^3$ or 1 ppb.

5.9 NO₂ Analyses

Following USEPA and AQB guidance, the NO₂ modeling analyses employed the recommended three tier screening approach. Initially, Tier 1 was employed with the conservative assumption that 100% of the available NOx converts to NO₂. Based on these results, HollyFrontier employed Tier 2 (the Ambient Ratio Method, ARM2) with the EPA default minimum and maximum ambient ratios of 0.5 and 0.9, respectively. Tier 3 was not employed. Tier 3 accounts for the chemical reactions that convert NOx to NO₂ in the presence of ozone.

5.10 Air Toxics Analysis

HollyFrontier conducted modeling for two toxic air pollutants, ammonia and sulfuric acid mist, which are emitted in excess of the levels specified in 20.2.72.502 NMAC – Permits for Toxic Air Pollutants. Maximum 8-hour impacts were compared to one-one hundredth of the Occupational Exposure Level ("OEL") listed in 20.2.72.502 NMAC.

5.11 Class II Visibility Analysis

In addition, a Class II visibility analysis was conducted using the VISCREEN model. The Living Desert State Park, which is located a minimum of 42km and a maximum of 49km south of the Artesia Refinery was used as an indicator of potential Class II visibility impacts. First level screening values of 1.00 for the color parameter ("delta E") and 0.02 for the contrast parameter ("C") were used. A background visible range of 110km was also used. This background visual range is recommended as the default value according to EPA's Workbook for Plume Visual Impact Screening and Analysis.⁹



6.0 CLASS I AREA ANALYSIS

6.1 Class I AQRV Analysis

There are five Class I areas located within 300km of the Artesia Refinery: Carlsbad Caverns, Guadalupe Mountains, White Mountains Wilderness, Salt Creek Wilderness, and Bosque del Apache (Figure 8). ¹ The closest Class I area is the Carlsbad Caverns National Park which is located 73km to the south. The Federal Land Manager's ("FLM") Q/D (maximum daily emissions in tons per year over distance in kilometers) method has been used to determine the potential for adverse Class I impacts for each Class I area (Table 8). We have presumed that no Class I Air Quality Related Values ("AQRV") evaluation was required for the Class I areas with calculated Q/D values below 10. Project emission estimates reveal a maximum annual, total SO₂, H₂SO₄, NOx and PM₁₀ emission rate of 787 tons per year which results in the Q/D values shown in Table 5. Annual emissions were calculated as the maximum daily emissions and 365 day/yr operation.

Table 8. Calculated Q/D Values for Each Class I Area

Class I	Map ID	Minimum Distance from the SRP Facility (km)	Maximum Distance from the SRP Facility (km)	Q/D
Bosque del Apache	bosq	245.1	259.6	3.2
Carlsbad Caverns	cave	73.8	93.9	10.7
Guadalupe Mountains	gumo	101.3	123.6	7.8
Salt Creek	sacr	79.1	84.7	9.9
White Mountain	whmo	134.2	153.4	5.9

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¹ Class I areas are pristine areas (e.g., National Parks and Wilderness Areas) that have been designated by Congress and are afforded a greater degree of air quality protection. All other areas are designated as Class II areas.



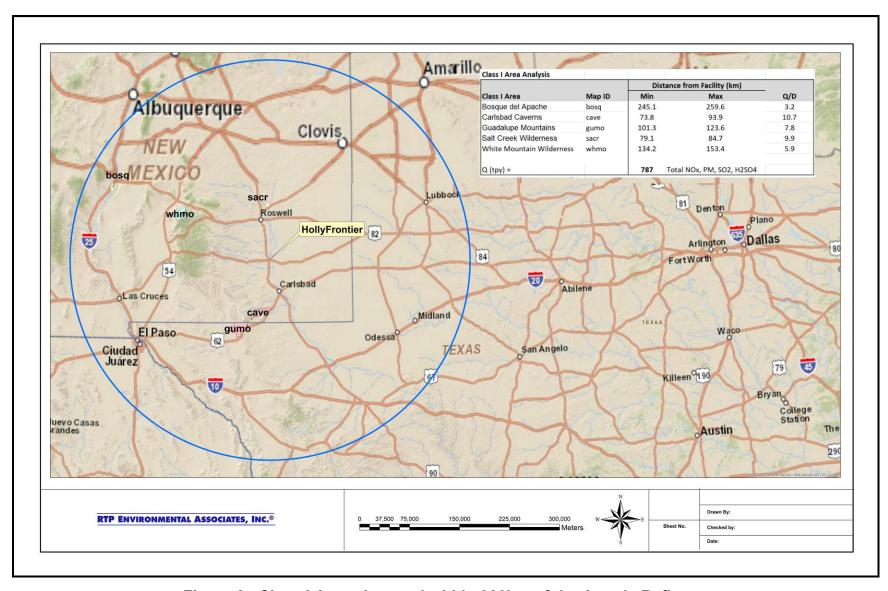


Figure 8. Class I Areas Located within 300km of the Artesia Refinery



For the Class I area, Carlsbad Caverns, with the Q/D values in excess of 10, AQRVs were calculated. Visibility and sulfur and nitrogen deposition were calculated using techniques prescribed by the Guideline for Air Quality Models (40 CFR 51, Appendix W), the EPA's Interagency Workgroup on Air Quality Modeling (IWAQM)¹⁰, and the FLM's Air Quality Related Values Work Group (FLAG) document.¹¹

6.2 Class I Increment Analysis

6.3 CALPUFF

The EPA-approved version of CALPUFF (Version 5.8) was used to assess Class I air quality impacts. The EPA-approved version of CALPUFF includes the CALMET meteorological model (Version 5.8.4, Level 130731), the non-steady-state puff model (CALPUFF, Version 5.8.5, Level 151214) with chemical transformation and deposition, and the post processors (POSTUTIL Version 1.5.6, Level 070627 and CALPOST, Version 6.221, Level 082724) for combining, converting, averaging, and ranking the concentrations, visibility impacts, and deposition.

CALMET

RTP used the Mesoscale Model Interface Program ("MMIF") Version 3.4 and the EPA's 2013-2015, 12km Weather Research and Forcasting Model ("WRF") for the Continental United States (CONUS) to develop a CALMET dataset.^b The extraction domain extended 50km beyond the Class I areas. The lower left and upper right coordinates of the extraction domain was -967.383, -923.424 and -631.767, -579.363 km, respectively (LCC, with the RPO projection). The origin was set to -972.0, -924.0km with 29 cells in each direction. The default vertical layers (ZFACE) of 0.0, 20.0, 40.0, 80.0, 160.0, 320.0, 640.0, 1200.0, 2000.0, 3000.0, 4000.0m were employed. MMIF was run in pass-through mode using the "CALSCI MIXH WRF" option.

-

^b Please note that the most current version of MMIF is Ver. 3.4.1. This version will not read WRF files larger than 2 gigabytes. The WRF data files in RTP's possession are 12gb. The only difference between versions 3.4 and 3.4.1 is 3.4.1's ability to estimate cloud cover. Lack of such estimates should not appreciably affect CALPUFF results.



Modeled Emissions

The Artesia Refinery's primary emission sources are refinery fuel gas-fired heaters. There are also several flares and a fluid catalytic cracking unit. The National Park Service ("NPS") PM speciation calculation for combustion turbines ("CTs") was employed for the gas fired units. This calculation assumes that all of the estimated PM emissions have an aerodynamic diameter of less than 1 micron and that 25% of the PM is filterable and 75% is condensable. All of the filterable PM is assumed to be elemental carbon. All of the condensable PM was assumed to be soluble organic carbon (SOA), while one third of the SO₂ emissions were assumed to be sulfate (SO₄).

CALPUFF Technical Settings

CALPUFF was run using the FLM-approved default parameters where available. These options generally follow EPA's Guideline on Air Quality Models (40 CFR 51, Appendix W) and the IWAQM Phase 2 guidance. The regulatory default switch was used (MREG = 1).

The Class I area receptors modeled were obtained from the NPS. Lambert-Conformal Conic (LCC) Coordinates were used with an origin of 49.0N and 97.0W and Standard Parallels of 33.0N and 45.0N (the RPO projection).

The modeling domain and Class I receptors are shown in Figure 9.

Ozone and Ammonia

Hourly background ozone concentrations were input to CALPUFF. The ozone observations were collected at the Carlsbad monitor (AQS No. 35-015-1005) concurrent with the three years of WRF data. Missing values from Carlsbad were filled with data from the Hobbs monitor (AQS No. 35-025-008) located approximately 100km east of the refinery.



Ammonia is not simulated by CALPUFF, but rather a background value is specified. Ammonia is important because the level of particulate nitrate (NO₃) can depend on the amount of ammonia present. The partitioning of total nitrate between gaseous HNO₃ and particulate NO₃ depends on the amount of ammonia present and other parameters (e.g., SO₄, temperature, and RH).

In the CALPUFF simulation, one value of background is assumed across the region and each puff uses the full background value in its equilibrium calculation. The IWAQM Phase II report contains the following recommendations for background ammonia: "typical (within a factor of 2) background values of ammonia are: 10 ppb for grasslands, 0.5 ppb for forest, and 1 ppb for arid lands at 20 C" (IWAQM, 1998). Based on the fact that all of the reviewed Class I areas lie in an arid region, a background ammonia value of 1 part per billion (ppb) was used.

Natural Conditions and Monthly Relative Humidity Factors f(RH)

Natural background conditions must be established to determine a change in natural conditions related to a source's emissions. The EPA lists three types of natural background conditions in their guidance document: Annual Average, Best 20% Days, and Worst 20% Days. Based on the FLAG 2010 guidance, Annual Average Natural Visibility Conditions were used for this analysis. The EPA, in its BART Guidelines (2005), concluded that by using monthly average Relative Humidity Adjustment Factors f(RH), the likelihood that the highest modeled visibility impacts that were caused by short-term and geographically different meteorological phenomena (e.g., weather events) would be minimized. The FLAG (2010) report agreed with the EPA; therefore, the visibility analysis was conducted using monthly average f(RH) values for large hygroscopic particles, small hygroscopic particles and sea salt, rather than hourly values.



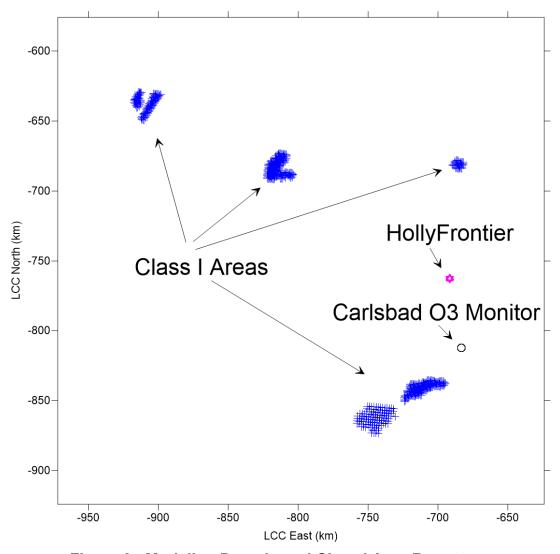


Figure 9. Modeling Domain and Class I Area Receptors



Light Extinction and Haze Impact Calculations

CALPOST was used to calculate light extinction. The EPA/IMPROVE formula will be used to calculate the change in light extinction due to increases in the particulate matter concentrations according to the following:

 $B_{\text{ext}} = 2.2 \text{ x f}_{\text{S}}(\text{RH}) \text{ x [Small Sulfates]} + 4.8 \text{ x f}_{\text{L}}(\text{RH}) \text{ x [Large Sulfate]}$

- + 2.4 x fs(RH) x [Small Nitrates] + 5.1 x fL(RH) x [Large Nitrates]
- + 2.8 x [Small Organic Mass] + 6.1 x [Large Organic Mass]
- + 10 x [Elemental Carbon]
- + 1 x [Fine Soil]
- + 0.6 x [Coarse Mass]
- + 1.7 x fss(RH) x [Sea Salt]
- + [Rayleigh Scattering]
- + 0.33 x [NO₂ (ppb)]

The concentrations, in square brackets, are in micrograms per cubic meter $\mu g/m^3$ and b_{ext} is in units of inverse mega-meters Mm^{-1} .

The values for f_s(RH), f_L(RH), f_{ss}(RH), and the Rayleigh scattering term were obtained from the 2010 FLAG Report in Tables 6, 7, 8 and 9. The assessment of visibility impacts employed CALPOST Method 8, sub-mode 5. CALPUFF assumes that all of the background ammonia is available for the formation of ammonium nitrate from each puff. However, where these puffs overlap in the model, puffs are actually in competition for the available ammonia. To prevent the overestimation of nitrate, the Ammonia Limiting Method option in the POSTUTIL processor (MNITRATE = 1) was used to compute the HNO₃/NO₃ concentration partition prior to executing the visibility calculations in CALPOST. In addition, the relative humidity in CALPOST was capped at 95% consistent with current FLM recommendations.



CALPOST calculates the change in light extinction for each 24-hour day. These results were reviewed to determine the number of days where the change in light extinction is at or above 5% change and 10% change at each Class I area.

Deposition Calculations

In addition to visibility, modeled deposition rates for total sulfur (S) and nitrogen (N) were calculated. POSTUTIL was used to summarize the total dry and wet deposition fluxes for the S and N species. Specifically, the N and S deposition was assumed to consist of the following composition of modeled species:

Total Nitrogen Flux (CSPECCMP) =

SO₄ x 0.291667

NOx x 0.304348

HNO₃ x 0.222222

NO₃ x 0.451613

Total Sulfur Flux (CSPECCMP)=

SO₂ x 0.500000

SO₄ x 0.333333

After the total N and S deposition rates were calculated in POSTUTIL, CALPOST was used to determine the average annual N and S deposition for each receptor in each Class I area. Two pollutant names were modeled in CALPUFF and passed to POSTUTIL and CALPOST. SO2 represented the maximum short term emissions from the refinery project. SO2LT represented the annual emissions increase. The SO2LT pollutant was used in the deposition analysis. SO2 was used in all other analyses. A scaling factor (A) of 316.224 was employed in CALPOST to convert the default deposition rates in units of $\mu g/m^2/sec$ to the units of kg/ha/yr needed for comparison to the Deposition Analysis Thresholds (DATs) of 0.005.

6.4 Class I Increment Analysis

Pollutant concentrations were also calculated for comparision to the proposed Class I



significance levels. CALPUFF was used to calculate concentrations at all Class I receptors located in excess of 50km from the source, regardless of Q/D. The model results were compared to the proposed Class I significant impact levels (Table 9).

Table 9. Proposed PSD Class I Significant Impact Levels

Pollutant	Averaging Time	PSD Class I Significant Impact Levels (µg/m³)
PM2.5	24-hour	0.27
	Annual	0.05
PM10	24-hour	0.30
	Annual	0.20
NO ₂	Annual	0.10
SO ₂	3-hour	1.00
	24-hour	0.20
	Annual	0.10



7.0 CLASS II ANALYSIS RESULTS

Attachment B provides the model summary output. Model input and output files, including the BPIP-PRIME and meteorological data files, are provided electronically.

7.1 Significant Impact Analysis Results

The project is expected to result in significant impacts for PM2.5, SO₂, NO₂ and H₂S (Table 10). Insignificant impacts were calculated for PM10 and O₃. Based upon the results of the significant impacts analysis, a cumulative analysis was conducted to assess compliance with the NAAQS/NMAAQS and increments.

Table 10. Class II Significant Impact Analysis Results

Pollutant	Avg Period	Maximum Modeled Impact (Including Secondary PM2.5) (μg/m³)	PSD Significant Class II Impact Level (μg/m³)	Significant Monitoring Concentration (µg/m³)	Maximum Distance to a Significant Impact (km)
PM2.5	Annual	0.42	0.2	NA	0.76
1 1012.5	24-hr	4.51	1.2	4.0	1.48
PM10	Annual	0.66	1.0	NA	NA
FIVITO	24-hr	2.13	5.0	10	NA
	1-hr	26.06	7.8	NA	10.7
SO ₂	24-hr	7.93	5.0	13	1.73
302	3-hr	22.3	25.0	NA	NA
	Annual	0.74	1.0	NA	NA
NO ₂	1-hr	35.1	7.5	14	1.82
NO ₂	Annual	2.63	1.0	NA	1.07
СО	1-hr	41.2	2000	NA	NA
	8-hr	25.4	500	575	NA
H ₂ S	1-hr	24.5	5.0	NA	0.76
O ₃	8-hr	1.69	1.96	NA	NA

NA- not applicable.



7.2 NAAQS/NMAAQS Analysis Results

Following the determination of significant impacts, an analysis was conducted to assess compliance with the NAAQS and NMAAQS for pollutants showing a significant impact. The offsite source inventories discuss in Section 5.4 were employed. Background concentrations were added to the model results to assess compliance. Evaluation of compliance with the 24-hr PM2.5 NAAQS was based on the 98th percentile of the annual distribution of daily maximum 24-hour concentrations. Compliance with the 1-hr NO₂ and SO₂ NAAQS was based on the 98th and 99th percentiles, respectively, of the annual distributions of daily maximum 1-hour concentrations. Compliance with the PM10 24-hr standard was based upon the sixth highest value. Annual NAAQS compliance was evaluated based upon the maximum modeled value. Only receptors showing significant project-related impacts were modeled in assessing compliance.

The results of the NAAQS analysis are presented in Table 11. As can be seen, the model demonstrates compliance.

Table 11. NAAQS/NMAAQS Analysis Results

Pollutant	Averaging Period	Modeled Concentration (µg/m³)	Background Concentration (µg/m³)	Total Concentration (µg/m³)	Standard (µg/m³)
H ₂ S	1-hr	28.9	NA	28.7	41.8
NO	Annual	17.3	5.0	22.3	94.02
NO ₂	1-hr	174	NA	174.0	188.0
PM2.5	Annual	5.71	5.9	11.6	12.0
FIVIZ.5	24-hour	20.99	13.4	34.4	35.0
SO ₂	1-hour	157.0	5.3	162.3	196.4

NA – not applicable. Background monitored values added within model.

PM2.5 modeled values includes secondary PM2.5 contribution.

7.3 <u>Increment Analysis Results</u>

Evaluation of compliance with the short-term increments was based upon the highestsecond-high modeled value. The maximum annual concentrations were used to assess compliance with the annual increments. All sources at the refinery were conservatively



assumed to consume increment at their potential to emit rates. Only receptors showing significant project-related impacts were modeled in assessing compliance.

The results of the increment analysis are presented in Table 12. As shown, the model demonstrates compliance.

Table 12. PSD Increment Analysis Results

Pollutant	Averaging Period	Modeled Concentration (µg/m³)ª	Standard (µg/m³)
NO_2	Annual	24.7	25
SO ₂	24-hr	67.1	91

7.4 Secondary PM2.5 Analysis

Following the the AQB's Guidelines, the MERPs calculations resulted in the following values for secondary PM2.5. These values were added to the modeled PM2.5 concentrations:

PM2.5 Annual (
$$\mu$$
g/m³) = ((NOx 240 tpy)/3184) + (SO₂ 446 tpy)/2289)) x 0.2 = **0.11** PM2.5 24-hr (μ g/m³) = ((NOx (240 tpy)/1155) + (SO₂ 446 tpy)/225)) x 1.2 = **2.6**

The calculated secondary PM2.5 impacts were added to the modeled concentrations to assess significant impacts as well as compliance with the NAAQS/NMAAQS and increments.

7.5 Ozone Analysis

Following the the AQB's Guidelines, the MERPs calculations resulted in the following estimate of ozone:

Ozone 8-hour (
$$\mu$$
g/m3) = ((NOx 240 tpy)/184) + (VOC 208 tpy)/1049)) x 1.96 = **1.69**

The calculated secondary O_3 impact was compared to the O_3 significant impact level of 1.96 μ g/m³ and determined to be insignificant.



7.6 Air Toxics

The results of the air toxics analysis for NH₃ and H₂SO₄ are presented in Table 13. Maximum 8-hour modeled impacts were compared to one-one hundredth of the Occupational Exposure Level ("OEL") listed in 20.2.72.502 NMAC. As shown, the maximum modeled impacts are less than standards.

Maximum Modeled Impact -1/100 of OEL **Avgeraging Pollutant** Period $(\mu g/m^3)$ $(\mu g/m^3)$ 8-hr NH_3 32.3 180 H_2SO_4 8-hr 4.9 10

Table 13. Air Toxics Analysis Results

7.7 Class II Visibility Analysis

The CAA Amendments of 1977 require evaluation of new and modified emission sources to determine potential impacts on visibility. The total hourly particulate matter and NO_x emissions from the project were used as input parameters in the visibility analysis. Emissions were evaluated as described in the EPA Workbook for Plume Visual Impact Screening and Analysis¹³ to determine potential contribution to atmospheric discoloration and visual range reduction.

Generally, atmospheric discoloration occurs when NO emissions from combustion sources react in the presence of atmospheric oxygen to form NO₂, a reddish-brown gas. Another form of atmospheric discoloration may be caused by particulate emissions and secondary aerosols formed by gaseous precursor emissions. The visual range reduction (increased haze) is caused primarily by particulate emissions and secondary aerosols such as sulfates and nitrates.¹⁴ Both secondary sulfate and primary particulate emissions are accounted for in the analysis. Emission of other pollutants do not materially affect visibility.



U.S. EPA visibility impairment analysis guidelines were followed in conducting the analysis. The analysis was performed for the Living Desert State Park, located a minimum of 42 km and a maximum of 49 km south of the refinery.

This analysis requires inputs of emission rates (PM and NO_X), regional visual range, distance between the source and the object of study, and worst-case dispersion parameters (i.e., wind speed and stability). Outputs from the model include:

- Plume contrast against the sky and terrain; and,
- Perceptibility of the plume (Delta E criteria).

Emission rates for PM and NOx for the analyses were set to 84.3 and 182 tons per year, respectively. The background visual range was set to 110km, which was determined from Figure 9 of the VISCREEN manual. The VISCREEN default screening values for Delta E (2.0) and contrast (0.05) were assumed.

As shown in Table 14, no exceedances of the default delta E parameter or green contrast parameters were calculated using the conservative meteorological conditions (F stability and 1 m/sec wind speed) and Level-1 procedures.

The VISCREEN input and output model files are also provided electronically...



Table 14. Level-1 Class II Visibility Analysis Results for the Living Desert State Park

Viewing	Theta	Azimuth	Distance	Alpha	Delta E		Green Contrast		
Background	(degrees)	(degrees)	(km)	(degrees)	Criterion	Plume	Criterion	Plume	
SKY	10	122	49	46	2.000	0.956	0.050	0.011	
SKY	140	122	49	46.000	2.000	0.435	0.05	-0.01	
TERRAIN	10	84	42	84.000	2.000	1.631	0.05	0.015	
TERRAIN	140	84	42	84.000	2.000	0.180	0.05	0.004	



8.0 CLASS I AREA ANALYSIS RESULTS

8.1 Class I Significant Impact Analysis

A Class I significant impacts analysis was conducted for all Class I areas located within 300km of the refinery, regardless of the Q/D screening result. The model results are shown in Table 15. As shown, all impacts are calculated to be insignificant. The SRU3 Tail Gas Incinerator (Model ID H3103) was modeled with a 24-hr average SO₂ emission rate of 28 lb/hr. SO₂ emissions of 50 lb/hr were modeled for SRU3 for the other SO₂ averaging periods.

Table 15. Class I Significant Impact Analysis Results

			Modeled	Class I
		Modeled	Conc.	SILa
Pollutant	Average	Year	(μg/m3)	(μ g/m ³)
		2013	1.88 x 10 ⁻²	
NO ₂	Annual	2014	1.89 x 10 ⁻²	0.10
		2015	2.00 x 10 ⁻²	
		2013	6.66 x 10 ⁻²	
	24-hour	2014	6.11 x 10 ⁻²	0.30
PM10		2015	5.78 x 10 ⁻²	
PIVITO		2013	7.76 x 10 ⁻³	
	Annual	2014	7.59 x 10 ⁻³	0.20
		2015	8.27 x 10 ⁻³	
		2013	3.52 x 10 ⁻²	
	Annual	2014	3.52 x 10 ⁻²	0.10
		2015	3.79 x 10 ⁻²	
		2013	1.93 x 10 ⁻¹	
SO ₂	24-hr	2014	1.78 x 10 ⁻¹	0.20
		2015	1.56 x 10 ⁻¹	
		2013	9.45 x 10 ⁻¹	
	3-hr	2014	9.82 x 10 ⁻¹	1.0
		2015	8.76 x 10 ⁻¹	

^aSee 61 FR 38249 (July 23, 1996) for the proposed Class I SILs.



8.2 Class I Visibility Analysis Results

HollyFrontier used the CALPUFF model and associated programs to evaluate the potential visibility impacts associated with the proposed project at the Carlsbad Caverns, the only Class I Area with a Q/D value that exceeded the FLM's screening criterion. The 98% (8th high) concentrations over all receptors, not by receptor, were conservatively used in the assessment.

Results are presented in Table 16. As shown, there are no exceedances of the 5% extinction criterion at Carlsbad Caverns.

Table 16. Class I 24-hr Visibility Analysis Results

Parameter	Meteorological Model Year	Modeled Value, Extinction (% change)	Change in Light Extinction (% change)	%Standard
	2013	2.78	5	56%
Visibility	2014	1.90	5	38%
	2015	2.24	5	45%

8.3 Class I Deposition Analysis Results

In addition to visibility, modeled deposition rates of total sulfur (S) and nitrogen (N) were calculated. These results were reviewed or comparison to the Deposition Analysis Thresholds (DATs) of 0.005 at each Class I area. Annual emission rates were used. In addition, all Class I areas were conservatively included eventhough only Carlsbad Caverns had a Q/D in excess of the FLM's screening criterion.

Results for nitrogen and sulfur deposition are presented in Table 17. No exceedances of the DATs were identified.



Table 17. Class I Annual Deposition Analysis Results

Parameter	Meteorological Model Year	Modeled Value, Deposition (ka/ha/yr)	Deposition Analysis Threshold (ka/ha/yr)	%Standard
	2013	2.56 x 10 ⁻³		51%
Nitrogen	2014	2.67 x 10 ⁻³		53%
	2015	2.87 x 10 ⁻³	0.005	57%
	2013	3.14 x 10 ⁻³		63%
Sulfur	2014	3.32 x 10 ⁻³		66%
	2015	3.77 x 10 ⁻³		75%



ATTACHMENT A

- HollyFrontier Model Input Data
- Off-Site Source Model Input Data
 - Volume Source Calculations
 - Flare Parameter Calculations
 - CALPUFF Model Input Data
 - CALPUFF CT PM Speciation

Last Update 1-6-21 Holly Frontier - Artesia Model Input NAD83, Zone 13 Point Sources

Model						Base	Stack						Pr	oject Relate	d Emissions	Increase (lb/	hr)		
Source				Easting (X)	Northing (Y)	Elevation	Height		Exit Velocity	Stack									
No.	Source ID		Source Description	(m)	(m)	(ft)	(ft)	Temp. (°F)	(ft/sec)	Diameter (ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT	co	H2S
1	B0007	DEFAULT	Boiler 7	556685.00	3634643.00	3363.5	74.8	275	47.90	5.25	0.00E+00								
2	B0008 B0009	DEFAULT DEFAULT	Boiler 8 Boiler 9	556686.00 556665.00	3634633.00 3634636.00	3363.5 3363.3	65.0 60.0	250 300	62.80 47.70	4.50 5.00	0.00E+00 0.00E+00								
4	H0009	DEFAULT	Unit 13 Naphtha Splitter Reboiler	556553.00	3634619.00	3363.4	77.5	530	47.70 17.90	4.50	8.42E-02	8.42E-02	8.42E-02	5.40E-01	5.40E-01	1.83E-01	0.00E+00 0.00E+00	8.76E-01	
5	H0011	DEFAULT	Unit 21 Vacuum Unit Heater	556821.00	3634014.00	3370.9	80.0	850	26.00	4.00	0.00E+00								
6	H0018	DEFAULT	Unit 06 HDS Reboiler	556556.00	3634718.00	3362.3	75.0	700	19.50	4.00	1.15E-01	1.15E-01	1.15E-01	1.52E+00	1.52E+00	4.25E-01	0.00E+00	1.27E+00	
7	H0019	DEFAULT	South Crude Charge Heater	556625.00	3634023.00	3370.3	155.7	450	21.40	4.38	6.70E-02	6.70E-02	6.70E-02	6.20E-01	5.66E-01	0.00E+00	0.00E+00	7.71E-01	0.00E+0
8	H0020 H0028	DEFAULT	South Crude Charge Heater	556644.00	3634021.00	3370.5 3370.9	175.0 50.3	330 850	12.20 18.80	6.50 2.67	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00 9.99E-02	0.00E+00	0.00E+00	
9 10	H0028 H0030	DEFAULT DEFAULT	Unit 21 Heater Unit 06 Charge Heater	556829.00 556556.00	3634014.00 3634724.00	3370.9	50.3 67.0	850 575	18.80 22.50	2.67 4.00	3.13E-02 0.00E+00	3.13E-02 0.00E+00	3.13E-02 0.00E+00	1.72E+00 1.00E+00	1.72E+00 1.00E+00	9.99E-02 1.88E-01	0.00E+00 0.00E+00	3.51E-01 2.75E+00	0.00E+0 0.00E+0
11	H0040	DEFAULT	Unit 13 Charge Heater	556557.00	3634730.00	3362.1	101.0	590	22.80	4.00	0.00E+00	0.00E+00	0.00E+00	7.20E-01	7.20E-01	0.00E+00	0.00E+00	7.73E-01	0.00E+0
12	H0312	DEFAULT	Unit 10 FCC Feed Heater	556690.00	3634676.00	3363.8	96.5	675	20.40	4.00	2.30E-01	2.30E-01	2.30E-01	3.35E+00	3.35E+00	9.69E-01	1.78E-01	2.95E+00	0.00E+0
13	H0352_54	DEFAULT	Unit 70 CCR Heaters	556734.00	3634728.00	3364.0	210.9	300	16.50	8.75	0.00E+00	3.01E+00							
14	H0355	DEFAULT	Unit 70 Stabilizer Reboiler Heater	556734.12	3634703.54	3364.0	135.2	442	28.70	2.50	1.18E-02	1.18E-02	1.18E-02	9.70E-01	9.70E-01	0.00E+00	0.00E+00	1.01E+00	
15 16	H0362_64 H0421	DEFAULT DEFAULT	Unit 70 CCR Heaters Unit 44 Charge Heater	556718.00 556755.00	3634728.00 3634642.00	3364.1 3364.0	205.5 81.7	338 650	16.90 23.70	7.00 3.25	3.10E-01 7.35E-02	3.10E-01 7.35E-02	3.10E-01 7.35E-02	2.51E+00 6.30E-01	2.51E+00 6.30E-01	1.34E+00 2.38E-01	0.00E+00 0.00E+00	3.45E+00 8.10E-01	0.00E+0 0.00E+0
17	H0464	DEFAULT	SRU Hot Oil Heater	556526.00	3634548.00	3364.3	79.8	450	9.60	2.75	9.47E-03	9.47E-03	9.47E-03	5.28E-02	5.28E-02	0.00E+00	0.00E+00	8.83E-02	
18	H0600	DEFAULT	Unit 09 Depropanizer Reboiler Heater	556795.00	3634716.00	3364.0	177.0	500	33.00	4.60	0.00E+00	2.55E+00							
19	H0601	DEFAULT	Unit 33 Charge Heater	556788.00	3634582.00	3364.3	131.0	300	11.60	6.50	2.35E-01	2.35E-01	2.35E-01	1.30E+00	1.30E+00	7.98E-01	0.00E+00	2.57E+00	0.00E+0
20	H2421	DEFAULT	Unit 45 Charge Heater	556769.00	3634573.00	3364.3	87.0	890	24.80	3.50	2.35E-02	2.35E-02	2.35E-02	2.30E-02	2.30E-02	0.00E+00	0.00E+00	2.98E-01	0.00E+0
21	H2501	DEFAULT	Unit 25 ROSE® Unit No. 2 Hot Oil Heater	556949.00	3634500.00	3364.5 3364.5	168.0 80.0	710	19.00	7.83	9.93E-01	9.93E-01	9.93E-01	3.60E+00	3.60E+00	4.35E+00	1.64E+00	7.20E+00	
22 23	H3101 H3402	DEFAULT DEFAULT	SRU3 Hot Oil Heater Unit 34 Hydrocracker Reboiler 1	556557.00 556947.00	3634512.00 3634510.00	3364.5 3364.4	80.0 67.0	450 575	9.62 27.90	2.75 4.00	9.21E-02 4.30E-01	9.21E-02 4.30E-01	9.21E-02 4.30E-01	3.30E-01 1.56E+00	3.30E-01 1.56E+00	4.11E-01 1.89E+00	1.62E-01 7.11E-01	9.87E-01 4.68E+00	0.00E+0
24	H3403	DEFAULT	Unit 34 Hydrocracker Reactor Charge Heater	556933.00	3634516.00	3364.4	86.1	705	19.40	4.00	2.65E-01	2.65E-01	2.65E-01	9.60E-01	9.60E-01	1.16E+00	4.38E-01	2.92E+00	
25	H8801_02	DEFAULT	Unit 63 Hydrogen Plant Reformer Furnaces	556903.00	3634585.00	3364.0	130.0	600	75.40	3.83	3.64E-01	3.64E-01	3.64E-01	4.46E+00	4.46E+00	0.00E+00	0.00E+00	4.02E+00	
26	H9851	DEFAULT	Unit 64 Hydrogen Plant Reformer	556901.00	3634616.00	3364.0	176.0	350	23.80	10.00	2.59E+00	2.59E+00	2.59E+00	1.12E+01	4.51E+00	0.00E+00	0.00E+00	1.81E+01	
27	H0473	DEFAULT	SRU2 Tail Gas Incinerator	556518.00	3634578.00	3364.1	150.0	1150	44.20	4.00	0.00E+00								
28 29	H3103 FCCREGEN	DEFAULT DEFAULT	SRU3 Tail Gas Incinerator FCC Regenerator	556553.00 556712.00	3634495.00 3634686.00	3364.7 3363.7	150.0 153.0	1200 125	49.90 28.30	4.00 6.00	1.33E+01 0.00E+00	1.33E+01 0.00E+00	1.91E+00 0.00E+00	6.50E+00 0.00E+00	6.51E+00 0.00E+00	5.00E+01 0.00E+00	1.87E+01 0.00E+00	1.50E+01 0.00E+00	
30	FL0400	DEFAULT	FL-0400, North Plant Flare	556647.00	3634806.00	3361.9	395.1	1832	65.60	16.11	0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	
31	FL0401	DEFAULT	FL-0401, South Plant Flare	556802.00	3634036.00	3370.6	342.2	1832	65.60	9.60	0.00E+00								
32	FL0402	DEFAULT	FL-0402, FCC Flare	556684.00	3634806.00	3363.8	304.6	1832	65.60	9.28	0.00E+00								
33	FL0403	DEFAULT	FL-0403, Alky Flare	556685.00	3634875.00	3363.3	499.1	1832	65.60	19.45	0.00E+00								
34 35	FL0404 TL4VCU	DEFAULT DEFAULT	FL-0404, GOHT Flare	556898.00	3634870.00	3361.8 3367.9	568.5	1832 1832	65.60	26.01	0.00E+00	0.00E+00 0.00E+00	0.00E+00	1.12E+01 0.00E+00	4.82E+00	3.98E+01 0.00E+00	2.46E+00	4.78E+01 0.00E+00	
36	H5401	DEFAULT	TL-4 VCU Unit 54 HDS Reactor Heater	556768.00 556917.00	3634222.00 3634721.00	3363.0	81.8 83.0	643	65.60 8.81	3.92 3.00	0.00E+00 0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00	
37	Y0001	DEFAULT	TCC Cooling Tower	556711.00	3634046.00	3370.5	14.0	100	25.00	8.00	0.00E+00								
38	Y0002	DEFAULT	S. Alky Cooling Tower (Marley Cooling Tower)	556770.00	3634059.00	3370.2	14.0	100	25.00	8.00	0.00E+00	0.00E+0							
39	Y0008	DEFAULT	North Alky Cooling Tower	556872.00	3634669.00	3363.8	14.0	100	25.00	8.00	0.00E+00								
40	Y0011	DEFAULT	FCC & NP Cooling Tower	556601.00	3634564.00	3363.9	14.0	100	25.00	8.00	0.00E+00								
41 42	Y0012 CTTT0006	DEFAULT DEFAULT	Hydrogen Plants Cooling Tower Unit 07 Amine W-0745 Cooling Tower	556898.00 556469.00	3634670.00 3634681.00	3363.7 3363.4	14.0 14.0	100 100	25.00 25.00	8.00	0.00E+00 0.00E+00								
43	FLHEP	DEFAULT	HEP Portable Flare	556740.00	3634216.00	3367.8	51.1	1832	65.60	2.29	0.00E+00								
44	TVCU	DEFAULT	Tank VCU	556458.00	3634605.00	3364.3	18.5	1832	65.60	0.20	0.00E+00								
45	H_2601	DEFAULT	RDU Reactor Heater	556954.24	3634430.58	3365.0	138.5	600	25.50	3.87	0.00E+00								
46	Y_0026A	DEFAULT	RDU Cooling Tower	556999.64	3634453.06	3364.6	21.0	90	25.80	12.19	0.00E+00								
47 48	Y_0026B Y_0093A	DEFAULT DEFAULT	RDU Cooling Tower PTU Cooling Tower	556999.55 556855.96	3634447.97 3633752.89	3364.7 3373.2	21.0 21.0	90 90	25.80 25.80	12.19 12.19	0.00E+00 0.00E+00								
49	Y 0093B	DEFAULT	PTU Cooling Tower	556855.87	3633747.81	3373.2	21.0	90	25.80	12.19	0.00E+00								
50	H 9301	DEFAULT	Vapor Combustor Unit	556871.00	3633812.00	3372.9	87.0	1600	2.60	4.00	0.00E+00								
51	082B6	DEFAULT	Filter Aid Tank Vent	556883.66	3633823.60	3372.9	80.0	100	127.30	0.25	0.00E+00								
52	26_2B25A	DEFAULT	26_2B25AP01 - Adsorption Train 1 Vent B	556854.36	3633819.49	3372.9	80.0	100	127.30	0.25	0.00E+00								
53 54	26_1B25B 26_2B25B	DEFAULT DEFAULT	26_1B25BP01 - Adsorption Train 2 Vent A	556859.14 556864.00	3633819.49 3633819.49	3372.9 3372.9	80.0 80.0	100 100	127.30 127.30	0.25 0.25	0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00 0.00E+00	
54 55	26_2B25B 26_2B26	DEFAULT	26_2B25BP01 - Adsorption Train 2 Vent B 26_2B26P01 - Adsorption Vent B	556872.17	3633819.49	3372.9	80.0	100	127.30	0.25	0.00E+00 0.00E+00								
56	26_2B26 26_1B26	DEFAULT	26_1B26P01 - Adsorption Vent A	556880.87	3633819.69	3372.9	80.0	100	127.30	0.25	0.00E+00								
57	26_1B25A	DEFAULT	26_1B25AP01 - Adsorption Train 1 Vent A	556890.55	3633819.76	3372.8	80.0	100	127.30	0.25	0.00E+00								
58	56B25C	DEFAULT	Silo 3 Vent	556846.62	3633816.62	3373.1	80.0	100	161.10	0.67	0.00E+00								
59	V0543	DEFAULT	Portable Air Compressor	556618.90	3634620.37	3363.4	6.0	1000	244.82	0.33	0.00E+00								
60 61	V0545 V0546	DEFAULT DEFAULT	Portable Air Compressor	556695.95 556765.80	3634556.00 3634115.08	3364.0 3369.5	6.0 6.0	1000 1000	244.82 225.99	0.33 0.33	0.00E+00 0.00E+00								
62	G0100	DEFAULT	Portable Air Compressor UPS backup generator	556695.06	3634115.08	3369.5	10.0	1000	225.99 229.84	0.33	0.00E+00 0.00E+00								
63	G0101	DEFAULT	UPS backup generator	556780.25	3634102.48	3369.7	12.0	1000	238.68	0.17	0.00E+00								
64	G0102	DEFAULT	Server Backup Generator	557026.11	3634058.67	3369.2	10.0	1000	354.00	0.33	0.00E+00	0.00E+0							
65	E0600W	DEFAULT	Fire Water Pump Engine	557227.00	3634864.00	3357.7	4.0	1000	354.04	0.33	0.00E+00								
66	E0601M	DEFAULT	Fire Water Pump Engine	557233.04	3634863.96	3357.6	4.0	1000	354.04	0.33	0.00E+00								
67 68	E0602E F0603	DEFAULT DEFAULT	Fire Water Pump Engine	557238.59	3634863.84 3634446.37	3357.5 3365.1	4.0 4.0	1000 1000	354.04 287.19	0.33 0.33	0.00E+00	0.00E+00 0.00E+00							
69	E0603 V0511	DEFAULT	Fire Water Pump Engine Portable Fire Water Pump Engine	556907.01 557058.55	3634446.37	3365.1	4.0 8.0	1000	287.19 287.19	0.33	0.00E+00 0.00E+00								
70	G2601	DEFAULT	Emergency Generator	556682.00	3634588.54	3363.7	10.0	1000	287.19	0.33	0.00E+00 0.00E+00	0.00E+00							
	G2602	DEFAULT	Emergency Generator	556698.90	3634587.41	3363.8	10.0	1000	287.19	0.33	0.00E+00	0.00E+0							
71																			
72	TRLO_9	DEFAULT	Molten Sulfur Railcar Loading Controlled rt of the HollyFrontier refinery. They are an adjac	556463.00	3634577.00	3364.5	15.0	130	97.48	0.33 Total (lb/hr)	0.00E+00 19.25	0.00E+00 19.25	0.00E+00 7.84	0.00E+00 54.74	0.00E+00 41.65	0.00E+00 101.88	0.00E+00 24.33	0.00E+00 124.26	4.75E-0:

Sources identified by the red font are not part of the HollyFrontier refinery. They are an adjacent, separate stationary source.

Per Table 8-2 of Appendix W, actual PM emissions were modeled in lieu of PTE for the FCC regenerator. This unit is not modified.

Pollutant names: pollutant names with a "ST" extension were used to assess compliance with short-term standards (i.e., 1-hr, 3-hr and 24-hr).

Pollutant names: pollutant names with a "LT" extension were used to assess compliance with annual standards.

Last Update 1-6-21 Holly Frontier - Artesia Model Input NAD83, Zone 13 Point Sources

Model								Poten	tial to Emit (lb/hr)				
Source														
No.	Source ID	DEFAULT	Source Description	PM10 1.78E+00	PM25_ST	PM25_LT	NO2_ST	NO2_LT	8.04E+00	SO2_24hr	CO	0.00E+00	H2SO4 0.00E+00	NH3
1 2	B0007 B0008	DEFAULT DEFAULT	Boiler 7 Boiler 8	1.78E+00 1.78E+00	1.78E+00 1.78E+00	1.78E+00 1.78E+00	1.29E+01 1.29E+01	1.29E+01 1.29E+01	8.04E+00 8.04E+00	8.04E+00 8.04E+00	1.97E+01 1.97E+01	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0
3	B0009	DEFAULT	Boiler 9	1.82E+00	1.82E+00	1.82E+00	4.89E+00	4.89E+00	2.89E+00	2.89E+00	9.04E+00	0.00E+00	0.00E+00	0.00E+
4	H0009	DEFAULT	Unit 13 Naphtha Splitter Reboiler	3.64E-01	3.64E-01	3.64E-01	3.96E+00	3.96E+00	1.64E+00	1.64E+00	4.03E+00	0.00E+00	0.00E+00	0.00E+
5	H0011	DEFAULT	Unit 21 Vacuum Unit Heater	3.15E-01	3.15E-01	3.15E-01	9.52E+00	7.24E+00	1.42E+00	1.42E+00	3.48E+00	0.00E+00	0.00E+00	0.00E+
6	H0018	DEFAULT	Unit 06 HDS Reboiler	2.65E-01	2.65E-01	2.65E-01	3.49E+00	3.49E+00	1.19E+00	1.19E+00	2.93E+00	0.00E+00	0.00E+00	0.00E+
7	H0019	DEFAULT	South Crude Charge Heater	4.47E-01	4.47E-01	4.57E-01	2.90E+00	2.85E+00	2.02E+00	2.02E+00	4.94E+00	0.00E+00	0.00E+00	0.00E+
8	H0020	DEFAULT	South Crude Charge Heater	7.45E-01	7.45E-01	7.45E-01	4.82E+00	4.82E+00	3.37E+00	3.37E+00	8.23E+00	0.00E+00	0.00E+00	
9	H0028	DEFAULT	Unit 21 Heater	1.02E-01	1.02E-01	1.02E-01	2.17E+00	2.17E+00	4.60E-01	4.60E-01	1.13E+00	0.00E+00	0.00E+00	0.00E+
10	H0030	DEFAULT	Unit 06 Charge Heater	4.00E-01	4.00E-01	3.48E-01	3.19E+00	3.19E+00	1.57E+00	1.57E+00	3.84E+00	0.00E+00	0.00E+00	0.00E+
11	H0040 H0312	DEFAULT	Unit 13 Charge Heater Unit 10 FCC Feed Heater	4.00E-01 2.90E-01	4.00E-01 2.90E-01	3.48E-01	3.78E+00	3.78E+00	1.57E+00	1.57E+00 1.31E+00	3.84E+00 3.20E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+0
12 13	H0352_54	DEFAULT DEFAULT	Unit 70 CCR Heaters	1.70E+00	1.70E+00	2.90E-01 1.66E+00	4.62E+00 9.00E+00	4.62E+00 9.00E+00	1.31E+00 8.07E+00	8.07E+00	1.83E+01	0.00E+00	0.00E+00 0.00E+00	0.00E+
14	H0355	DEFAULT	Unit 70 Stabilizer Reboiler Heater	2.32E-01	2.32E-01	2.32E-01	2.52E+00	2.52E+00	1.13E+00	1.13E+00	2.56E+00	0.00E+00	0.00E+00	0.00E+
15	H0362 64	DEFAULT	Unit 70 CCR Heaters	1.03E+00	1.03E+00	1.03E+00	6.88E+00	6.88E+00	5.04E+00	5.04E+00	1.14E+01	0.00E+00	0.00E+00	0.00E+
16	H0421	DEFAULT	Unit 44 Charge Heater	2.24E-01	2.24E-01	2.24E-01	2.43E+00	2.43E+00	1.01E+00	1.01E+00	2.47E+00	0.00E+00	0.00E+00	0.00E+
17	H0464	DEFAULT	SRU Hot Oil Heater	7.95E-02	7.95E-02	9.13E-02	5.23E-01	5.23E-01	3.58E-01	3.58E-01	8.78E-01	0.00E+00	0.00E+00	0.00E+0
18	H0600	DEFAULT	Unit 09 Depropanizer Reboiler Heater	6.95E-01	6.95E-01	6.95E-01	4.70E+00	4.67E+00	3.14E+00	3.14E+00	7.69E+00	0.00E+00	0.00E+00	0.00E+0
19	H0601	DEFAULT	Unit 33 Charge Heater	6.46E-01	6.46E-01	6.46E-01	3.51E+00	3.51E+00	2.91E+00	2.91E+00	7.14E+00	0.00E+00	0.00E+00	0.00E+0
20	H2421	DEFAULT	Unit 45 Charge Heater	2.24E-01	2.24E-01	2.24E-01	1.22E+00	1.22E+00	9.77E-01	9.77E-01	2.47E+00	0.00E+00	0.00E+00	0.00E+
21	H2501	DEFAULT	Unit 25 ROSE® Unit No. 2 Hot Oil Heater	9.93E-01	9.93E-01	9.93E-01	3.60E+00	3.60E+00	4.35E+00	4.35E+00	7.20E+00	0.00E+00	0.00E+00	0.00E+
22	H3101	DEFAULT	SRU3 Hot Oil Heater	9.11E-02	9.11E-02	9.13E-02	3.30E-01	3.30E-01	4.11E-01	4.11E-01	9.90E-01	0.00E+00	0.00E+00	0.00E+
23 24	H3402 H3403	DEFAULT DEFAULT	Unit 34 Hydrocracker Reboiler 1 Unit 34 Hydrocracker Reactor Charge Heater	4.30E-01 2.65E-01	4.30E-01 2.65E-01	4.30E-01 2.65E-01	1.56E+00 9.60E-01	1.56E+00 9.60E-01	1.89E+00 1.16E+00	1.89E+00 1.16E+00	4.68E+00 2.93E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0
25	H8801 02	DEFAULT	Unit 63 Hydrogen Plant Reformer Furnaces	1.26E+00	1.26E+00	1.26E+00	8.66E+00	8.66E+00	2.85E+00	2.85E+00	1.39E+01	0.00E+00	0.00E+00	
26	H9851	DEFAULT	Unit 64 Hydrogen Plant Reformer	2.79E+00	2.79E+00	2.81E+00	1.12E+01	4.52E+00	6.32E+00	6.32E+00	2.02E+01	0.00E+00	0.00E+00	1.38E+
27	H0473	DEFAULT	SRU2 Tail Gas Incinerator	1.15E+01	1.15E+01	1.92F+00	6.50E+00	6.51E+00	1.35E+02	1.35E+02	2.77F+01	1.44F+00	1.03E+01	0.00E+
28	H3103	DEFAULT	SRU3 Tail Gas Incinerator	4.93E+00	4.93E+00	1.91E+00	6.50E+00	6.51E+00	5.00E+01	5.00E+01	1.50E+01	5.32E-01	3.83E+00	0.00E+
29	FCCREGEN	DEFAULT	FCC Regenerator	2.29E+01	1.90E+01	1.57E+01	3.49E+01	2.32E+01	2.79E+01	2.79E+01	1.22E+02	0.00E+00	2.13E+00	1.63E+0
30	FL0400	DEFAULT	FL-0400, North Plant Flare	0.00E+00	0.00E+00	0.00E+00	3.47E+00	1.24E+00	4.48E+00	4.48E+00	1.42E+01	4.75E-02	0.00E+00	0.00E+0
31	FL0401	DEFAULT	FL-0401, South Plant Flare	0.00E+00	0.00E+00	0.00E+00	1.66E+00	4.22E-01	5.73E+01	5.73E+01	6.82E+00	6.09E-01	0.00E+00	0.00E+0
32	FL0402	DEFAULT	FL-0402, FCC Flare	0.00E+00	0.00E+00	0.00E+00	1.63E+02	4.68E+00	1.13E+03	1.13E+03	1.24E+03	1.20E+01	0.00E+00	0.00E+0
33	FL0403	DEFAULT	FL-0403, Alky Flare	0.00E+00	0.00E+00	0.00E+00	2.74E+00	5.78E-01	1.10E+00	1.10E+00	1.13E+01	1.17E-02	0.00E+00	0.00E+0
34	FL0404	DEFAULT	FL-0404, GOHT Flare	0.00E+00	0.00E+00	0.00E+00	1.17E+01	5.36E+00	3.99E+01	3.99E+01	4.80E+01	4.24E-01	0.00E+00	0.00E+0
35 36	TL4VCU H5401	DEFAULT DEFAULT	TL-4 VCU	1.05E-01	1.05E-01 1.60E-01	1.50E-02 1.60E-01	1.97E+00 7.73E-01	2.80E-01 7.73E-01	5.14E-01 7.22E-01	5.14E-01 7.22E-01	1.97E+00 6.44E-01	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0
37	Y0001	DEFAULT	Unit 54 HDS Reactor Heater TCC Cooling Tower	1.60E-01 1.58E-01	5.94E-04	5.94E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0
38	Y0001	DEFAULT	S. Alky Cooling Tower (Marley Cooling Tower)	1.58E-01	5.94E-04 5.94E-04	5.94E-04 5.94E-04	0.00E+00	0.00E+0						
39	Y0008	DEFAULT	North Alky Cooling Tower	3.69E-01	1.39E-03	1.39E-03	0.00E+00	0.00E+0						
40	Y0011	DEFAULT	FCC & NP Cooling Tower	3.16E-01	1.19E-03	1.19E-03	0.00E+00	0.00E+0						
41	Y0012	DEFAULT	Hydrogen Plants Cooling Tower	1.05E-01	3.96E-04	3.96E-04	0.00E+00	0.00E+0						
42	CTTT0006	DEFAULT	Unit 07 Amine W-0745 Cooling Tower	9.48E-02	3.56E-04	3.56E-04	0.00E+00	0.00E+0						
43	FLHEP	DEFAULT	HEP Portable Flare	0.00E+00	0.00E+00	0.00E+00	1.16E+01	1.98E-02	1.10E-01	1.10E-01	5.01E+01	1.19E-03	0.00E+00	
44	TVCU	DEFAULT	Tank VCU	9.39E-03	9.39E-03	5.71E-04	1.74E-01	8.42E-03	4.96E-02	4.96E-02	1.73E-01	1.24E-03	0.00E+00	0.00E+0
45	H_2601	DEFAULT	RDU Reactor Heater	3.21E-01	3.21E-01	3.21E-01	1.29E+00	1.29E+00	5.78E-01	5.78E-01	2.59E+00	0.00E+00	0.00E+00	0.00E+0
46	Y_0026A	DEFAULT	RDU Cooling Tower	1.32E-02	4.95E-05	4.95E-05	0.00E+00	0.00E+0						
47	Y_0026B	DEFAULT	RDU Cooling Tower	1.32E-02	4.95E-05	4.95E-05	0.00E+00	0.00E+0						
48 49	Y_0093A Y_0093B	DEFAULT DEFAULT	PTU Cooling Tower PTU Cooling Tower	1.30E-02 1.30E-02	5.00E-05 5.00E-05	5.00E-05 5.00E-05	0.00E+00 0.00E+00	0.00E+0						
50	H 9301	DEFAULT	Vapor Combustor Unit	1.40E-02	1.40E-02	1.40E-02	4.27E-01	4.27E-01	1.10E-02	1.10E-02	1.56E-01	0.00E+00	0.00E+00	0.00E+0
51	082B6	DEFAULT	Filter Aid Tank Vent	6.40E-03	6.40E-03	6.40E-03	0.00E+00	0.00E+0						
52	26 2B25A	DEFAULT	26 2B25AP01 - Adsorption Train 1 Vent B	6.40E-03	6.40E-03	6.40E-03	0.00E+00							
53	26 1B25B	DEFAULT	26_1B25BP01 - Adsorption Train 2 Vent A	6.40E-03	6.40E-03	6.40E-03	0.00E+00	0.00E+0						
54	26 2B25B	DEFAULT	26 2B25BP01 - Adsorption Train 2 Vent B	6.40E-03	6.40E-03	6.40E-03	0.00E+00	0.00E+0						
55	26_2B26	DEFAULT	26_2B26P01 - Adsorption Vent B	6.40E-03	6.40E-03	6.40E-03	0.00E+00	0.00E+0						
56	26_1B26	DEFAULT	26_1B26P01 - Adsorption Vent A	6.40E-03	6.40E-03	6.40E-03	0.00E+00	0.00E+0						
57	26_1B25A	DEFAULT	26_1B25AP01 - Adsorption Train 1 Vent A	6.40E-03	6.40E-03	6.40E-03	0.00E+00	0.00E+0						
58	56B25C	DEFAULT	Silo 3 Vent	5.80E-02	5.80E-02	5.80E-02	0.00E+00	0.00E+0						
59	V0543	DEFAULT	Portable Air Compressor	9.21E-02	9.21E-02	9.21E-02	1.84E+00	1.84E+00	3.48E-03	3.48E-03	1.61E+00	0.00E+00	0.00E+00	0.00E+
60	V0545	DEFAULT	Portable Air Compressor	9.21E-02	9.21E-02	9.21E-02	1.84E+00	1.84E+00	3.48E-03	3.48E-03	1.61E+00	0.00E+00	0.00E+00	0.00E+
61 62	V0546 G0100	DEFAULT DEFAULT	Portable Air Compressor	4.54E-03 0.00E+00	4.54E-03 0.00E+00	4.54E-03 0.00E+00	9.07E-02 0.00E+00	9.07E-02 0.00E+00	1.72E-03 0.00E+00	1.72E-03 0.00E+00	1.13E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0
63	G0100 G0101	DEFAULT	UPS backup generator UPS backup generator	0.00E+00 0.00E+00	0.00E+0									
64	G0101 G0102	DEFAULT	Server Backup Generator	0.00E+00 0.00E+00	0.00E+0									
65	E0600W	DEFAULT	Server Backup Generator Fire Water Pump Engine	1.24E-01	1.24E-01	1.42E-03	2.49E+00	2.84E-02	4.68E-03	4.68E-03	2.16E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0
66	E0601M	DEFAULT	Fire Water Pump Engine	1.24E-01	1.24E-01	1.42E-03	2.49E+00	2.84E-02	4.68E-03	4.68E-03	2.16E+00	0.00E+00	0.00E+00	0.00E+
67	E0602E	DEFAULT	Fire Water Pump Engine	1.24E-01	1.24E-01	1.42E-03	2.49E+00	2.84E-02	4.68E-03	4.68E-03	2.16E+00	0.00E+00	0.00E+00	0.00E+
68	E0603	DEFAULT	Fire Water Pump Engine	1.01E-01	1.01E-01	1.15E-03	2.02E+00	2.30E-02	3.79E-03	3.79E-03	1.75E+00	0.00E+00	0.00E+00	0.00E+
69	V0511	DEFAULT	Portable Fire Water Pump Engine	2.30E-01	2.30E-01	2.63E-03	4.60E+00	5.25E-02	8.70E-03	8.70E-03	4.03E+00	0.00E+00	0.00E+00	
70	G2601	DEFAULT	Emergency Generator	0.00E+00	0.00E+0									
71	G2602	DEFAULT	Emergency Generator	0.00E+00	0.00E+0									
72	TRLO_9	DEFAULT	Molten Sulfur Railcar Loading Controlled	0.00E+00	4.75E-03	0.00E+00	0.00E+0							
			art of the HollyFrontier refinery. They are an adjac	61.57	56.44	39.62	390.70	172.47	1524.25	1524.25	1746.92	15.11	16.29	17.63
er Table 8	2 of Annendiy M	/ actual PM em	nissions were modeled in lieu of PTE for the FCC	269.68	247.21	173.52	1711.27	755.40	6676.20	6676.20	7651.51	66.18	71.37	77.23

Per Table 8-2 of Appendix W, actual PM emissions were modeled in lieu of PTE for the FCC 269.68 247.21 173.52 1711.27 755.40 6676.20 6676.20 7651.51 66.18 71.37 77.23 Pollutant names: pollutant names with a "ST" extension were used to assess compliance with "Tollutant names: pollutant names with a "LT" extension were used to assess compliance with "Tollutant names: pollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT" extension were used to assess compliance with "Tollutant names with a "LT"

HollyFrontier - Volume Sources (H2S and Toxics Only)

Model Source No.	Source ID	Source Description	Easting (X)	Northing (Y)	Base Elevation (ft)	Release Height (ft)		Vertical Dimension - Sigma Z (ft)
73	TLO_1	TLO-1 Asphalt Truck Loading Rack	556951.00	3634033.00	3370.5	15.0	2.3	7.0
74	TL_2	TL-2 Asphalt Truck Loading Rack #2	556913.00	3634267.00	3366.9	15.0	2.3	7.0
75	TL_4	TL-4 Fuels Truck Loading Rack e, f	556740.00	3634364.00	3365.9	15.0	2.3	7.0
76	TL_7	TL-7 CBO/LCO Truck Loading Rack	556410.00	3634889.00	3365.3	15.0	2.3	7.0
77	RLO_8	RLO-8 Railcar Loading Rack	556379.00	3634966.00	3366.5	15.0	2.3	7.0
78	RLO_19	RLO-19 Railcar Loading Rack	556513.00	3634124.00	3369.6	15.0	2.3	7.0
79	TLO_20	TLO-20 Asphalt/Pitch Truck Loading Rack	557316.00	3634568.00	3360.1	15.0	2.3	7.0
80	TRLO_9F	Molten Sulfur Railcar Loading	556463.00	3634577.00	3364.5	15.0	2.3	7.0
81	T_0049	Slop Oil Tank	556806.00	3634183.00	3368.3	36.0	2.3	16.7
82	T_0059	T-0059, Light Cycle Oil (LCO) tank	556498.59	3634850.62	3363.5	30.0	7.2	14.0
83	T_0061	Light Cycle Oil (LCO) fixed roof tank	556497.48	3634911.00	3364.1	30.0	10.3	14.0
84	T_0063	Heavy Cycle Oil (HCO) fixed roof tank	556531.58	3634945.66	3363.7	30.0	10.5	14.0
85	T_0065	Heavy Cycle Oil (HCO) fixed roof tank	556528.22	3634909.88	3363.7	30.0	10.3	14.0
86	T_0075	Heavy Cycle Oil (HCO)fixed roof tank	556464.49	3634916.03	3364.6	32.0	13.4	14.9
87	T_0081	Asphalt/Pitch Tank	557350.20	3634629.35	3358.7	40.0	22.4	18.6
88	T_0082	Asphalt/Pitch Tank	557294.90	3634635.86	3359.7	40.0	28.8	18.6
89	T_0110	Asphalt/Pitch Tank	556900.88	3634231.86	3367.6	35.0	22.3	16.3
90	T_0400	Gas Oil fixed roof tank	556712.93	3634475.65	3364.7	48.0	24.7	22.3
91	T_0402	T-0402 Light Cat Naphtha tank	557231.49	3634376.15	3362.9	50.0	18.5	23.3
92	T_0410	Asphalt/Pitch Tank	556898.32	3634106.89	3369.3	40.0	16.3	18.6
93	T_0411	T-0411 Gasolines & Gasoline Blendstocks	557083.75	3634253.22	3365.3	40.0	20.6	18.6
94	T_0419	No. 2 Fuel Oil (Diesel) fixed roof tank	556713.81	3634160.70	3368.9	28.0	10.9	13.0
95	T_0420	Asphalt/Pitch Tank	556940.51	3634116.91	3369.1	30.0	10.3	14.0
96	T_0422	Light Cycle Oil (LCO) fixed roof tank	556963.72	3634117.96	3369.0	30.0	10.3	14.0
97	T_0423	Light Cycle Oil (LCO) fixed roof tank	556964.77	3634090.54	3369.4	30.0	10.3	14.0
98	T_0431	Fuel Oil fixed roof tank	556896.67	3634180.59	3368.3	32.0	22.5	14.9
99	T_0432	Fuel Oil fixed roof tank	556943.73	3634184.42	3368.0	32.0	22.5	14.9
100	T_0433	Straight Run Gas Oil fixed roof tank	556890.24	3634326.64	3366.2	42.0	24.1	19.5
101	T_0434	Straight Run Diesel fixed roof tank	556609.74	3634191.31	3368.4	42.0	24.1	19.5
102	T_0914	Slop Oil Tank	556918.87	3634034.06	3370.5	40.0	15.5	18.6
103	T_1227	Asphalt/Pitch Tank	556788.69	3634425.75	3365.3	40.0	15.9	18.6
104	T_0106	T-0106 Sour Water Tank	556846.55	3634177.91	3368.4	40.0	13.8	18.6
105	T_0435	T-0435 Sour Water Tank	556807.39	3634533.97	3364.5	40.0	6.2	18.6
106	T_0437	T-0437 Crude Oil Tank	557154.64	3634557.61	3362.4	40.0	24.7	18.6
107	T_0438	Straight Run Gas Oil fixed roof tank	556854.20	3634228.42	3367.7	48.0	18.5	22.3
108	T_0439	T-0439 Sour Naphtha Tank	556780.49	3634480.62	3364.7	46.0	26.8	21.4
109	T_0450	T-0450 Sour Naphtha Tank	557152.77	3634475.54	3363.0	40.0	24.7	18.6
110	T_0451	T-0451 Straight Run Diesel tank	556842.85	3634358.19	3365.8	40.0	7.2	18.6
111	T_0737	T-0737 Sour Water Tank	556450.62	3634620.57	3364.1	40.0	13.0	18.6
112	T_0802	T-0802 Sour Water Tank	556445.16	3634595.97	3364.4	40.0	9.3	18.6
113	T_0814	Asphalt/Pitch Tank	556943.68	3634088.43	3369.6	32.0	10.3	14.9
114	T_0815	No. 2 Fuel Oil (Diesel) tank	556520.39	3635063.61	3364.6	43.0	23.9	20.0
115	T_0821	Light Cat Naphtha tank	557195.90	3634451.64	3362.7	50.0	21.8	23.3
116	T_0830	T-0830 Slop Oil Tank	556813.69	3634957.68	3362.5	40.0	28.8	18.6
117	T_0834	Straight Run Diesel tank	556427.01	3634979.64	3365.6	40.0	17.5	18.6
118	T_0835	Straight Run Diesel tank	556643.07	3635144.08	3363.0	40.0	22.9	18.6
119	T_0838	No. 2 Fuel Oil (Diesel) tank	556486.78	3634955.24	3364.5	40.0	15.2	18.6
120	T_1225	T-1225 Crude Oil Tank	557155.26	3634634.07	3362.1	40.0	30.9	18.6

		urces (H2S and Toxics Only)			Pro	ject Related	Emissions Ir	ncrease (lb/h	r)		
Model Source No.	Source ID	Source Description	PM10	PM25_ST	PM25 LT	NO2 ST	NO2 LT	SO2 ST	SO2_LT	со	H2S
73	TLO 1	TLO-1 Asphalt Truck Loading Rack	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	7.28E-03
74	TL 2	TL-2 Asphalt Truck Loading Rack #2	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	6.24E-03
75	TL_2 TL 4	TL-4 Fuels Truck Loading Rack e, f	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.86E-02
76	TL 7	TL-7 CBO/LCO Truck Loading Rack	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.19E-05
77	RLO 8	RLO-8 Railcar Loading Rack	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	6.24E-03
78	RLO_0	RLO-19 Railcar Loading Rack	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.28E-02
79	TLO 20	TLO-20 Asphalt/Pitch Truck Loading Rack	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.25E-02
80	TRLO_9F	Molten Sulfur Railcar Loading	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.34E-02
81	T 0049	Slop Oil Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.88E-01
82	T_0059	T-0059, Light Cycle Oil (LCO) tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.82E-05
83	T 0061	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.78E-05
84	T 0063	Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.61E-04
85	T_0065	Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.59E-02
86	T 0075	Heavy Cycle Oil (HCO)fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.59E-02
87	T 0081	Asphalt/Pitch Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	5.92E-02
88	T 0082	Asphalt/Pitch Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	6.24E-02
89	T 0110	Asphalt/Pitch Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.57E-03
90	T 0400	Gas Oil fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.91E-02
91	T 0402	T-0402 Light Cat Naphtha tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.52E-04
92	T 0410	Asphalt/Pitch Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.68E-02
93	T 0411	T-0411 Gasolines & Gasoline Blendstocks	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.66E-05
94	T 0419	No. 2 Fuel Oil (Diesel) fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.79E-03
95	T 0420	Asphalt/Pitch Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.42E-03
96	T 0422	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.59E-04
97	T 0423	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.89E-04
98	T 0431	Fuel Oil fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.04E-02
99	T 0432	Fuel Oil fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	9.04E-03
100	T 0433	Straight Run Gas Oil fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.48E-04
101	T 0434	Straight Run Diesel fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.72E-02
102	T 0914	Slop Oil Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
103	T 1227	Asphalt/Pitch Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.34E-02
104	T 0106	T-0106 Sour Water Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-1.36E-01
105	T_0435	T-0435 Sour Water Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-1.28E-01
106	T 0437	T-0437 Crude Oil Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-3.21E-01
107	T_0438	Straight Run Gas Oil fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.92E-03
108	T_0439	T-0439 Sour Naphtha Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.10E-03
109	T_0450	T-0450 Sour Naphtha Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.74E-03
110	T_0451	T-0451 Straight Run Diesel tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.55E-04
111	T_0737	T-0737 Sour Water Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-9.18E-02
112	T_0802	T-0802 Sour Water Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-8.79E-02
113	T_0814	Asphalt/Pitch Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.19E-02
114	T_0815	No. 2 Fuel Oil (Diesel) tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.72E-02
115	T_0821	Light Cat Naphtha tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.87E-04
116	T_0830	T-0830 Slop Oil Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
117	T_0834	Straight Run Diesel tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.03E-03
118	T_0835	Straight Run Diesel tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.79E-03
119	T_0838	No. 2 Fuel Oil (Diesel) tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	7.40E-03
120	T_1225	T-1225 Crude Oil Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-4.32E-01

HollyFrontier - Volume Sources (H2S and Toxics Only)

yı ronue	, - volume 300	urces (H2S and Toxics Only)					Pote	ntial to Em	it (lb/hr)				
Model Source No.	Source ID	Course Persyllation	PM10	DMOE CT	DMOS LT	NO2 ST	NO2 LT	502.57	CO2 24bm	со	H2S	H2SO4	NH3
		Source Description		_	PM25_LT	_	_	_	_	-			-
73	TLO_1	TLO-1 Asphalt Truck Loading Rack	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00	0.00E+00	7.28E-03	0.00E+00	0.00E+00
74	TL_2	TL-2 Asphalt Truck Loading Rack #2	0.00E+00	0.00E+00	0.00E+00		0.00E+00		0.00E+00	0.00E+00	6.24E-03	0.00E+00	0.00E+00
75 76	TL_4	TL-4 Fuels Truck Loading Rack e, f	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.86E-02	0.00E+00	0.00E+00
76 77	TL_7	TL-7 CBO/LCO Truck Loading Rack	0.00E+00			0.00E+00			0.00E+00	0.00E+00	3.19E-05 6.24E-03	0.00E+00 0.00E+00	0.00E+00 0.00E+00
77 78	RLO_8	RLO-8 Railcar Loading Rack	0.00E+00 0.00E+00			0.00E+00 0.00E+00			0.00E+00 0.00E+00	0.00E+00 0.00E+00	6.24E-03 3.28E-02	0.00E+00 0.00E+00	0.00E+00 0.00E+00
78 79	RLO_19 TLO 20	RLO-19 Railcar Loading Rack	0.00E+00	0.00E+00		0.00E+00 0.00E+00			0.00E+00 0.00E+00	0.00E+00 0.00E+00	1.25E-02	0.00E+00 0.00E+00	0.00E+00 0.00E+00
80	TRLO 9F	TLO-20 Asphalt/Pitch Truck Loading Rack Molten Sulfur Railcar Loading	0.00E+00			0.00E+00 0.00E+00			0.00E+00 0.00E+00	0.00E+00 0.00E+00	4.34E-02	0.00E+00 0.00E+00	0.00E+00 0.00E+00
81	T 0049	Slop Oil Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00 0.00E+00	4.34E-02 3.88E-01	0.00E+00 0.00E+00	0.00E+00 0.00E+00
82	T_0049 T_0059	T-0059, Light Cycle Oil (LCO) tank	0.00E+00	0.00E+00		0.00E+00			0.00E+00	0.00E+00 0.00E+00	1.82E-05	0.00E+00 0.00E+00	0.00E+00
83	T_0059	Light Cycle Oil (LCO) fixed roof tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	2.78E-05	0.00E+00	
84	T 0063	Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00						0.00E+00	0.00E+00	3.61E-04	0.00E+00	0.00E+00
85	T_0065	Heavy Cycle Oil (HCO) fixed roof tank Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.59E-02	0.00E+00	0.00E+00
86	T_0005	Heavy Cycle Oil (HCO)fixed roof tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.59E-02	0.00E+00	
87	T 0081	Asphalt/Pitch Tank	0.00E+00		0.00E+00		0.00E+00		0.00E+00	0.00E+00	5.92E-02	0.00E+00	0.00E+00
88	T 0082	Asphalt/Pitch Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	6.24E-02	0.00E+00	0.00E+00
89	T 0110	Asphalt/Pitch Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.57E-03	0.00E+00	0.00E+00
90	T 0400	Gas Oil fixed roof tank	0.00E+00		0.00E+00		0.00E+00		0.00E+00	0.00E+00	1.91E-02	0.00E+00	0.00E+00
91	T 0402	T-0402 Light Cat Naphtha tank	0.00E+00		0.00E+00		0.00E+00		0.00E+00	0.00E+00	4.52E-04	0.00E+00	0.00E+00
92	T 0410	Asphalt/Pitch Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	2.68E-02	0.00E+00	0.00E+00
93	T 0411	T-0411 Gasolines & Gasoline Blendstocks	0.00E+00	0.00E+00		0.00E+00			0.00E+00	0.00E+00	2.66E-05	0.00E+00	0.00E+00
94	T 0419	No. 2 Fuel Oil (Diesel) fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.79E-03	0.00E+00	0.00E+00
95	T 0420	Asphalt/Pitch Tank	0.00E+00	0.00E+00		0.00E+00			0.00E+00	0.00E+00	3.42E-03	0.00E+00	0.00E+00
96	T 0422	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.59E-04	0.00E+00	0.00E+00
97	T 0423	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.89E-04	0.00E+00	0.00E+00
98	T_0431	Fuel Oil fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.04E-02	0.00E+00	0.00E+00
99	T_0432	Fuel Oil fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	9.04E-03	0.00E+00	0.00E+00
100	T_0433	Straight Run Gas Oil fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.48E-04	0.00E+00	0.00E+00
101	T_0434	Straight Run Diesel fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.72E-02	0.00E+00	0.00E+00
102	T_0914	Slop Oil Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
103	T_1227	Asphalt/Pitch Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.34E-02	0.00E+00	0.00E+00
104	T_0106	T-0106 Sour Water Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.48E-02	0.00E+00	0.00E+00
105	T_0435	T-0435 Sour Water Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.63E-03	0.00E+00	0.00E+00
106	T_0437	T-0437 Crude Oil Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.02E-03	0.00E+00	0.00E+00
107	T_0438	Straight Run Gas Oil fixed roof tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.92E-03	0.00E+00	0.00E+00
108	T_0439	T-0439 Sour Naphtha Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	2.10E-03	0.00E+00	
109	T_0450	T-0450 Sour Naphtha Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.74E-03	0.00E+00	0.00E+00
110	T_0451	T-0451 Straight Run Diesel tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.55E-04	0.00E+00	0.00E+00
111	T_0737	T-0737 Sour Water Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	2.05E-02	0.00E+00	0.00E+00
112	T_0802	T-0802 Sour Water Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.04E-02	0.00E+00	0.00E+00
113	T_0814	Asphalt/Pitch Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.19E-02	0.00E+00	0.00E+00
114	T_0815	No. 2 Fuel Oil (Diesel) tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	2.72E-02	0.00E+00	0.00E+00
115	T_0821	Light Cat Naphtha tank	0.00E+00		0.00E+00		0.00E+00		0.00E+00	0.00E+00	4.87E-04	0.00E+00	0.00E+00
116	T_0830	T-0830 Slop Oil Tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
117	T_0834	Straight Run Diesel tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	1.03E-03	0.00E+00	0.00E+00
118	T_0835	Straight Run Diesel tank	0.00E+00	0.00E+00		0.00E+00			0.00E+00	0.00E+00	1.79E-03	0.00E+00	0.00E+00
119	T_0838	No. 2 Fuel Oil (Diesel) tank	0.00E+00			0.00E+00			0.00E+00	0.00E+00	7.40E-03	0.00E+00	0.00E+00
120	T_1225	T-1225 Crude Oil Tank	0.00E+00	0.00E+00	0.00E+00	0.00E+00	U.UUE+00	0.00E+00	0.00E+00	0.00E+00	1.57E-03	0.00E+00	0.00E+00

HollyFrontier Off-Site Point Source NAAQS/NMAAQS Input Data (Updated 7-12-21)

													Potenti	al to Emit (lb/hr)			
	Stack				Base				Stack									
	Release			Northing (Y)	Elevation	Stack		Exit Velocity										
Source ID	Type	Source Description	(m)	(m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT	СО	H2S
352E1	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556292.63	3637097.65	3373.8	80.0	400	50.98	1.12	0.798	0.798	0.798					1.395	
352E2	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556300.17	3637104.67	3373.6	35.0	110	45.21	1.51	1.587	1.587	1.587						
352E4	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556285.79	3637106.13	3373.9	35.0	110	45.21	1.51	1.587	1.587	1.587						!
402E3	DEFAULT	Holly Frontier Asphalt Company	556992.61	3637197.56	3359.9	15.0	500	29.89	1.51	6.508	6.508	6.508					7.937	!
402E6	DEFAULT	Holly Frontier Asphalt Company	557000.15	3637204.58	3359.9	25.0	285	7.19	1.51	0.906	0.906	0.906					9.524	!
402E8	DEFAULT	Holly Frontier Asphalt Company	557000.15	3637204.58	3359.9	25.0	500	29.89	1.51								3.080	
402E7	DEFAULT	Holly Frontier Asphalt Company	556981.53	3637199.14	3360.1	25.0	285	7.19	1.51								7.143	
402E9	DEFAULT	Holly Frontier Asphalt Company	556983.18	3637190.99	3360.0	25.0	500	29.89	1.51								3.080	!
203R2	DEFAULT	DCP - Shadow Booster Station	557393.94	3622548.16	3367.7	23.0	854	91.86	0.98									0.363
191E64	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569332.26	3626710.82	3554.0	54.5	1150	19.88	3.51									3.987
191R15	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569339.80	3626717.84	3555.0	115.0	1832	65.58	28.44									3.443
191R16	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569333.01	3626721.39	3554.8	115.0	1832	65.58	28.44									8.154
191R17	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569325.42	3626719.30	3554.1	115.0	1832	65.58	28.44									8.154
191R18	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569321.18	3626712.40	3553.4	115.0	1832	65.58	28.44									0.725
191R19	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569322.83	3626704.25	3553.2	115.0	1832	65.58	28.44									0.363
191R20	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569329.78	3626699.28	3553.3	115.0	1832	65.58	28.44									16.308
211E25	DEFAULT	Lucid Artesia - Dagger Draw Gas Plant	551931.36	3619797.52	3472.0	200.0	1832	65.62	9.81									223.020
39270R3	DEFAULT	Lucid Artesia - North Pen Compressor Station	551454.28	3619910.64	3477.6	23.0	854	91.86	0.98									2.537
199E38	DEFAULT	Artesia Gas Plant	574000.18	3624399.74	3609.0	70.6	1832	65.62	68.26									26.455
31815E15	DEFAULT	Frontier - Coyote Compressor Station	578708.30	3628257.94	3668.9	23.0	854	91.86	0.98									1.825
39714E8	DEFAULT	Spur - Shelby 23 Tank Battery	551738.94	3611091.61	3409.5	35.0	1832	65.62	8.64									6.197
39714E9	DEFAULT	Spur - Shelby 23 Tank Battery	551746.48	3611098.63	3409.0	30.0	1832	65.62	8.64									6.197
39003E5	DEFAULT	Spur Energy - Ross Ranch Battery	548838.12	3611188.93	3472.3	35.0	1832	65.62	29.75									13.391

Rest of sources provided by NMAQB are located in excess of 10km from refinery. Not included in NAQS/MMAQS model.

All sources within 25km and large (1,000lb/hr) emitters within 50km were evaluated for inclusion in the H2S NMAQS analysis.

PM10, PM2.5 and SO2 sources located beyond 10km were excluded. There are no SO2 sources located within 10km of the refinery.

No cummulative NAAQS/NMAAQS modeling conducted for pollutants other than PM10, PM25, H2S and SO2 as the nearby source contribution is reflected in the background concentration.

HollyFrontier Off-Site Source NAAQS/NMAAQS Volume Source Input Data (Updated 5-5-21)

											Potentia	al to Emit (II	b/hr)			
Source ID	Source Description	Easting (X) (m)	Northing (Y) (m)	Base Elevation (ft)		Sigma Y (ft)	Sigma Z (ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT	со	H2S
3403E2	Schlumberger - Artesia District Bulk Facility	556719.31	3635718.50	3362.8	3.3	1.54	3.05	2.38	2.381	2.381						
3403R1	Schlumberger - Artesia District Bulk Facility	556726.85	3635725.52	3362.7	3.3	1.54	3.05	0.72	0.725	0.725						
359@1	Southeast Readi-Mix - Artesia Plant	557117.00	3635667.03	3356.9	32.8	721.78	30.51	16.27	4.08	4.081						ļ
352E3	Land O' Lakes Purina Feed - Artesia Feed Mill	556293.38	3637108.22	3373.8	20.0	1.54	3.05	0.79	0.794	0.794						ļ
402R2	Holly Frontier Asphalt Company	556993.36	3637208.13	3360.0	32.8	32.81	30.51	6.51	6.508	6.508						
402R3	Holly Frontier Asphalt Company	556985.77	3637206.04	3360.1	32.8	32.81	30.51	6.50	6.505	6.505						
402R6	Holly Frontier Asphalt Company	556981.53	3637199.14	3360.1	32.8	32.81	30.51	6.35	6.349	6.349						ļ
30254@1	Par Five Energy LLC - Par Five Energy	564319.69	3632835.00	3342.9	3.3	1.54	3.05	2.38	2.381	2.381						ļ
30254R1	Par Five Energy LLC - Par Five Energy	564327.22	3632842.02	3343.0	32.8	32.81	30.51	5.56	5.556	5.556						
28959E1	Lime Rock - Condor 7 Battery	563709.45	3625436.95	3287.2	17.0	1.54	3.05									0.544
26441E1	Lime Rock - Atoka San Andreas Unit Battery	561619.20	3623917.88	3302.5	3.3	1.54	3.05									0.363
26441E2	Lime Rock - Atoka San Andreas Unit Battery	561626.73	3623924.91	3302.4	3.3	1.54	3.05									0.363
26441E3	Lime Rock - Atoka San Andreas Unit Battery	561619.95	3623928.46	3302.4	3.3	1.54	3.05									0.363
203R1	DCP - Shadow Booster Station	557400.73	3622544.60	3367.6	3.3	1.54	3.05									0.317
29063R1	Chesapeake Operating Inc - Hondo Federal Gas	568814.07	3629620.53	3468.8	3.3	1.54	3.05									4.762
39270E3	Lucid Artesia - North Pen Compressor Station	551465.37	3619909.06	3477.3	3.3	1.54	3.05									7.143
39270E4	Lucid Artesia - North Pen Compressor Station	551472.91	3619916.08	3477.1	3.3	1.54	3.05									7.143
39270R1	Lucid Artesia - North Pen Compressor Station	551466.12	3619919.63	3477.1	3.3	1.54	3.05									0.238
39270R2	Lucid Artesia - North Pen Compressor Station	551458.53	3619917.54	3477.3	3.3	1.54	3.05									1.825
199R2	Artesia Gas Plant	574007.71	3624406.77	3608.9	3.3	1.54	3.05									0.000
199R3	Artesia Gas Plant	574000.93	3624410.32	3609.0	3.3	1.54	3.05									0.000
31815R1	Frontier - Coyote Compressor Station	578715.83	3628264.96	3668.9	3.3	1.54	3.05									3.571
31815R3	Frontier - Coyote Compressor Station	578709.05	3628268.51	3668.9	3.3	1.54	3.05									18.120
39714R1	Spur - Shelby 23 Tank Battery	551739.69	3611102.18	3408.9	3.3	1.54	3.05									0.159

Note: The volume sources at the Artesia Gas Plant (Source IDs. 199R2 and 199R3 represent emissions from the acid gas flare. These emissions were therefore modeles as a flare (Source ID 199E38).

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

,		oint Source increment input Data (Updated 5-5-21)									Potenti	ial to Emit (l	b/hr)		
	Stack Release		Easting (X) Northing (Y)	Base Elevation	Stack		Exit Velocity	Stack Diameter							
Source IE		Source Description	(m) (m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC1	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556292.63 3637097.65	3373.8	80.0	400	51.0	1.1	0.798						
INC2	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556300.170 3637104.670		35.0	110	45.2	1.5	1.587						
INC3	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556285.790 3637106.130		35.0	110	45.2	1.5	1.587						
INC4 INC5	DEFAULT	Holly Frontier Asphalt Company	556992.610 3637197.560		15.0 25.0	500 285	29.9	1.5	6.508						
INC5	DEFAULT DEFAULT	Holly Frontier Asphalt Company DCP - Shadow Booster Station	557000.150 3637204.580 557393.190 3622537.580		25.0 15.0	285 1125	7.2 118.2	1.5 0.1	0.906 1.746						
INC6	DEFAULT	DCP - Shadow Booster Station	557400.730 3622544.600		42.5	780	136.0	0.1	1.746						
INC8	DEFAULT	Chesapeake Operating Inc - Hondo Federal Gas	568814.070 3629620.530		6.0	860	53.3	0.8	0.794						
INC9	DEFAULT	DCP - Pecos Diamond Gas Plant	568071.310 3625977.910	3541.9	50.0	600	105.0	1.0	1.587						
INC10	DEFAULT	DCP - Pecos Diamond Gas Plant	568061.290 3625977.950		40.0	600	105.1	1.0	1.587						
INC11	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569341.200 3626597.800		27.0	670	200.0	1.3	-2.356						
INC12 INC13	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		27.0	670 670	200.0 200.0	1.3	-3.080						
INC13	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760 569351.590 3626398.760		40.0 31.1	730	200.0 181.0	1.3 1.5	-11.905 -2.537						
INC14 INC15	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		35.0	955	200.0	1.6	-3.443						
INC16	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		36.0	759	170.0	1.4	-3.262						
INC17	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		40.0	759	160.0	1.5	-3.806						
INC18	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		21.0	600	34.0	2.0	-0.127						
INC19	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		33.0	925	200.0	1.6	-1.449						
INC20	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569336.770 3626723.010		54.5	1150	19.9	3.5	0.159						
INC21	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569327.130 3626723.090		54.5	1150	27.7	3.5	0.037						
INC22	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569319.870 3626716.420		120.0	600 600	17.2 17.2	6.2 6.2	4.762						
INC23 INC24	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant	569319.090 3626706.380 571606.690 3638669.910		120.0 15.0	1125	118.2	1.2	4.762 1.812						
INC24 INC25	DEFAULT	DCP - Carbon Valley Booster DCP - Carbon Valley Booster	571614.220 3638676.940		15.0	1125	118.2	1.2	1.812						
INC26	DEFAULT	DCP - Carbon Valley Booster	571599.840 3638678.400		15.0	1125	118.2	1.2	1.812						
INC27	DEFAULT	Lucid Artesia - North Pen Compressor Station	552193.100 3619498.130		21.0	869	152.3	1.0	0.556						
INC28	DEFAULT	Lucid Artesia - North Pen Compressor Station	552193.100 3619498.130		21.0	869	152.3	1.0	0.556						
INC29	DEFAULT	EOG - Rumble State No4	547037.570 3620834.180		15.0	600	3.8	1.0	0.018						
INC30	DEFAULT	EOG - Rumble State No5	547018.950 3620828.740		15.0	832	171.6	1.0	0.794						
INC31	DEFAULT	EOG - Rumble State No6	547020.600 3620820.590		15.0	832	171.6	1.0	0.794						
INC32 INC33	DEFAULT	EOG - Lacama 20 State Com 602H	545079.800 3621969.940		15.0	1131 931	30.0 192.9	0.7 0.7	0.159						
INC33	DEFAULT DEFAULT	EOG - Lacama 20 State Com 602H EOG - Lacama 20 State Com 602H	545073.020 3621973.500 545065.420 3621971.400		15.0 15.0	832	192.9 349.9	0.7	0.397 0.794						
INC35	DEFAULT	EOG - Lacama 20 State Com 602H	545061.180 3621964.500		15.0	1255	161.9	0.7	0.952						
INC36	DEFAULT	Yates Petroleum - Pierre State No1 Facility	570982.950 3620931.670		23.0	854	91.9	1.0	0.037						
INC37	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		40.3	1340	89.2	1.0	1.957						
INC38	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	40.3	1340	89.2	1.0	0.979						
INC39	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		44.7	750	21.2	3.0	2.175						
INC40	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	-0.544						
INC41	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	1.957						
INC42	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	1.957						
INC43	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	1.957						
INC44	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2 91.9	1.0	0.979						
INC45 INC46	DEFAULT DEFAULT	Artesia Gas Plant Artesia Gas Plant	574011.520 3624405.460		62.3 62.3	-460 -460	91.9	15.1	3.175						
INC46 INC47	DEFAULT	Artesia Gas Plant Artesia Gas Plant	574004.680 3624411.940 573990.740 3624597.900		40.3	-460 1340	91.9 89.2	15.1 1.0	2.857 0.979						
INC47 INC48	DEFAULT	Artesia Gas Plant Artesia Gas Plant	573990.740 3624597.900		46.0	1125	89.2 147.9	1.0	1.268						
INC49	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	0.979						
INC50	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	0.979						
INC51	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	46.0	1340	89.2	1.0	1.957						
INC52	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	1.957						
INC53	DEFAULT	Frontier - Coyote Compressor Station	578708.300 3628257.940		16.0	1500	0.1	2.8	0.018						
INC54	DEFAULT	Frontier - Coyote Compressor Station	578715.830 3628264.960		20.0	990	142.0	1.1	0.794						
INC55	DEFAULT	Frontier - Coyote Compressor Station	578709.050 3628268.510		22.0	600	18.0	0.8	0.317						
INC56	DEFAULT	Frontier - Coyote Compressor Station	578701.450 3628266.420		20.0	990	142.0	1.1	0.794						
INC57 INC58	DEFAULT DEFAULT	Frontier - Coyote Compressor Station Shelby 23 Tank Battery	578697.210 3628259.520 551738.940 3611091.610		23.0 25.0	873 250	128.0 21.6	0.9 0.7	0.794 0.079						
INC58	DEFAULT	Shelby 23 Tank Battery Shelby 23 Tank Battery	551746.480 3611098.630		25.0 25.0	250 250	21.6	0.7	0.079						
INC60	DEFAULT	Shelby 23 Tank Battery	551739.690 3611102.180		25.0	250	21.6	0.7	0.079						
INC61	DEFAULT	Shelby 23 Tank Battery	551732.090 3611100.090		25.0	250	21.6	0.7	0.079						
INC62	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556292.630 3637097.650		79.987	399.992	50.984	1.115		0.798	0.798				
INC63	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556300.170 3637104.670	3373.6	35.007	109.994	45.210	1.509		1.587	1.587				

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

		oint Source increment input Data (Opdated 5-5-21)									Potenti	ial to Emit (I	b/hr)		
	Stack Release		Easting (X) Northing (Y)	Base Elevation	Stack		Exit Velocity	Stack Diameter							
Source IE		Source Description	(m) (m)		Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC64	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556285.790 3637106.130	3373.9	35.007	109.994	45.210	1.509		1.587	1.587				
INC65	DEFAULT	Holly Frontier Asphalt Company	556992.610 3637197.560	3359.9	14.993	500.000	29.888	1.509		6.508	6.508				
INC66 INC67	DEFAULT DEFAULT	Holly Frontier Asphalt Company DCP - Shadow Booster Station	557000.150 3637204.580 557393.190 3622537.580	3359.9 3367.9	25.000 14.993	285.008 1124.996	7.185 118.209	1.509 0.098		0.906 1.746	0.906 1.746				
INC67	DEFAULT	DCP - Shadow Booster Station	557400.730 3622544.600	3367.6	42.487	780.008	135.991	0.096		1.740	1.746				
INC69	DEFAULT	DCP - Pecos Diamond Gas Plant	568071.310 3625977.910	3541.9	50.000	600.008	104.987	0.984		1.587	1.587				
INC70	DEFAULT	DCP - Pecos Diamond Gas Plant	568061.290 3625977.950	3540.7	39.993	600.008	105.085	0.984		1.587	1.587				
INC71	DEFAULT	Durango Midatraara Empire Abo Gas Plant	569341.200 3626597.800	3548.5 3534.7	27.001	669.992	200.000	1.280		-2.356	-2.356				
INC72 INC73	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760 569351.590 3626398.760	3534.7 3534.7	27.001 39.993	669.992 669.992	200.000 200.000	1.280 1.280		-3.080 -11.905	-3.080 -11.905				
INC74	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7	37.992	719.996	185.007	1.280		-2.718	-2.718				
INC75	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7	31.102	730.004	181.004	1.476		-2.537	-2.537				
INC76	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7	35.991	759.002	170.013	1.444		-3.262	-3.262				
INC77 INC78	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760 569351.590 3626398.760	3534.7 3534.7	39.993 20.997	759.002 600.008	160.007 33.990	1.509 1.969		-3.806 -0.127	-3.806 -0.127				
INC79	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7	33.005	924.998	200.000	1.608		-1.449	-1.449				
INC80	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569336.770 3626723.010	3555.2	54.495	1149.998	19.882	3.510		0.159	0.159				
INC81	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569327.130 3626723.090	3554.4	54.495	1149.998	27.690	3.510		0.037	0.037				
INC82 INC83	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569319.870 3626716.420 569319.090 3626706.380	3553.4 3553.0	120.013 120.013	600.008 600.008	17.192 17.192	6.168 6.168		4.762 4.762	4.762 4.762				
INC83	DEFAULT	Lucid Artesia - North Pen Compressor Station	552193.100 3619498.130	3473.5	20.997	869.000	152.297	0.168		0.556	0.556				
INC85	DEFAULT	Lucid Artesia - North Pen Compressor Station	552193.100 3619498.130	3473.5	20.997	869.000	152.297	0.984		0.556	0.556				
INC86	DEFAULT	EOG - Rumble State No4	547037.570 3620834.180	3568.8	14.993	600.008	3.806	0.984		0.018	0.018				
INC87	DEFAULT	EOG - Rumble State No5	547018.950 3620828.740	3569.5	14.993	831.992	171.588	0.984		0.794	0.794				
INC88	DEFAULT	EOG - Rumble State No6	547020.600 3620820.590	3569.5	14.993	831.992	171.588	0.984		0.794	0.794				
INC89 INC90	DEFAULT DEFAULT	EOG - Lacama 20 State Com 602H EOG - Lacama 20 State Com 602H	545079.800 3621969.940 545073.020 3621973.500	3613.0 3613.1	14.993 14.993	1131.008 930.992	30.020 192.946	0.689 0.689		0.159 0.397	0.159 0.397				
INC91	DEFAULT	EOG - Lacama 20 State Com 602H	545065.420 3621971.400	3613.7	14.993	831.992	349.934	0.689		0.794	0.794				
INC92	DEFAULT	EOG - Lacama 20 State Com 602H	545061.180 3621964.500	3614.7	14.993	1254.992	161.877	0.689		0.952	0.952				
INC93	DEFAULT	Artesia Gas Plant	574011.520 3624405.460	3608.9	62.336	-459.670	91.864	15.092		3.175	3.175				
INC94	DEFAULT	Artesia Gas Plant	574004.680 3624411.940	3609.1	62.336	-459.670	91.864	15.092		2.857	2.857				
INC95 INC96	DEFAULT DEFAULT	Artesia Gas Plant Frontier - Coyote Compressor Station	573990.740 3624597.900 578708.300 3628257.940	3613.9 3668.9	45.997 16.010	1124.996 1500.008	147.900 0.098	0.984 2.756		2.537 0.018	2.537 0.018				
INC97	DEFAULT	Frontier - Coyote Compressor Station	578715.830 3628264.960	3668.9	20.013	989.996	141.995	1.148		0.794	0.794				
INC98	DEFAULT	Frontier - Coyote Compressor Station	578709.050 3628268.510	3668.9	22.014	600.008	18.012	0.820		0.317	0.317				
INC99	DEFAULT	Frontier - Coyote Compressor Station	578701.450 3628266.420	3668.9	20.013	989.996	141.995	1.148		0.794	0.794				
INC100 INC101	DEFAULT DEFAULT	Frontier - Coyote Compressor Station Shelby 23 Tank Battery	578697.210 3628259.520 551738.940 3611091.610	3668.9 3409.5	22.999 25.000	872.996 249.998	127.986 21.621	0.919 0.656		0.794 0.079	0.794 0.079				
INC101	DEFAULT	Shelby 23 Tank Battery	551746.480 3611091.610	3409.0	25.000	249.998	21.621	0.656		0.079	0.079				
INC103	DEFAULT	Shelby 23 Tank Battery	551739.690 3611102.180	3408.9	25.000	249.998	21.621	0.656		0.079	0.079				
INC104	DEFAULT	Shelby 23 Tank Battery	551732.090 3611100.090	3409.2	25.000	249.998	21.621	0.656		0.079	0.079				
INC105	DEFAULT	Lime Rock - Malco B Battery	563966.960 3627073.850	3441.4	25.000	1831.730	65.617	68.261						5.556	5.556
INC106 INC107	DEFAULT DEFAULT	Lime Rock -Kaiser B Battery Lime Rock -Kaiser B Battery	563767.890 3625655.950 563775.430 3625662.970	3319.3 3320.9	25.000 22.014	1831.730 100.004	65.617 18.012	68.261 0.492						3.968 34.128	3.968 34.128
INC107	DEFAULT	Lime Rock - West Red Lake Battery	564130.550 3625904.740	3422.4	22.014	100.004	18.012	0.492						11.053	11.053
INC109	DEFAULT	Lime Rock - West Red Lake Battery	564138.090 3625911.760	3422.6	22.014	100.004	18.012	0.492						11.053	11.053
INC110	DEFAULT	Lime Rock - West Red Lake Battery	564131.300 3625915.310	3421.9	22.014	100.004	18.012	0.492						11.053	11.053
INC111	DEFAULT	Lime Rock - Atoka San Andreas Unit Battery	561626.730 3623924.910	3302.4	22.014	100.004	18.012	0.492						15.873	15.873
INC112 INC113	DEFAULT DEFAULT	DCP - Shadow Booster Station DCP - Shadow Booster Station	557400.730 3622544.600 557393.940 3622548.160	3367.6 3367.7	14.993 42.487	1124.996 780.008	118.209 135.991	0.098 0.131						2.302 2.302	2.302 2.302
INC113	DEFAULT	Lime Rock - Hawk 8 Battery	565542.390 3624866.860	3444.5	22.014	1831.730	65.617	68.261						3.968	3.968
INC115	DEFAULT	Lime Rock - Hondo Federal Battery	567428.660 3626819.640	3582.9	22.014	1831.730	65.617	68.261						2.718	2.718
INC116	DEFAULT	EOG - War Dog State No1H	569708.850 3637607.080	3427.3	60.007	1831.730	65.617	1.673						14.445	14.445
INC117	DEFAULT	Lime Rock - Hawk 9 Battery	566922.460 3624722.080	3519.9	22.014	100.004	18.012	0.492						11.053	11.053
INC118 INC119	DEFAULT DEFAULT	Lime Rock - Hawk 9 Battery Lime Rock - Falcon 3 Battery	566930.000 3624729.100 568831.750 3627075.620	3520.3 3578.3	22.014 22.014	100.004 100.004	18.012 18.012	0.492 0.492						11.053 10.318	11.053 10.318
INC119	DEFAULT	Lime Rock - Falcon 3 Battery	568839.280 3627073.020	3578.6	22.014	100.004	18.012	0.492						10.318	10.318
INC121	DEFAULT	Lime Rock - Eagle 35 Sat Battery	569992.810 3628438.870	3589.9	25.000	1831.730	65.617	68.261						2.356	2.356
INC122	DEFAULT	Lime Rock - Eagle 35 Sat Battery	570000.350 3628445.890	3589.6	22.014	100.004	18.012	0.492						11.905	11.905
INC123 INC124	DEFAULT DEFAULT	Lime Rock - Eagle 35 Sat Battery	569993.560 3628449.440 569351.590 3626398.760	3589.0 3534.7	22.014 114.993	100.004 1831.730	18.012 65.617	0.492 68.261						11.905 0.079	11.905 0.079
INC 124 INC 125	DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7 3534.7	114.993	1831.730	65.617	68.261						0.079	0.079
INC126	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569333.010 3626721.390	3554.8	54.495	1149.998	19.882	3.510						378.578	378.578
INC127	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569325.420 3626719.300	3554.1	54.495	1149.998	27.690	3.510						0.079	0.079
INC128	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569321.180 3626712.400	3553.4	120.013	600.008	17.192	6.168						8.730	8.730

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

		nt Source Increment Input Data (Updated 5-5-21)			_						Poten	tial to Emit (lb/hr)		
	Stack Release		Fasting (X)	Northing (Y)	Base Elevation	Stack		Exit Velocity	Stack Diameter						
Source ID		Source Description	(m)	(m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC129	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569322.830	3626704.250	3553.2	120.013	600.008	17.192	6.168					8.730	8.730
INC130	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626699.280	3553.3	29.987	600.008	25.098	2.493					2.381	2.381
INC131	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626700.430	3553.8	114.993	1832.000 1832.000	65.584	28.445 28.445					118.143	118.143
INC132 INC133	DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626707.350 3626716.530	3554.6 3555.2	114.993 114.993	1832.000	65.584 65.584	28.445					9.060 9.060	9.060 9.060
INC133	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626723.010	3555.2	114.993	1832.000	65.584	28.445					68.857	68.857
INC135	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626723.090	3554.4	114.993	1832.000	65.584	28.445					26.093	26.093
INC136	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626716.420	3553.4	114.993	1832.000	65.584	28.445					18.120	18.120
INC137	DEFAULT	Lucid Artesia - Dagger Draw Gas Plant		3619797.520	3472.0	200.000	1831.730	65.617	9.810					22333.709	
INC138 INC139	DEFAULT DEFAULT	Lucid Artesia - North Pen Compressor Station Lucid Artesia - North Pen Compressor Station		3619498.130 3619498.130	3473.5 3473.5	20.997 20.997	869.000 869.000	152.297 152.297	0.984 0.984					0.079 0.079	0.079 0.079
INC139	DEFAULT	Lucid Artesia - North Pen Compressor Station		3619919.630	3477.1	22.966	854.330	91.864	0.984					94.225	94.225
INC141	DEFAULT	EOG - Rumble State No5		3620827.160	3569.2	25.000	1831.730	65.617	68.261					0.476	0.476
INC142	DEFAULT	EOG - Rumble State No5		3620837.730	3569.0	14.993	831.992	171.588	0.984					0.397	0.397
INC143	DEFAULT	EOG - Rumble State No6		3620835.640	3569.4	14.993	831.992	171.588	0.984					0.397	0.397
INC144	DEFAULT	EOG - Lacama 20 State Com 602H		3621962.920	3614.3	14.993	1131.008	30.020	0.689					0.079	0.079
INC145 INC146	DEFAULT DEFAULT	EOG - Lacama 20 State Com 602H EOG - Lacama 20 State Com 602H		3621969.940 3621973.500	3613.0 3613.1	14.993 14.993	930.992 831.992	192.946 349.934	0.689 0.689					0.238 3.968	0.238 3.968
INC 140	DEFAULT	EOG - Lacama 20 State Com 602H		3621971.400	3613.7	14.993	1254.992	161.877	0.689					0.238	0.238
INC148	DEFAULT	Chalk Compressor Station		3621748.040	3460.6	22.014	465.008	49.803	1.115					34.048	34.048
INC149	DEFAULT	Artesia Gas Plant		3624597.900	3613.9	44.685	750.002	21.194	2.986					0.326	0.326
INC150	DEFAULT	Artesia Gas Plant		3624406.770	3608.9	70.604	1831.730	65.617	68.261					0.159	0.159
INC151	DEFAULT	Artesia Gas Plant		3624410.320	3609.0	70.604	1831.730	65.617	68.261					0.079	0.079
INC152	DEFAULT	Artesia Gas Plant		3624597.900	3613.9	45.997	1124.996	147.900	0.984					1.812	1.812
INC153 INC154	DEFAULT DEFAULT	EOG - Badboy CTB		3613604.540	3454.8 3454.6	60.007	1831.730	65.617	1.673					2.381 2.381	2.381
INC 154 INC 155	DEFAULT	EOG - Badboy CTB Frontier - Coyote Compressor Station		3613611.560 3628257.940	3668.9	60.007 16.010	1831.730 1500.008	65.617 0.098	1.673 2.756					1.508	2.381 1.508
INC156	DEFAULT	Frontier - Coyote Compressor Station		3628264.960	3668.9	20.013	989.996	141.995	1.148					0.079	0.079
INC157	DEFAULT	Frontier - Coyote Compressor Station		3628268.510	3668.9	22.014	600.008	18.012	0.820					0.159	0.159
INC158	DEFAULT	Frontier - Coyote Compressor Station	578701.450	3628266.420	3668.9	20.013	989.996	141.995	1.148					0.079	0.079
INC159	DEFAULT	Frontier - Coyote Compressor Station		3628259.520	3668.9	22.999	872.996	127.986	0.919					0.079	0.079
INC160	DEFAULT	Spur - Shelby 23 Tank Battery		3611091.610	3409.5	35.007	1831.730	65.617	8.635					8.390	8.390
INC161 INC162	DEFAULT DEFAULT	Spur - Shelby 23 Tank Battery EOG- Falcata Battery		3611098.630	3409.0 3695.3	29.987 14.993	1831.730 1131.008	65.617	8.635 0.689					8.390 0.079	8.390
INC 162	DEFAULT	EOG- Falcata Battery		3616360.840 3576089.170	3002.3	14.993	930.992	29.987 192.946	0.689					0.079	0.079 0.238
INC164	DEFAULT	EOG- Falcata Battery		3616371.420	3696.4	14.993	831.992	349.934	0.689					0.397	0.397
INC165	DEFAULT	EOG- Falcata Battery	540682.320	3616369.320	3695.0	14.993	600.008	161.877	0.689					0.238	0.238
INC166	DEFAULT	EOG- Falcata Battery		3616362.420	3693.9	14.993	600.008	17.848	0.689					0.079	0.079
INC167	DEFAULT	Spur Energy - Ross Ranch Battery		3611188.930	3472.3	35.007	1831.730	65.617	29.754					25.873	25.873
INC168	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill		3637097.650	3373.8	79.987	399.992	50.984	1.115			6.667	6.667		
INC169 INC170	DEFAULT DEFAULT	Holly Frontier Asphalt Company Holly Frontier Asphalt Company		3637197.560 3637208.130	3359.9 3360.0	14.993 25.000	500.000 285.008	29.888 7.185	1.509 1.509			9.524 11.111	9.524 11.111		
INC170	DEFAULT	Holly Frontier Asphalt Company		3637206.040	3360.0	25.000	285.008	7.185	1.509			7.937	7.937		
INC172	DEFAULT	Holly Frontier Asphalt Company		3637199.140	3360.1	25.000	500.000	29.888	1.509			3.624	3.624		
INC173	DEFAULT	Holly Frontier Asphalt Company	556983.180	3637190.990	3360.0	25.000	500.000	29.888	1.509			3.624	3.624		
INC174	DEFAULT	Lady Luck No1 Facility		3638398.310	3413.2	14.993	489.992	22.014	0.984			22.223	22.223		
INC175	DEFAULT	Lady Luck No1 Facility		3638405.330	3413.5	22.966	854.330	91.864	0.984			0.794	0.794		
INC176	DEFAULT	Atoka Dehydration Facility		3624129.050	3309.6	22.966	854.330	91.864	0.984			1.812	1.812		
INC177 INC178	DEFAULT DEFAULT	Lime Rock - Atoka San Andreas Unit Battery Lucky Lobo ASX #2 Facility		3623917.880 3639898.520	3302.5 3484.5	22.014 14.993	100.004 469.994	18.012 21.490	0.492 0.984			0.363 44.445	0.363 44.445		
INC178	DEFAULT	DCP - Shadow Booster Station		3622544.600	3367.6	14.993	1124.996	118.209	0.984			32.302	32.302		
INC180	DEFAULT	DCP - Shadow Booster Station		3622548.160	3367.7	42.487	780.008	135.991	0.131			86.906	86.906		
INC181	DEFAULT	Chesapeake Operating Inc - Hondo Federal Gas	568814.070	3629620.530	3468.8	6.004	860.000	53.314	0.787			18.254	18.254		
INC182	DEFAULT	EOG - War Dog State No1H		3637607.080	3427.3	60.007	1831.730	65.617	1.673			1.429	1.429		
INC183	DEFAULT	DCP - Pecos Booster Station		3623798.120	3405.4	14.009	1000.004	47.014	0.656			53.969	53.969		
INC184	DEFAULT	DCP - Pecos Booster Station		3623798.120	3405.4	14.009	1000.004	47.014	0.656			53.969	53.969		
INC185 INC186	DEFAULT DEFAULT	DCP - Pecos Booster Station DCP - Pecos Diamond Gas Plant		3623798.120 3625977.910	3405.4 3541.9	14.009 50.000	1000.004 600.008	47.014 104.987	0.656 0.984			53.969 118.256	53.969 118.256		
INC 186	DEFAULT	DCP - Pecos Diamond Gas Plant DCP - Pecos Diamond Gas Plant		3625977.910	3541.9	39.993	600.008	104.987	0.984			116.669	116.669		
INC188	DEFAULT	DCP - Pecos Diamond Gas Plant		3625987.940	3546.4	20.013	800.006	6.988	1.509			2.381	2.381		
INC189	DEFAULT	DCP - Pecos Diamond Gas Plant		3626095.860	3539.0	20.013	600.008	8.990	0.492			1.631	1.631		
INC190	DEFAULT	Lucid Artesia - Southern Union Compressor Station		3631625.290	3507.3	22.966	854.330	91.864	0.984			0.794	0.794		
INC191	DEFAULT	Lucid Artesia - Southern Union Compressor Station		3631620.330	3507.0	23.589	1011.992	135.007	1.247			15.080	15.080		
INC192	DEFAULT	Lucid Artesia - Southern Union Compressor Station		3631621.470	3506.1	23.589	1011.992	135.007	1.247			15.080	15.080		
INC193	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590	3626398.760	3534.7	27.001	669.992	200.000	1.280			-117.419	-117.419		ı

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

7101191 101		nt Source Increment Input Data (Updated 5-5-21)								Potential to Emit (lb/hr)					
	Stack Release		Easting (X)	Northing (Y)	Base Elevation	Stack		Exit Velocity	Stack Diameter						
Source IE		Source Description	(m)	(m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC194	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	39.993	669.992	200.000	1.280			-103.466	-103.466		
INC195	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	37.992	719.996	185.007	1.280			-331.056	-331.056		
INC196 INC197	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626398.760 3626398.760	3534.7 3534.7	31.102 22.966	730.004 854.330	181.004 91.864	1.476 0.984			-357.512 -105.478	-357.512 -105.478		
INC 197	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	955.004	200.000	1.575			-444.850	-444.850		
INC199	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.991	759.002	170.013	1.444			-215.630	-215.630		
INC200	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	39.993	759.002	160.007	1.509			-329.244	-329.244		
INC201 INC202	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7 3554.4	29.987 31.004	1085.000 899.996	100.000	0.656 1.969			-8.879 -0.725	-8.879 -0.725		
INC202 INC203	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626723.090 3626398.760	3534.4	20.997	600.008	12.992 33.990	1.969			-0.725 -1.812	-0.725 -1.812		
INC204	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	33.005	924.998	200.000	1.608			-143.512	-143.512		
INC205	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	24.016	687.992	100.000	0.656			-5.436	-5.436		
INC206	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	26.411	861.998	187.106	0.853			-39.286	-39.286		
INC207 INC208	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626398.760 3626398.760	3534.7 3534.7	26.411 114.993	861.998 1831.730	187.106 65.617	0.853 68.261			-59.525 0.714	-59.525 0.714		
INC200	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	114.993	1831.730	65.617	68.261			0.714	0.714		
INC210	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	854.006	162.008	0.984			34.818	34.818		
INC211	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	854.006	162.008	0.984			30.223	30.223		
INC212 INC213	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7 3552.8	35.007 54.495	854.006 1149.998	162.008 19.882	0.984 3.510			32.744	32.744		
INC213 INC214	DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626699.000 3626693.930	3553.1	35.007	854.006	162.008	0.984			1.587 33.351	1.587 33.351		
INC215	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	854.006	162.008	0.984			34.921	34.921		
INC216	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626709.080	3555.0	54.495	1149.998	27.690	3.510			0.397	0.397		
INC217	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	854.006	162.008	0.984			34.921	34.921		
INC218	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	989.996	184.908	0.984			23.810	23.810		
INC219 INC220	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626398.760 3626715.280	3534.7 3552.9	35.007 120.013	989.996 600.008	184.908 17.192	0.984 6.168			23.810 61.112	23.810 61.112		
INC221	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626701.560	3552.6	120.013	600.008	17.192	6.168			61.112	61.112		
INC222	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626692.450	3552.8	120.013	600.008	13.911	2.493			7.937	7.937		
INC223	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626693.070	3553.5	29.987	600.008	25.098	2.493			14.286	14.286		
INC224	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626703.390	3554.8	114.993 114.993	1832.000	65.584	28.445			37.509	37.509		
INC225 INC226	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626718.070 3626729.250	3555.6 3556.0	114.993	1832.000 1832.000	65.584 65.584	28.445 28.445			9.060 9.060	9.060 9.060		
INC227	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626730.710	3554.9	114.993	1832.000	65.584	28.445			2.537	2.537		
INC228	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626721.380	3553.1	114.993	1832.000	65.584	28.445			1.812	1.812		
INC229	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626706.030	3552.3	114.993	1832.000	65.584	28.445			18.120	18.120		
INC230 INC231	DEFAULT DEFAULT	Lucid Artesia - Four Dinkus Compressor Station GCP4 Lucid Artesia - Four Dinkus Compressor Station GCP5		3625305.660 3625305.660	3622.6 3622.6	20.013 20.013	860.000 860.000	60.499 60.499	0.984 0.984			20.635 20.635	20.635 20.635		
INC231	DEFAULT	DCP - Carbon Valley Booster		3638669.910	3469.5	50.000	1831.730	65.617	68.261			521.437	521.437		
INC233	DEFAULT	DCP - Carbon Valley Booster		3638676.940	3468.6	14.993	1124.996	118.209	1.247			18.254	18.254		
INC234	DEFAULT	DCP - Carbon Valley Booster	571607.440	3638680.490	3468.3	14.993	1124.996	118.209	1.247			18.254	18.254		
INC235	DEFAULT	DCP - Carbon Valley Booster		3638671.500	3469.6	14.993	1124.996	118.209	1.247			18.254	18.254		
INC236 INC237	DEFAULT DEFAULT	DCP - Carbon Valley Booster DCP - Carbon Valley Booster		3619797.520 3619458.070	3472.0 3476.6	14.993 18.406	1831.730 350.006	65.617 4.298	68.261 0.984			0.000 -118.126	0.000 -118.126		
INC237	DEFAULT	DCP - Carbon Valley Booster		3620198.100	3465.0	60.007	600.008	20.013	2.001			11.905	11.905		
INC239	DEFAULT	DCP - Carbon Valley Booster		3619806.000	3471.9	10.007	219.992	100.000	0.492			2.381	2.381		
INC240	DEFAULT	Lucid Artesia - North Pen Compressor Station		3619909.060	3477.3	20.013	1831.730	65.617	68.261			0.079	0.079		
INC241	DEFAULT	Lucid Artesia - North Pen Compressor Station		3619498.130	3473.5	20.997	869.000	152.297	0.984			44.445	44.445		
INC242 INC243	DEFAULT DEFAULT	Lucid Artesia - North Pen Compressor Station		3619498.130 3619917.540	3473.5 3477.3	20.997 22.966	869.000 854.330	152.297 91.864	0.984 0.984			44.445 2.356	44.445 2.356		
INC243	DEFAULT	Lucid Artesia - North Pen Compressor Station Carbon Valley 14 Fed Com No2		3643077.800	3585.2	10.499	1045.004	1.706	2.395			26.191	26.191		
INC245	DEFAULT	EOG - Rumble State No5		3620827.160	3569.2	25.000	1831.730	65.617	68.261			0.079	0.079		
INC246	DEFAULT	EOG - Rumble State No5		3620834.180	3568.8	25.000	1831.730	65.617	68.261			1.746	1.746		
INC247	DEFAULT	EOG - Rumble State No4		3620837.730	3569.0	14.993	600.008	3.806	0.984			0.238	0.238		
INC248 INC249	DEFAULT DEFAULT	EOG - Rumble State No5 EOG - Rumble State No6		3620820.590 3620815.620	3569.5 3569.2	14.993 14.993	831.992 831.992	171.588 171.588	0.984 0.984			12.064 12.064	12.064 12.064		
INC249 INC250	DEFAULT	EOG - Rumble State Noo EOG - Lacama 20 State Com 602H		3621962.920	3614.3	25.000	1831.730	65.617	68.261			0.079	0.079		
INC251	DEFAULT	EOG - Lacama 20 State Com 602H		3621969.940	3613.0	25.000	1831.730	65.617	68.261			3.016	3.016		
INC252	DEFAULT	EOG - Lacama 20 State Com 602H	545073.020	3621973.500	3613.1	14.993	1131.008	30.020	0.689			1.270	1.270		
INC253	DEFAULT	EOG - Lacama 20 State Com 602H		3621971.400	3613.7	14.993	930.992	192.946	0.689			6.032	6.032		
INC254 INC255	DEFAULT DEFAULT	EOG - Lacama 20 State Com 602H EOG - Lacama 20 State Com 602H		3621964.500 3621956.350	3614.7 3615.7	14.993 14.993	831.992 1254.992	349.934 161.877	0.689 0.689			12.064 13.334	12.064 13.334		
INC255	DEFAULT	Atoka No1 Compressor Station		3627167.900	3665.9	16.601	1099.994	131.004	0.656			21.429	21.429		
INC257	DEFAULT	Atoka No1 Compressor Station		3627167.900	3665.9	50.000	1200.002	102.986	0.656			17.461	17.461		
INC258	DEFAULT	Atoka No1 Compressor Station	572460.800	3627167.900	3665.9	50.000	1200.002	102.986	0.656			17.461	17.461		

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

		ont Source increment input Data (Opuated 3-3-21)								Potenti	al to Emit (b/hr)		
	Stack			Base				Stack						
Source ID	Release Type	Source Description	Easting (X) Northing (Y) (m) (m)	Elevation (ft)	Stack Height (ft)	Temp (F)	Exit Velocity (ft/sec)	Diameter (ft)	PM10	PM25 ST PM25 LT	NO2 ST	NO2 LT	SO2_ST	SO2 LT
INC259	DEFAULT	Atoka No1 Compressor Station	572460.800 3627167.900		60.007	1025.006	81.004	0.984	1 141 10	1 M25_51 1 M25_E1	38.096	38.096	002_01	002_L1
INC259	DEFAULT	Atoka No1 Compressor Station	572460.800 3627167.900		50.007	1200.002	102.986	0.964			17.461	17.461		
INC261	DEFAULT	Illinois Camp Booster Station	574661.630 3627054.860		35.007	1340.006	57.415	0.656			39.683	39.683		
INC262	DEFAULT	Illinois Camp Booster Station	574634.650 3627054.880	3659.7	35.007	1340.006	57.415	0.656			39.683	39.683		
INC263	DEFAULT	Illinois Camp Booster Station	574643.640 3627054.830		35.007	1340.006	57.415	0.656			39.683	39.683		
INC264	DEFAULT	Illinois Camp Booster Station	574652.630 3627054.900		35.007	1340.006	57.415	0.656			39.683	39.683		
INC265 INC266	DEFAULT DEFAULT	Chalk Compressor Station Cimarex Enegy - Montana 1 Fee 3	569361.150 3621748.040 551935.760 3616514.870		22.014 10.007	465.008 887.000	49.803 358.301	1.115 0.492			12.540 11.349	12.540 11.349		
INC260	DEFAULT	Kristina Booster Station	572690.330 3624526.200		20.013	780.008	366.010	0.492			69.842	69.842		
INC268	DEFAULT	Mack - Mark Twain Federal Com Battery	575824.070 3636427.600		6.988	224.996	381.988	6.988			3.968	3.968		
INC269	DEFAULT	Dickens 29 Federal Battery	575704.960 3639831.920		6.988	224.996	381.988	6.988			3.968	3.968		
INC270	DEFAULT	Oxy USA IncSpurck 16 State Com No2	576460.460 3633013.760		22.966	854.330	91.864	0.984			7.143	7.143		
INC271	DEFAULT	Yates Petroleum - Pierre State No1 Facility	570982.950 3620931.670		22.966	854.330	91.864	0.984			4.457	4.457		
INC272 INC273	DEFAULT DEFAULT	Shakespeare 20 Federal No1 Artesia Gas Plant	575701.430 3640657.870 573990.740 3624597.900		10.991 40.289	564.998 1340.006	32.251 89.206	0.492 0.984			3.262 41.584	3.262 41.584		
INC273	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		40.289	1340.006	89.206	0.984			42.064	42.064		
INC275	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		44.685	750.002	21.194	2.986			57.144	57.144		
INC276	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		58.005	800.006	60.991	0.984			-324.532	-324.532		
INC277	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	58.005	800.006	60.991	0.984			-302.788	-302.788		
INC278	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		58.005	800.006	60.991	0.984			-241.179	-241.179		
INC279	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		58.990	800.006	54.987	0.984			-311.304	-311.304		
INC280 INC281	DEFAULT DEFAULT	Artesia Gas Plant Artesia Gas Plant	573990.740 3624597.900 573990.740 3624597.900		41.010 43.996	1000.004 986.000	49.016 58.005	0.984 0.984			-132.821 -140.613	-132.821 -140.613		
INC281	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		43.990	986.000	58.005	0.984			-164.658	-164.658		
INC283	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			-36.240	-36.240		
INC284	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			28.196	28.196		
INC285	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			84.128	84.128		
INC286	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			84.128	84.128		
INC287	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		75.000	1832.000	65.584	1.673			-17.690	-17.690		
INC288	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		42.290	750.002	21.194	3.609			57.144	57.144		
INC289 INC290	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		41.995 41.995	899.996	60.007	0.820 0.984			-5.056	-5.056		
INC290 INC291	DEFAULT DEFAULT	Artesia Gas Plant Artesia Gas Plant	573990.740 3624597.900 573999.690 3624382.850		70.604	854.996 1831.730	162.992 65.617	68.261			37.076 1.667	37.076 1.667		
INC291	DEFAULT	Artesia Gas Plant	574011.530 3624386.830		70.604	1831.730	65.617	68.261			0.714	0.714		
INC293	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		33.104	629.996	20.801	3.609			2.381	2.381		
INC294	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	45.997	1340.006	89.206	0.984			42.064	42.064		
INC295	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		41.995	854.996	162.992	0.984			35.772	35.772		
INC296	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		41.995	854.996	162.992	0.984			32.394	32.394		
INC297	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		41.995	854.996	162.992	0.984			39.637	39.637		
INC298 INC299	DEFAULT DEFAULT	Artesia Gas Plant Artesia Gas Plant	573990.740 3624597.900 573990.740 3624597.900		40.289 41.995	1340.006 854.996	89.206 162.992	0.984 0.984			41.584 34.604	41.584 34.604		
INC299	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1124.996	147.900	0.984			68.255	68.255		
INC301	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			42.064	42.064		
INC302	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	45.997	1340.006	89.206	0.984			42.064	42.064		
INC303	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			84.128	84.128		
INC304	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			84.128	84.128		
INC305	DEFAULT	Yates - Eastern Shores QW No1 Facility	565479.650 3615436.960		9.843	571.010	49.213	0.328			33.096	33.096		
INC306 INC307	DEFAULT DEFAULT	EOG - Secretariat 3 Fed Com No501H Frontier - Coyote Compressor Station	569284.850 3617086.880 578708.300 3628257.940		60.007 16.010	1831.730 1500.008	65.617 0.098	1.673 2.756			9.048 0.238	9.048 0.238		
INC307	DEFAULT	Frontier - Coyote Compressor Station Frontier - Coyote Compressor Station	578715.830 3628264.960		20.013	989.996	141.995	2.756 1.148			17.866	17.866		
INC309	DEFAULT	Frontier - Coyote Compressor Station	578701.450 3628266.420		22.014	600.008	18.012	0.820			0.079	0.079		
INC310	DEFAULT	Frontier - Coyote Compressor Station	578697.210 3628259.520		20.013	989.996	141.995	1.148			24.127	24.127		
INC311	DEFAULT	Frontier - Coyote Compressor Station	578698.860 3628251.370		22.999	872.996	127.986	0.919			46.906	46.906		
INC312	DEFAULT	Parallel - Hagerman Plant GCP4-3380	562777.140 3657403.570		22.966	854.330	91.864	0.984			0.556	0.556		
INC313	DEFAULT	Parallel - Hagerman Plant GCP4-3381	562784.680 3657410.590		22.966	854.330	91.864	0.984			1.429	1.429		
INC314 INC315	DEFAULT DEFAULT	Parallel - Hagerman Plant GCP4-3382 Parallel - Hagerman Plant GCP4-3383	562777.890 3657414.140 562770.300 3657412.050		22.999 22.999	854.006 854.006	162.008 162.008	0.984 0.984			35.153 35.153	35.153 35.153		
INC315	DEFAULT	COG - Man State 2H Battery	574496.980 3618616.590		16.010	1831.730	65.617	2.592			9.524	9.524		
INC310	DEFAULT	COG - Man State 2H Battery	574504.510 3618623.610		12.008	1043.006	189.993	0.328			3.968	3.968		
INC318	DEFAULT	Shelby 23 Tank Battery	551738.940 3611091.610		25.000	249.998	21.621	0.656			0.714	0.714		
INC319	DEFAULT	Shelby 23 Tank Battery	551746.480 3611098.630	3409.0	25.000	249.998	21.621	0.656			0.714	0.714		
INC320	DEFAULT	Shelby 23 Tank Battery	551739.690 3611102.180		25.000	249.998	21.621	0.656			0.714	0.714		
INC321	DEFAULT	Shelby 23 Tank Battery	551732.090 3611100.090		25.000	249.998	21.621	0.656			0.714	0.714		
INC322	DEFAULT	Spur - Shelby 23 Tank Battery	551729.500 3611085.030		35.007	1831.730	65.617	8.635			4.048	4.048		
INC323	DEFAULT	Spur - Shelby 23 Tank Battery	551736.450 3611080.070	3410.2	29.987	1831.730	65.617	8.635			4.048	4.048		I

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

											Potenti	al to Emit (l	b/hr)		
	Stack				Base				Stack						
	Release		Easting (X)	Northing (Y)	Elevation	Stack		Exit Velocity							
Source ID	Type	Source Description	(m)	(m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC324	DEFAULT	EOG- Falcata Battery	540689.170	3616360.840	3695.3	14.993	1131.008	29.987	0.689			1.270	1.270		
INC325	DEFAULT	EOG- Falcata Battery	586879.330	3576089.170	3002.3	14.993	930.992	192.946	0.689			6.032	6.032		
INC326	DEFAULT	EOG- Falcata Battery	540689.920	3616371.420	3696.4	14.993	831.992	349.934	0.689			12.064	12.064		
INC327	DEFAULT	EOG- Falcata Battery	540682.320	3616369.320	3695.0	14.993	600.008	161.877	0.689			13.334	13.334		
INC328	DEFAULT	EOG- Falcata Battery	540678.080	3616362.420	3693.9	39.993	1831.730	65.617	8.635			5.079	5.079		
INC329	DEFAULT	EOG- Falcata Battery	540679.740	3616354.270	3693.4	39.993	1831.730	65.617	68.261			0.794	0.794		
INC330	DEFAULT	EOG- Falcata Battery	540686.680	3616349.310	3694.0	14.993	600.008	17.848	0.689			0.873	0.873		
INC331	DEFAULT	Winchester Compressor Station	567991.310	3612198.320	3519.7	39.993	960.998	41.010	1.214			33.334	33.334		
INC332	DEFAULT	Winchester Compressor Station	567991.310	3612198.320	3519.7	39.993	960.998	41.010	1.214			33.334	33.334		
INC333	DEFAULT	Winchester Compressor Station	567991.310	3612198.320	3519.7	39.993	960.998	41.010	1.214			33.334	33.334		
INC334	DEFAULT	Spur Energy - Ross Ranch Battery	548845.660	3611195.950	3472.1	35.007	1831.730	65.617	29.754			89.208	89.208		

All sources within 25km and large (1,000lb/hr) emitters within 50km were included in the increment analysis.

HollyFrontier Off-Site Volume Source Increment Input Data (Updated 5-5-21)

,	m-Site Volume Source increment input Data (Opuater									Potent	ial to Emit (lb/hr)		
		5	N . 41	Base	D.1									
Source ID	Source Description	Easting (X)	Northing (Y) (m)	(ft)		Sigma Y (ft)	Sigma 7 (ft)	PM10	PM25 ST	PM25 I T	NO2 ST	NO2_LT	SO2 ST	SO2 LT
INC335	Schlumberger - Artesia District Bulk Facility	556719.31	3635718.50	3362.8	3.28	1.54	3.05	2.38	FIMIZU_UI	FWIZ5_LT	1402_31	NOZ_L1	302_31	302_L1
INC336	Schlumberger - Artesia District Bulk Facility	556726.85	3635725.52	3362.7	3.28	1.54	3.05	0.72						
INC337	Land O' Lakes Purina Feed - Artesia Feed Mill	556293.38	3637108.22	3373.8	20.01	1.54	3.05	0.72						
INC338	Holly Frontier Asphalt Company	556993.36	3637208.13	3360.0	32.81	32.81	30.51	6.51						
INC339	Holly Frontier Asphalt Company	556985.77	3637206.04	3360.1	32.81	32.81	30.51	6.50						
INC340	Holly Frontier Asphalt Company	556981.53	3637199.14	3360.1	32.81	32.81	30.51	6.35						
INC341	Par Five Energy LLC - Par Five Energy	564319.69	3632835.00	3342.9	3.28	1.54	3.05	2.38						
INC342	Par Five Energy LLC - Par Five Energy	564327.22	3632842.02	3343.0	32.81	32.81	30.51	5.56						
INC343	Helena Chemical Co - Artesia New Mexico	557950.20	3646037.75	3342.1	3.28	1.54	3.05	0.24						
INC344	Helena Chemical Co - Artesia New Mexico	557957.74	3646044.77	3341.9	3.28	1.54	3.05	0.56						
INC345	Helena Chemical Co - Artesia New Mexico	557950.95	3646048.32	3341.9	3.28	1.54	3.05	2.38						
INC346	Helena Chemical Co - Artesia New Mexico	557943.36	3646046.23	3342.0	3.28	1.54	3.05	0.24						
INC347	Helena Chemical Co - Artesia New Mexico	557939.12	3646039.33	3342.2	3.28	1.54	3.05	0.16						
INC348	Helena Chemical Co - Artesia New Mexico	557940.77	3646031.17	3342.2	3.28	1.54	3.05	0.48						
INC349	EOG - Rumble State No4	547030.03	3620827.16	3569.2	32.81	32.81	30.51	4.52						
INC350	EOG - Rumble State No5	547030.78	3620837.73	3569.0	14.99	1.54	3.05	0.08						
INC351	EOG - Rumble State No6	547023.19	3620835.64	3569.4	14.99	1.54	3.05	0.04						
INC352	EOG - Lacama 20 State Com 602H	545072.27	3621962.92	3614.3	32.81	32.81	30.51	4.92						
INC353	EOG - Lacama 20 State Com 602H	545062.83	3621956.35	3615.7	14.99	1.54	3.05	80.0						
INC354	Shelby 23 Tank Battery	551727.85	3611093.19	3409.7	25.00	1.54	3.05	0.08						
INC355	EOG- Falcata Battery	540689.17	3616360.84	3695.3	3.28	1.54	3.05	3.65						
INC356	Spur Energy - Ross Ranch Battery	548838.12	3611188.93	3472.3	25.00	1.54	3.05	0.04						
INC357	Spur Energy - Ross Ranch Battery	548845.66	3611195.95	3472.1	25.00	1.54	3.05	0.04						
INC358	Spur Energy - Ross Ranch Battery	548838.87	3611199.51	3472.7	25.00	1.54	3.05	0.04						
INC359	Spur Energy - Ross Ranch Battery	548831.28	3611197.41	3473.0	25.00	1.54	3.05	0.04						
INC360	Schlumberger - Artesia District Bulk Facility	556719.31	3635718.50	3362.8	3.28	1.54	3.05		2.381	2.381				
INC361	Schlumberger - Artesia District Bulk Facility	556726.85	3635725.52	3362.7	3.28	1.54	3.05		0.725	0.725				
INC362	EOG - Rumble State No4	547030.03	3620827.16	3569.2	32.81	32.81	30.51		0.476	0.476				
INC363	EOG - Rumble State No5	547030.78	3620837.73	3569.0	14.99	1.54	3.05		0.079	0.079				
INC364	EOG - Rumble State No6	547023.19	3620835.64	3569.4	14.99	1.54	3.05		0.037	0.037				
INC365	EOG - Lacama 20 State Com 602H	545072.27	3621962.92	3614.3	32.81	32.81	30.51		0.476	0.476				
INC366	EOG - Lacama 20 State Com 602H	545062.83	3621956.35	3615.7	14.99	1.54	3.05		0.079	0.079				
INC367	COG - Man State 2H Battery	574496.98	3618616.59	3549.2	3.28	1.54	3.05		1.812	1.812				
INC368	Shelby 23 Tank Battery	551727.85	3611093.19	3409.7	25.00	1.54	3.05		0.079	0.079				
INC369	EOG- Falcata Battery	540689.17	3616360.84	3695.3	3.28	1.54	3.05		0.317	0.317				
INC370	Spur Energy - Ross Ranch Battery	548838.12		3472.3	25.00	1.54	3.05		0.037	0.037				
INC371	Spur Energy - Ross Ranch Battery	548845.66	3611195.95	3472.1	25.00	1.54	3.05		0.037	0.037				
INC372 INC373	Spur Energy - Ross Ranch Battery Spur Energy - Ross Ranch Battery	548838.87 548831.28	3611199.51 3611197.41	3472.7 3473.0	25.00 25.00	1.54 1.54	3.05 3.05		0.037 0.037	0.037 0.037				
INC374	Lime Rock - Malco B Battery	563974.50	3627080.87	3442.5	22.01	1.54	3.05		0.037	0.037			26.191	26.191
INC375	Lime Rock - Condor 7 Battery	563709.45	3625436.95	3287.2	22.01	1.54	3.05						3.968	3.968
INC376	Lime Rock - Condor 7 Battery	563716.98	3625443.97	3287.6	22.01	1.54	3.05						3.968	3.968
INC377	Ramirez & Sons Inc - Crusher No2	552788.48	3623752.45	3448.6	32.81	1410.76	30.51						181.202	181.202
INC378	Lime Rock - Condor Stirling Battery	563708.44	3625403.35	3286.5	22.01	1.54	3.05						6.349	6.349
INC379	Lime Rock - Condor Stirling Battery	563715.98	3625410.37	3286.7	22.01	1.54	3.05						6.349	6.349
INC380	Lime Rock - Condor Stirling Battery	563709.19	3625413.92	3286.7	22.01	1.54	3.05						10.318	10.318
INC381	Lime Rock - Hawk 8 Battery	565549.93	3624873.88	3444.8	22.01	1.54	3.05						18.254	18.254
INC382	Lime Rock - Hawk 8 Battery	565543.14	3624877.43	3444.7	20.01	1.54	3.05						18.254	18.254
INC383	Lime Rock - Hondo Federal Battery	567436.20	3626826.66	3582.7	22.01	1.54	3.05						13.492	13.492
INC384	Lime Rock - Hondo Federal Battery	567429.41	3626830.21	3582.7	22.01	1.54	3.05						13.492	13.492
INC385	EOG - Rumble State No4	547037.57	3620834.18	3568.8	14.99	1.54	3.05						0.079	0.079
INC386	Cimarex Enegy - Montana 1	551943.30	3616521.89	3422.5	3.28	1.54	3.05						10.000	10.000
INC387	Total Malfunction Construction	573989.09	3624401.33	3608.9	3.28	1.54	3.05						685.124	685.124
INC388	Total Malfunction Construction	573990.74	3624393.17	3608.6	3.28	1.54	3.05						18.120	18.120
INC389	Frontier - Coyote Compressor Station	578698.86	3628251.37	3668.9	3.28	1.54	3.05						18.120	18.120
INC390	Southeast Readi-Mix - Artesia Plant	557117.00	3635667.03	3356.9	32.81	721.78	30.51				172.142	172.142		
INC391	Ramirez & Sons Inc - Crusher No2	552788.48	3623752.45	3448.6	32.81	1410.76	30.51				344.284	344.284		
INC392	EOG - Rumble State No4	547023.19	3620835.64	3569.4	14.99	1.54	3.05				0.873	0.873		

HollyFrontier Off-Site Volume Source Increment Input Data (Updated 5-5-21)

										Potentia	al to Emit (lb/hr)		
Source ID	Source Description	Easting (X) (m)	Northing (Y) (m)	Base Elevation (ft)		Sigma Y (ft)	Sigma Z (ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC393	EOG - Rumble State No5	547018.95	3620828.74	3569.5	14.99	1.54	3.05				0.476	0.476		
INC394	EOG - Lacama 20 State Com 602H	545069.78	3621951.39	3615.9	14.99	1.54	3.05				0.873	0.873		
INC395	Artesia Gas Plant	573981.91	3624410.31	3609.4	3.28	1.54	3.05				17.939	17.939		
INC396	Artesia Gas Plant	573979.32	3624394.96	3608.8	3.28	1.54	3.05				18.120	18.120		
INC397	Frontier - Coyote Compressor Station	578705.81	3628246.40	3669.1	3.28	1.54	3.05				18.120	18.120		
INC398	Spur - Shelby 23 Tank Battery	551727.85	3611093.19	3409.7	25.00	1.54	3.05				0.476	0.476		
INC399	Spur Energy - Ross Ranch Battery	548838.12	3611188.93	3472.3	25.00	1.54	3.05				0.476	0.476		
INC400	Spur Energy - Ross Ranch Battery	548838.87	3611199.51	3472.7	25.00	1.54	3.05				0.476	0.476		
INC401	Spur Energy - Ross Ranch Battery	548831.28	3611197.41	3473.0	25.00	1.54	3.05				0.476	0.476		
INC402	Spur Energy - Ross Ranch Battery	548827.04	3611190.51	3472.9	25.00	1.54	3.05				0.476	0.476		
INC403	WPX - DD and EE Federal Leases	543610.96	3613500.45	3619.1	3.28	1.54	3.05				0.397	0.397		

HollyFrontier Navajo Volume Source Parameter Calculation

				Source Dime	nsions				Initial Dispers	sion Coefficients	
									Initial		
					Square	Structure		Tank	Horizontal		
					Root of	Height/Vertical	Release	Diameter	Dimension s _Y	Initial Vertical	
Source ID	Source Description	Length (ft)	Width (ft)	Area (ft2)	Area (ft)	Dimension (ft)	Height (ft)	(ft)	(ft)	Dimension sz (ft)	Note
TRLO_9	Molten Sulfur Railcar Loading	10.0	10.0	100.00	10.00	15.00	15.00	NA	2.33	6.98	Elevated source on or adjacent to building
T_0049	Slop Oil Tank	NA	NA	94.99	9.75	36.00	36.00	11.00	2.27	16.74	Elevated source on or adjacent to building
T_0081	Asphalt/Pitch Tank	NA	NA	9241.22	96.13	40.00	40.00	108.50	22.36	18.60	Elevated source on or adjacent to building
T_0082	Asphalt/Pitch Tank	NA	NA	15386.00	124.04	40.00	40.00	140.00	28.85	18.60	Elevated source on or adjacent to building
T_0110	Asphalt/Pitch Tank	NA	NA	9156.24	95.69	35.00	35.00	108.00	22.25	16.28	Elevated source on or adjacent to building
T_0410	Asphalt/Pitch Tank	NA	NA	4899.19	69.99	40.00	40.00	79.00	16.28	18.60	Elevated source on or adjacent to building
T_0420	Asphalt/Pitch Tank	NA	NA	1962.50	44.30	30.00	30.00	50.00	10.30	13.95	Elevated source on or adjacent to building
T_0814	Asphalt/Pitch Tank	NA	NA	1962.50	44.30	32.00	32.00	50.00	10.30	14.88	Elevated source on or adjacent to building
T_0914	Slop Oil Tank	NA	NA	4415.63	66.45	40.00	40.00	75.00	15.45	18.60	Elevated source on or adjacent to building
T_1227	Asphalt/Pitch Tank	NA	NA	4654.27	68.22	40.00	40.00	77.00	15.87	18.60	Elevated source on or adjacent to building
T_0106	T-0106 Sour Water Tank	NA	NA	3523.87	59.36	40.00	40.00	67.00	13.81	18.60	Elevated source on or adjacent to building
T_0435	T-0435 Sour Water Tank	NA	NA	706.50	26.58	40.00	40.00	30.00	6.18	18.60	Elevated source on or adjacent to building
T_0437	T-0437 Crude Oil Tank	NA	NA	11304.00	106.32	40.00	40.00	120.00	24.73	18.60	Elevated source on or adjacent to building
T_0439	T-0439 Sour Naphtha Tank	NA	NA	13266.50	115.18	46.00	46.00	130.00	26.79	21.40	Elevated source on or adjacent to building
T_0450	T-0450 Sour Naphtha Tank	NA	NA	11304.00	106.32	40.00	40.00	120.00	24.73	18.60	Elevated source on or adjacent to building
T_0737	T-0737 Sour Water Tank	NA	NA	3115.67	55.82	40.00	40.00	63.00	12.98	18.60	Elevated source on or adjacent to building
T_0802	T-0802 Sour Water Tank	NA	NA	1589.63	39.87	40.00	40.00	45.00	9.27	18.60	Elevated source on or adjacent to building
T_0830	T-0830 Slop Oil Tank	NA	NA	15386.00	124.04	40.00	40.00	140.00	28.85	18.60	Elevated source on or adjacent to building
T_1225	T-1225 Crude Oil Tank	NA	NA	17662.50	132.90	40.00	40.00	150.00	30.91	18.60	Elevated source on or adjacent to building

NA - Not applicable.

Sigma Y values calculated as the square root of the area, or average length of side, divided by 4.3 (Table 3-1 of AERMOD Manual for Single Volume Source). Area for tanks calculated from diameter.

Sigma Z values for surface based sources calculated as the initial vertical dimension of source divided by 2.15 (Table 3-1 of AERMOD Manual for Elevated Source Not on or Adjacent to Building).

Sigma Z values for elevated sources on or adjacent to a building calculated as the building height divided by 2.15 (Table 3-1 of AERMOD Manual for Elevated Source on or Adjacent to Building).

Sigma Z values for elevated sources not on or adjacent to a building calculated as the initial vertical dimension of source divided by 4.3 (Table 3-1 of AERMOD Manual for Elevated Source Not on or Adjacent to Building).

Release height for tanks and railcar loading equal to top of tank/railcar as this is where emissions occur.

HollyFrontier Flare Stack Parameter Calculation

Source ID	Source Description	Effective Stack Height (ft)	Temp. (°F)	Exit Velocity (ft/sec)	Effective Stack Diameter (ft)	MMBtu/hr	cal/sec	Actual Stack Height (ft)
FL0400	FL-0400, North Plant Flare	395.1	1832	65.6	16.11	8440	5.91E+08	162.0
FL0401	FL-0401, South Plant Flare	342.2	1832	65.6	9.60	3000	2.10E+08	200.0
FL0402	FL-0402, FCC Flare	304.6	1832	65.6	9.28	2800	1.96E+08	167.0
FL0403	FL-0403, Alky Flare	499.1	1832	65.6	19.45	12300	8.61E+08	220.0
FL0404	FL-0404, GOHT Flare	568.5	1832	65.6	26.01	22000	1.54E+09	200.0
TL4VCU	TL-4 VCU	81.8	1832	65.6	3.92	500	3.50E+07	21.4
FLHEP	HEP Portable Flare	51.1	1832	65.6	2.29	170	1.19E+07	15.0
TVCU	Tank VCU	18.5	1832	65.6	0.20	1.26	8.82E+04	15.0

Per AERSCREEN Manual

2.1.2 *Flares*

Flare sources are denoted by the term "** FLARE DATA" in the input file in the line above the source parameters. Flare source inputs are, with English and metric units:

- emission rate (lb/hr or g/s)
- stack height (feet or meters)
- total heat release rate (cal/sec)
- radiative heat loss fraction

The heat loss fraction can be user selected or the SCREEN3 default value of 0.55. For information about heat loss fractions, see Leahey and Davies (1984). AERSCREEN will process

the flare in AERMOD as a POINT source type. For the exit velocity and exit temperature, AERSCREEN defaults these values to 20 m/s and 1,273 K, respectively as done in SCREEN3 (U.S. EPA, 1995). The stack diameter and effective stack height used in AERMOD are calculated from the inputs as:

$$D = 9.88 \times 10^{-4} \times \sqrt{HR \times (1 - HL)} \tag{1}$$

$$h_{eff} = H_s + 4.56 \times 10^{-3} \times HR^{0.478} \tag{2}$$

Where D is effective stack diameter, HR is the heat release rate, HL is the heat loss fraction, H_{eff} is effective stack height and H_s is the stack height entered by the user.

1 MMBtu (IT)/hour [MMBtu/h] = 69998.8225308643 calorie (IT)/second [cal/s] HL is assumed to be 0.55 per AERSCREEN Manual

Holly Frontier - Artesia CALPUFF Input

	Model	LCC East	LCC North	Stack Height	Base Elevation	Stack Diameter	Exit Velocity		Sigma Y	Sigma Z	Momentum	SO ₂	SO2LT	SO ₄	SO₄LT	NOx	РМС	EC	SOA
Model Source Description	Source ID	(km)	(km)	(m)	(m)	(m)	•	Temp. (K)	•	(m)	Flux	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)
Unit 13 Naphtha Splitter Reboiler	H0009	-691.753	-762.453	23.63	1025.42	1.37	5.46	549.82	0	0	1	0.183	0.000	0.091	0.000	0.540	0.084	0.021	0.000
Unit 06 HDS Reboiler	H0018	-691.742	-762.355	22.87	1025.08	1.22	5.95	644.26	0	0	1	0.425	0.000	0.212	0.000	1.515	0.115	0.029	0.000
South Crude Charge Heater	H0019	-691.733	-763.054	47.46	1027.53	1.33	6.52	505.37	0	0	1	0.000	0.000	0.000	0.000	0.620	0.067	0.017	0.050
Unit 21 Heater	H0028	-691.531	-763.081	15.34	1027.71	0.81	5.73	727.59	0	0	1	0.100	0.000	0.050	0.000	1.718	0.031	0.008	0.000
Unit 06 Charge Heater	H0030	-691.741	-762.349	20.43	1025.05	1.22	6.86	574.82	0	0	1	0.188	0.000	0.094	0.000	1.002	0.000	0.000	0.000
Unit 13 Charge Heater	H0040	-691.740	-762.343	30.79	1025.02	1.22	6.95	583.15	0	0	1	0.000	0.000	0.000	0.000	0.720	0.000	0.000	0.000
Unit 10 FCC Feed Heater	H0312	-691.612	-762.409	29.41	1025.54	1.22	6.22	630.37	0	0	1	0.969	0.178	0.484	0.089	3.350	0.230	0.057	0.000
Unit 70 Stabilizer Reboiler Heater	H0355	-691.566	-762.385	41.21	1025.62	0.76	8.75	500.93	0	0	1	0.000	0.000	0.000	0.000	0.970	0.012	0.003	0.009
Unit 70 CCR Heaters	H0362_64	-691.579	-762.359	62.65	1025.63	2.13	5.15	443.15	0	0	1	1.338	0.000	0.669	0.000	2.506	0.310	0.077	0.000
Unit 44 Charge Heater	H0421	-691.550	-762.448	24.90	1025.61	0.99	7.23	616.48	0	0	1	0.238	0.000	0.119	0.000	0.630	0.074	0.018	0.000
SRU Hot Oil Heater	H0464	-691.786	-762.522	24.33	1025.71	0.84	2.93	505.37	0	0	1	0.000	0.000	0.000	0.000	0.053	0.009	0.002	0.007
Unit 33 Charge Heater	H0601	-691.522	-762.511	39.94	1025.71	1.98	3.54	422.04	0	0	1	0.798	0.000	0.399	0.000	1.304	0.235	0.059	0.000
Unit 45 Charge Heater	H2421	-691.542	-762.518	26.52	1025.69	1.07	7.56	749.82	0	0	1	0.000	0.000	0.000	0.000	0.023	0.024	0.006	0.018
Unit 25 ROSE® Unit No. 2 Hot Oil Heater	H2501	-691.369	-762.607	51.22	1025.76	2.39	5.79	649.82	0	0	1	4.352	1.641	2.176	0.821	3.600	0.993	0.248	0.000
SRU3 Hot Oil Heater	H3101	-691.759	-762.560	24.39	1025.75	0.84	2.93	505.37	0	0	1	0.411	0.162	0.205	0.081	0.330	0.092	0.023	0.000
Unit 34 Hydrocracker Reboiler 1	H3402	-691.370	-762.596	20.43	1025.72	1.22	8.51	574.82	0	0	1	1.886	0.711	0.943	0.356	1.560	0.430	0.108	0.000
Unit 34 Hydrocracker Reactor Charge Heat	H3403	-691.383	-762.589	26.24	1025.73	1.22	5.91	647.04	0	0	1	1.160	0.438	0.580	0.219	0.960	0.265	0.066	0.000
Unit 63 Hydrogen Plant Reformer Furnaces	H8801_02	-691.407	-762.518	39.63	1025.62	1.17	22.99	588.71	0	0	1	0.000	0.000	0.000	0.000	4.458	0.364	0.091	0.273
Unit 64 Hydrogen Plant Reformer	H9851	-691.407	-762.487	53.66	1025.62	3.05	7.26	449.82	0	0	1	0.000	0.000	0.000	0.000	11.222	2.594	0.648	1.945
SRU2 Tail Gas Incinerator	H0473	-691.792	-762.491	45.73	1025.63	1.22	13.48	894.26	0	0	1	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
SRU3 Tail Gas Incinerator	H3103	-691.764	-762.577	45.73	1025.82	1.22	15.21	922.04	0	0	1	50.000	18.740	25.000	9.370	6.500	13.320	3.330	0.000
FL-0404, GOHT Flare	FL0404	-691.387	-762.233	173.33	1024.95	7.93	20.00	1273.15	0	0	1	39.833	2.458	19.917	1.229	11.156	0.000	0.000	0.000
Notes:												101.88	24.33	50.94	12.16	54.74	19.25	4.81	2.30

Notes:
LCC Origin: 40.0N, 97.0W, Standard (Matching) Parallels: 33.0N, 45.0N. Datum: NWS-84.
PMCoarse (PMC) = PM between 2.5 and 10 um in diameter.
EC = elemental carbon

SOA = secondary organic aerosols

PM speciation based upon NPS guidance for NG Combustion Turbines.

Consensus Gas-fired Turbine

Example of Consensus Approach where H2SO4 emissions are not provided by applicant Applicant's estimates are in ${\it BoLD}$.

	Heat Input	Filterable PM	(25% Estimate)	Condensible P	M (75% Estimate)	Total PM (A	pplicant)	SO2 (Applicant)			
Turbine	(mmBtu/hr)	(lb/mmBtu)	(lb/hr)	(lb/mmBtu)	(lb/hr)	(lb/mmBtu)	(lb/hr)	(gr/100scf)		(lb/hr)	
			0.00		0.00		0.00	2.0		0.00	

SO4	
(lb/hr)	
	0.00

SO2 (Applicant-33%)	
(lb/hr)	
0	0.00

Organic Carbon
(lb/hr)
0.00

Impact of Consensus Combined Cycle Turbine Example on Extinction

Total

Relative hext

		Extinction			Emissions	bext	
Туре	Name	Coef.	f(RH)*	Efficiency	(lb/hr)	1/Mm	
Filterable	EC	10		10	0.00	0.00	
Inorganic CPM	SOIL	1		1		0.00	
Inorganic CPM	SO4	3	2	6	0.00	0.00	* f(RH) will vary
Organic CPM	SOA	4		4	0.00	0.00	
					0.00	0.00	•



ATTACHMENT B

Model Summary Results

8-25-21 HollyFror	ntier Artesia SIL Model, Full Grid (Includes 1	-22 H2S Remo	del)										
Model	File	Pollutant	Average	Group	Rank	Conc/Dep East	(X) N	lorth (Y) Elev	ı	Hill Fla	a	Time	е
AERMOD 21112	Artesia SIL 2020 CO.SUM	CO	1-HR	ALL	1ST	41.21148	556397.63	3634797.91	1025.65	1025.65		0	20012818
AERMOD 21112	Artesia SIL 2019 CO.SUM	CO	1-HR	ALL	1ST	41.05966	556390.61	3634800.06	1025.67	1025.67		0	19011518
AERMOD 21112	Artesia SIL 2017 CO.SUM	CO	1-HR	ALL	1ST	40.16028	556379.06	3634896.87	1025.9	1025.9		0	17012302
AERMOD 21112	Artesia SIL 2018 CO.SUM	CO	1-HR	ALL	1ST	40.14757	556381.95	3634872.66	1025.85	1025.85		0	18111006
AERMOD 21112	Artesia SIL 2016 CO.SUM	CO	1-HR	ALL	1ST	39.89154	556381.95	3634872.66	1025.85	1025.85		0	16101103
AERMOD 21112	Artesia SIL 2016 CO.SUM	CO	8-HR	ALL	1ST	25.414	556381.95	3634872.66	1025.85	1025.85		0	16051516
AERMOD 21112	Artesia SIL 2020 CO.SUM	CO	8-HR	ALL	1ST	24.41507	556384.84	3634848.46	1025.81	1025.81		0	20031516
AERMOD 21112	Artesia SIL 2017 CO.SUM	CO	8-HR	ALL	1ST	23.04333	556384.84	3634848.46	1025.81	1025.81		0	17092816
AERMOD 21112	Artesia SIL 2018 CO.SUM	CO	8-HR	ALL	1ST	22.1883	556384.84	3634848.46	1025.81	1025.81		0	18070524
AERMOD 21112	Artesia SIL 2019 CO.SUM	CO	8-HR	ALL	1ST	22.05946	556384.84	3634848.46	1025.81	1025.81		0	19021816
AERMOD 21112	Artesia SIL 2016 H2S.SUM	H2S	1-HR	ALL	1ST	24.44764	556500	3634100	1027.15	1027.15		0	16121303
AERMOD 21112	Artesia SIL 2018 H2S.SUM	H2S	1-HR	ALL	1ST	23.62346	556854.85	3634006.44	1027.45	1027.45		0	18090722
AERMOD 21112	Artesia SIL 2019 H2S.SUM	H2S	1-HR	ALL	1ST	22.44775	556854.85	3634006.44	1027.45	1027.45		0	19111903
AERMOD 21112	Artesia SIL 2017 H2S.SUM	H2S	1-HR	ALL	1ST	21.22834	556902.06	3634007.39	1027.52	1027.52		0	17113021
AERMOD 21112	Artesia SIL 2020 H2S.SUM	H2S	1-HR	ALL	1ST	21.15178	556854.85	3634006.44	1027.45	1027.45		0	20122506
AERMOD 21112	Artesia SIL 2016-2020 NO2 ST.SUM	NO2	1ST-HIGHEST MAX D	ALL	1ST	35.14309	556588.18	3634040.29	1027.2	1027.2		0 5 YE	EARS
AERMOD 21112	Artesia SIL 2018 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.62696	556382.56	3635002.7	1026.13	1026.13		0 1 YE	EARS
AERMOD 21112	Artesia SIL 2019 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.40098	556382.56	3635002.7	1026.13	1026.13		0 1 YE	
AERMOD 21112	Artesia SIL 2017 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.33655	556382.56	3635002.7	1026.13	1026.13		0 1 YE	
AERMOD 21112	Artesia SIL 2020 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.25856	556382.56	3635002.7	1026.13	1026.13		0 1 YE	
AERMOD 21112	Artesia SIL 2016 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.09455	556382.56	3635002.7	1026.13	1026.13		0 1 YE	
AERMOD 21112	Artesia SIL 2020 PM10.SUM	PM10	24-HR	ALL	1ST	2.12842	556300	3635000	1026.57	1026.57		0	20060624
AERMOD 21112	Artesia SIL 2018 PM10.SUM	PM10	24-HR	ALL	1ST	2.09536	556379.06	3634896.87	1025.9	1025.9		0	18073124
AERMOD 21112	Artesia SIL 2016 PM10.SUM	PM10	24-HR	ALL	1ST	1.98536	556370.4	3634969.47	1026.16	1026.16		0	16082224
AERMOD 21112	Artesia SIL 2017 PM10.SUM	PM10	24-HR	ALL	1ST	1.91596	556300	3635000	1026.57	1026.57		0	17050724
AERMOD 21112	Artesia SIL 2019 PM10.SUM	PM10	24-HR	ALL	1ST	1.91181	556300	3634900	1026.41	1026.41		0	19033124
AERMOD 21112	Artesia SIL 2018 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.6628	556379.06	3634896.87	1025.9	1025.9		0 1 YE	
AERMOD 21112	Artesia SIL 2019 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.65634	556379.06	3634896.87	1025.9	1025.9		0 1 YE	
AERMOD 21112	Artesia SIL 2020 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.6208	556376.17	3634921.07	1026.01	1026.01		0 1 YE	
AERMOD 21112	Artesia SIL 2017 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.60552	556379.06	3634896.87	1025.9	1025.9		0 1 YE	
AERMOD 21112	Artesia SIL 2016 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.57825	556379.06	3634896.87	1025.9	1025.9		0 1 YE	
AERMOD 21112	Artesia SIL 2016-2020 PM25 ST.SUM	PM25	1ST-HIGHEST 24-HR		1ST	1.92291	556376.17	3634921.07	1026.01	1026.01		0 5 YE	
AERMOD 21112	Artesia SIL 2016-2020 PM25 LT.SUM	PM25	ANNUAL	ALL	1ST	0.30301	556505.52	3635129.2	1025.74	1025.74		0 5 YE	
AERMOD 21112	Artesia SIL 2019 SO2 ST.SUM	SO2	1-HR	ALL	1ST	26.06468	556300	3634500	1026.17	1026.17		0	19041611
AERMOD 21112	Artesia SIL 2020 SO2 ST.SUM	SO2	1-HR	ALL	1ST	25.45004	556300	3634400	1026.36	1026.36		0	20103111
AERMOD 21112	Artesia SIL 2017 SO2 ST.SUM	SO2	1-HR	ALL	1ST	25.26063	556300	3634400	1026.36	1026.36		0	17031812
AERMOD 21112	Artesia SIL_2016_SO2_ST.SUM	SO2	1-HR	ALL	1ST	25.05872	556445.7	3634255.43	1026.77	1026.77		0	16061309
AERMOD 21112	Artesia SIL 2018 SO2 ST.SUM	SO2	1-HR	ALL	1ST	24.60504	556300	3634300	1026.78	1026.78		0	18103010
AERMOD 21112	Artesia SIL 2020 SO2 ST.SUM	SO2	24-HR	ALL	1ST	7.93385	556300	3635000	1026.57	1026.57		0	20060624
AERMOD 21112	Artesia SIL 2018 SO2 ST.SUM	SO2	24-HR	ALL	1ST	7.77685	556379.06	3634896.87	1025.9	1025.9		0	18073124
AERMOD 21112	Artesia SIL 2016 SO2 ST.SUM	SO2	24-HR	ALL	1ST	7.28096	556376.17	3634921.07	1026.01	1026.01		0	16092224
AERMOD 21112	Artesia SIL 2019 SO2 ST.SUM	SO2	24-HR	ALL	1ST	7.0093	556382.56	3635002.7	1026.13	1026.13		0	19072624
AERMOD 21112	Artesia SIL 2017 SO2 ST.SUM	SO2	24-HR	ALL	1ST	6.91898	556300	3635000	1026.57	1026.57		0	17050724
AERMOD 21112	Artesia SIL 2019 SO2 ST.SUM	SO2	3-HR	ALL	1ST	22.27776	556390.61	3634800.06	1025.67	1025.67		0	19111312
AERMOD 21112	Artesia SIL 2017 SO2 ST.SUM	SO2	3-HR	ALL	1ST	22.24497	556300	3634700	1026.14	1026.14		0	17040712
AERMOD 21112	Artesia SIL 2020 SO2 ST.SUM	SO2	3-HR	ALL	1ST	22.17742	556400	3634200	1027.1	1027.1		0	20032012
AERMOD 21112	Artesia SIL 2018 SO2 ST.SUM	SO2	3-HR	ALL	1ST	21.39588	556300	3634300	1026.78	1026.78		0	18040512
AERMOD 21112	Artesia SIL 2016 SO2 ST.SUM	SO2	3-HR	ALL	1ST	21.31755	556400	3634200	1020.76	1027.1		0	16040312
AERMOD 21112	Artesia SIL 2019 SO2 LT.SUM	SO2	ANNUAL	ALL	1ST	0.74039	556379.06	3634896.87	1027.1	1025.9		0 0 1 YE	
AERMOD 21112	Artesia SIL 2018 SO2 LT.SUM	SO2	ANNUAL	ALL	1ST	0.73197	556300	3634900	1025.9	1026.41		0 1 YE	
AERMOD 21112 AERMOD 21112	Artesia SIL 2016_SO2_LT.SUM Artesia SIL 2020 SO2 LT.SUM	SO2	ANNUAL	ALL	1ST	0.70143	556379.06	3634896.87	1020.41	1025.9		0 1 YE	
AERMOD 21112 AERMOD 21112	Artesia SIL 2017 SO2 LT.SUM	SO2	ANNUAL	ALL	1ST	0.76143	556300	3634900	1025.9	1025.9		0 1 YE	
AERMOD 21112	Artesia SIL 2016 SO2 LT.SUM	SO2	ANNUAL	ALL	1ST	0.6453	556381.95	3634872.66	1025.85	1025.85		0 1 YE	
ALINIOD 21112	AITG3IA GIE_2010_GOZ_E1.GOW	302	AINIVAL	ALL	101	0.0400	330301.83	JUJ401 2.00	1023.03	1023.03		0 1 1	-A110

8-25-21 HollyFrontier Artesia SIL Model, Full Grid (Includes 1-22 H2S Remodel)

				Conc.	Secondary PM2.5	Total Conc.			
Pollutant	Average	Group	Rank	(ug/m3)	Conc. (ug/m3)	(ug/m3)	SIL (ug/m3)	%SIL	Max Distance to SIL (km)
PM25	ANNUAL	ALL	1ST	0.30	0.11	0.42	0.2	209%	0.76
PM25	1ST-HIGHEST 24-HR	ALL	1ST	1.92	2.59	4.51	1.2	376%	1.48
PM10	ANNUAL	ALL	1ST	0.66	NA	0.66	1.0	66%	NA
PM10	24-HR	ALL	1ST	2.13	NA	2.13	5.0	43%	NA
SO2	1-HR	ALL	1ST	26.06	NA	26.06	7.8	334%	10.7
SO2	24-HR	ALL	1ST	7.93	NA	7.93	5.0	159%	1.73
SO2	3-HR	ALL	1ST	22.28	NA	22.28	25.0	89%	NA
SO2	ANNUAL	ALL	1ST	0.74	NA	0.74	1.0	74%	NA
NO2	1ST-HIGHEST MAX D	ALL	1ST	35.14	NA	35.14	7.5	467%	1.82
NO2	ANNUAL	ALL	1ST	2.63	NA	2.63	1.0	263%	1.07
со	1-HR	ALL	1ST	41.21	NA	41.21	2000.0	2%	NA
со	8-HR	ALL	1ST	25.41	NA	25.41	500.0	5%	NA
H2S	1-HR	ALL	1ST	24.45	NA	24.45	5.0	489%	1.01

NA - not applicable

Maximum 5-yr 1-hr SO2 impact conservatively used in lieu of 5-yr average of maxima.

NO2 modeling included the ARM2 method to account for NOx to NO2 conversion. The default minimum and maximum NO2/NOx ratios of 0.5 and 0.9 were employed.

8-25-21 Holly	yFrontier Artesia	NAAQS Model, Significance	e Grid (Includes 1-2	2 H2S Remodel)
Model	File		Pollutant	Average

8-25-21 HollyFroi	ntier Artesia NAAQS Model, Significance Grid	(Includes 1-2	22 H2S Remodel)														
Model	File	Pollutant	Average	Group	Rank		East (X)		North (Y)	Elev	Н		Flag	Ti	me	Met File	e
AERMOD 21112	Artesia NAAQS_2019_H2S.SUM	H2S	1-HR	ALL	1ST	28.94206		556415.7	3634620.21		025.46	1025.46		0		17 Artes	
AERMOD 21112	Artesia NAAQS_2018_H2S.SUM	H2S	1-HR	ALL	1ST	27.66808		556854.85			027.45	1027.45		0		22 Artes	
AERMOD 21112	Artesia NAAQS_2016_H2S.SUM	H2S	1-HR	ALL	1ST	27.65655		556664.07	3634229.22	2 10	026.56	1026.56		0	161010	07 Artes	
AERMOD 21112	Artesia NAAQS_2017_H2S.SUM	H2S	1-HR	ALL	1ST	27.34274		556413.44	3634642.42	2 10	025.43	1025.43		0		308 Artes	
AERMOD 21112	Artesia NAAQS_2020_H2S.SUM	H2S	1-HR	ALL	1ST	26.3362		556664.07	3634229.22	2 10	026.56	1026.56		0	20071	06 Artes	
AERMOD 21112	Artesia NAAQS_2019_H2S.SUM	H2S	1-HR	HOLLY	1ST	28.87117		556415.7	3634620.21	1 10	025.46	1025.46		0	191230	17 Artes	
AERMOD 21112	Artesia NAAQS 2018 H2S.SUM	H2S	1-HR	HOLLY	1ST	27.59325		556854.85	3634006.44	1 10	027.45	1027.45		0	180907	22 Artes	
AERMOD 21112	Artesia NAAQS_2016_H2S.SUM	H2S	1-HR	HOLLY	1ST	27.28641		556878.45	3634006.92	2 10	027.46	1027.46		0	160112	205 Artes	
AERMOD 21112	Artesia NAAQS 2017 H2S.SUM	H2S	1-HR	HOLLY	1ST	26.89261		556413.44	3634642.42	2 10	025.43	1025.43		0	170203	308 Artes	
AERMOD 21112	Artesia NAAQS_2020_H2S.SUM	H2S	1-HR	HOLLY	1ST	26.03605		556972.87	3634008.83	3 10	027.38	1027.38		0	200112	207 Artes	
AERMOD 21112	Artesia NAAQS_2020_H2S.SUM	H2S	1-HR	NEARBY	1ST	14.58068		556300	3633900) 10	028.29	1028.29		0	201213	320 Artes	
AERMOD 21112	Artesia NAAQS 2016 H2S.SUM	H2S	1-HR	NEARBY	1ST	14.38897		556300	3633900) 10	028.29	1028.29		0	160117	24 Artes	
AERMOD 21112	Artesia NAAQS_2019_H2S.SUM	H2S	1-HR	NEARBY	1ST	14.28026		555800	3634200)	1028.6	1028.6		0	190104	21 Artes	
AERMOD 21112	Artesia NAAQS_2018_H2S.SUM	H2S	1-HR	NEARBY	1ST	14.00066		557157.31	3633991.57	7 10	026.38	1026.38		0	180130	002 Artes	
AERMOD 21112	Artesia NAAQS 2017 H2S.SUM	H2S	1-HR	NEARBY	1ST	13.52761		557731.89	3633992.58	3 10	023.46	1023.46		0	17022	05 Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_NO2_ST.SUM	NO2	8TH-HIGHEST MAX D	ALL	1ST	173.99957		556460.99	3635129.21	1 10	025.95	1025.95		0 5	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_NO2_ST.SUM	NO2	8TH-HIGHEST MAX D	HOLLY	1ST	138.43808		556382.56	3635002.7	7 10	026.13	1026.13		0 5	YEARS	Artes	
AERMOD 21112	Artesia NAAQS 2018 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	17.29712		556460.99	3635129.21	1 10	025.95	1025.95		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2019_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	16.43736		556460.99	3635129.21	1 10	025.95	1025.95		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2020_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	16.04415		556483.26	3635129.2	2 10	025.85	1025.85		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS 2017 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	15.11576		556460.99	3635129.21	1 10	025.95	1025.95		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	13.56671		556483.26	3635129.2	2 10	025.85	1025.85		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2018_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	17.29712		556460.99	3635129.21	1 10	025.95	1025.95		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2019_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	16.43736		556460.99	3635129.21	1 10	025.95	1025.95		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2020_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	16.04415		556483.26	3635129.2	2 10	025.85	1025.85		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2017_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	15.11576		556460.99	3635129.21	l 10	025.95	1025.95		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	13.56671		556483.26	3635129.2	2 10	025.85	1025.85		0 1	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_PM25_ST.SUM	PM25	8TH-HIGHEST 24-HR	ALL	1ST	18.42716		556505.52	3635129.2	2 10	025.74	1025.74		0 5	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_PM25_ST.SUM	PM25	8TH-HIGHEST 24-HR	HOLLY	1ST	17.88599		556505.52	3635129.2	2 10	025.74	1025.74		0 5	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_PM25_ST.SUM	PM25	8TH-HIGHEST 24-HR	NEARBY	1ST	8.71237		556571.66	3635263.01	1 10	025.55	1025.55		0 5	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_PM25_LT.SUM	PM25	ANNUAL	ALL	1ST	5.56499		556505.52	3635129.2	2 10	025.74	1025.74		0 5	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_PM25_LT.SUM	PM25	ANNUAL	HOLLY	1ST	4.37949		556505.52	3635129.2	2 10	025.74	1025.74		0 5	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_PM25_LT.SUM	PM25	ANNUAL	NEARBY	1ST	1.86594		556570.94	3635328.83	3 10	025.74	1025.74		0 5	YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_SO2_ST.SUM	SO2	4TH-HIGHEST MAX D		1ST	156.97927		556300	3634300		026.78	1026.78			YEARS	Artes	
AERMOD 21112	Artesia NAAQS_2016-2020_SO2_ST.SUM	SO2	4TH-HIGHEST MAX D	HOLLY	1ST	156.97927		556300	3634300) 10	026.78	1026.78		0 5	YEARS	Artes	

8-25-21 HollyFrontier Artesia NAAQS Model, Significance Grid (Includes 1-22 H2S Remodel)

				Modeled		Secondary		NMAAQS/		
				Conc.	Background	PM2.5 Conc.	Total Conc.	NAAQS		
Pollutant	Average	Group	Rank	(ug/m3)	Conc. (ug/m3)	(ug/m3)	(ug/m3)	(ug/m3)	% NMAAQS/NAAQS	Comments
H2S	1-HR	ALL	1ST	28.94	NA	NA	28.9	41.8	69%	Includes off-site source inventory.
H2S	1-HR	HOLLY	1ST	28.87	NA	NA	28.9	41.8	69%	•
H2S	1-HR	NEARBY	1ST	14.6	NA	NA	14.6	41.8	35%	
NO2	ANNUAL	ALL	1ST	17.3	5.0	NA	22.3	94.02	24%	Oustide Carlsbad monitor
NO2	8TH-HIGHEST MAX [ALL	1ST	174.0	NA	NA	174.0	188.03	93%	No offsite source inventory required.
PM25	ANNUAL	ALL	1ST	5.6	5.9	0.11	11.6	12.0	96%	Eastern NM monitor.
PM25	ANNUAL	HOLLY	1ST	4.4	5.9	0.11	10	12.0	87%	Includes off-site source inventory
PM25	ANNUAL	NEARBY	1ST	1.9	5.9	0.11	8	12.0	66%	•
PM25	8TH-HIGHEST 24-HR	ALL	1ST	18.4	13.4	2.59	34.4	35.0	98%	
PM25	8TH-HIGHEST 24-HR	HOLLY	1ST	17.9	13.4	2.59	33.9	35.0	97%	
PM25	8TH-HIGHEST 24-HR	NEARBY	1ST	8.7	13.4	2.59	24.7	35.0	71%	
SO2	4TH-HIGHEST MAX D	ALL	1ST	157.0	5.3	NA	162.3	196.4	83%	Bloomfield monitor. There are no offsite SO2 sources within 10km.

NA - Not applicable.
Background concentrations as recommended by the NMAQB.
1-hr NO2 background concentrations from the Carlsbad monitor added within model.
"HOLLY" source group includes only the Artesia refinery sources.
NO2 modeling included the ARM2 method to account for NOx to NO2 conversion. The default minimum and maximum NO2/NOx ratios of 0.5 and 0.9 were employed.
SO2 24-hr NMAAQS modeling was not conducted as compliance is demonstrated using the 1-hr NAAQS (per NMED policy).

8-25-21 HollyFro	ntier Artesia Increment Model, PTE Assumed	for Holly, Sig	gnificance Gri														
Model	File	Pollutant	Average	Group	Rank	Conc/Dep East ((X) N	orth (Y) Ele	v Hi	il Flag	1	ime	Met File	Sources	Groups	Recepto	ors
AERMOD 21112	Artesia Increment_2018_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	24.67837	556505.52	3635129.2	1025.74	1025.74	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment 2019 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	24.16853	556505.52	3635129.2	1025.74	1025.74	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment 2020 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	23.67046	556505.52	3635129.2	1025.74	1025.74	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment_2017_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	23.2157	556505.52	3635129.2	1025.74	1025.74	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment 2016 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	22.19136	556527.78	3635129.2	1025.58	1025.58	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment 2018 NO2 LT.SUM	NO2	ANNUAL	HOLLY	1ST	17.21266	556460.99	3635129.21	1025.95	1025.95	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment 2019 NO2 LT.SUM	NO2	ANNUAL	HOLLY	1ST	16.35653	556460.99	3635129.21	1025.95	1025.95	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment_2020_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	15.97009	556483.26	3635129.2	1025.85	1025.85	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment_2017_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	15.04591	556460.99	3635129.21	1025.95	1025.95	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment_2016_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	13.51191	556483.26	3635129.2	1025.85	1025.85	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment_2017_NO2_LT.SUM	NO2	ANNUAL	NEARBY	1ST	17.79712	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment_2016_NO2_LT.SUM	NO2	ANNUAL	NEARBY	1ST	16.83571	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment 2018 NO2 LT.SUM	NO2	ANNUAL	NEARBY	1ST	16.60564	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment 2019 NO2 LT.SUM	NO2	ANNUAL	NEARBY	1ST	16.57839	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment 2020 NO2 LT.SUM	NO2	ANNUAL	NEARBY	1ST	15.69278	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artes	2	28	3	132
AERMOD 21112	Artesia Increment 2017 SO2 ST.SUM	SO2	24-HR	ALL	2ND	67.11136	556375.48	3635087.04	1026.35	1026.35	0	17040	324 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2019 SO2 ST.SUM	SO2	24-HR	ALL	2ND	65.72592	556527.78	3635129.2	1025.58	1025.58	0	190820	24 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2016 SO2 ST.SUM	SO2	24-HR	ALL	2ND	63.32752	556505.52	3635129.2	1025.74	1025.74	0	16100	324 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2018 SO2 ST.SUM	SO2	24-HR	ALL	2ND	60.36211	556416.47	3635129.21	1026.2	1026.2	0	18100	124 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2020 SO2 ST.SUM	SO2	24-HR	ALL	2ND	60.19588	556483.26	3635129.2	1025.85	1025.85	0	200610	324 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2019 SO2 ST.SUM	SO2	24-HR	HOLLY	2ND	63.5348	556527.78	3635129.2	1025.58	1025.58	0	190820	24 Artes	1	27	3	245
	Artesia Increment_2018_SO2_ST.SUM	SO2	24-HR	HOLLY	2ND	58.85538	556416.47	3635129.21	1026.2	1026.2	0	18091	724 Artes	1	27	3	245
AERMOD 21112	Artesia Increment_2017_SO2_ST.SUM	SO2	24-HR	HOLLY	2ND	57.47117	556375.48	3635087.04	1026.35	1026.35	0	170910	24 Artes	1	27	3	245
AERMOD 21112	Artesia Increment_2016_SO2_ST.SUM	SO2	24-HR	HOLLY	2ND	57.27247	556416.47	3635129.21	1026.2	1026.2	0	160720	24 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2020 SO2 ST.SUM	SO2	24-HR	HOLLY	2ND	54.91992	556483.26	3635129.2	1025.85	1025.85	0	20022	124 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2020 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	38.16688	557200	3634100	1025.78	1025.78	0	20022	224 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2019 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	31.71447	555900	3633100	1032.5	1032.5	0		524 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2016 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	31.52081	555900	3635300	1031.49	1031.49	0	16122	324 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2017 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	29.08133	557537.74	3634690.06	1022.56	1022.56	0	171220	24 Artes	1	27	3	245
AERMOD 21112	Artesia Increment 2018 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	25.97896	555800	3635200	1030.06	1030.06	0	18032	324 Artes	1	27	3	245

8-25-21 HollyFrontier Artesia Increment Model, PTE Assumed for Holly, Significance Gri

Pollutant	Average	Group	Rank	Modeled Conc. (ug/m3)	Secondary PM2.5 Conc. (ug/m3)	Total Conc. (ug/m3)	Increment (ug/m3)	% Increment	Comments
NO2	ANNUAL	ALL	1ST	24.7	NA	24.7	25	99%	
NO2	ANNUAL	HOLLY	1ST	17.2	NA	17.2	25	69%	
NO2	ANNUAL	NEARBY	1ST	17.8	NA	17.8	25	71%	
SO2	24-HR	ALL	2ND	67.1	NA	67.1	91	74%	
SO2	24-HR	HOLLY	2ND	63.5	NA	63.5	91	70%	
SO2	24-HR	NEARBY	2ND	38.2	NA	38.2	91	42%	

NA - Not applicable.
PM2.5 increment not triggered due to project.

8-25-21 HollyFrontier Artesia TAP Mode

Model	File
AERMOD 21112	Artesia TAP_2017_H2SO4.SUM
AERMOD 21112	Artesia TAP 2020 H2SO4.SUM
AERMOD 21112	Artesia TAP 2016 H2SO4.SUM
AERMOD 21112	Artesia TAP 2018 H2SO4.SUM
AERMOD 21112	Artesia TAP 2019 H2SO4.SUM
AERMOD 21112	Artesia TAP 2020 NH3.SUM
AERMOD 21112	Artesia TAP_2018_NH3.SUM
AERMOD 21112	Artesia TAP_2017_NH3.SUM
AERMOD 21112	Artesia TAP_2019_NH3.SUM
AERMOD 21112	Artesia TAP_2016_NH3.SUM

Pollutant	Average	Group	Rank	Conc/Dep	East (X)	North (Y)	Elev	Hill	Flag	Т	Γime	Met File	Sources	Groups	Recep	ptors
H2SO4	8-HR	ALL	1ST	4.86031	556300	3634900	1026.41	1026.41		0		17020416 Artes		3	1 .	8195
H2SO4	8-HR	ALL	1ST	4.59695	556575.62	3634197.94	1026.68	1026.68		0	- 2	20040316 Artes		3	1	8195
H2SO4	8-HR	ALL	1ST	4.26709	556500	3634200	1026.85	1026.85		0		16011116 Artes		3	1	8195
H2SO4	8-HR	ALL	1ST	4.25832	556300	3634900	1026.41	1026.41		0		18010616 Artes		3	1	8195
H2SO4	8-HR	ALL	1ST	4.11581	556370.4	3634969.47	7 1026.16	1026.16		0		19110216 Artes		3	1	8195
NH3	8-HR	ALL	1ST	32.28275	556380.79	3635023.79	1026.17	1026.17		0	- 2	20112308 Artes		2	1	8195
NH3	8-HR	ALL	1ST	32.01996	556587.86	3634326.98	3 1026.22	1026.22		0		18110908 Artes		2	1	8195
NH3	8-HR	ALL	1ST	29.49	556400	3634500	1025.86	1025.86		0		17082824 Artes		2	1	8195
NH3	8-HR	ALL	1ST	28.23331	556416.92	3634389.47	7 1026.21	1026.21		0		19111124 Artes		2	1	8195
NH3	8-HR	ALL	1ST	26.04177	556572.31	3635129.2	2 1025.36	1025.36		0		16080108 Artes		2	1	8195

8-25-21 HollyFrontier Artesia TAP Mode

Pollutant	Average	Group	Rank	Modeled Conc. (ug/m3)	1/100 OEL(ug/m3)	% Standard
NH3	8-HR	ALL	1ST	32.3	180	18%
H2SO4	8-HR	ALL	1ST	4.9	10	49%

CALPUFF Results (9/6/21)

CALI OTT REsults (5) 0	•	Meteorological	Modeled				
Parameter	Averaging Time	Year Modeled	Value	Modeled Value Units	Standard	% Standard	Comments
AQRV - Visibility	24-hour	2013	2.78	Extinction (%)	5.0	56%	Only Carlsbad Caverns has Q/d > 10.
		2014	1.90	98% (8th high)	5.0	38%	8th high over all receptors, not by receptor, conservatively used.
		2015	2.24		5.0	45%	
SIL - PM10 (PMC)	24-hour	2013	6.66E-02	Concentration (ug/m3)	0.30	22%	Class I SIL
		2014	6.11E-02	(-8,)	0.30	20%	All Class I areas modeled.
		2015	5.78E-02		0.30	19%	
	Annual	2013	7.76E-03		0.20	4%	
	Allitual	2013	7.70E-03 7.59E-03		0.20	4%	
		2015	8.27E-03		0.20	4%	
		2015	6.27E-U3		0.20	470	
SIL - SO2	Annual	2013	3.52E-02	Concentration (ug/m3)	0.10	35%	Class I SIL
		2014	3.52E-02		0.10	35%	All Class I areas modeled.
		2015	3.79E-02		0.10	38%	
	24-hour	2013	3.01E-01		0.20	150%	SRU3 at 50 lb/hr.
		2013	1.93E-01		0.20	97%	SRU3 at 28 lb/hr.
		2014	2.70E-01		0.20	135%	SRU3 at 50 lb/hr.
		2014	1.78E-01		0.20	89%	SRU3 at 28 lb/hr.
		2015	2.41E-01		0.20	120%	SRU3 at 50 lb/hr.
		2015	1.56E-01		0.20	78%	SRU3 at 28 lb/hr.
	3-hour	2013	9.45E-01		1.00	95%	
	3 11001	2014	9.82E-01		1.00	98%	
		2015	8.76E-01		1.00	88%	
CII. NO.	Ammont	2012	1 005 03	C	0.10	100/	Class I SIL
SIL - NOx	Annual	2013 2014	1.88E-02 1.89E-02	Concentration (ug/m3)	0.10	19% 19%	All Class I areas modeled.
					0.10		All Class I areas modeled.
		2015	2.00E-02		0.10	20%	
AQRV	Annual	2013	2.56E-03	Deposition (kg/ha/yr)	0.005	51%	All Class I areas conservatively modeled.
Nitrogen Deposition		2014	2.67E-03		0.005	53%	
		2015	2.87E-03		0.005	57%	
Sulfur Deposition	Annual	2013	3.14E-03		0.005	63%	Used annual SO2 and SO4 emissions.
		2014	3.32E-03		0.005	66%	
		2015	3.77E-03		0.005	75%	



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- 4. Auer, Jr., A.H. "Correlation of Land Use and Cover with Meteorological Anomalies." <u>Journal of Applied Meteorology</u>, 17:636-643, 1978.
- 5. <u>Engineering Guide #69, Air Dispersion Modeling Guidance</u>. Ohio EPA, Division of Air Pollution Control, 2003.
- 6. U.S. EPA, <u>Guideline for Determination of Good Engineering Practice Stack Height (Technical Support Document for Stack Height Regulations (Revised)</u>. EPA-450/4-80-023R, U.S. Environmental Protection Agency, June 1985.
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- 9. U.S. EPA., Workbook for Estimating Visibility Impairment. EPA Pub. No. 450/4-80-031. RTP, NC. November 1980.
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- 11. <u>Federal Land Managers Air Quality Related Values Workgroup (FLAG) Phase I Report-Revised (2010)</u>, US Forest Service, National Parks Service, US Fish and Wildlife Service, 2010.
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AIR DISPERSION MODELING FOR HOLLYFRONTIER NAVAJO REFINING LLC IN ARTESIA, NEW MEXICO



Prepared for: HollyFrontier Navajo Refining LLC 501 E. Main St, Artesia, NM 88210

Prepared by: RTP Environmental Associates, Inc. 304A West Millbrook Road Raleigh, North Carolina 27609

Original Submittal September 2021 Updated January 2022 Second Update July 2022



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1.0 INTRODUCTION

This document presents the results of the air quality dispersion modeling analysis conducted for HollyFrontier Navajo Refining LLC ("HollyFrontier") for its petroleum refinery in Artesia, New Mexico. This analysis was conducted in support of an air quality constructon permit application submitted to correct several permit conditions and to authorize changes to several emissions units. This analysis has been conducted by RTP Environmental Associates, Inc. ("RTP") on behalf of HollyFrontier.

The analysis evaluated emissions of the criteria and toxic air pollutants regulated under the applicable provisions of the New Mexico Administrative Code ("NMAC"). The New Mexico Air Quality Bureau ("AQB") requires an analysis of air quality standards with any construction permit application. The ambient standards that evaluated include the National Ambient Air Quality Standards ("NAAQS"), New Mexico Ambient Air Quality Standards ("NMAAQS"), Prevention of Significant Deterioration ("PSD") increments, and toxic air pollutants subject to 20.2.72.403.A(2).

This analysis conforms with the modeling procedures outlined in the Environmental Protection Agency's <u>Guideline on Air Quality Models</u>¹ ("Guideline" or "Appendix W"), the AQB's <u>Air Dispersion Modeling Guidelines</u>², and associated EPA modeling policy and guidance. The analysis also conforms with the modeling protocol submitted to the AQB and Federal Land Managers ("FLMs") on May 26, 2021 and approved, with a requested revision to the proposed treatment of intermittent emissions, by the AQB on August 2, 2021. No comments on the protocol were received from the FLMs.

RTP had proposed to exclude emergency engines and firewater pumps that emit intermittently from the demonstration of compliance with the 1-hr standards. The AQB stated that these sources should be included unless they were exempt from permitting. HollyFrontier has therefore elected to request an exemption from permitting for the emergency engines. The firewater pumps have been included in the 1-hr modeling demonstrations.



This second revision to the analysis includes a change to the fence line along the southern portion of the refinery as well as a change to the Modeled Emission Rates for Percursors ("MERPS") values used in calculating the potential for secondary particulate matter and ozone formation due to the project.



2.0 PROJECT DESCRIPTION

The Artesia Refinery occupies approximately 466 acres and has a crude oil capacity of 100,000 barrels per day. The Refinery has been in operation since the mid-1920s when oil wells were first drilled in southeastern New Mexico. The Refinery can process heavy, sour and light, sweet crude oils and runs a predominant slate of Permian Basin crudes that are gathered in West Texas and Southeast New Mexico. The refinery can also source a variety of crude oils from Cushing, Oklahoma including Canadian crudes.

With the permit application, HollyFrontier is requesting revisions to existing emission limits and other permit terms for several permitted emissions units; to add existing, unpermitted emissions units to the permit; to add permitted emission rates to the permit for certain emissions units from which not all emitted pollutants have previously been permitted; to authorize changes to the refinery's flares, including increases in emission limits; and to authorize changes in changes in fuel composition for three process heaters. The flare project is a major modification for VOC. None of the requested changes are major modifications under the PSD program for any pollutant other than VOC. However, several of the emission limits for which HollyFrontier is requesting revisions were considered in the impact analyses for two historical major modifications at the Artesia Refinery: The GOHT Project authorized by Permit No. 0195-M15, which was a major modification for emissions of CO and NOx, and the Refinery Expansion Project authorized by Permit No. PSD-NM-0195-M25, which was a major modification for emissions of CO, VOC, NOx, SO₂, PM10, and PM. The air dispersion modeling analysis discussed herein therefore includes updates to the impact analyses for those two major modifications.



3.0 SITE DESCRIPTION

The Artesia Refinery is located in Eddy County, in southeastern NM, approximately 62km south of Roswell and 225km northeast of El Paso. The approximate Universal Transverse Mercator ("UTM") coordinates of the refinery are 556,690 meters east and 3,634,600 meters north (NAD 83, UTM Zone 13) at an elevation of 3400 feet above sea level. Figure 1 shows the general location of the refinery. Figure 2 shows the specific refinery location on a 7.5-minute U.S. Geological Survey ("USGS") topographic map.

Eddy County is classified as attainment or unclassified for all regulated pollutants.

The refinery is classified under the regulations governing PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC) as a major stationary source.



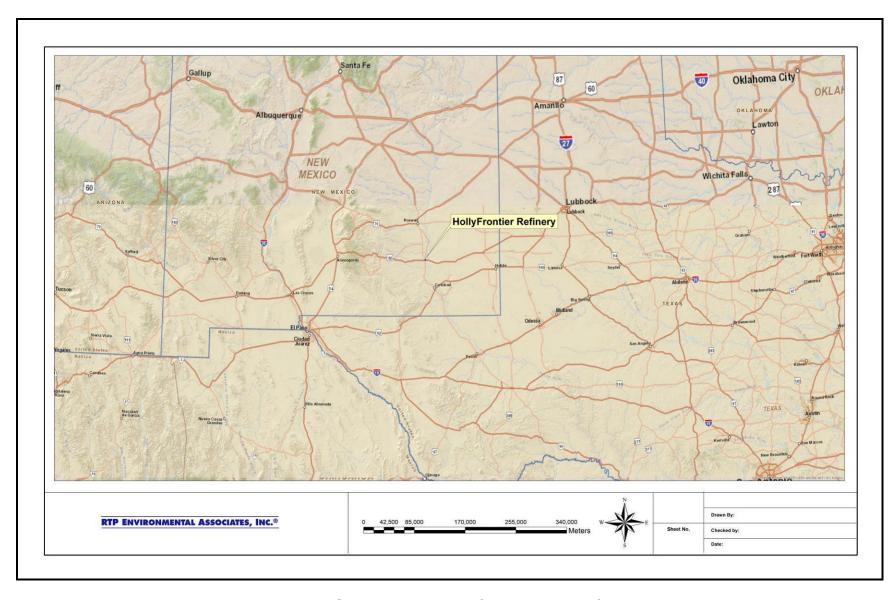


Figure 1. General Location of the Artesia Refinery



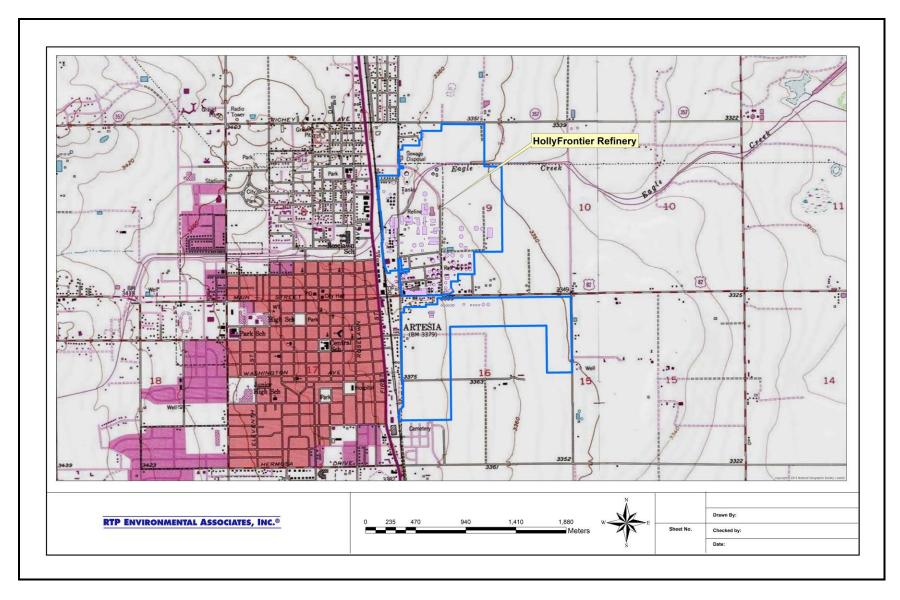


Figure 2. Specific Location of the Artesia Refinery



4.0 CLASS II AREA MODEL SELECTION AND MODEL INPUT

4.1 Model Selection

The latest version of the AMS/EPA Regulatory Model (AERMOD, Version 21112) was used to conduct the near-field dispersion modeling analysis. The modeling protocol stated that AERMOD Version 19191 would be used. However, EPA released an updated version of the model after the protocol was submitted. RTP has elected to use the most recent version of AERMOD in the analysis.

AERMOD is a Gaussian plume dispersion model that is based on planetary boundary layer principles for characterizing atmospheric stability. The model evaluates the non-Gaussian vertical behavior of plumes during convective conditions with the probability density function and the superposition of several Gaussian plumes. AERMOD is a modeling system with three components: AERMAP is the terrain preprocessor program, AERMET is the meteorological data preprocessor and AERMOD includes the dispersion modeling algorithms.

AERMOD is an appropriate model for calculating ambient concentrations near the Artesia Refinery based on the model's ability to incorporate multiple sources and source types. The model can also account for convective updrafts and downdrafts and meteorological data throughout the plume depth. The model also provides parameters required for use with up to date planetary boundary layer parameterization. The model also has the ability to incorporate building wake effects and to calculate concentrations within the cavity recirculation zone. All model options were selected as recommended in the EPA Guideline on Air Quality Models.

Oris Solution's BEEST Graphical User Interface ("GUI") was used to run AERMOD.

The GUI uses an altered version of the AERMOD code to allow for flexibility in the file naming convention. The dispersion algorithms of AERMOD are not altered. Therefore,



a model equivalency evaluation pursuant to Section 3.2 of Appendix W was not warranted.

The VISCREEN model is designed to assist in the evaluation of plume visual impacts as required under PSD. The model implements the visibility calculation procedures as outlined in the EPA's Workbook for Visual Impact Screening and Analysis.³ VISCREEN was used to assess the potential for the 2001 and 2007 major modifications to cause a visual plume within 50km of the proposed facility.

For more distant locations (i.e., areas located in excess of 50km from the proposed site), the AERMOD and VISCREEN models are not appropriate as the steady state assumptions in the models tend to degrade. Therefore, the EPA-approved version of the CALPUFF model (Version 5.8.5) was used to assess pollutant concentrations, deposition rates, and the potential for visibility impacts at these distant locations, namely PSD Class I areas. The CALPUFF modeling methodology is discussed in Section 6 of this report.

4.2 <u>Model Control Options and Land Use</u>

AERMOD was run in the regulatory default mode for all pollutants with the default rural dispersion coefficients. The use of rural dispersion coefficients is supported by the Land Use Procedure consistent with subsection 7.2.1.1.b.i of the Guideline and Section 5.1 of the AERMOD Implementation Guide. The USGS 2016 National Land Cover Data ("NLCD") within 3km of the site were converted to Auer 1978 land use types and evaluated.⁴ It was determined that the land use in the vicinity of the refinery is predominantly rural as defined by Auer (less than 50% of the area is classified as urban - Figure 3). Only the red and dark red regions in Figure 3 (NLCD categories 23 and 24) are considered urban.



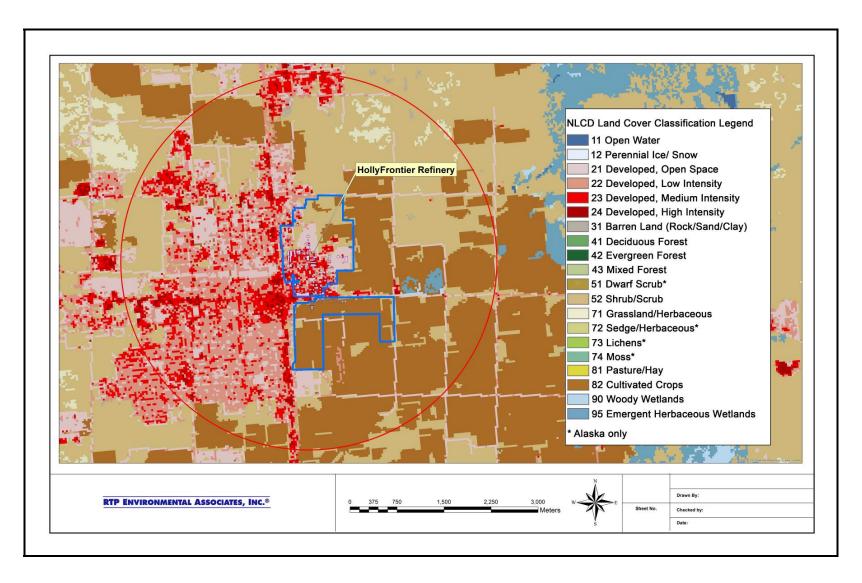


Figure 3. Land Use within Three Kilometers (Three Kilometer Radius Shown as Red Circle)



4.3 Source Data

Source Characterization

Point Sources

Most emission sources at the refinery vent to stacks with well-defined openings. These sources were modeled as point sources in AERMOD. Several other types of sources such as fugitive emissions from storage tanks and equipment leaks also required evaluation.

Fugitive Emissions

Fugitive emissions are those that are not emitted from a well-defined opening. These were modeled as volume sources. The initial dispersion coefficients (sigma y and sigma z) were calculated based upon the dimensions of the area of release and the equations contained in Table 3-1 of the AERMOD <u>User's Guide</u>.

All source locations were based upon a NAD83, UTM Zone 13 projection.

Flares

There are eight flares at the refinery for which emissions during periods of malfunction may exceed those during routine operation, including startup and shutdown periods. Malfunction emissions are not required to be modeled per 40 CFR Part 51 Appendix W. Emissions during startup or shutdown (i.e., non-emergency flaring) and other foreseeable operations were modeled using the proceedures outlined in the EPA's AERSCREEN manual⁵. These proceedures are slightly different than those contained in the AQB's Modeling Guidelines; however, the AQB approved of the AERSCREEN method on May 20, 2021. The effective stack height (H, in meters) was calculated as a function of heat release rate according to the following equation, where Q is the heat release rate of the flare in calories per second:

$$H_{\text{equivalent}} = H_{\text{actual}} + 4.56 \times 10^{-3} \times (Q)^{0.478}$$



The effective flare diameter (d, in meters) was calculated as a function of heat release rate according to the following equation, where Q is the heat release rate of the flare in calories per second:

$$d_{equivalent} = 9.88 \times 10^{-4} \times ((Q \times (1-0.55))^{0.5})$$

An exit temperature of 1273K and velocity of 20 m/sec was assumed.

All modeling input data, including the volume source and flare parameter calculations can be found in Attachment A to this report.

Good Engineering Practice Stack Height Analysis

A Good Engineering Practice ("GEP") stack height evaluation was conducted to determine appropriate building dimensions to include in the model. Procedures used were in accordance with those described in the EPA <u>Guidelines for Determination of Good Engineering Practice Stack Height (Technical Support Document for the Stack Height Regulations-Revised)</u>⁶. GEP formula stack height, as defined in 20.2.72.300 NMAC and in 40 CFR 51, is expressed as GEP = H_b + 1.5L, where H_b is the building height and L is the lesser of the building height or maximum projected width. Building/structure locations were determined from refinery construction drawings and prior modeling submissions. The structure locations and heights were input to the EPA's Building Profile Input Program ("BPIP-PRIME") computer program to calculate the direction-specific building dimensions needed for AERMOD. The Artesia Refinery plot plan and the ambient air boundaries are shown in Figure 4. A three dimensional rendering of the refinery is shown in Figure 5. All stacks and significant structures were included in the BPIP runs.



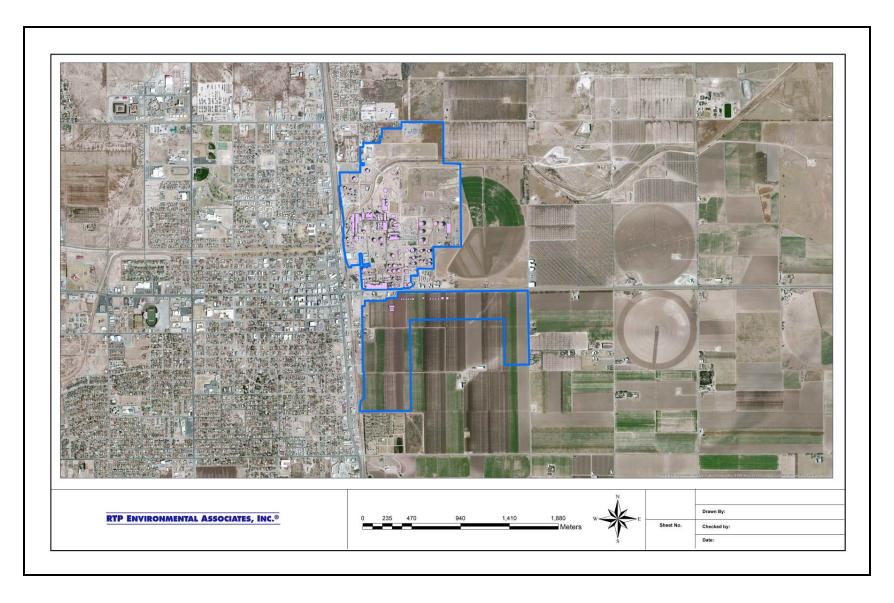


Figure 4. HollyFrontier Plot Plan and Ambient Air Boundary



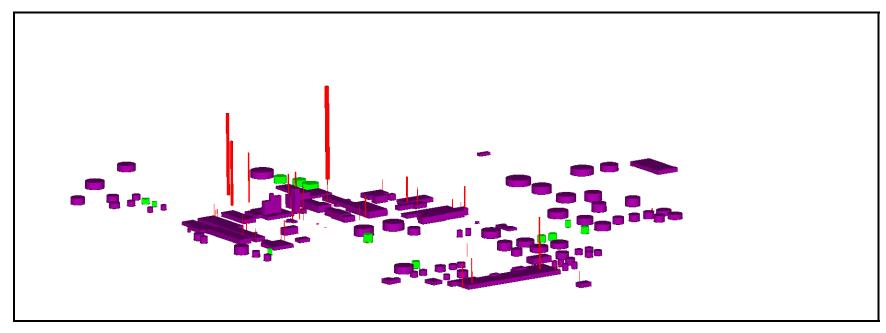


Figure 5. Artesia Refinery Three-Dimensional Plot Plan (View from SW)



4.4 Monitored Background Data

Ambient, background pollutant concentrations are needed to establish a representative background concentration to complete the NAAQS portion of the *Source Impact Analysis* of 20.2.74.303.B NMAC and 40 CFR § 52.21(k). The background concentrations are added to the modeled concentrations to assess NAAQS compliance. Ambient pollutant concentrations are also needed to fulfill the *Air Quality Analysis* requirement of 20.2.74.306.A NMAC and 40 CFR § 52.21(m), as discussed in Section 5.3 herein.

The AQB has recommended background concentrations established for New Mexico. These values are provided in the <u>Air Dispersion Modeling Guidelines</u> and were used in this analysis. These data satisfy the criteria provided in EPA's <u>Ambient Monitoring</u> Guidelines⁷ as being representative of the HollyFrontier site.

The background data employed are presented in Table 1.

Table 1. Background Concentrations

Pollutant	Averaging Time	Value (µg/m³)	Monitor Location
CO	8-hr	1524	Del Norte High School
	1-hr	2203	301001
NO ₂	Annual	5.0	Outside
1,02	1-hr	See Table 2	Carlsbad
PM ₁₀	24-hour	100.7	Eastern NM,
PM ₂₅	24-hour	13.4	Hobbs
	Annual	5.9	
О3	1-hour	150.5	

A range of monitored background NO₂ values that consider seasonal and diurnal variation was used to assess compliance with the 1-hr NO₂ NAAQS. These seasonal



values reflect the three year average of the 98th percentile value by hour of day and by season. Data from the Carlsbad monitor (AQS No. 35-015-1005) were used. Since the 2020 monitor values were not available, the lastest three years (2017-2019) were used. These seasonal NO₂ values (Table 2) were added to the modeled value within AERMOD.

Table 2. Carlsbad 98% Hourly NO₂ (ppb) By Season and Hour of Day

Model Ending				
Hour	Winter	Spring	Summer	Fall
01	24.67	13.67	10.67	19.00
02	23.00	15.33	13.33	17.33
03	21.67	15.67	14.33	20.67
04	25.33	16.33	14.67	22.67
05	23.33	19.00	15.33	22.00
06	24.67	20.67	16.67	21.67
07	24.67	21.33	17.67	19.67
08	21.33	18.33	14.33	19.00
09	20.00	14.67	14.33	18.67
10	20.00	12.00	10.67	16.00
11	18.00	10.33	7.67	14.00
12	16.33	8.00	5.33	12.00
13	15.67	7.33	5.00	11.00
14	12.00	5.67	4.33	10.33
15	12.33	5.33	4.00	9.33
16	14.67	5.00	3.33	8.67
17	18.00	4.67	3.33	11.00
18	20.00	6.33	4.00	12.33
19	18.33	10.33	6.67	12.00
20	16.00	11.67	9.67	12.00
21	15.67	10.33	10.67	12.67
22	19.00	10.00	11.00	14.33
23	21.33	10.00	10.00	14.67
24	23.33	10.33	10.33	19.00

4.5 Receptor Data

Modeled receptors were placed in all areas considered as "ambient air" pursuant to 40 CFR § 50.1(e). Ambient air is defined as that portion of the atmosphere, external to



buildings, to which the general public has access. Approximately 8,200 receptors were employed. The receptor grid consisted of three cartesian grids and receptors spaced at 25m intervals along the ambient boundary. The first cartesian grid extended to approximately 2.5km from the boundary in all directions. Receptors in this region were spaced at 100m intervals. The second grid extended to 7.5km. Receptor spacing in this region was 250m. The third grid extended to 10km with a spacing of 500m. The receptor grid was designed such that maximum impacts fall within the 100m spacing of receptors. The receptor grid spacing is presented in Table 3.

Table 3. Receptor Grid Spacing

Receptor Spacing (m)	Distance from Fence (m)
100	2,500
250	7,500
500	10,000

The Artesia Refinery is located in southeastern New Mexico. The terrain in the area is generally flat. Receptor elevations and hill height scale factors were calculated with AERMAP (18081). The elevation data were obtained from one arc-second National Elevation Data ("NED") obtained from the USGS. Locations were based upon a NAD83, UTM Zone 13 projection. The near-field receptor grid is presented in Figure 6.

4.6 Meteorological Data

Data Selection and Processing

The 2016-2020, 5-year sequential hourly surface meteorological data collected at the National Weather Service ("NWS") station in Artesia, NM (WBAN No. 03035) and upper air data from Midland, TX (WBAN No. 23023) were used in the near-field modeling analysis performed using AERMOD. These data were processed into a "model-ready" format using the latest version of AERMET (version 21112).



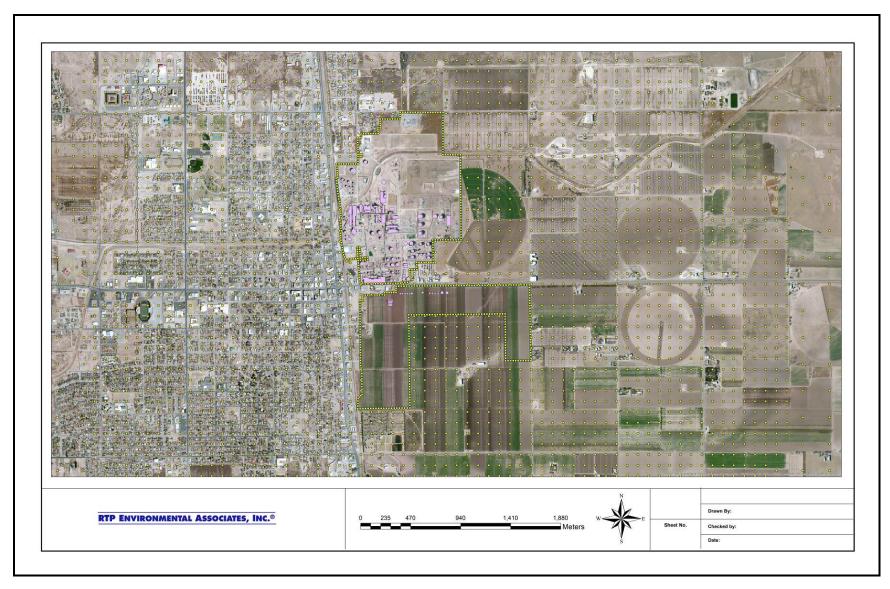


Figure 6. HollyFrontier Near-field Receptor Grid



In AERMET Stage 1, the Artesia surface meteorological data in the Integrated Surface Data ("ISD") format were extracted. Midland upper air meteorological data in the Forecast Systems Laboratory ("FSL") format were also extracted.

The AERMET meteorological processor requires estimates of the following surface characteristics: surface roughness length, albedo, and Bowen ratio. The surface roughness length is related to the height of obstacles to the wind flow. It is the height above the surface where the average wind speed is zero. The smoother the surface, the lower the roughness length. The surface roughness length influences the surface shear stress and is an important factor in calculating mechanical turbulence and stability. The albedo is the fraction of the total incident solar radiation reflected by the surface back to space without absorption. The Bowen ratio is an indicator of surface moisture and is the ratio of the sensible heat flux to the latent heat flux. The albedo and Bowen ratio are used for determining the planetary boundary layer parameters for convective conditions due to the surface sensible heat flux. RTP developed estimates of the surface characteristics using EPA's AERSURFACE program (Version 20060). A 1km search radius was employed at the location of the meteorological tower. Twelve sectors of 30 degrees each and seasonal resolution were used in the AERSURFACE analysis. The default season definitions were used with no continuous snow cover for one or more months during the winter and dry moisture. The "ADJ U*" option to allow for adjustments to the friction velocity under low wind speeds was employed. The 2016-2020 wind rose is shown in Figure 7.



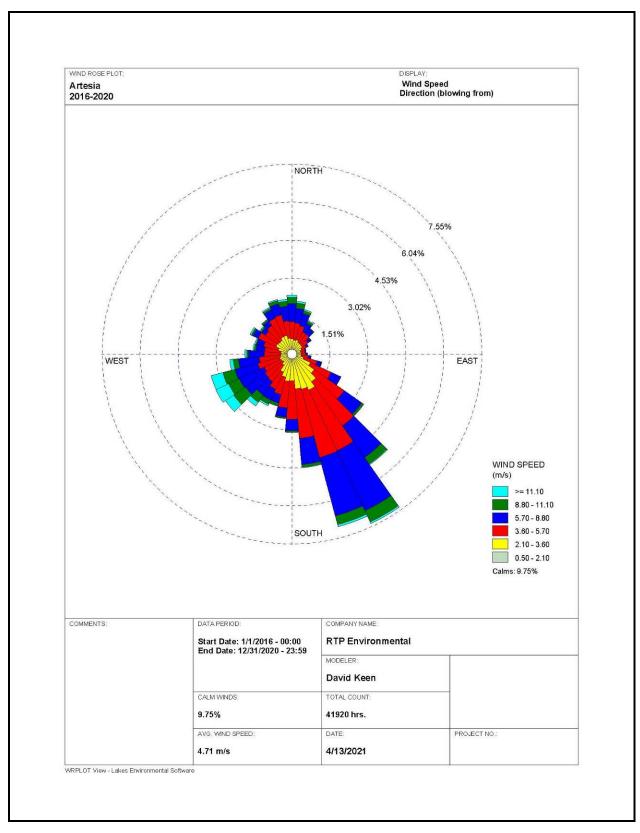


Figure 7. 2016-2020 Artesia Windrose



5.0 CLASS II AREA MODELING METHODOLOGY

5.1 Pollutants Subject to Review

The proposed permitting action will potentially allow for an increase in emissions of all criteria pollutants, with the exception of lead, as well as H₂S and two air toxics: ammonia and sulfuric acid mist. HollyFrontier has therefore elected to conduct a facility wide model for all pollutants using the requested permit to emit rates. Since precursor VOC emissions will also increase, ozone impacts were addressed.

5.2 Significant Impact Analysis

The criteria pollutant air quality analysis was conducted in two phases: an initial or significant impact analysis, and a refined phase including an increment analysis and a NAAQS/NMAAQS analysis. In the significant impacts analysis, the calculated maximum impacts associated with the project were determined for each pollutant. These impacts determined the net change in air quality resulting from the proposed modification. Five years of meteorological data were used in the significant impact analysis. Maximum modeled concentrations were compared to the pollutant-specific significance levels for all pollutants and averaging times except for the 1-hour NO₂, SO₂ and 24-hr PM2.5 impacts. For these pollutants and averaging times, the five-year average of the maximum impact at each receptor were used to assess significance. The PSD Class II and AQB Significant Impact Levels are listed in Table 4.



Table 4. PSD Class II and AQB Significant Impact Levels

Pollutant	Averaging Time	PSD Class II Significant Impact Levels (µg/m³)		
CO	1-hour	2,000		
	8-hour	500		
H ₂ S	1-hour	5.0		
PM10	24-hour	5.0		
	Annual	1.0		
PM2.5 ^a	24-hour	1.2		
	Annual	0.3		
NO ₂	1-hour	7.52 ^b		
	Annual	1.0		
SO ₂	1-hour	7.8 ^b		
	3-hour	25.0		
	24-hour	5.0		
	Annual	1.0		
O ₃	8-hour	1.96		

^aPlease note that on January 22, 2013, the US Court of Appeals for the District of Columbia Circuit Court granted a request from the EPA to vacate and remand the PM_{2.5} SILs codified in the federal PSD rule. EPA modeling guidance (August 1, 2016), issued subsequent to the remand, continues to recommend use of the SILs listed above to justify permitting decisions for PM2.5 NAAQS and increment evaluations.

Pollutants with impacts that exceeded the ambient air significance levels, as defined in 40 CFR 51.165, were included in both the NAAQS/NMAAQS and increment analyses. In these latter analyses, impacts from the Artesia Refinery were added to concentrations calculated from other nearby PM10, PM2.5, SO₂ and H₂S sources, plus a regional background concentration (for the NAAQS/NMAAQS analysis only). The resultant total concentration was compared to the NAAQS/NMAAQS and increments to determine compliance.

5.3 <u>Preconstruction Monitoring</u>

In order to satisfy the requirement for an air quality analysis pursuant to 20.2.74.306.A NMAC and 40 CFR § 52.21(m)(1), HollyFrontier used the AQB's recommended background values discussed in Section 4.4 herein. HollyFrontier requested that the

^bThere are no 1-hr NO₂ or SO₂ SILs promulgated at 40 CFR 51.165. The EPA proposed interim SILs for NO₂ of 4ppb and SO₂ of 3ppb will be used.



existing ambient monitoring data be allowed for use in lieu of site-specific preconstruction data.

5.4 Nearby Source Inventories

Off-site sources were included in the H₂S, SO₂, PM2.5, PM10 NAAQS/NMAAQS analyses as well as the increment analyses. Modeled impacts from the nearby sources were added to impacts from HollyFrontier in assessing compliance. Prior to the most recent 2017 Appendix W (40 CFR Part 51) revisions, the maximum distance to a significant impact plus 50km was historically used as a radius to define the screening area. The most recent Appendix W modeling guideline now states that professional judgment must be exercised in assessing sources to be included in the modeling analysis. Appendix W as well as the NM Modeling Guidelines further state that the number of nearby sources explicitly modeled in the air quality analysis is expected to be few, except in unusual situations, and that these sources will typically be located within the first 10-20 kilometers from the proposed source (see January 17, 2017, 82 Federal Register 5182 at page 5221).

The AQB provided RTP Environmental with the offsite source inventories required to conduct the analyses. HollyFrontier modeled all SO₂, PM10, and PM2.5 sources located within 10km of the refinery. Background concentrations adequately represent any PM10/PM2.5 sources beyond 10km. No nearby sources were modeled in the NAAQS/NMAAQS for the remaining pollutants as the background values also adequately represent impacts. For the H₂S and increment analysis where backgound concentrations are not considered, all sources located within 25km of the refinery as well as any large sources (1,000 lb/hr) located within 50km of the refinery were modeled.

5.5 NAAQS/NMAAQS Analysis

A refined air quality analysis to determine compliance with the NAAQS/NMAAQS was conducted. As stated, this analysis was conducted to determine compliance with the



NAAQS/NMAAQS for all regulated pollutants with impacts that exceeded the significant impact levels. Lead emissions were not evaluated because the facility does not have appreciable lead emissions. Each new or modified source's potential emission rate was used. Average emissions were used for the existing FCC regenerator, which is not part of the project, in assessing NAAQS compliance. Average emissions are allowed to be modeled for non-modified units pursuant to Table 8-2 of the EPA's Modeling Guideline (Appendix W).

Only those receptors showing a significant impact were modeled for NAAQS/NMAAQS compliance. In assessing NAAQS/NMAAQS compliance for most pollutants, the AQB allows for applicants either to model nearby sources or to use a background concentration to represent impacts from the nearby sources. The AQB, however, recommends inclusion of both nearby sources located within 10km of the refinery and background in assessing PM2.5 and PM10 compliance. The form of the modeled values and whether nearby sources or background were included to assess NAAQS/NMAAQS compliance are shown in Table 5. The more stringent of either the NAAQS or NMAAQS are shown in Table 6. These are the standards HollyFrontier used to assess compliance. Modeling was not conducted for the SO₂ 24-hour NAAQS eventhough significant impacts were calculated because the AQB considers a compliance demonstration using the 1-hr standard as a surrogate for compliance with the 24-hr standard.



Table 5. Form of Modeled Values Used to Assess NAAQS/NMAAQS Compliance

Pollutant	Averaging Time	Add Background Concentration or Include Nearby Sources	Modeled Value	
CO	8-hour	Background	Maximum	
	1-hour	Background	Maximum	
H ₂ S	1-hour	Nearby Sources	Maximum	
NO ₂	Annual	Background	Average	
	1-hour	Background	98 th percentile max daily 1-hour	
PM2.5	Annual	Both	Average	
	24-hour	Both	98 th percentile	
PM10	24-hour	Both	High 6 th high	
SO ₂	1-hour	Background	99 th percentile max daily 1-hour	

Table 6. National and New Mexico Ambient Air Quality Standards

Pollutant	Averaging Time	Ambient Air Quality Standards (µg/m³)
CO	8-hour	9,960.1
	1-hour	14,997.5
H ₂ S	1-hour	41.8
NO ₂	Annual	94.02
	1-hour	188.03
O ₃	8-hour	137.3
PM2.5	Annual	12
	24-hour	35
PM10	24-hour	150
SO ₂ ^a	1-hour	196.4

^aModeling not required for the other SO2 averaging periods if compliance can be demonstrated with the 1-hour standard.



5.6 **PSD Increment Analysis**

The Artesia Refinery is located in Air Quality Control Region No. 155. The PSD Minor Source Baseline dates have been triggered in this baseline area for all pollutants. NO₂ was triggered 3/16/1988, SO₂ was triggered 7/28/1978, PM10 was triggered 8/4/1978, and PM2.5 was triggered 11/13/2013. The Artesia Refinery was constructed in the mid-1920's and modifications have been made since the increment trigger dates for all pollutants except PM2.5. Increment compliance was therefore evaluated for all pollutants except PM2.5. As a conservative means of assessing increment compliance, HollyFrontier modeled potential emissions from all sources at the refinery. Only those receptors showing a significant impact were modeled for increment compliance.

Compliance with the PSD increments was based on the cumulative impacts of the Artesia Refinery and other increment consuming sources identified in the nearby source emissions inventory. All nearby sources located within 25km of the refinery and any large (>1000 lb/hr) sources within 50km of the refinery were included in the Class II increment demonstration. The resultant cumulative impacts were compared to the PSD Class II increment levels. The highest modeled annual averages was used for evaluating compliance with the annual increments and the <a href="https://example.com/high-second-hi

The PSD Class I and Class II increments are shown in Table 7.



Table 7. PSD Class I and II Increments

Pollutant	Averaging Time	PSD Class I Increment (µg/m³)	PSD Class II Increment (μg/m³)
NO ₂	Annual	2.5	25
PM2.5	Annual	1	4
	24-hour	2	9
PM10	Annual	4	17
	24-hour	8	30
SO ₂	Annual	2	20
	24-hour	5	91
	3-hour	25	512

5.7 <u>Secondary PM2.5 Analyses</u>

On February 10, 2020, the USEPA issued draft guidance for assessing ozone and fine particulate matter modeling.⁸ The guidance addresses both primary and secondary PM2.5 impacts. Primary PM2.5 impacts refer to the impacts due to direct emissions of PM2.5. Secondary impacts refer to the PM2.5 impacts attributable to nitrates and sulfates formed due to precursor NO₂ and SO₂ emissions. The AQB's Guidelines, which follow EPA's, were followed in assessing secondary PM2.5 impacts. Specifically, the following Modeled Emission Rates for Precursors ("MERPs") values and equations was used:

PM2.5 Annual (
$$\mu$$
g/m³) = ((NOx (tpy)/26,780) + (SO₂ (tpy)/14,978)) x 0.2 PM2.5 24-hr (μ g/m³) = ((NOx (tpy)/7,331) + (SO₂ (tpy)/1,981)) x 1.2

The AQB in consultation with EPA Region 6 requested use of the most conservative MERPs value for each category from hypothetical single source modeling reported on the EPA website https://www.epa.gov/scram/merps-view-qlik. Selected values were from either Terry, Texas or Roosevelt County, NM. The calculated secondary PM2.5 impacts were added to the modeled concentrations to assess significant impacts as well as compliance with the NAAQS/NMAAQS and increments.



5.8 O₃ Analyses

Ozone impacts were calculated using the AQB's Guidelines, which follow the EPA's MERPS guidance. Specifically, the following values and equations was used:

Ozone 8-hour (μ g/m3) = ((NOx (tpy)/340) + (VOC (tpy)/9,578)) x 1.96

The AQB in consultation with EPA Region 6 requested use of the most conservative MERPs value for each category from hypothetical single source modeling reported on the EPA website https://www.epa.gov/scram/merps-view-qlik. Selected values were from either Terry, Texas or Roosevelt County, NM. The calculated secondary O₃ impacts were compared to the O3 significant impact level of 1.96 μg/m³ or 1 ppb.

5.9 NO₂ Analyses

Following USEPA and AQB guidance, the NO₂ modeling analyses employed the recommended three tier screening approach. Initially, Tier 1 was employed with the conservative assumption that 100% of the available NOx converts to NO₂. Based on these results, HollyFrontier employed Tier 2 (the Ambient Ratio Method, ARM2) with the EPA default minimum and maximum ambient ratios of 0.5 and 0.9, respectively. Tier 3 was not employed. Tier 3 accounts for the chemical reactions that convert NOx to NO₂ in the presence of ozone.

5.10 Air Toxics Analysis

HollyFrontier conducted modeling for two toxic air pollutants, ammonia and sulfuric acid mist, which are emitted in excess of the levels specified in 20.2.72.502 NMAC – Permits for Toxic Air Pollutants. Maximum 8-hour impacts were compared to one-one hundredth of the Occupational Exposure Level ("OEL") listed in 20.2.72.502 NMAC.



5.11 Class II Visibility Analysis

In addition, a Class II visibility analysis was conducted using the VISCREEN model. The Living Desert State Park, which is located a minimum of 42km and a maximum of 49km south of the Artesia Refinery was used as an indicator of potential Class II visibility impacts. First level screening values of 1.00 for the color parameter ("delta E") and 0.02 for the contrast parameter ("C") were used. A background visible range of 110km was also used. This background visual range is recommended as the default value according to EPA's Workbook for Plume Visual Impact Screening and Analysis.⁹



6.0 CLASS I AREA ANALYSIS

6.1 Class I AQRV Analysis

There are five Class I areas located within 300km of the Artesia Refinery: Carlsbad Caverns, Guadalupe Mountains, White Mountains Wilderness, Salt Creek Wilderness, and Bosque del Apache (Figure 8). ¹ The closest Class I area is the Carlsbad Caverns National Park which is located 73km to the south. The Federal Land Manager's ("FLM") Q/D (maximum daily emissions in tons per year over distance in kilometers) method has been used to determine the potential for adverse Class I impacts for each Class I area (Table 8). We have presumed that no Class I Air Quality Related Values ("AQRV") evaluation was required for the Class I areas with calculated Q/D values below 10. Project emission estimates reveal a maximum annual, total SO₂, H₂SO₄, NOx and PM₁₀ emission rate of 787 tons per year which results in the Q/D values shown in Table 5. Annual emissions were calculated as the maximum daily emissions and 365 day/yr operation.

Table 8. Calculated Q/D Values for Each Class I Area

Class I	Map ID	Minimum Distance from the SRP Facility (km)	Maximum Distance from the SRP Facility (km)	Q/D
Bosque del Apache	bosq	245.1	259.6	3.2
Carlsbad Caverns	cave	73.8	93.9	10.7
Guadalupe Mountains	gumo	101.3	123.6	7.8
Salt Creek	sacr	79.1	84.7	9.9
White Mountain	whmo	134.2	153.4	5.9

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¹ Class I areas are pristine areas (e.g., National Parks and Wilderness Areas) that have been designated by Congress and are afforded a greater degree of air quality protection. All other areas are designated as Class II areas.



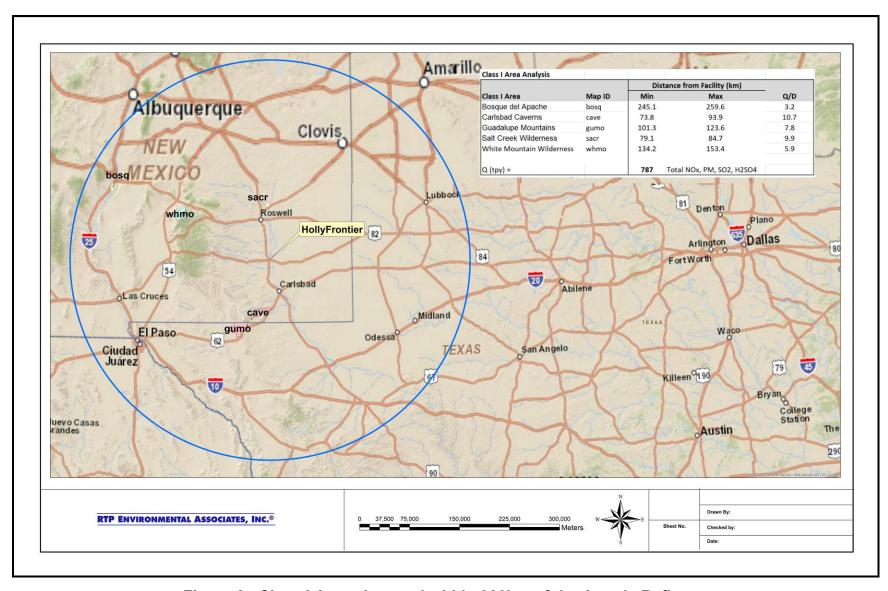


Figure 8. Class I Areas Located within 300km of the Artesia Refinery



For the Class I area, Carlsbad Caverns, with the Q/D values in excess of 10, AQRVs were calculated. Visibility and sulfur and nitrogen deposition were calculated using techniques prescribed by the Guideline for Air Quality Models (40 CFR 51, Appendix W), the EPA's Interagency Workgroup on Air Quality Modeling (IWAQM)¹⁰, and the FLM's Air Quality Related Values Work Group (FLAG) document.¹¹

6.2 Class I Increment Analysis

6.3 CALPUFF

The EPA-approved version of CALPUFF (Version 5.8) was used to assess Class I air quality impacts. The EPA-approved version of CALPUFF includes the CALMET meteorological model (Version 5.8.4, Level 130731), the non-steady-state puff model (CALPUFF, Version 5.8.5, Level 151214) with chemical transformation and deposition, and the post processors (POSTUTIL Version 1.5.6, Level 070627 and CALPOST, Version 6.221, Level 082724) for combining, converting, averaging, and ranking the concentrations, visibility impacts, and deposition.

CALMET

RTP used the Mesoscale Model Interface Program ("MMIF") Version 3.4 and the EPA's 2013-2015, 12km Weather Research and Forcasting Model ("WRF") for the Continental United States (CONUS) to develop a CALMET dataset.^b The extraction domain extended 50km beyond the Class I areas. The lower left and upper right coordinates of the extraction domain was -967.383, -923.424 and -631.767, -579.363 km, respectively (LCC, with the RPO projection). The origin was set to -972.0, -924.0km with 29 cells in each direction. The default vertical layers (ZFACE) of 0.0, 20.0, 40.0, 80.0, 160.0, 320.0, 640.0, 1200.0, 2000.0, 3000.0, 4000.0m were employed. MMIF was run in pass-through mode using the "CALSCI MIXH WRF" option.

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^b Please note that the most current version of MMIF is Ver. 3.4.1. This version will not read WRF files larger than 2 gigabytes. The WRF data files in RTP's possession are 12gb. The only difference between versions 3.4 and 3.4.1 is 3.4.1's ability to estimate cloud cover. Lack of such estimates should not appreciably affect CALPUFF results.



Modeled Emissions

The Artesia Refinery's primary emission sources are refinery fuel gas-fired heaters. There are also several flares and a fluid catalytic cracking unit. The National Park Service ("NPS") PM speciation calculation for combustion turbines ("CTs") was employed for the gas fired units. This calculation assumes that all of the estimated PM emissions have an aerodynamic diameter of less than 1 micron and that 25% of the PM is filterable and 75% is condensable. All of the filterable PM is assumed to be elemental carbon. All of the condensable PM was assumed to be soluble organic carbon (SOA), while one third of the SO₂ emissions were assumed to be sulfate (SO₄).

CALPUFF Technical Settings

CALPUFF was run using the FLM-approved default parameters where available. These options generally follow EPA's Guideline on Air Quality Models (40 CFR 51, Appendix W) and the IWAQM Phase 2 guidance. The regulatory default switch was used (MREG = 1).

The Class I area receptors modeled were obtained from the NPS. Lambert-Conformal Conic (LCC) Coordinates were used with an origin of 49.0N and 97.0W and Standard Parallels of 33.0N and 45.0N (the RPO projection).

The modeling domain and Class I receptors are shown in Figure 9.

Ozone and Ammonia

Hourly background ozone concentrations were input to CALPUFF. The ozone observations were collected at the Carlsbad monitor (AQS No. 35-015-1005) concurrent with the three years of WRF data. Missing values from Carlsbad were filled with data from the Hobbs monitor (AQS No. 35-025-008) located approximately 100km east of the refinery.



Ammonia is not simulated by CALPUFF, but rather a background value is specified. Ammonia is important because the level of particulate nitrate (NO₃) can depend on the amount of ammonia present. The partitioning of total nitrate between gaseous HNO₃ and particulate NO₃ depends on the amount of ammonia present and other parameters (e.g., SO₄, temperature, and RH).

In the CALPUFF simulation, one value of background is assumed across the region and each puff uses the full background value in its equilibrium calculation. The IWAQM Phase II report contains the following recommendations for background ammonia: "typical (within a factor of 2) background values of ammonia are: 10 ppb for grasslands, 0.5 ppb for forest, and 1 ppb for arid lands at 20 C" (IWAQM, 1998). Based on the fact that all of the reviewed Class I areas lie in an arid region, a background ammonia value of 1 part per billion (ppb) was used.

Natural Conditions and Monthly Relative Humidity Factors f(RH)

Natural background conditions must be established to determine a change in natural conditions related to a source's emissions. The EPA lists three types of natural background conditions in their guidance document: Annual Average, Best 20% Days, and Worst 20% Days. Based on the FLAG 2010 guidance, Annual Average Natural Visibility Conditions were used for this analysis. The EPA, in its BART Guidelines (2005), concluded that by using monthly average Relative Humidity Adjustment Factors f(RH), the likelihood that the highest modeled visibility impacts that were caused by short-term and geographically different meteorological phenomena (e.g., weather events) would be minimized. The FLAG (2010) report agreed with the EPA; therefore, the visibility analysis was conducted using monthly average f(RH) values for large hygroscopic particles, small hygroscopic particles and sea salt, rather than hourly values.



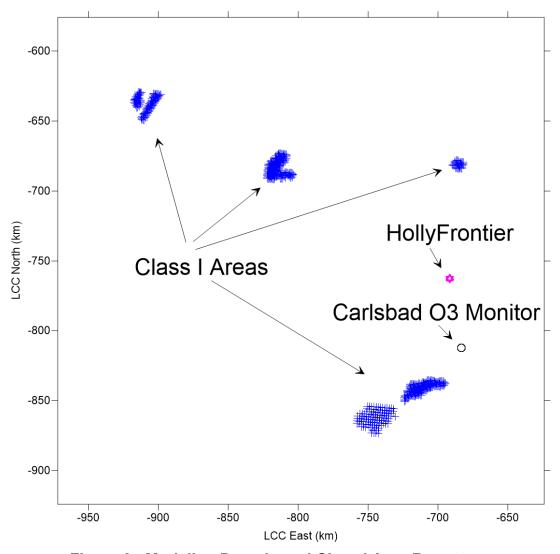


Figure 9. Modeling Domain and Class I Area Receptors



Light Extinction and Haze Impact Calculations

CALPOST was used to calculate light extinction. The EPA/IMPROVE formula will be used to calculate the change in light extinction due to increases in the particulate matter concentrations according to the following:

 $B_{\text{ext}} = 2.2 \text{ x f}_{\text{S}}(\text{RH}) \text{ x [Small Sulfates]} + 4.8 \text{ x f}_{\text{L}}(\text{RH}) \text{ x [Large Sulfate]}$

- + 2.4 x fs(RH) x [Small Nitrates] + 5.1 x fL(RH) x [Large Nitrates]
- + 2.8 x [Small Organic Mass] + 6.1 x [Large Organic Mass]
- + 10 x [Elemental Carbon]
- + 1 x [Fine Soil]
- + 0.6 x [Coarse Mass]
- + 1.7 x fss(RH) x [Sea Salt]
- + [Rayleigh Scattering]
- + 0.33 x [NO₂ (ppb)]

The concentrations, in square brackets, are in micrograms per cubic meter $\mu g/m^3$ and b_{ext} is in units of inverse mega-meters Mm^{-1} .

The values for f_s(RH), f_L(RH), f_{ss}(RH), and the Rayleigh scattering term were obtained from the 2010 FLAG Report in Tables 6, 7, 8 and 9. The assessment of visibility impacts employed CALPOST Method 8, sub-mode 5. CALPUFF assumes that all of the background ammonia is available for the formation of ammonium nitrate from each puff. However, where these puffs overlap in the model, puffs are actually in competition for the available ammonia. To prevent the overestimation of nitrate, the Ammonia Limiting Method option in the POSTUTIL processor (MNITRATE = 1) was used to compute the HNO₃/NO₃ concentration partition prior to executing the visibility calculations in CALPOST. In addition, the relative humidity in CALPOST was capped at 95% consistent with current FLM recommendations.



CALPOST calculates the change in light extinction for each 24-hour day. These results were reviewed to determine the number of days where the change in light extinction is at or above 5% change and 10% change at each Class I area.

Deposition Calculations

In addition to visibility, modeled deposition rates for total sulfur (S) and nitrogen (N) were calculated. POSTUTIL was used to summarize the total dry and wet deposition fluxes for the S and N species. Specifically, the N and S deposition was assumed to consist of the following composition of modeled species:

Total Nitrogen Flux (CSPECCMP) =

SO₄ x 0.291667

NOx x 0.304348

HNO₃ x 0.222222

NO₃ x 0.451613

Total Sulfur Flux (CSPECCMP)=

SO₂ x 0.500000

SO₄ x 0.333333

After the total N and S deposition rates were calculated in POSTUTIL, CALPOST was used to determine the average annual N and S deposition for each receptor in each Class I area. Two pollutant names were modeled in CALPUFF and passed to POSTUTIL and CALPOST. SO2 represented the maximum short term emissions from the refinery project. SO2LT represented the annual emissions increase. The SO2LT pollutant was used in the deposition analysis. SO2 was used in all other analyses. A scaling factor (A) of 316.224 was employed in CALPOST to convert the default deposition rates in units of $\mu g/m^2/sec$ to the units of kg/ha/yr needed for comparison to the Deposition Analysis Thresholds (DATs) of 0.005.

6.4 Class I Increment Analysis

Pollutant concentrations were also calculated for comparision to the proposed Class I



significance levels. CALPUFF was used to calculate concentrations at all Class I receptors located in excess of 50km from the source, regardless of Q/D. The model results were compared to the proposed Class I significant impact levels (Table 9).

Table 9. Proposed PSD Class I Significant Impact Levels

Pollutant	Averaging Time	PSD Class I Significant Impact Levels (µg/m³)
PM2.5	24-hour	0.27
	Annual	0.05
PM10	24-hour	0.30
	Annual	0.20
NO ₂	Annual	0.10
SO ₂	3-hour	1.00
	24-hour	0.20
	Annual	0.10



7.0 CLASS II ANALYSIS RESULTS

Attachment B provides the model summary output. Model input and output files, including the BPIP-PRIME and meteorological data files, are provided electronically.

7.1 Significant Impact Analysis Results

The project is expected to result in significant impacts for PM2.5, SO₂, NO₂ and H₂S (Table 10). Insignificant impacts were calculated for PM10 and O₃. Based upon the results of the significant impacts analysis, a cumulative analysis was conducted to assess compliance with the NAAQS/NMAAQS and increments.

Table 10. Class II Significant Impact Analysis Results

Pollutant	Avg Period	Maximum Modeled Impact (Including Secondary PM2.5) (μg/m³)	PSD Significant Class II Impact Level (μg/m³)	Significant Monitoring Concentration (µg/m³)	Maximum Distance to a Significant Impact (km)	
PM2.5	Annual	0.31	0.2	NA	0.76	
F IVIZ.3	24-hr	2.23	1.2	4.0	1.48	
PM10	Annual	0.66	1.0	NA	NA	
PIVITO	24-hr	2.13	5.0	10	NA	
	1-hr	26.06	7.8	NA	10.7	
SO ₂	24-hr	7.93	5.0	13	1.73	
302	3-hr	22.3	25.0	NA	NA	
	Annual	0.74	1.0	NA	NA	
NO ₂	1-hr	35.1	7.5	14	1.82	
NO ₂	Annual	2.63	1.0	NA	1.07	
CO	1-hr	41.2	2000	NA	NA	
	8-hr	25.4	500	575	NA	
H ₂ S	1-hr	24.5	5.0	NA	1.44	
O ₃	8-hr	1.43	1.96	NA	NA	

NA- not applicable.



7.2 NAAQS/NMAAQS Analysis Results

Following the determination of significant impacts, an analysis was conducted to assess compliance with the NAAQS and NMAAQS for pollutants showing a significant impact. The offsite source inventories discuss in Section 5.4 were employed. Background concentrations were added to the model results to assess compliance. Evaluation of compliance with the 24-hr PM2.5 NAAQS was based on the 98th percentile of the annual distribution of daily maximum 24-hour concentrations. Compliance with the 1-hr NO₂ and SO₂ NAAQS was based on the 98th and 99th percentiles, respectively, of the annual distributions of daily maximum 1-hour concentrations. Compliance with the PM10 24-hr standard was based upon the sixth highest value. Annual NAAQS compliance was evaluated based upon the maximum modeled value. Only receptors showing significant project-related impacts were modeled in assessing compliance.

The results of the NAAQS analysis are presented in Table 11. As can be seen, the model demonstrates compliance.

Table 11. NAAQS/NMAAQS Analysis Results

Pollutant	Averaging Period	Modeled Concentration (µg/m³)	Background Concentration (µg/m³)	Total Concentration (µg/m³)	Standard (µg/m³)		
H ₂ S	1-hr	28.9	NA	28.9	41.8		
NO	Annual	17.3	5.0	22.3	94.02		
NO ₂	1-hr	174	NA	174.0	188.0		
PM2.5	Annual	5.56	5.9	11.5	12.0		
FIVIZ.5	24-hour	18.4	13.4	32.1	35.0		
SO ₂	1-hour	157.0	5.3	162.1	196.4		

NA – not applicable. Background monitored values added within model.

PM2.5 modeled values includes secondary PM2.5 contribution.

7.3 <u>Increment Analysis Results</u>

Evaluation of compliance with the short-term increments was based upon the highestsecond-high modeled value. The maximum annual concentrations were used to assess compliance with the annual increments. All sources at the refinery were conservatively



assumed to consume increment at their potential to emit rates. Only receptors showing significant project-related impacts were modeled in assessing compliance.

The results of the increment analysis are presented in Table 12. As shown, the model demonstrates compliance.

Table 12. PSD Increment Analysis Results

Pollutant	Averaging Period	Modeled Concentration (µg/m³)ª	Standard (µg/m³)
NO_2	Annual	24.7	25
SO ₂	24-hr	67.1	91

7.4 <u>Secondary PM2.5 Analysis</u>

Following the the AQB's recommendations, the MERPs calculations resulted in the following values for secondary PM2.5. These values were added to the modeled PM2.5 concentrations:

PM2.5 MERP Calculation					
Facility NOx (tpy) =	239.75				
Facility SO2 (tpy) =	446.23				
MERP _{NOxannual} =	26780				
MERP _{SO2annual} =	14978				
MERP _{NOx24hr} =	7331				
MERP _{SO2 24hrl} =	1981				
PM2.5 Annual (ug/m3) = (NOxannual) +	(SO2 (tpy),	/MERP _{SO}	_{Zannual})) x 0.2
	(NOx (tpy)/MERI 0.008	NOxannual) +	(SO2 (tpy)	/MERP _{so.}	_{2annuai})) x 0.2
PM2.5 Annual (ug/m3) =	0.008				
PM2.5 Annual (ug/m3) = (PM2.5 Annual (ug/m3) = PM2.5 24-hr (ug/m3) = ((N PM2.5 24-hr (ug/m3) =	0.008				



The calculated secondary PM2.5 impacts were added to the modeled concentrations to assess significant impacts as well as compliance with the NAAQS/NMAAQS (refer to Tables 10 and 11 on pages 7-1 and 7-2, respectively).

7.5 Ozone Analysis

Following the the AQB's Guidelines, the MERPs calculations resulted in the following estimate of ozone:

O3 MERP Calculation				
Facility NOx (tpy) =	239.75			
Facility VOC (tpy) =	208.00			
MERP _{NOx} =	340			
MERP _{voc} =	9578			
O3 8-hr (ug/m3) =	1.425			
MERPs values were dete from hypothetical single https://www.epa.gov/sc	source mode	ing reported on	the EPA website	

The calculated secondary O_3 impact was compared to the O_3 significant impact level of $1.96 \ \mu g/m^3$ and determined to be insignificant.

7.6 Air Toxics

The results of the air toxics analysis for NH₃ and H₂SO₄ are presented in Table 13. Maximum 8-hour modeled impacts were compared to one-one hundredth of the Occupational Exposure Level ("OEL") listed in 20.2.72.502 NMAC. As shown, the maximum modeled impacts are less than standards.



Table 13. Air Toxics Analysis Results

Pollutant	Avgeraging Period	Maximum Modeled Impact - (μg/m³)	1/100 of OEL (μg/m³)
NH ₃	8-hr	32.3	180
H ₂ SO ₄	8-hr	4.9	10

7.7 Class II Visibility Analysis

The CAA Amendments of 1977 require evaluation of new and modified emission sources to determine potential impacts on visibility. The total hourly particulate matter and NO_X emissions from the project were used as input parameters in the visibility analysis. Emissions were evaluated as described in the EPA Workbook for Plume Visual Impact Screening and Analysis 13 to determine potential contribution to atmospheric discoloration and visual range reduction.

Generally, atmospheric discoloration occurs when NO emissions from combustion sources react in the presence of atmospheric oxygen to form NO₂, a reddish-brown gas. Another form of atmospheric discoloration may be caused by particulate emissions and secondary aerosols formed by gaseous precursor emissions. The visual range reduction (increased haze) is caused primarily by particulate emissions and secondary aerosols such as sulfates and nitrates.¹⁴ Both secondary sulfate and primary particulate emissions are accounted for in the analysis. Emission of other pollutants do not materially affect visibility.

U.S. EPA visibility impairment analysis guidelines were followed in conducting the analysis. The analysis was performed for the Living Desert State Park, located a minimum of 42 km and a maximum of 49 km south of the refinery.

This analysis requires inputs of emission rates (PM and NO_X), regional visual range, distance between the source and the object of study, and worst-case dispersion parameters (i.e., wind speed and stability). Outputs from the model include:



- Plume contrast against the sky and terrain; and,
- Perceptibility of the plume (Delta E criteria).

Emission rates for PM and NOx for the analyses were set to 84.3 and 182 tons per year, respectively. The background visual range was set to 110km, which was determined from Figure 9 of the VISCREEN manual. The VISCREEN default screening values for Delta E (2.0) and contrast (0.05) were assumed.

As shown in Table 14, no exceedances of the default delta E parameter or green contrast paramters were calculated using the conservative meteorological conditions (F stability and 1 m/sec wind speed) and Level-1 procedures.

The VISCREEN input and output model files are also provided electronically...



Table 14. Level-1 Class II Visibility Analysis Results for the Living Desert State Park

Viewing	Theta	Azimuth	Distance	Alpha	Delta E		Green Contrast		
Background	(degrees)	(degrees)	(km)	(degrees)	Criterion	Plume	Criterion	Plume	
SKY	10	122	49	46	2.000	0.956	0.050	0.011	
SKY	140	122	49	46.000	2.000	0.435	0.05	-0.01	
TERRAIN	10	84	42	84.000	2.000	1.631	0.05	0.015	
TERRAIN	140	84	42	84.000	2.000	0.180	0.05	0.004	



8.0 CLASS I AREA ANALYSIS RESULTS

8.1 Class I Significant Impact Analysis

A Class I significant impacts analysis was conducted for all Class I areas located within 300km of the refinery, regardless of the Q/D screening result. The model results are shown in Table 15. As shown, all impacts are calculated to be insignificant. The SRU3 Tail Gas Incinerator (Model ID H3103) was modeled with a 24-hr average SO₂ emission rate of 28 lb/hr. SO₂ emissions of 50 lb/hr were modeled for SRU3 for the other SO₂ averaging periods.

Table 15. Class I Significant Impact Analysis Results

			Modeled	Class I			
		Modeled	Conc.	SILa			
Pollutant	Average	Year	(μg/m3)	(μ g/m ³)			
		2013	1.88 x 10 ⁻²				
NO ₂	Annual	2014	1.89 x 10 ⁻²	0.10			
		2015	2.00 x 10 ⁻²				
		2013	6.66 x 10 ⁻²				
	24-hour	2014	6.11 x 10 ⁻²	0.30			
PM10		2015	5.78 x 10 ⁻²				
PIVITO		2013	7.76 x 10 ⁻³				
	Annual	2014	7.59 x 10 ⁻³	0.20			
		2015	8.27 x 10 ⁻³				
		2013	3.52 x 10 ⁻²				
	Annual	2014	3.52 x 10 ⁻²	0.10			
		2015	3.79 x 10 ⁻²				
		2013	1.93 x 10 ⁻¹				
SO ₂	24-hr	2014	1.78 x 10 ⁻¹	0.20			
		2015	1.56 x 10 ⁻¹				
		2013	9.45 x 10 ⁻¹				
	3-hr	2014	9.82 x 10 ⁻¹	1.0			
		2015	8.76 x 10 ⁻¹				

^aSee 61 FR 38249 (July 23, 1996) for the proposed Class I SILs.



8.2 Class I Visibility Analysis Results

HollyFrontier used the CALPUFF model and associated programs to evaluate the potential visibility impacts associated with the proposed project at the Carlsbad Caverns, the only Class I Area with a Q/D value that exceeded the FLM's screening criterion. The 98% (8th high) concentrations over all receptors, not by receptor, were conservatively used in the assessment.

Results are presented in Table 16. As shown, there are no exceedances of the 5% extinction criterion at Carlsbad Caverns.

Table 16. Class I 24-hr Visibility Analysis Results

Parameter	Meteorological Model Year	Modeled Value, Extinction (% change)	Change in Light Extinction (% change)	%Standard
	2013	2.78	5	56%
Visibility	2014	1.90	5	38%
	2015	2.24	5	45%

8.3 Class I Deposition Analysis Results

In addition to visibility, modeled deposition rates of total sulfur (S) and nitrogen (N) were calculated. These results were reviewed or comparison to the Deposition Analysis Thresholds (DATs) of 0.005 at each Class I area. Annual emission rates were used. In addition, all Class I areas were conservatively included eventhough only Carlsbad Caverns had a Q/D in excess of the FLM's screening criterion.

Results for nitrogen and sulfur deposition are presented in Table 17. No exceedances of the DATs were identified.



Table 17. Class I Annual Deposition Analysis Results

Parameter	Meteorological Model Year	Modeled Value, Deposition (ka/ha/yr)	Deposition Analysis Threshold (ka/ha/yr)	%Standard
	2013	2.56 x 10 ⁻³		51%
Nitrogen	2014	2.67 x 10 ⁻³		53%
	2015	2.87 x 10 ⁻³	0.005	57%
	2013	3.14 x 10 ⁻³		63%
Sulfur	2014	3.32 x 10 ⁻³		66%
	2015	3.77 x 10 ⁻³		75%



ATTACHMENT A

- HollyFrontier Model Input Data
- Off-Site Source Model Input Data
 - Volume Source Calculations
 - Flare Parameter Calculations
 - CALPUFF Model Input Data
 - CALPUFF CT PM Speciation

Last Update 7-7-22 Holly Frontier - Artesia Model Input NAD83, Zone 13 Point Sources

	nces												Pi	roject Relate	d Emissions	Increase (lb/h	nr)		
Model Source				Easting (X)	Northing (Y)	Base Elevation	Stack Height		Exit Velocity	Stack									
No.	Source ID		Source Description	(m)	(m)	(ft)	(ft)	Temp. (°F)	(ft/sec)	Diameter (ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT	со	H2S
1	B0007 B0008	DEFAULT	Boiler 7	556685.00	3634643.00	3363.5	74.8	275	47.90	5.25	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
2	B0009	DEFAULT DEFAULT	Boiler 8 Boiler 9	556686.00 556665.00	3634633.00 3634636.00	3363.5 3363.3	65.0 60.0	250 300	62.80 47.70	4.50 5.00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00
4	H0009	DEFAULT	Unit 13 Naphtha Splitter Reboiler	556553.00	3634619.00	3363.4	77.5	530	17.90	4.50	8.42E-02	8.42E-02	8.42E-02	5.40E-01	5.40E-01	1.83E-01	0.00E+00	8.76E-01	0.00E+00
5	H0011	DEFAULT	Unit 21 Vacuum Unit Heater	556821.00	3634014.00	3370.9	80.0	850	26.00	4.00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
6 7	H0018 H0019	DEFAULT DEFAULT	Unit 06 HDS Reboiler South Crude Charge Heater	556556.00 556625.00	3634718.00 3634023.00	3362.3 3370.3	75.0 155.7	700 450	19.50 21.40	4.00 4.38	1.15E-01 6.70E-02	1.15E-01 6.70E-02	1.15E-01 6.70E-02	1.52E+00 6.20E-01	1.52E+00 5.66E-01	4.25E-01 0.00E+00	0.00E+00 0.00E+00	1.27E+00 7.71E-01	0.00E+00 0.00E+00
8	H0020	DEFAULT	South Crude Charge Heater	556644.00	3634023.00	3370.5	175.0	330	12.20	6.50	0.70E-02 0.00E+00	0.70E-02 0.00E+00	0.70E-02 0.00E+00	0.20E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
9	H0028	DEFAULT	Unit 21 Heater	556829.00	3634014.00	3370.9	50.3	850	18.80	2.67	3.13E-02	3.13E-02	3.13E-02	1.72E+00	1.72E+00	9.99E-02	0.00E+00	3.51E-01	0.00E+00
10	H0030	DEFAULT	Unit 06 Charge Heater	556556.00	3634724.00	3362.2	67.0	575	22.50	4.00	0.00E+00	0.00E+00	0.00E+00	1.00E+00	1.00E+00	1.88E-01	0.00E+00	2.75E+00	0.00E+00
11 12	H0040 H0312	DEFAULT DEFAULT	Unit 13 Charge Heater Unit 10 FCC Feed Heater	556557.00 556690.00	3634730.00 3634676.00	3362.1 3363.8	101.0 96.5	590 675	22.80 20.40	4.00 4.00	0.00E+00 2.30E-01	0.00E+00 2.30E-01	0.00E+00 2.30E-01	7.20E-01 3.35E+00	7.20E-01 3.35E+00	0.00E+00 9.69E-01	0.00E+00 1.78E-01	7.73E-01 2.95E+00	0.00E+00 0.00E+00
13	H0352 54	DEFAULT	Unit 70 CCR Heaters	556734.00	3634728.00	3364.0	210.9	300	16.50	8.75	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.01E+00	0.00E+00
14	H0355	DEFAULT	Unit 70 Stabilizer Reboiler Heater	556734.12	3634703.54	3364.0	135.2	442	28.70	2.50	1.18E-02	1.18E-02	1.18E-02	9.70E-01	9.70E-01	0.00E+00	0.00E+00	1.01E+00	0.00E+00
15	H0362_64	DEFAULT	Unit 70 CCR Heaters	556718.00	3634728.00	3364.1	205.5	338	16.90	7.00	3.10E-01	3.10E-01	3.10E-01	2.51E+00	2.51E+00	1.34E+00	0.00E+00	3.45E+00	0.00E+00
16 17	H0421 H0464	DEFAULT DEFAULT	Unit 44 Charge Heater SRU Hot Oil Heater	556755.00 556526.00	3634642.00 3634548.00	3364.0 3364.3	81.7 79.8	650 450	23.70 9.60	3.25 2.75	7.35E-02 9.47E-03	7.35E-02 9.47E-03	7.35E-02 9.47E-03	6.30E-01 5.28E-02	6.30E-01 5.28E-02	2.38E-01 0.00E+00	0.00E+00 0.00E+00	8.10E-01 8.83E-02	0.00E+00 0.00E+00
18	H0600	DEFAULT	Unit 09 Depropanizer Reboiler Heater	556795.00	3634716.00	3364.0	177.0	500	33.00	4.60	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.55E+00	0.00E+00
19	H0601	DEFAULT	Unit 33 Charge Heater	556788.00	3634582.00	3364.3	131.0	300	11.60	6.50	2.35E-01	2.35E-01	2.35E-01	1.30E+00	1.30E+00	7.98E-01	0.00E+00	2.57E+00	0.00E+00
20	H2421	DEFAULT	Unit 45 Charge Heater	556769.00	3634573.00	3364.3	87.0	890	24.80	3.50	2.35E-02	2.35E-02	2.35E-02	2.30E-02	2.30E-02	0.00E+00	0.00E+00	2.98E-01	0.00E+00
21 22	H2501 H3101	DEFAULT DEFAULT	Unit 25 ROSE® Unit No. 2 Hot Oil Heater SRU3 Hot Oil Heater	556949.00 556557.00	3634500.00 3634512.00	3364.5 3364.5	168.0 80.0	710 450	19.00 9.62	7.83 2.75	9.93E-01 9.21E-02	9.93E-01 9.21E-02	9.93E-01 9.21E-02	3.60E+00 3.30E-01	3.60E+00 3.30E-01	4.35E+00 4.11E-01	1.64E+00 1.62E-01	7.20E+00 9.87E-01	0.00E+00 0.00E+00
23	H3402	DEFAULT	Unit 34 Hydrocracker Reboiler 1	556947.00	3634510.00	3364.4	67.0	575	27.90	4.00	4.30E-01	4.30E-01	4.30E-01	1.56E+00	1.56E+00	1.89E+00	7.11E-01	4.68E+00	0.00E+00
24	H3403	DEFAULT	Unit 34 Hydrocracker Reactor Charge Heate	556933.00	3634516.00	3364.4	86.1	705	19.40	4.00	2.65E-01	2.65E-01	2.65E-01	9.60E-01	9.60E-01	1.16E+00	4.38E-01	2.92E+00	0.00E+00
25	H8801_02	DEFAULT	Unit 63 Hydrogen Plant Reformer Furnaces	556903.00	3634585.00	3364.0	130.0	600	75.40	3.83	3.64E-01	3.64E-01	3.64E-01	4.46E+00	4.46E+00	0.00E+00	0.00E+00	4.02E+00	0.00E+00
26 27	H9851 H0473	DEFAULT DEFAULT	Unit 64 Hydrogen Plant Reformer SRU2 Tail Gas Incinerator	556901.00 556518.00	3634616.00 3634578.00	3364.0 3364.1	176.0 150.0	350 1150	23.80 44.20	10.00 4.00	2.59E+00 0.00E+00	2.59E+00 0.00E+00	2.59E+00 0.00E+00	1.12E+01 0.00E+00	4.51E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	1.81E+01 0.00E+00	0.00E+00 0.00E+00
28	H3103	DEFAULT	SRU3 Tail Gas Incinerator	556553.00	3634495.00	3364.7	150.0	1200	49.90	4.00	1.33E+01	1.33E+01	1.91E+00	6.50E+00	6.51E+00	5.00E+01	1.87E+01	1.50E+01	2.32E-01
29	FCCREGEN	DEFAULT	FCC Regenerator	556712.00	3634686.00	3363.7	153.0	125	28.30	6.00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
30	FL0400	DEFAULT	FL-0400, North Plant Flare	556647.00	3634806.00	3361.9	395.1	1832	65.60	16.11	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.75E-02
31 32	FL0401 FL0402	DEFAULT DEFAULT	FL-0401, South Plant Flare FL-0402, FCC Flare	556802.00 556684.00	3634036.00 3634806.00	3370.6 3363.8	342.2 304.6	1832 1832	65.60 65.60	9.60 9.28	0.00E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	6.09E-01 1.20E+01
33	FL0402	DEFAULT	FL-0403, Alky Flare	556685.00	3634875.00	3363.3	499.1	1832	65.60	19.45	0.00E+00 0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.17E-02
34	FL0404	DEFAULT	FL-0404, GOHT Flare	556898.00	3634870.00	3361.8	568.5	1832	65.60	26.01	0.00E+00	0.00E+00	0.00E+00	1.12E+01	4.82E+00	3.98E+01	2.46E+00	4.78E+01	4.24E-01
35	TL4VCU	DEFAULT	TL-4 VCU	556768.00	3634222.00	3367.9	81.8	1832	65.60	3.92	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
36 37	H5401 Y0001	DEFAULT DEFAULT	Unit 54 HDS Reactor Heater TCC Cooling Tower	556917.00 556711.00	3634721.00 3634046.00	3363.0 3370.5	83.0 14.0	643 100	8.81 25.00	3.00 8.00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00F+00	0.00E+00 0.00E+00
38	Y0002	DEFAULT	S. Alky Cooling Tower (Marley Cooling Towe		3634059.00	3370.3	14.0	100	25.00	8.00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
39	Y0008	DEFAULT	North Alky Cooling Tower	556872.00	3634669.00	3363.8	14.0	100	25.00	8.00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
40	Y0011	DEFAULT	FCC & NP Cooling Tower	556601.00	3634564.00	3363.9	14.0	100	25.00	8.00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
41 42	Y0012 CTTT0006	DEFAULT DEFAULT	Hydrogen Plants Cooling Tower Unit 07 Amine W-0745 Cooling Tower	556898.00 556469.00	3634670.00 3634681.00	3363.7 3363.4	14.0 14.0	100 100	25.00 25.00	8.00 8.00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00
42	FLHEP	DEFAULT	HEP Portable Flare	556740.00	3634216.00	3367.8	51.1	1832	65.60	2.29	0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-1.88F-02
44	TVCU	DEFAULT	Tank VCU	556458.00	3634605.00	3364.3	18.5	1832	65.60	0.20	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
45	H_2601	DEFAULT	RDU Reactor Heater	556954.24	3634430.58	3365.0	138.5	600	25.50	3.87	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
46 47	Y_0026A	DEFAULT	RDU Cooling Tower	556999.64	3634453.06	3364.6	21.0	90	25.80	12.19	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
47	Y_0026B Y_0093A	DEFAULT DEFAULT	RDU Cooling Tower PTU Cooling Tower	556999.55 556855.96	3634447.97 3633752.89	3364.7 3373.2	21.0 21.0	90 90	25.80 25.80	12.19 12.19	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00
49	Y_0093B	DEFAULT	PTU Cooling Tower	556855.87	3633747.81	3373.3	21.0	90	25.80	12.19	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
50	H_9301	DEFAULT	Vapor Combustor Unit	556871.00	3633812.00	3372.9	87.0	1600	2.60	4.00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
51 52	082B6 26 2B25A	DEFAULT DEFAULT	Filter Aid Tank Vent 26 2B25AP01 - Adsorption Train 1 Vent B	556883.66 556854.36	3633823.60 3633819.49	3372.9 3372.9	80.0 80.0	100 100	127.30 127.30	0.25 0.25	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00
53	26_2B25A 26_1B25B	DEFAULT	26_1B25BP01 - Adsorption Train 2 Vent A	556859.14	3633819.49	3372.9	80.0	100	127.30	0.25	0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
54	26_2B25B	DEFAULT	26_2B25BP01 - Adsorption Train 2 Vent B	556864.00	3633819.49	3372.9	80.0	100	127.30	0.25	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
55	26_2B26	DEFAULT	26_2B26P01 - Adsorption Vent B	556872.17	3633819.84	3372.9	80.0	100	127.30	0.25	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
56	26_1B26	DEFAULT	26_1B26P01 - Adsorption Vent A	556880.87	3633819.69	3372.9	80.0	100	127.30	0.25	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
57 58	26_1B25A 56B25C	DEFAULT DEFAULT	26_1B25AP01 - Adsorption Train 1 Vent A Silo 3 Vent	556890.55 556846.62	3633819.76 3633816.62	3372.8 3373.1	80.0 80.0	100 100	127.30 161.10	0.25 0.67	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00
59	V0543	DEFAULT	Portable Air Compressor	556618.90	3634620.37	3363.4	6.0	1000	244.82	0.33	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
60	V0545	DEFAULT	Portable Air Compressor	556695.95	3634556.00	3364.0	6.0	1000	244.82	0.33	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
61	V0546 G0100	DEFAULT	Portable Air Compressor	556765.80	3634115.08	3369.5 3364.0	6.0 10.0	1000	225.99	0.33	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
62 63	G0100 G0101	DEFAULT DEFAULT	UPS backup generator UPS backup generator	556695.06 556780.25	3634566.59 3634102.48	3364.0 3369.7	10.0 12.0	1000 1000	229.84 238.68	0.17	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00
64	G0102	DEFAULT	Server Backup Generator	557026.11	3634058.67	3369.2	10.0	1000	354.00	0.33	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
65	E0600W	DEFAULT	Fire Water Pump Engine	557227.00	3634864.00	3357.7	4.0	1000	354.04	0.33	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
66	E0601M	DEFAULT	Fire Water Pump Engine	557233.04	3634863.96	3357.6	4.0	1000	354.04	0.33	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
67 68	E0602E E0603	DEFAULT DEFAULT	Fire Water Pump Engine Fire Water Pump Engine	557238.59 556907.01	3634863.84 3634446.37	3357.5 3365.1	4.0 4.0	1000 1000	354.04 287.19	0.33	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00
69	V0511	DEFAULT	Portable Fire Water Pump Engine	557058.55	3634424.95	3365.1	8.0	1000	287.19	0.33	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00
70	G2601	DEFAULT	Emergency Generator	556682.00	3634588.54	3363.7	10.0	1000	287.19	0.33	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
71	G2602	DEFAULT	Emergency Generator	556698.90	3634587.41	3363.8	10.0	1000	287.19	0.33	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
72	TRLO_9	DEFAULT	Molten Sulfur Railcar Loading Controlled	556463.00	3634577.00	3364.5	15.0	130	97.48	0.33	0.00E+00	0.00E+00 19.25	0.00E+00	0.00E+00 54.74	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.75E-03
			t part of the HollyFrontier refinery. They are an l emissions were modeled in lieu of PTE for the							Total (lb/hr) Total (tpy)	19.25 84.31	19.25 84.31	7.84 34.35	54.74 239.75	41.65 182.42	101.88 446.23	24.33 106.56	124.26 544.24	13.35 58.48
			"ST" extension were used to assess complianc				nd 24-hr			rotal (tpy)	04.01	04.01	04.00	200.10	102.72	440.23	100.00	544.24	30.40

Sources definited by the feb ont are not part or the new product enterinery. They are an adjacent, separate stationary source. Per Table 8-2 of Appendix W, actual PM emissions were modeled in lieu of PTE for the FCC regenerator. This unit is not modified. Pollutant names: pollutant names with a "ST" extension were used to assess compliance with short-term standards (i.e., 1-hr, 3-hr and 24-hr Pollutant names: pollutant names with a "ST" extension were used to assess compliance with annual standards.

Last Update 7-7-22 Holly Frontier - Artesia Model Input NAD83, Zone 13 Point Sources

								Pote	ntial to Em	it (lb/hr)				
Model Source			·											
No.	Source ID		Source Description	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_24hr	со	H2S	H2SO4	NH
1	B0007	DEFAULT	Boiler 7	1.78E+00	1.78E+00	1.78E+00	1.29E+01	1.29E+01	8.04E+00	8.04E+00	1.97E+01	0.00E+00	0.00E+00	0.00E
2	B0008	DEFAULT	Boiler 8	1.78E+00	1.78E+00	1.78E+00			8.04E+00	8.04E+00	1.97E+01	0.00E+00	0.00E+00	0.00
3	B0009	DEFAULT	Boiler 9	1.82E+00	1.82E+00	1.82E+00		4.89E+00	2.89E+00	2.89E+00	9.04E+00	0.00E+00	0.00E+00	0.00
4 5	H0009 H0011	DEFAULT DEFAULT	Unit 13 Naphtha Splitter Reboiler Unit 21 Vacuum Unit Heater	3.64E-01 3.15E-01	3.64E-01 3.15E-01	3.64E-01 3.15E-01	3.96E+00	3.96E+00 7.24E+00	1.64E+00 1.42F+00	1.64E+00 1.42E+00	4.03E+00 3.48F+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00
6	H0018	DEFAULT	Unit 06 HDS Reboiler	2.65E-01	2.65E-01	2.65E-01		3.49E+00	1.42E+00	1.42E+00	2.93E+00	0.00E+00	0.00E+00	0.00
7	H0019	DEFAULT	South Crude Charge Heater	4.47E-01	4.47E-01	4.57E-01		2.85E+00	2.02E+00	2.02E+00	4.94E+00	0.00E+00	0.00E+00	0.00
8	H0020	DEFAULT	South Crude Charge Heater	7.45F-01	7.45F-01	7.45F-01		4.82F+00	3.37F+00	3.37F+00	8.23F+00	0.00E+00	0.00E+00	0.0
9	H0028	DEFAULT	Unit 21 Heater	1.02E-01	1.02E-01	1.02E-01	2.17E+00	2.17E+00	4.60E-01	4.60E-01	1.13E+00	0.00E+00	0.00E+00	0.0
10	H0030	DEFAULT	Unit 06 Charge Heater	4.00E-01	4.00E-01	3.48E-01	3.19E+00		1.57E+00	1.57E+00	3.84E+00	0.00E+00	0.00E+00	0.00
11	H0040	DEFAULT	Unit 13 Charge Heater	4.00E-01	4.00E-01	3.48E-01	3.78E+00		1.57E+00	1.57E+00	3.84E+00	0.00E+00	0.00E+00	0.0
12	H0312	DEFAULT	Unit 10 FCC Feed Heater	2.90E-01	2.90E-01	2.90E-01	4.62E+00	4.62E+00	1.31E+00	1.31E+00	3.20E+00	0.00E+00	0.00E+00	0.00
13	H0352_54	DEFAULT	Unit 70 CCR Heaters	1.70E+00	1.70E+00	1.66E+00	9.00E+00			8.07E+00	1.83E+01	0.00E+00	0.00E+00	0.0
14	H0355	DEFAULT	Unit 70 Stabilizer Reboiler Heater	2.32E-01	2.32E-01	2.32E-01		2.52E+00	1.13E+00	1.13E+00	2.56E+00	0.00E+00	0.00E+00	0.0
15	H0362_64	DEFAULT	Unit 70 CCR Heaters	1.03E+00	1.03E+00	1.03E+00		6.88E+00	5.04E+00	5.04E+00	1.14E+01	0.00E+00	0.00E+00	0.0
16	H0421	DEFAULT	Unit 44 Charge Heater	2.24E-01	2.24E-01	2.24E-01	2.43E+00		1.01E+00	1.01E+00	2.47E+00	0.00E+00	0.00E+00	0.0
17	H0464	DEFAULT	SRU Hot Oil Heater	7.95E-02	7.95E-02	9.13E-02		5.23E-01	3.58E-01	3.58E-01	8.78E-01	0.00E+00	0.00E+00	0.00
18	H0600	DEFAULT	Unit 09 Depropanizer Reboiler Heater	6.95E-01	6.95E-01	6.95E-01		4.67E+00	3.14E+00	3.14E+00	7.69E+00	0.00E+00	0.00E+00	0.0
19	H0601	DEFAULT	Unit 33 Charge Heater	6.46E-01	6.46E-01	6.46E-01	3.51E+00		2.91E+00	2.91E+00	7.14E+00	0.00E+00	0.00E+00	0.0
20	H2421	DEFAULT	Unit 45 Charge Heater	2.24E-01	2.24E-01	2.24E-01	1.22E+00	1.22E+00	9.77E-01	9.77E-01	2.47E+00	0.00E+00	0.00E+00	0.0
21	H2501 H3101	DEFAULT	Unit 25 ROSE® Unit No. 2 Hot Oil Heater SRU3 Hot Oil Heater	9.93E-01 9.11F-02	9.93E-01 9.11F-02	9.93E-01 9.13E-02	3.60E+00 3.30F-01	3.60E+00 3.30F-01	4.35E+00 4.11F-01	4.35E+00 4.11E-01	7.20E+00 9.90F=01	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.0
22	H3101 H3402	DEFAULT	Unit 34 Hydrocracker Reboiler 1	9.11E-02 4.30E-01	9.11E-02 4.30E-01	9.13E-02 4.30E-01	3.30E-01 1.56E+00	3.30E-01 1.56E+00	4.11E-01 1.89E+00	4.11E-01 1.89E+00	9.90E-01 4.68E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.0
24	H3403	DEFAULT	Unit 34 Hydrocracker Reactor Charge Heate		2.65E-01	2.65E-01		9.60E-01	1.09E+00	1.16E+00	2.93E+00	0.00E+00	0.00E+00	0.0
25	H8801 02	DEFAULT	Unit 63 Hydrogen Plant Reformer Furnaces	1.26F+00	1.26F+00	1.26E+00		8.66E+00	2.85F+00	2.85E+00	1.39F+01	0.00E+00	0.00E+00	0.0
26	H9851	DEFAULT	Unit 64 Hydrogen Plant Reformer	2.79E+00	2.79E+00	2.81E+00		4.52E+00	6.32E+00	6.32E+00	2.02E+01	0.00E+00	0.00E+00	1.3
27	H0473	DEFAULT	SRU2 Tail Gas Incinerator	1.15E+01	1.15F+01	1.92F+00	6.50E+00		1.35E+02	1.35F+02	2.77F+01	1.44F+00	1.03F+01	0.0
28	H3103	DEFAULT	SRU3 Tail Gas Incinerator	4.93E+00	4.93E+00	1.91E+00		6.51E+00		5.00E+01	1.50E+01	5.32E-01	3.83E+00	0.0
29	FCCREGEN	DEFAULT	FCC Regenerator	2.29E+01	1.90E+01	1.57E+01		2.32E+01	2.79E+01	2.79E+01	1.22E+02	0.00E+00	2.13E+00	1.6
30	FL0400	DEFAULT	FL-0400, North Plant Flare	0.00E+00	0.00E+00	0.00E+00	3.47E+00	1.24E+00	4.48E+00	4.48E+00	1.42E+01	4.75E-02	0.00E+00	0.0
31	FL0401	DEFAULT	FL-0401, South Plant Flare	0.00E+00	0.00E+00	0.00E+00	1.66E+00	4.22E-01	5.73E+01	5.73E+01	6.82E+00	6.09E-01	0.00E+00	0.0
32	FL0402	DEFAULT	FL-0402, FCC Flare	0.00E+00	0.00E+00	0.00E+00	1.63E+02	4.68E+00	1.13E+03	1.13E+03	1.24E+03	1.20E+01	0.00E+00	0.0
33	FL0403	DEFAULT	FL-0403, Alky Flare	0.00E+00	0.00E+00	0.00E+00	2.74E+00		1.10E+00	1.10E+00	1.13E+01	1.17E-02	0.00E+00	0.0
34	FL0404	DEFAULT	FL-0404, GOHT Flare	0.00E+00	0.00E+00	0.00E+00		5.36E+00	3.99E+01	3.99E+01	4.80E+01	4.24E-01	0.00E+00	0.0
35	TL4VCU	DEFAULT	TL-4 VCU	1.05E-01	1.05E-01	1.50E-02	1.97E+00		5.14E-01	5.14E-01	1.97E+00	0.00E+00	0.00E+00	0.0
36	H5401	DEFAULT	Unit 54 HDS Reactor Heater	1.60E-01	1.60E-01	1.60E-01	7.73E-01	7.73E-01	7.22E-01	7.22E-01	6.44E-01	0.00E+00	0.00E+00	0.0
37	Y0001	DEFAULT	TCC Cooling Tower	1.58E-01	5.94E-04	5.94E-04	0.00E+00	0.0						
38	Y0002	DEFAULT	S. Alky Cooling Tower (Marley Cooling Towe		5.94E-04	5.94E-04	0.00E+00		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
39	Y0008	DEFAULT	North Alky Cooling Tower	3.69E-01	1.39E-03	1.39E-03		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
40	Y0011	DEFAULT	FCC & NP Cooling Tower	3.16E-01	1.19E-03	1.19E-03			0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
41	Y0012	DEFAULT	Hydrogen Plants Cooling Tower	1.05E-01	3.96E-04	3.96E-04 3.56F-04	0.00E+00 0.00F+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.0
42	CTTT0006	DEFAULT	Unit 07 Amine W-0745 Cooling Tower	9.48E-02	3.56E-04									0.00
43 44	FLHEP TVCU	DEFAULT DEFAULT	HEP Portable Flare Tank VCU	0.00E+00 9.39E-03	0.00E+00 9.39E-03	0.00E+00 5.71E-04	1.16E+01 1.74E-01	1.98E-02 8.42F-03	1.10E-01 4.96F-02	1.10E-01 4.96E-02	5.01E+01 1.73E-01	1.19E-03 1.24E-03	0.00E+00 0.00E+00	0.0
45	H 2601	DEFAULT	RDU Reactor Heater	3.21E-01	3.21E-01	3.21E-04 3.21E-01		1.29E+00	5.78E-01	5.78E-01	2.59E+00	0.00E+00	0.00E+00	0.0
46	Y_0026A	DEFAULT	RDU Cooling Tower	1.32E-01	4.95E-05	4.95E-05		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
47	Y 0026B	DEFAULT	RDU Cooling Tower	1.32E-02	4.95E-05	4.95E-05		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
48	Y 0093A	DEFAULT	PTU Cooling Tower	1.30E-02	5.00E-05	5.00E-05		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00
49	Y 0093B	DEFAULT	PTU Cooling Tower	1.30E-02	5.00E-05	5.00E-05	0.00E+00		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00
50	H 9301	DEFAULT	Vapor Combustor Unit	1.40E-02	1.40E-02	1.40E-02	4.27E-01	4.27E-01	1.10E-02	1.10E-02	1.56E-01	0.00E+00	0.00E+00	0.00
51	082B6	DEFAULT	Filter Aid Tank Vent	6.40E-03	6.40E-03	6.40E-03		0.00E+00		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
52	26_2B25A	DEFAULT	26_2B25AP01 - Adsorption Train 1 Vent B	6.40E-03	6.40E-03	6.40E-03		0.00E+00		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
53	26_1B25B	DEFAULT	26_1B25BP01 - Adsorption Train 2 Vent A	6.40E-03	6.40E-03	6.40E-03	0.00E+00	0.0						
54	26_2B25B	DEFAULT	26_2B25BP01 - Adsorption Train 2 Vent B	6.40E-03	6.40E-03	6.40E-03	0.00E+00	0.0						
55	26_2B26	DEFAULT	26_2B26P01 - Adsorption Vent B	6.40E-03	6.40E-03	6.40E-03	0.00E+00	0.0						
56	26_1B26	DEFAULT	26_1B26P01 - Adsorption Vent A	6.40E-03	6.40E-03	6.40E-03		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
57	26_1B25A	DEFAULT	26_1B25AP01 - Adsorption Train 1 Vent A	6.40E-03	6.40E-03	6.40E-03		0.00E+00		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
58	56B25C	DEFAULT	Silo 3 Vent	5.80E-02	5.80E-02	5.80E-02		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
59	V0543	DEFAULT	Portable Air Compressor	9.21E-02	9.21E-02	9.21E-02	1.84E+00	1.84E+00	3.48E-03	3.48E-03	1.61E+00	0.00E+00	0.00E+00	0.0
60	V0545	DEFAULT	Portable Air Compressor	9.21E-02	9.21E-02	9.21E-02		1.84E+00	3.48E-03	3.48E-03	1.61E+00	0.00E+00	0.00E+00	0.0
61	V0546	DEFAULT	Portable Air Compressor	4.54E-03	4.54E-03	4.54E-03	9.07E-02	9.07E-02	1.72E-03	1.72E-03	1.13E+00	0.00E+00	0.00E+00	0.0
62	G0100	DEFAULT	UPS backup generator	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
63	G0101	DEFAULT	UPS backup generator	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.0
64	G0102	DEFAULT	Server Backup Generator	0.00E+00	0.0									
65	E0600W E0601M	DEFAULT	Fire Water Pump Engine	1.24E-01 1.24E-01	1.24E-01 1.24E-01	1.42E-03 1.42E-03	2.49E+00 2.49E+00	2.84E-02 2.84E-02	4.68E-03 4.68E-03	4.68E-03 4.68E-03	2.16E+00 2.16E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.0
66			Fire Water Pump Engine											0.0
67	E0602E	DEFAULT	Fire Water Pump Engine	1.24E-01	1.24E-01	1.42E-03	2.49E+00		4.68E-03	4.68E-03	2.16E+00	0.00E+00	0.00E+00	0.0
68	E0603	DEFAULT	Fire Water Pump Engine	1.01E-01	1.01E-01	1.15E-03	2.02E+00		3.79E-03	3.79E-03	1.75E+00	0.00E+00	0.00E+00	0.0
69	V0511	DEFAULT	Portable Fire Water Pump Engine	2.30E-01	2.30E-01	2.63E-03	4.60E+00		8.70E-03	8.70E-03	4.03E+00	0.00E+00	0.00E+00	0.0
70 71	G2601 G2602	DEFAULT DEFAULT	Emergency Generator	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00		0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.0
71 72	TRLO 9	DEFAULT	Emergency Generator Molten Sulfur Railcar Loading Controlled	0.00E+00 0.00E+00	0.00E+00 0.00F+00	0.00E+00 0.00F+00		0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00F+00	0.00E+00 0.00E+00	4.75E-03	0.00E+00 0.00E+00	0.00
			part of the HollyFrontier refinery. They are an		56.44	39.62	390.70	172.47	1524.25	1524.25	1746.92	4.75E-03	16.29	
		eu ioni are noi	i pari oi irie HollyFrontier reilliery. They are an	01.07	50.44	39.62	390.70	1/4.4/	1024.25	1524.25	1740.92	15.11	10.29	1
		M/ noticel Day	emissions were modeled in lieu of PTE for the	269.68	247.21	173.52	1711.27	755.40	6676.20	6676.20	7651.51	66.18	71.37	77

HollyFrontier - Volume Sources (H2S and Toxics Only)

Model Source	Source				Base Elevation	Release Height	Horizontal Dimension -	
No.	ID	Source Description	Easting (X)	Northing (Y)	(ft)	(ft)	Sigma Y (ft)	Sigma Z (ft)
73	TLO_1	TLO-1 Asphalt Truck Loading Rack	556951.00	3634033.00	3370.5	15.0	2.3	7.0
74	TL_2	TL-2 Asphalt Truck Loading Rack #2	556913.00	3634267.00	3366.9	15.0	2.3	7.0
75	TL_4	TL-4 Fuels Truck Loading Rack e, f	556740.00	3634364.00	3365.9	15.0	2.3	7.0
76	TL_7	TL-7 CBO/LCO Truck Loading Rack	556410.00	3634889.00	3365.3	15.0	2.3	7.0
77	RLO_8	RLO-8 Railcar Loading Rack	556379.00	3634966.00	3366.5	15.0	2.3	7.0
78	RLO_19	RLO-19 Railcar Loading Rack	556513.00	3634124.00	3369.6	15.0	2.3	7.0
79	TLO_20	TLO-20 Asphalt/Pitch Truck Loading Rack	557316.00	3634568.00	3360.1	15.0	2.3	7.0
80	TRLO_9F	Molten Sulfur Railcar Loading	556463.00	3634577.00	3364.5	15.0	2.3	7.0
81	T_0049	Slop Oil Tank	556806.00	3634183.00	3368.3	36.0	2.3	16.7
82	T_0059	T-0059, Light Cycle Oil (LCO) tank	556498.59	3634850.62	3363.5	30.0	7.2	14.0
83	T_0061	Light Cycle Oil (LCO) fixed roof tank	556497.48	3634911.00	3364.1	30.0	10.3	14.0
84	T_0063	Heavy Cycle Oil (HCO) fixed roof tank	556531.58	3634945.66	3363.7	30.0	10.5	14.0
85	T_0065	Heavy Cycle Oil (HCO) fixed roof tank	556528.22	3634909.88	3363.7	30.0	10.3	14.0
86	T_0075	Heavy Cycle Oil (HCO)fixed roof tank	556464.49	3634916.03	3364.6	32.0	13.4	14.9
87	T_0081	Asphalt/Pitch Tank	557350.20	3634629.35	3358.7	40.0	22.4	18.6
88	T_0082	Asphalt/Pitch Tank	557294.90	3634635.86	3359.7	40.0	28.8	18.6
89	T_0110	Asphalt/Pitch Tank	556900.88	3634231.86	3367.6	35.0	22.3	16.3
90	T_0400	Gas Oil fixed roof tank	556712.93	3634475.65	3364.7	48.0	24.7	22.3
91	T 0402	T-0402 Light Cat Naphtha tank	557231.49	3634376.15	3362.9	50.0	18.5	23.3
92	T 0410	Asphalt/Pitch Tank	556898.32	3634106.89	3369.3	40.0	16.3	18.6
93	T 0411	T-0411 Gasolines & Gasoline Blendstocks	557083.75	3634253.22	3365.3	40.0	20.6	18.6
94	T 0419	No. 2 Fuel Oil (Diesel) fixed roof tank	556713.81	3634160.70	3368.9	28.0	10.9	13.0
95	T 0420	Asphalt/Pitch Tank	556940.51	3634116.91	3369.1	30.0	10.3	14.0
96	T 0422	Light Cycle Oil (LCO) fixed roof tank	556963.72	3634117.96	3369.0	30.0	10.3	14.0
97	T 0423	Light Cycle Oil (LCO) fixed roof tank	556964.77	3634090.54	3369.4	30.0	10.3	14.0
98	T 0431	Fuel Oil fixed roof tank	556896.67	3634180.59	3368.3	32.0	22.5	14.9
99	T 0432	Fuel Oil fixed roof tank	556943.73	3634184.42	3368.0	32.0	22.5	14.9
100	T 0433	Straight Run Gas Oil fixed roof tank	556890.24	3634326.64	3366.2	42.0	24.1	19.5
101	T 0434	Straight Run Diesel fixed roof tank	556609.74	3634191.31	3368.4	42.0	24.1	19.5
102	T 0914	Slop Oil Tank	556918.87	3634034.06	3370.5	40.0	15.5	18.6
103	T 1227	Asphalt/Pitch Tank	556788.69	3634425.75	3365.3	40.0	15.9	18.6
104	T 0106	T-0106 Sour Water Tank	556846.55	3634177.91	3368.4	40.0	13.8	18.6
105	T 0435	T-0435 Sour Water Tank	556807.39	3634533.97	3364.5	40.0	6.2	18.6
106	T 0437	T-0437 Crude Oil Tank	557154.64	3634557.61	3362.4	40.0	24.7	18.6
107	T 0438	Straight Run Gas Oil fixed roof tank	556854.20	3634228.42	3367.7	48.0	18.5	22.3
108	T 0439	T-0439 Sour Naphtha Tank	556780.49	3634480.62	3364.7	46.0	26.8	21.4
109	T 0450	T-0450 Sour Naphtha Tank	557152.77	3634475.54	3363.0	40.0	24.7	18.6
110	T_0450	T-0450 Straight Run Diesel tank	556842.85	3634358.19	3365.8	40.0	7.2	18.6
111	T 0737	T-0737 Sour Water Tank	556450.62	3634620.57	3364.1	40.0	13.0	18.6
112	T_0737 T_0802	T-0737 Sour Water Tank T-0802 Sour Water Tank	556445.16	3634595.97	3364.4	40.0	9.3	18.6
113	T_0802 T_0814	Asphalt/Pitch Tank	556943.68	3634088.43	3369.6	32.0	9.3 10.3	14.9
114	T_0814 T_0815	No. 2 Fuel Oil (Diesel) tank	556520.39	3635063.61	3364.6	43.0	23.9	20.0
115	T_0813	Light Cat Naphtha tank	557195.90	3634451.64	3362.7	50.0	23.9	23.3
116	T 0830	T-0830 Slop Oil Tank	556813.69	3634957.68	3362.7	40.0	28.8	23.3 18.6
117	T_0834	Straight Run Diesel tank	556427.01	3634979.64	3365.6	40.0	20.0 17.5	18.6
118	_						22.9	18.6
119	T_0835 T_0838	Straight Run Diesel tank	556643.07 556486.78	3635144.08 3634955.24	3363.0 3364.5	40.0 40.0	22.9 15.2	18.6
120	T 1225	No. 2 Fuel Oil (Diesel) tank T-1225 Crude Oil Tank	557155.26	3634634.07	3364.5 3362.1	40.0 40.0	30.9	18.6

HollyFrontier - Volume Sources (H2S and Toxics Only)

HollyFrontier - Vo	olume Sources (H2S	s and Toxics Only)			Pro	ject Related	Fmissions Ir	crease (lh/h	r)		
					110	joot Related	5510115 11	iorease (ib/ii	•,		
Model											
Source	Source										
No.	ID	Source Description	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT	со	H2S
73	TLO 1	TLO-1 Asphalt Truck Loading Rack	0.00E+00	7.28E-03							
74	TLO_1	TL-2 Asphalt Truck Loading Rack #2	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	6.24E-03
75	TL_2	TL-4 Fuels Truck Loading Rack e, f	0.00E+00	1.86E-02							
76 76	TL 7	TL-7 CBO/LCO Truck Loading Rack	0.00E+00	3.19E-05							
77	RLO 8	RLO-8 Railcar Loading Rack	0.00E+00	6.24E-03							
78	RLO_0	RLO-19 Railcar Loading Rack	0.00E+00	3.28E-02							
79	TLO 20	TLO-20 Asphalt/Pitch Truck Loading Rack	0.00E+00	1.25E-02							
80	TRLO 9F	Molten Sulfur Railcar Loading	0.00E+00	4.34E-02							
81	T 0049	Slop Oil Tank	0.00E+00	3.88E-01							
82	T 0059	T-0059, Light Cycle Oil (LCO) tank	0.00E+00	1.82E-05							
83	T 0061	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	2.78E-05							
84	T 0063	Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00	3.61E-04							
85	T 0065	Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00	1.59E-02							
86	T_0075	Heavy Cycle Oil (HCO)fixed roof tank	0.00E+00	1.59E-02							
87	T_0081	Asphalt/Pitch Tank	0.00E+00	5.92E-02							
88	T_0082	Asphalt/Pitch Tank	0.00E+00	6.24E-02							
89	T_0110	Asphalt/Pitch Tank	0.00E+00	1.57E-03							
90	T_0400	Gas Oil fixed roof tank	0.00E+00	1.91E-02							
91	T_0402	T-0402 Light Cat Naphtha tank	0.00E+00	4.52E-04							
92	T_0410	Asphalt/Pitch Tank	0.00E+00	2.68E-02							
93	T 0411	T-0411 Gasolines & Gasoline Blendstocks	0.00E+00	2.66E-05							
94	T_0419	No. 2 Fuel Oil (Diesel) fixed roof tank	0.00E+00	1.79E-03							
95	T_0420	Asphalt/Pitch Tank	0.00E+00	3.42E-03							
96	T_0422	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	1.59E-04							
97	T_0423	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	1.89E-04							
98	T_0431	Fuel Oil fixed roof tank	0.00E+00	1.04E-02							
99	T_0432	Fuel Oil fixed roof tank	0.00E+00	9.04E-03							
100	T_0433	Straight Run Gas Oil fixed roof tank	0.00E+00	2.48E-04							
101	T_0434	Straight Run Diesel fixed roof tank	0.00E+00	2.72E-02							
102	T_0914	Slop Oil Tank	0.00E+00								
103	T_1227	Asphalt/Pitch Tank	0.00E+00	2.34E-02							
104	T_0106	T-0106 Sour Water Tank	0.00E+00	-1.36E-01							
105	T_0435	T-0435 Sour Water Tank	0.00E+00	-1.28E-01							
106	T_0437	T-0437 Crude Oil Tank	0.00E+00	-3.21E-01							
107	T_0438	Straight Run Gas Oil fixed roof tank	0.00E+00	4.92E-03							
108	T_0439	T-0439 Sour Naphtha Tank	0.00E+00	2.10E-03							
109	T_0450	T-0450 Sour Naphtha Tank	0.00E+00	1.74E-03							
110	T_0451	T-0451 Straight Run Diesel tank	0.00E+00	1.55E-04							
111	T_0737	T-0737 Sour Water Tank	0.00E+00	-9.18E-02							
112	T_0802	T-0802 Sour Water Tank	0.00E+00	-8.79E-02							
113 114	T_0814 T_0815	Asphalt/Pitch Tank No. 2 Fuel Oil (Diesel) tank	0.00E+00 0.00E+00	1.19E-02 2.72E-02							
115	T 0821	Light Cat Naphtha tank	0.00E+00 0.00E+00	2.72E-02 4.87E-04							
116	T 0830	T-0830 Slop Oil Tank	0.00E+00 0.00E+00	4.87E-04 0.00E+00							
117	T 0834	Straight Run Diesel tank	0.00E+00 0.00E+00	1.03E-03							
118	T_0835	Straight Run Diesel tank Straight Run Diesel tank	0.00E+00 0.00E+00	1.03E-03 1.79E-03							
119	T_0838	No. 2 Fuel Oil (Diesel) tank	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00	7.40E-03
120	T 1225										-4.32E-01
120	I_1225	T-1225 Crude Oil Tank	0.00E+00	-4.32E-0							

HollyFrontier - Volume Sources (H2S and Toxics Only)

	,	and Toxics Only)					Pote	ntial to Em	it (lb/hr)		
Model Source No.	Source ID	Source Description	PM10	PM25 ST	PM25 LT	NO2 ST	NO2 LT	SO2 ST	SO2 24hr	СО	H2S
73	TLO 1	TLO-1 Asphalt Truck Loading Rack	0.00E+00	0.00E+00	0.00E+00		0.00E+00		0.00E+00	0.00E+00	7.28E-03
74	TL 2	TL-2 Asphalt Truck Loading Rack #2	0.00E+00	0.00E+00	0.00E+00			0.00E+00	0.00E+00	0.00E+00	6.24E-03
75	TL 4	TL-4 Fuels Truck Loading Rack e, f	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.86E-02
76	TL 7	TL-7 CBO/LCO Truck Loading Rack	0.00E+00		0.00E+00				0.00E+00	0.00E+00	3.19E-05
77	RLO 8	RLO-8 Railcar Loading Rack	0.00E+00		0.00E+00				0.00E+00	0.00E+00	6.24E-03
78	RLO 19	RLO-19 Railcar Loading Rack	0.00E+00		0.00E+00				0.00E+00	0.00E+00	3.28E-02
79	TLO 20	TLO-20 Asphalt/Pitch Truck Loading Rack	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.25E-02
80	TRLO 9F	Molten Sulfur Railcar Loading	0.00E+00		0.00E+00				0.00E+00	0.00E+00	4.34E-02
81	T 0049	Slop Oil Tank			0.00E+00				0.00E+00	0.00E+00	3.88E-01
82	T 0059	T-0059, Light Cycle Oil (LCO) tank	0.00E+00					0.00E+00	0.00E+00	0.00E+00	1.82E-05
83	T 0061	Light Cycle Oil (LCO) fixed roof tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	2.78E-05
84	T 0063	Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	3.61E-04
85	T 0065	Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00	0.00E+00					0.00E+00	0.00E+00	1.59E-02
86	T 0075	Heavy Cycle Oil (HCO)fixed roof tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.59E-02
87	T 0081	Asphalt/Pitch Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	
88	T 0082	Asphalt/Pitch Tank	0.00E+00	0.00E+00					0.00E+00	0.00E+00	6.24E-02
89	T 0110	Asphalt/Pitch Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.57E-03
90	T 0400	Gas Oil fixed roof tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.91E-02
91	T 0402	T-0402 Light Cat Naphtha tank	0.00E+00	0.00E+00					0.00E+00	0.00E+00	4.52E-04
92	T 0410	Asphalt/Pitch Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	2.68E-02
93	T 0411	T-0411 Gasolines & Gasoline Blendstocks	0.00E+00	0.00E+00	0.00E+00			0.00E+00	0.00E+00	0.00E+00	2.66E-05
94	T_0411	No. 2 Fuel Oil (Diesel) fixed roof tank	0.00E+00		0.00E+00			0.00E+00	0.00E+00	0.00E+00	1.79E-03
95	T 0420	Asphalt/Pitch Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	3.42E-03
96	T_0420	Light Cycle Oil (LCO) fixed roof tank	0.00E+00		0.00E+00			0.00E+00	0.00E+00	0.00E+00	1.59E-04
97	T 0423	Light Cycle Oil (LCO) fixed roof tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.89E-04
98	T 0431	Fuel Oil fixed roof tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.04E-02
99	T 0432	Fuel Oil fixed roof tank	0.00E+00		0.00E+00			0.00E+00	0.00E+00	0.00E+00	9.04E-03
100	T 0433	Straight Run Gas Oil fixed roof tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	2.48E-04
101	T 0434	Straight Run Diesel fixed roof tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	2.72E-02
102	T 0914	Slop Oil Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	0.00E+00
103	T 1227	Asphalt/Pitch Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	2.34E-02
104	T 0106	T-0106 Sour Water Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	2.48E-02
105	T 0435	T-0435 Sour Water Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	4.63E-03
106	T 0437	T-0437 Crude Oil Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.02E-03
107	T 0438	Straight Run Gas Oil fixed roof tank	0.00E+00	0.00E+00				0.00E+00	0.00E+00	0.00E+00	4.92E-03
108	T 0439	T-0439 Sour Naphtha Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	2.10E-03
109	T_0450	T-0450 Sour Naphtha Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.74E-03
110	T 0451	T-0451 Straight Run Diesel tank	0.00E+00	0.00E+00	0.00E+00			0.00E+00	0.00E+00	0.00E+00	1.55E-04
111	T 0737	T-0737 Sour Water Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	2.05E-02
112	T 0802	T-0802 Sour Water Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.04E-02
113	T 0814	Asphalt/Pitch Tank	0.00E+00	0.00E+00				0.00E+00	0.00E+00	0.00E+00	1.19E-02
114	T 0815	No. 2 Fuel Oil (Diesel) tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	2.72E-02
115	T 0821	Light Cat Naphtha tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	4.87E-04
116	T 0830	T-0830 Slop Oil Tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	0.00E+00
117	T 0834	Straight Run Diesel tank			0.00E+00				0.00E+00	0.00E+00	1.03E-03
118	T 0835	Straight Run Diesel tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	1.79E-03
119	T_0838	No. 2 Fuel Oil (Diesel) tank	0.00E+00		0.00E+00				0.00E+00	0.00E+00	7.40E-03
120	T 1225	T-1225 Crude Oil Tank			0.00E+00					0.00E+00	1.57E-03

HollyFrontier - Volume Sources (H2S and Toxics Only)

yi iondei - VO	lume Sources (H2S	and Toxido Only)		
Model				
Source	Source			
No.	ID	Source Description	H2SO4	NH3
73	TLO_1	TLO-1 Asphalt Truck Loading Rack	0.00E+00	0.00E+00
74	TL_2	TL-2 Asphalt Truck Loading Rack #2	0.00E+00	0.00E+00
75	TL_4	TL-4 Fuels Truck Loading Rack e, f	0.00E+00	0.00E+00
76	TL_7	TL-7 CBO/LCO Truck Loading Rack	0.00E+00	0.00E+00
77	RLO_8	RLO-8 Railcar Loading Rack	0.00E+00	0.00E+00
78	RLO_19	RLO-19 Railcar Loading Rack	0.00E+00	0.00E+00
79	TLO_20	TLO-20 Asphalt/Pitch Truck Loading Rack	0.00E+00	0.00E+00
80	TRLO_9F	Molten Sulfur Railcar Loading	0.00E+00	0.00E+00
81	T_0049	Slop Oil Tank	0.00E+00	0.00E+00
82	T_0059	T-0059, Light Cycle Oil (LCO) tank	0.00E+00	0.00E+00
83	T_0061	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	0.00E+00
84	T_0063	Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00	0.00E+00
85	T_0065	Heavy Cycle Oil (HCO) fixed roof tank	0.00E+00	0.00E+00
86	T_0075	Heavy Cycle Oil (HCO)fixed roof tank	0.00E+00	0.00E+00
87	T_0081	Asphalt/Pitch Tank	0.00E+00	0.00E+00
88	T 0082	Asphalt/Pitch Tank	0.00E+00	0.00E+00
89	T_0110	Asphalt/Pitch Tank	0.00E+00	0.00E+00
90	T 0400	Gas Oil fixed roof tank	0.00E+00	0.00E+00
91	T 0402	T-0402 Light Cat Naphtha tank	0.00E+00	0.00E+00
92	T 0410	Asphalt/Pitch Tank	0.00E+00	0.00E+00
93	T 0411	T-0411 Gasolines & Gasoline Blendstocks	0.00E+00	0.00E+00
94	T 0419	No. 2 Fuel Oil (Diesel) fixed roof tank	0.00E+00	0.00E+00
95	T 0420	Asphalt/Pitch Tank	0.00E+00	0.00E+00
96	T 0422	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	0.00E+00
97	T 0423	Light Cycle Oil (LCO) fixed roof tank	0.00E+00	0.00E+00
98	T 0431	Fuel Oil fixed roof tank	0.00E+00	0.00E+00
99	T 0432	Fuel Oil fixed roof tank	0.00E+00	0.00E+00
100	T 0433	Straight Run Gas Oil fixed roof tank	0.00E+00	0.00E+00
101	T_0433	Straight Run Diesel fixed roof tank	0.00E+00	0.00E+00
102	_	Slop Oil Tank	0.00E+00	0.00E+00
103	T_0914 T_1227	Asphalt/Pitch Tank		
104	_	T-0106 Sour Water Tank	0.00E+00	0.00E+00
	T_0106		0.00E+00	0.00E+00
105	T_0435	T-0435 Sour Water Tank	0.00E+00	0.00E+00
106	T_0437	T-0437 Crude Oil Tank	0.00E+00	0.00E+00
107	T_0438	Straight Run Gas Oil fixed roof tank	0.00E+00	0.00E+00
108	T_0439	T-0439 Sour Naphtha Tank	0.00E+00	0.00E+00
109	T_0450	T-0450 Sour Naphtha Tank	0.00E+00	0.00E+00
110	T_0451	T-0451 Straight Run Diesel tank	0.00E+00	0.00E+00
111	T_0737	T-0737 Sour Water Tank	0.00E+00	0.00E+00
112	T_0802	T-0802 Sour Water Tank	0.00E+00	0.00E+00
113	T_0814	Asphalt/Pitch Tank	0.00E+00	0.00E+00
114	T_0815	No. 2 Fuel Oil (Diesel) tank	0.00E+00	0.00E+00
115	T_0821	Light Cat Naphtha tank	0.00E+00	0.00E+00
116	T_0830	T-0830 Slop Oil Tank	0.00E+00	0.00E+00
117	T_0834	Straight Run Diesel tank	0.00E+00	0.00E+00
118	T_0835	Straight Run Diesel tank	0.00E+00	0.00E+00
119	T_0838	No. 2 Fuel Oil (Diesel) tank	0.00E+00	0.00E+00
120	T_1225	T-1225 Crude Oil Tank	0.00E+00	0.00E+00

HollyFrontier Off-Site Point Source NAAQS/NMAAQS Input Data (Updated 7-12-21)

													Potenti	al to Emit (lb/hr)			
	Stack				Base	- · ·			Stack									
	Release			Northing (Y)	Elevation	Stack		Exit Velocity										
Source ID	Type	Source Description	(m)	(m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT	СО	H2S
352E1	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556292.63	3637097.65	3373.8	80.0	400	50.98	1.12	0.798	0.798	0.798					1.395	
352E2	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556300.17	3637104.67	3373.6	35.0	110	45.21	1.51	1.587	1.587	1.587						
352E4	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556285.79	3637106.13	3373.9	35.0	110	45.21	1.51	1.587	1.587	1.587						!
402E3	DEFAULT	Holly Frontier Asphalt Company	556992.61	3637197.56	3359.9	15.0	500	29.89	1.51	6.508	6.508	6.508					7.937	!
402E6	DEFAULT	Holly Frontier Asphalt Company	557000.15	3637204.58	3359.9	25.0	285	7.19	1.51	0.906	0.906	0.906					9.524	!
402E8	DEFAULT	Holly Frontier Asphalt Company	557000.15	3637204.58	3359.9	25.0	500	29.89	1.51								3.080	
402E7	DEFAULT	Holly Frontier Asphalt Company	556981.53	3637199.14	3360.1	25.0	285	7.19	1.51								7.143	
402E9	DEFAULT	Holly Frontier Asphalt Company	556983.18	3637190.99	3360.0	25.0	500	29.89	1.51								3.080	!
203R2	DEFAULT	DCP - Shadow Booster Station	557393.94	3622548.16	3367.7	23.0	854	91.86	0.98									0.363
191E64	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569332.26	3626710.82	3554.0	54.5	1150	19.88	3.51									3.987
191R15	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569339.80	3626717.84	3555.0	115.0	1832	65.58	28.44									3.443
191R16	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569333.01	3626721.39	3554.8	115.0	1832	65.58	28.44									8.154
191R17	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569325.42	3626719.30	3554.1	115.0	1832	65.58	28.44									8.154
191R18	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569321.18	3626712.40	3553.4	115.0	1832	65.58	28.44									0.725
191R19	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569322.83	3626704.25	3553.2	115.0	1832	65.58	28.44									0.363
191R20	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569329.78	3626699.28	3553.3	115.0	1832	65.58	28.44									16.308
211E25	DEFAULT	Lucid Artesia - Dagger Draw Gas Plant	551931.36	3619797.52	3472.0	200.0	1832	65.62	9.81									223.020
39270R3	DEFAULT	Lucid Artesia - North Pen Compressor Station	551454.28	3619910.64	3477.6	23.0	854	91.86	0.98									2.537
199E38	DEFAULT	Artesia Gas Plant	574000.18	3624399.74	3609.0	70.6	1832	65.62	68.26									26.455
31815E15	DEFAULT	Frontier - Coyote Compressor Station	578708.30	3628257.94	3668.9	23.0	854	91.86	0.98									1.825
39714E8	DEFAULT	Spur - Shelby 23 Tank Battery	551738.94	3611091.61	3409.5	35.0	1832	65.62	8.64									6.197
39714E9	DEFAULT	Spur - Shelby 23 Tank Battery	551746.48	3611098.63	3409.0	30.0	1832	65.62	8.64									6.197
39003E5	DEFAULT	Spur Energy - Ross Ranch Battery	548838.12	3611188.93	3472.3	35.0	1832	65.62	29.75									13.391

Rest of sources provided by NMAQB are located in excess of 10km from refinery. Not included in NAQS/MMAQS model.

All sources within 25km and large (1,000lb/hr) emitters within 50km were evaluated for inclusion in the H2S NMAQS analysis.

PM10, PM2.5 and SO2 sources located beyond 10km were excluded. There are no SO2 sources located within 10km of the refinery.

No cummulative NAAQS/NMAAQS modeling conducted for pollutants other than PM10, PM25, H2S and SO2 as the nearby source contribution is reflected in the background concentration.

HollyFrontier Off-Site Source NAAQS/NMAAQS Volume Source Input Data (Updated 5-5-21)

											Potentia	al to Emit (II	b/hr)			
Source ID	Source Description	Easting (X) (m)	Northing (Y) (m)	Base Elevation (ft)		Sigma Y (ft)	Sigma Z (ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT	со	H2S
3403E2	Schlumberger - Artesia District Bulk Facility	556719.31	3635718.50	3362.8	3.3	1.54	3.05	2.38	2.381	2.381						
3403R1	Schlumberger - Artesia District Bulk Facility	556726.85	3635725.52	3362.7	3.3	1.54	3.05	0.72	0.725	0.725						
359@1	Southeast Readi-Mix - Artesia Plant	557117.00	3635667.03	3356.9	32.8	721.78	30.51	16.27	4.08	4.081						ļ
352E3	Land O' Lakes Purina Feed - Artesia Feed Mill	556293.38	3637108.22	3373.8	20.0	1.54	3.05	0.79	0.794	0.794						ļ
402R2	Holly Frontier Asphalt Company	556993.36	3637208.13	3360.0	32.8	32.81	30.51	6.51	6.508	6.508						
402R3	Holly Frontier Asphalt Company	556985.77	3637206.04	3360.1	32.8	32.81	30.51	6.50	6.505	6.505						
402R6	Holly Frontier Asphalt Company	556981.53	3637199.14	3360.1	32.8	32.81	30.51	6.35	6.349	6.349						ļ
30254@1	Par Five Energy LLC - Par Five Energy	564319.69	3632835.00	3342.9	3.3	1.54	3.05	2.38	2.381	2.381						ļ
30254R1	Par Five Energy LLC - Par Five Energy	564327.22	3632842.02	3343.0	32.8	32.81	30.51	5.56	5.556	5.556						
28959E1	Lime Rock - Condor 7 Battery	563709.45	3625436.95	3287.2	17.0	1.54	3.05									0.544
26441E1	Lime Rock - Atoka San Andreas Unit Battery	561619.20	3623917.88	3302.5	3.3	1.54	3.05									0.363
26441E2	Lime Rock - Atoka San Andreas Unit Battery	561626.73	3623924.91	3302.4	3.3	1.54	3.05									0.363
26441E3	Lime Rock - Atoka San Andreas Unit Battery	561619.95	3623928.46	3302.4	3.3	1.54	3.05									0.363
203R1	DCP - Shadow Booster Station	557400.73	3622544.60	3367.6	3.3	1.54	3.05									0.317
29063R1	Chesapeake Operating Inc - Hondo Federal Gas	568814.07	3629620.53	3468.8	3.3	1.54	3.05									4.762
39270E3	Lucid Artesia - North Pen Compressor Station	551465.37	3619909.06	3477.3	3.3	1.54	3.05									7.143
39270E4	Lucid Artesia - North Pen Compressor Station	551472.91	3619916.08	3477.1	3.3	1.54	3.05									7.143
39270R1	Lucid Artesia - North Pen Compressor Station	551466.12	3619919.63	3477.1	3.3	1.54	3.05									0.238
39270R2	Lucid Artesia - North Pen Compressor Station	551458.53	3619917.54	3477.3	3.3	1.54	3.05									1.825
199R2	Artesia Gas Plant	574007.71	3624406.77	3608.9	3.3	1.54	3.05									0.000
199R3	Artesia Gas Plant	574000.93	3624410.32	3609.0	3.3	1.54	3.05									0.000
31815R1	Frontier - Coyote Compressor Station	578715.83	3628264.96	3668.9	3.3	1.54	3.05									3.571
31815R3	Frontier - Coyote Compressor Station	578709.05	3628268.51	3668.9	3.3	1.54	3.05									18.120
39714R1	Spur - Shelby 23 Tank Battery	551739.69	3611102.18	3408.9	3.3	1.54	3.05									0.159

Note: The volume sources at the Artesia Gas Plant (Source IDs. 199R2 and 199R3 represent emissions from the acid gas flare. These emissions were therefore modeles as a flare (Source ID 199E38).

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

,		oint Source increment input Data (Updated 5-5-21)									Potenti	ial to Emit (l	b/hr)		
	Stack Release		Easting (X) Northing (Y)	Base Elevation	Stack		Exit Velocity	Stack Diameter							
Source IE		Source Description	(m) (m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC1	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556292.63 3637097.65	3373.8	80.0	400	51.0	1.1	0.798						
INC2	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556300.170 3637104.670		35.0	110	45.2	1.5	1.587						
INC3	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556285.790 3637106.130		35.0	110	45.2	1.5	1.587						
INC4 INC5	DEFAULT	Holly Frontier Asphalt Company	556992.610 3637197.560		15.0 25.0	500 285	29.9	1.5	6.508						
INC5	DEFAULT DEFAULT	Holly Frontier Asphalt Company DCP - Shadow Booster Station	557000.150 3637204.580 557393.190 3622537.580		25.0 15.0	285 1125	7.2 118.2	1.5 0.1	0.906 1.746						
INC6	DEFAULT	DCP - Shadow Booster Station	557400.730 3622544.600		42.5	780	136.0	0.1	1.746						
INC8	DEFAULT	Chesapeake Operating Inc - Hondo Federal Gas	568814.070 3629620.530		6.0	860	53.3	0.8	0.794						
INC9	DEFAULT	DCP - Pecos Diamond Gas Plant	568071.310 3625977.910	3541.9	50.0	600	105.0	1.0	1.587						
INC10	DEFAULT	DCP - Pecos Diamond Gas Plant	568061.290 3625977.950		40.0	600	105.1	1.0	1.587						
INC11	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569341.200 3626597.800		27.0	670	200.0	1.3	-2.356						
INC12 INC13	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		27.0	670 670	200.0 200.0	1.3	-3.080						
INC13	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760 569351.590 3626398.760		40.0 31.1	730	200.0 181.0	1.3 1.5	-11.905 -2.537						
INC14 INC15	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		35.0	955	200.0	1.6	-3.443						
INC16	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		36.0	759	170.0	1.4	-3.262						
INC17	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		40.0	759	160.0	1.5	-3.806						
INC18	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		21.0	600	34.0	2.0	-0.127						
INC19	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760		33.0	925	200.0	1.6	-1.449						
INC20	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569336.770 3626723.010		54.5	1150	19.9	3.5	0.159						
INC21	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569327.130 3626723.090		54.5	1150	27.7	3.5	0.037						
INC22	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569319.870 3626716.420		120.0	600 600	17.2 17.2	6.2 6.2	4.762						
INC23 INC24	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant	569319.090 3626706.380 571606.690 3638669.910		120.0 15.0	1125	118.2	1.2	4.762 1.812						
INC24 INC25	DEFAULT	DCP - Carbon Valley Booster DCP - Carbon Valley Booster	571614.220 3638676.940		15.0	1125	118.2	1.2	1.812						
INC26	DEFAULT	DCP - Carbon Valley Booster	571599.840 3638678.400		15.0	1125	118.2	1.2	1.812						
INC27	DEFAULT	Lucid Artesia - North Pen Compressor Station	552193.100 3619498.130		21.0	869	152.3	1.0	0.556						
INC28	DEFAULT	Lucid Artesia - North Pen Compressor Station	552193.100 3619498.130		21.0	869	152.3	1.0	0.556						
INC29	DEFAULT	EOG - Rumble State No4	547037.570 3620834.180		15.0	600	3.8	1.0	0.018						
INC30	DEFAULT	EOG - Rumble State No5	547018.950 3620828.740		15.0	832	171.6	1.0	0.794						
INC31	DEFAULT	EOG - Rumble State No6	547020.600 3620820.590		15.0	832	171.6	1.0	0.794						
INC32 INC33	DEFAULT	EOG - Lacama 20 State Com 602H	545079.800 3621969.940		15.0	1131 931	30.0 192.9	0.7 0.7	0.159						
INC33	DEFAULT DEFAULT	EOG - Lacama 20 State Com 602H EOG - Lacama 20 State Com 602H	545073.020 3621973.500 545065.420 3621971.400		15.0 15.0	832	192.9 349.9	0.7	0.397 0.794						
INC35	DEFAULT	EOG - Lacama 20 State Com 602H	545061.180 3621964.500		15.0	1255	161.9	0.7	0.952						
INC36	DEFAULT	Yates Petroleum - Pierre State No1 Facility	570982.950 3620931.670		23.0	854	91.9	1.0	0.037						
INC37	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		40.3	1340	89.2	1.0	1.957						
INC38	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	40.3	1340	89.2	1.0	0.979						
INC39	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		44.7	750	21.2	3.0	2.175						
INC40	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	-0.544						
INC41	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	1.957						
INC42	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	1.957						
INC43	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	1.957						
INC44	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2 91.9	1.0	0.979						
INC45 INC46	DEFAULT DEFAULT	Artesia Gas Plant Artesia Gas Plant	574011.520 3624405.460		62.3 62.3	-460 -460	91.9	15.1	3.175						
INC46 INC47	DEFAULT	Artesia Gas Plant Artesia Gas Plant	574004.680 3624411.940 573990.740 3624597.900		40.3	-460 1340	91.9 89.2	15.1 1.0	2.857 0.979						
INC47 INC48	DEFAULT	Artesia Gas Plant Artesia Gas Plant	573990.740 3624597.900		46.0	1125	89.2 147.9	1.0	1.268						
INC49	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	0.979						
INC50	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	0.979						
INC51	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	46.0	1340	89.2	1.0	1.957						
INC52	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		46.0	1340	89.2	1.0	1.957						
INC53	DEFAULT	Frontier - Coyote Compressor Station	578708.300 3628257.940		16.0	1500	0.1	2.8	0.018						
INC54	DEFAULT	Frontier - Coyote Compressor Station	578715.830 3628264.960		20.0	990	142.0	1.1	0.794						
INC55	DEFAULT	Frontier - Coyote Compressor Station	578709.050 3628268.510		22.0	600	18.0	0.8	0.317						
INC56	DEFAULT	Frontier - Coyote Compressor Station	578701.450 3628266.420		20.0	990	142.0	1.1	0.794						
INC57 INC58	DEFAULT DEFAULT	Frontier - Coyote Compressor Station Shelby 23 Tank Battery	578697.210 3628259.520 551738.940 3611091.610		23.0 25.0	873 250	128.0 21.6	0.9 0.7	0.794 0.079						
INC58	DEFAULT	Shelby 23 Tank Battery Shelby 23 Tank Battery	551746.480 3611098.630		25.0 25.0	250 250	21.6	0.7	0.079						
INC60	DEFAULT	Shelby 23 Tank Battery	551739.690 3611102.180		25.0	250	21.6	0.7	0.079						
INC61	DEFAULT	Shelby 23 Tank Battery	551732.090 3611100.090		25.0	250	21.6	0.7	0.079						
INC62	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556292.630 3637097.650		79.987	399.992	50.984	1.115		0.798	0.798				
INC63	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556300.170 3637104.670	3373.6	35.007	109.994	45.210	1.509		1.587	1.587				

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

		oint Source increment input Data (Opdated 5-5-21)									Potenti	ial to Emit (I	b/hr)		
	Stack Release		Easting (X) Northing (Y)	Base Elevation	Stack		Exit Velocity	Stack Diameter							
Source IE		Source Description	(m) (m)		Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC64	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill	556285.790 3637106.130	3373.9	35.007	109.994	45.210	1.509		1.587	1.587				
INC65	DEFAULT	Holly Frontier Asphalt Company	556992.610 3637197.560	3359.9	14.993	500.000	29.888	1.509		6.508	6.508				
INC66 INC67	DEFAULT DEFAULT	Holly Frontier Asphalt Company DCP - Shadow Booster Station	557000.150 3637204.580 557393.190 3622537.580	3359.9 3367.9	25.000 14.993	285.008 1124.996	7.185 118.209	1.509 0.098		0.906 1.746	0.906 1.746				
INC67	DEFAULT	DCP - Shadow Booster Station	557400.730 3622544.600	3367.6	42.487	780.008	135.991	0.096		1.740	1.746				
INC69	DEFAULT	DCP - Pecos Diamond Gas Plant	568071.310 3625977.910	3541.9	50.000	600.008	104.987	0.984		1.587	1.587				
INC70	DEFAULT	DCP - Pecos Diamond Gas Plant	568061.290 3625977.950	3540.7	39.993	600.008	105.085	0.984		1.587	1.587				
INC71	DEFAULT	Durango Midatragas - Empire Abo Gas Plant	569341.200 3626597.800	3548.5 3534.7	27.001	669.992	200.000	1.280		-2.356	-2.356				
INC72 INC73	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760 569351.590 3626398.760	3534.7 3534.7	27.001 39.993	669.992 669.992	200.000 200.000	1.280 1.280		-3.080 -11.905	-3.080 -11.905				
INC74	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7	37.992	719.996	185.007	1.280		-2.718	-2.718				
INC75	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7	31.102	730.004	181.004	1.476		-2.537	-2.537				
INC76	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7	35.991	759.002	170.013	1.444		-3.262	-3.262				
INC77 INC78	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760 569351.590 3626398.760	3534.7 3534.7	39.993 20.997	759.002 600.008	160.007 33.990	1.509 1.969		-3.806 -0.127	-3.806 -0.127				
INC79	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7	33.005	924.998	200.000	1.608		-1.449	-1.449				
INC80	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569336.770 3626723.010	3555.2	54.495	1149.998	19.882	3.510		0.159	0.159				
INC81	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569327.130 3626723.090	3554.4	54.495	1149.998	27.690	3.510		0.037	0.037				
INC82 INC83	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569319.870 3626716.420 569319.090 3626706.380	3553.4 3553.0	120.013 120.013	600.008 600.008	17.192 17.192	6.168 6.168		4.762 4.762	4.762 4.762				
INC83	DEFAULT	Lucid Artesia - North Pen Compressor Station	552193.100 3619498.130	3473.5	20.997	869.000	152.297	0.168		0.556	0.556				
INC85	DEFAULT	Lucid Artesia - North Pen Compressor Station	552193.100 3619498.130	3473.5	20.997	869.000	152.297	0.984		0.556	0.556				
INC86	DEFAULT	EOG - Rumble State No4	547037.570 3620834.180	3568.8	14.993	600.008	3.806	0.984		0.018	0.018				
INC87	DEFAULT	EOG - Rumble State No5	547018.950 3620828.740	3569.5	14.993	831.992	171.588	0.984		0.794	0.794				
INC88	DEFAULT	EOG - Rumble State No6	547020.600 3620820.590	3569.5	14.993	831.992	171.588	0.984		0.794	0.794				
INC89 INC90	DEFAULT DEFAULT	EOG - Lacama 20 State Com 602H EOG - Lacama 20 State Com 602H	545079.800 3621969.940 545073.020 3621973.500	3613.0 3613.1	14.993 14.993	1131.008 930.992	30.020 192.946	0.689 0.689		0.159 0.397	0.159 0.397				
INC91	DEFAULT	EOG - Lacama 20 State Com 602H	545065.420 3621971.400	3613.7	14.993	831.992	349.934	0.689		0.794	0.794				
INC92	DEFAULT	EOG - Lacama 20 State Com 602H	545061.180 3621964.500	3614.7	14.993	1254.992	161.877	0.689		0.952	0.952				
INC93	DEFAULT	Artesia Gas Plant	574011.520 3624405.460	3608.9	62.336	-459.670	91.864	15.092		3.175	3.175				
INC94	DEFAULT	Artesia Gas Plant	574004.680 3624411.940	3609.1	62.336	-459.670	91.864	15.092		2.857	2.857				
INC95 INC96	DEFAULT DEFAULT	Artesia Gas Plant Frontier - Coyote Compressor Station	573990.740 3624597.900 578708.300 3628257.940	3613.9 3668.9	45.997 16.010	1124.996 1500.008	147.900 0.098	0.984 2.756		2.537 0.018	2.537 0.018				
INC97	DEFAULT	Frontier - Coyote Compressor Station	578715.830 3628264.960	3668.9	20.013	989.996	141.995	1.148		0.794	0.794				
INC98	DEFAULT	Frontier - Coyote Compressor Station	578709.050 3628268.510	3668.9	22.014	600.008	18.012	0.820		0.317	0.317				
INC99	DEFAULT	Frontier - Coyote Compressor Station	578701.450 3628266.420	3668.9	20.013	989.996	141.995	1.148		0.794	0.794				
INC100 INC101	DEFAULT DEFAULT	Frontier - Coyote Compressor Station Shelby 23 Tank Battery	578697.210 3628259.520 551738.940 3611091.610	3668.9 3409.5	22.999 25.000	872.996 249.998	127.986 21.621	0.919 0.656		0.794 0.079	0.794 0.079				
INC101	DEFAULT	Shelby 23 Tank Battery	551746.480 3611098.630	3409.0	25.000	249.998	21.621	0.656		0.079	0.079				
INC103	DEFAULT	Shelby 23 Tank Battery	551739.690 3611102.180	3408.9	25.000	249.998	21.621	0.656		0.079	0.079				
INC104	DEFAULT	Shelby 23 Tank Battery	551732.090 3611100.090	3409.2	25.000	249.998	21.621	0.656		0.079	0.079				
INC105	DEFAULT	Lime Rock - Malco B Battery	563966.960 3627073.850	3441.4	25.000	1831.730	65.617	68.261						5.556	5.556
INC106 INC107	DEFAULT DEFAULT	Lime Rock -Kaiser B Battery Lime Rock -Kaiser B Battery	563767.890 3625655.950 563775.430 3625662.970	3319.3 3320.9	25.000 22.014	1831.730 100.004	65.617 18.012	68.261 0.492						3.968 34.128	3.968 34.128
INC107	DEFAULT	Lime Rock - West Red Lake Battery	564130.550 3625904.740	3422.4	22.014	100.004	18.012	0.492						11.053	11.053
INC109	DEFAULT	Lime Rock - West Red Lake Battery	564138.090 3625911.760	3422.6	22.014	100.004	18.012	0.492						11.053	11.053
INC110	DEFAULT	Lime Rock - West Red Lake Battery	564131.300 3625915.310	3421.9	22.014	100.004	18.012	0.492						11.053	11.053
INC111	DEFAULT	Lime Rock - Atoka San Andreas Unit Battery	561626.730 3623924.910	3302.4	22.014	100.004	18.012	0.492						15.873	15.873
INC112 INC113	DEFAULT DEFAULT	DCP - Shadow Booster Station DCP - Shadow Booster Station	557400.730 3622544.600 557393.940 3622548.160	3367.6 3367.7	14.993 42.487	1124.996 780.008	118.209 135.991	0.098 0.131						2.302 2.302	2.302 2.302
INC113	DEFAULT	Lime Rock - Hawk 8 Battery	565542.390 3624866.860	3444.5	22.014	1831.730	65.617	68.261						3.968	3.968
INC115	DEFAULT	Lime Rock - Hondo Federal Battery	567428.660 3626819.640	3582.9	22.014	1831.730	65.617	68.261						2.718	2.718
INC116	DEFAULT	EOG - War Dog State No1H	569708.850 3637607.080	3427.3	60.007	1831.730	65.617	1.673						14.445	14.445
INC117	DEFAULT	Lime Rock - Hawk 9 Battery	566922.460 3624722.080	3519.9	22.014	100.004	18.012	0.492						11.053	11.053
INC118 INC119	DEFAULT DEFAULT	Lime Rock - Hawk 9 Battery Lime Rock - Falcon 3 Battery	566930.000 3624729.100 568831.750 3627075.620	3520.3 3578.3	22.014 22.014	100.004 100.004	18.012 18.012	0.492 0.492						11.053 10.318	11.053 10.318
INC119	DEFAULT	Lime Rock - Falcon 3 Battery	568839.280 3627073.020	3578.6	22.014	100.004	18.012	0.492						10.318	10.318
INC121	DEFAULT	Lime Rock - Eagle 35 Sat Battery	569992.810 3628438.870	3589.9	25.000	1831.730	65.617	68.261						2.356	2.356
INC122	DEFAULT	Lime Rock - Eagle 35 Sat Battery	570000.350 3628445.890	3589.6	22.014	100.004	18.012	0.492						11.905	11.905
INC123 INC124	DEFAULT DEFAULT	Lime Rock - Eagle 35 Sat Battery	569993.560 3628449.440 569351.590 3626398.760	3589.0 3534.7	22.014 114.993	100.004 1831.730	18.012 65.617	0.492 68.261						11.905 0.079	11.905 0.079
INC 124 INC 125	DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant	569351.590 3626398.760	3534.7 3534.7	114.993	1831.730	65.617	68.261						0.079	0.079
INC126	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569333.010 3626721.390	3554.8	54.495	1149.998	19.882	3.510						378.578	378.578
INC127	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569325.420 3626719.300	3554.1	54.495	1149.998	27.690	3.510						0.079	0.079
INC128	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569321.180 3626712.400	3553.4	120.013	600.008	17.192	6.168						8.730	8.730

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

		nt Source Increment Input Data (Updated 5-5-21)			_						Poten	tial to Emit (lb/hr)		
	Stack Release		Fasting (X)	Northing (Y)	Base Elevation	Stack		Exit Velocity	Stack Diameter						
Source ID		Source Description	(m)	(m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC129	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569322.830	3626704.250	3553.2	120.013	600.008	17.192	6.168					8.730	8.730
INC130	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626699.280	3553.3	29.987	600.008	25.098	2.493					2.381	2.381
INC131	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626700.430	3553.8	114.993	1832.000 1832.000	65.584	28.445 28.445					118.143	118.143
INC132 INC133	DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626707.350 3626716.530	3554.6 3555.2	114.993 114.993	1832.000	65.584 65.584	28.445					9.060 9.060	9.060 9.060
INC133	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626723.010	3555.2	114.993	1832.000	65.584	28.445					68.857	68.857
INC135	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626723.090	3554.4	114.993	1832.000	65.584	28.445					26.093	26.093
INC136	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626716.420	3553.4	114.993	1832.000	65.584	28.445					18.120	18.120
INC137	DEFAULT	Lucid Artesia - Dagger Draw Gas Plant		3619797.520	3472.0	200.000	1831.730	65.617	9.810					22333.709	
INC138 INC139	DEFAULT DEFAULT	Lucid Artesia - North Pen Compressor Station Lucid Artesia - North Pen Compressor Station		3619498.130 3619498.130	3473.5 3473.5	20.997 20.997	869.000 869.000	152.297 152.297	0.984 0.984					0.079 0.079	0.079 0.079
INC139	DEFAULT	Lucid Artesia - North Pen Compressor Station		3619919.630	3477.1	22.966	854.330	91.864	0.984					94.225	94.225
INC141	DEFAULT	EOG - Rumble State No5		3620827.160	3569.2	25.000	1831.730	65.617	68.261					0.476	0.476
INC142	DEFAULT	EOG - Rumble State No5		3620837.730	3569.0	14.993	831.992	171.588	0.984					0.397	0.397
INC143	DEFAULT	EOG - Rumble State No6		3620835.640	3569.4	14.993	831.992	171.588	0.984					0.397	0.397
INC144	DEFAULT	EOG - Lacama 20 State Com 602H		3621962.920	3614.3	14.993	1131.008	30.020	0.689					0.079	0.079
INC145 INC146	DEFAULT DEFAULT	EOG - Lacama 20 State Com 602H EOG - Lacama 20 State Com 602H		3621969.940 3621973.500	3613.0 3613.1	14.993 14.993	930.992 831.992	192.946 349.934	0.689 0.689					0.238 3.968	0.238 3.968
INC 140	DEFAULT	EOG - Lacama 20 State Com 602H		3621971.400	3613.7	14.993	1254.992	161.877	0.689					0.238	0.238
INC148	DEFAULT	Chalk Compressor Station		3621748.040	3460.6	22.014	465.008	49.803	1.115					34.048	34.048
INC149	DEFAULT	Artesia Gas Plant		3624597.900	3613.9	44.685	750.002	21.194	2.986					0.326	0.326
INC150	DEFAULT	Artesia Gas Plant		3624406.770	3608.9	70.604	1831.730	65.617	68.261					0.159	0.159
INC151	DEFAULT	Artesia Gas Plant		3624410.320	3609.0	70.604	1831.730	65.617	68.261					0.079	0.079
INC152	DEFAULT	Artesia Gas Plant		3624597.900	3613.9	45.997	1124.996	147.900	0.984					1.812	1.812
INC153 INC154	DEFAULT DEFAULT	EOG - Badboy CTB		3613604.540	3454.8 3454.6	60.007	1831.730	65.617	1.673					2.381 2.381	2.381
INC 154 INC 155	DEFAULT	EOG - Badboy CTB Frontier - Coyote Compressor Station		3613611.560 3628257.940	3668.9	60.007 16.010	1831.730 1500.008	65.617 0.098	1.673 2.756					1.508	2.381 1.508
INC156	DEFAULT	Frontier - Coyote Compressor Station		3628264.960	3668.9	20.013	989.996	141.995	1.148					0.079	0.079
INC157	DEFAULT	Frontier - Coyote Compressor Station		3628268.510	3668.9	22.014	600.008	18.012	0.820					0.159	0.159
INC158	DEFAULT	Frontier - Coyote Compressor Station	578701.450	3628266.420	3668.9	20.013	989.996	141.995	1.148					0.079	0.079
INC159	DEFAULT	Frontier - Coyote Compressor Station		3628259.520	3668.9	22.999	872.996	127.986	0.919					0.079	0.079
INC160	DEFAULT	Spur - Shelby 23 Tank Battery		3611091.610	3409.5	35.007	1831.730	65.617	8.635					8.390	8.390
INC161 INC162	DEFAULT DEFAULT	Spur - Shelby 23 Tank Battery EOG- Falcata Battery		3611098.630	3409.0 3695.3	29.987 14.993	1831.730 1131.008	65.617	8.635 0.689					8.390 0.079	8.390
INC 162	DEFAULT	EOG- Falcata Battery		3616360.840 3576089.170	3002.3	14.993	930.992	29.987 192.946	0.689					0.079	0.079 0.238
INC164	DEFAULT	EOG- Falcata Battery		3616371.420	3696.4	14.993	831.992	349.934	0.689					0.397	0.397
INC165	DEFAULT	EOG- Falcata Battery	540682.320	3616369.320	3695.0	14.993	600.008	161.877	0.689					0.238	0.238
INC166	DEFAULT	EOG- Falcata Battery		3616362.420	3693.9	14.993	600.008	17.848	0.689					0.079	0.079
INC167	DEFAULT	Spur Energy - Ross Ranch Battery		3611188.930	3472.3	35.007	1831.730	65.617	29.754					25.873	25.873
INC168	DEFAULT	Land O' Lakes Purina Feed - Artesia Feed Mill		3637097.650	3373.8	79.987	399.992	50.984	1.115			6.667	6.667		
INC169 INC170	DEFAULT DEFAULT	Holly Frontier Asphalt Company Holly Frontier Asphalt Company		3637197.560 3637208.130	3359.9 3360.0	14.993 25.000	500.000 285.008	29.888 7.185	1.509 1.509			9.524 11.111	9.524 11.111		
INC170	DEFAULT	Holly Frontier Asphalt Company		3637206.040	3360.0	25.000	285.008	7.185	1.509			7.937	7.937		
INC172	DEFAULT	Holly Frontier Asphalt Company		3637199.140	3360.1	25.000	500.000	29.888	1.509			3.624	3.624		
INC173	DEFAULT	Holly Frontier Asphalt Company	556983.180	3637190.990	3360.0	25.000	500.000	29.888	1.509			3.624	3.624		
INC174	DEFAULT	Lady Luck No1 Facility		3638398.310	3413.2	14.993	489.992	22.014	0.984			22.223	22.223		
INC175	DEFAULT	Lady Luck No1 Facility		3638405.330	3413.5	22.966	854.330	91.864	0.984			0.794	0.794		
INC176	DEFAULT	Atoka Dehydration Facility		3624129.050	3309.6	22.966	854.330	91.864	0.984			1.812	1.812		
INC177 INC178	DEFAULT DEFAULT	Lime Rock - Atoka San Andreas Unit Battery Lucky Lobo ASX #2 Facility		3623917.880 3639898.520	3302.5 3484.5	22.014 14.993	100.004 469.994	18.012 21.490	0.492 0.984			0.363 44.445	0.363 44.445		
INC178	DEFAULT	DCP - Shadow Booster Station		3622544.600	3367.6	14.993	1124.996	118.209	0.984			32.302	32.302		
INC180	DEFAULT	DCP - Shadow Booster Station		3622548.160	3367.7	42.487	780.008	135.991	0.131			86.906	86.906		
INC181	DEFAULT	Chesapeake Operating Inc - Hondo Federal Gas	568814.070	3629620.530	3468.8	6.004	860.000	53.314	0.787			18.254	18.254		
INC182	DEFAULT	EOG - War Dog State No1H		3637607.080	3427.3	60.007	1831.730	65.617	1.673			1.429	1.429		
INC183	DEFAULT	DCP - Pecos Booster Station		3623798.120	3405.4	14.009	1000.004	47.014	0.656			53.969	53.969		
INC184	DEFAULT	DCP - Pecos Booster Station		3623798.120	3405.4	14.009	1000.004	47.014	0.656			53.969	53.969		
INC185 INC186	DEFAULT DEFAULT	DCP - Pecos Booster Station DCP - Pecos Diamond Gas Plant		3623798.120 3625977.910	3405.4 3541.9	14.009 50.000	1000.004 600.008	47.014 104.987	0.656 0.984			53.969 118.256	53.969 118.256		
INC 186	DEFAULT	DCP - Pecos Diamond Gas Plant DCP - Pecos Diamond Gas Plant		3625977.910	3541.9	39.993	600.008	104.987	0.984			116.669	116.669		
INC188	DEFAULT	DCP - Pecos Diamond Gas Plant		3625987.940	3546.4	20.013	800.006	6.988	1.509			2.381	2.381		
INC189	DEFAULT	DCP - Pecos Diamond Gas Plant		3626095.860	3539.0	20.013	600.008	8.990	0.492			1.631	1.631		
INC190	DEFAULT	Lucid Artesia - Southern Union Compressor Station		3631625.290	3507.3	22.966	854.330	91.864	0.984			0.794	0.794		
INC191	DEFAULT	Lucid Artesia - Southern Union Compressor Station		3631620.330	3507.0	23.589	1011.992	135.007	1.247			15.080	15.080		
INC192	DEFAULT	Lucid Artesia - Southern Union Compressor Station		3631621.470	3506.1	23.589	1011.992	135.007	1.247			15.080	15.080		
INC193	DEFAULT	Durango Midstream - Empire Abo Gas Plant	569351.590	3626398.760	3534.7	27.001	669.992	200.000	1.280			-117.419	-117.419		ı

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

7101191 101		nt Source Increment Input Data (Updated 5-5-21)									Potenti	al to Emit (lb/hr)		
	Stack Release		Easting (X)	Northing (Y)	Base Elevation	Stack		Exit Velocity	Stack Diameter						
Source IE		Source Description	(m)	(m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC194	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	39.993	669.992	200.000	1.280			-103.466	-103.466		
INC195	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	37.992	719.996	185.007	1.280			-331.056	-331.056		
INC196 INC197	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626398.760 3626398.760	3534.7 3534.7	31.102 22.966	730.004 854.330	181.004 91.864	1.476 0.984			-357.512 -105.478	-357.512 -105.478		
INC 197	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	955.004	200.000	1.575			-444.850	-444.850		
INC199	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.991	759.002	170.013	1.444			-215.630	-215.630		
INC200	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	39.993	759.002	160.007	1.509			-329.244	-329.244		
INC201 INC202	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7 3554.4	29.987 31.004	1085.000 899.996	100.000	0.656 1.969			-8.879 -0.725	-8.879 -0.725		
INC202 INC203	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626723.090 3626398.760	3534.4	20.997	600.008	12.992 33.990	1.969			-0.725 -1.812	-0.725 -1.812		
INC204	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	33.005	924.998	200.000	1.608			-143.512	-143.512		
INC205	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	24.016	687.992	100.000	0.656			-5.436	-5.436		
INC206	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	26.411	861.998	187.106	0.853			-39.286	-39.286		
INC207 INC208	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626398.760 3626398.760	3534.7 3534.7	26.411 114.993	861.998 1831.730	187.106 65.617	0.853 68.261			-59.525 0.714	-59.525 0.714		
INC200	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	114.993	1831.730	65.617	68.261			0.714	0.714		
INC210	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	854.006	162.008	0.984			34.818	34.818		
INC211	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	854.006	162.008	0.984			30.223	30.223		
INC212 INC213	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7 3552.8	35.007 54.495	854.006 1149.998	162.008 19.882	0.984 3.510			32.744	32.744		
INC213 INC214	DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626699.000 3626693.930	3553.1	35.007	854.006	162.008	0.984			1.587 33.351	1.587 33.351		
INC215	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	854.006	162.008	0.984			34.921	34.921		
INC216	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626709.080	3555.0	54.495	1149.998	27.690	3.510			0.397	0.397		
INC217	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	854.006	162.008	0.984			34.921	34.921		
INC218	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626398.760	3534.7	35.007	989.996	184.908	0.984			23.810	23.810		
INC219 INC220	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626398.760 3626715.280	3534.7 3552.9	35.007 120.013	989.996 600.008	184.908 17.192	0.984 6.168			23.810 61.112	23.810 61.112		
INC221	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626701.560	3552.6	120.013	600.008	17.192	6.168			61.112	61.112		
INC222	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626692.450	3552.8	120.013	600.008	13.911	2.493			7.937	7.937		
INC223	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626693.070	3553.5	29.987	600.008	25.098	2.493			14.286	14.286		
INC224	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626703.390	3554.8	114.993 114.993	1832.000	65.584	28.445			37.509	37.509		
INC225 INC226	DEFAULT DEFAULT	Durango Midstream - Empire Abo Gas Plant Durango Midstream - Empire Abo Gas Plant		3626718.070 3626729.250	3555.6 3556.0	114.993	1832.000 1832.000	65.584 65.584	28.445 28.445			9.060 9.060	9.060 9.060		
INC227	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626730.710	3554.9	114.993	1832.000	65.584	28.445			2.537	2.537		
INC228	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626721.380	3553.1	114.993	1832.000	65.584	28.445			1.812	1.812		
INC229	DEFAULT	Durango Midstream - Empire Abo Gas Plant		3626706.030	3552.3	114.993	1832.000	65.584	28.445			18.120	18.120		
INC230 INC231	DEFAULT DEFAULT	Lucid Artesia - Four Dinkus Compressor Station GCP4 Lucid Artesia - Four Dinkus Compressor Station GCP5		3625305.660 3625305.660	3622.6 3622.6	20.013 20.013	860.000 860.000	60.499 60.499	0.984 0.984			20.635 20.635	20.635 20.635		
INC231	DEFAULT	DCP - Carbon Valley Booster		3638669.910	3469.5	50.000	1831.730	65.617	68.261			521.437	521.437		
INC233	DEFAULT	DCP - Carbon Valley Booster		3638676.940	3468.6	14.993	1124.996	118.209	1.247			18.254	18.254		
INC234	DEFAULT	DCP - Carbon Valley Booster	571607.440	3638680.490	3468.3	14.993	1124.996	118.209	1.247			18.254	18.254		
INC235	DEFAULT	DCP - Carbon Valley Booster		3638671.500	3469.6	14.993	1124.996	118.209	1.247			18.254	18.254		
INC236 INC237	DEFAULT DEFAULT	DCP - Carbon Valley Booster DCP - Carbon Valley Booster		3619797.520 3619458.070	3472.0 3476.6	14.993 18.406	1831.730 350.006	65.617 4.298	68.261 0.984			0.000 -118.126	0.000 -118.126		
INC237	DEFAULT	DCP - Carbon Valley Booster		3620198.100	3465.0	60.007	600.008	20.013	2.001			11.905	11.905		
INC239	DEFAULT	DCP - Carbon Valley Booster		3619806.000	3471.9	10.007	219.992	100.000	0.492			2.381	2.381		
INC240	DEFAULT	Lucid Artesia - North Pen Compressor Station		3619909.060	3477.3	20.013	1831.730	65.617	68.261			0.079	0.079		
INC241	DEFAULT	Lucid Artesia - North Pen Compressor Station		3619498.130	3473.5	20.997	869.000	152.297	0.984			44.445	44.445		
INC242 INC243	DEFAULT DEFAULT	Lucid Artesia - North Pen Compressor Station		3619498.130 3619917.540	3473.5 3477.3	20.997 22.966	869.000 854.330	152.297 91.864	0.984 0.984			44.445 2.356	44.445 2.356		
INC243	DEFAULT	Lucid Artesia - North Pen Compressor Station Carbon Valley 14 Fed Com No2		3643077.800	3585.2	10.499	1045.004	1.706	2.395			26.191	26.191		
INC245	DEFAULT	EOG - Rumble State No5		3620827.160	3569.2	25.000	1831.730	65.617	68.261			0.079	0.079		
INC246	DEFAULT	EOG - Rumble State No5		3620834.180	3568.8	25.000	1831.730	65.617	68.261			1.746	1.746		
INC247	DEFAULT	EOG - Rumble State No4		3620837.730	3569.0	14.993	600.008	3.806	0.984			0.238	0.238		
INC248 INC249	DEFAULT DEFAULT	EOG - Rumble State No5 EOG - Rumble State No6		3620820.590 3620815.620	3569.5 3569.2	14.993 14.993	831.992 831.992	171.588 171.588	0.984 0.984			12.064 12.064	12.064 12.064		
INC249 INC250	DEFAULT	EOG - Rumble State Noo EOG - Lacama 20 State Com 602H		3621962.920	3614.3	25.000	1831.730	65.617	68.261			0.079	0.079		
INC251	DEFAULT	EOG - Lacama 20 State Com 602H		3621969.940	3613.0	25.000	1831.730	65.617	68.261			3.016	3.016		
INC252	DEFAULT	EOG - Lacama 20 State Com 602H	545073.020	3621973.500	3613.1	14.993	1131.008	30.020	0.689			1.270	1.270		
INC253	DEFAULT	EOG - Lacama 20 State Com 602H		3621971.400	3613.7	14.993	930.992	192.946	0.689			6.032	6.032		
INC254 INC255	DEFAULT DEFAULT	EOG - Lacama 20 State Com 602H EOG - Lacama 20 State Com 602H		3621964.500 3621956.350	3614.7 3615.7	14.993 14.993	831.992 1254.992	349.934 161.877	0.689 0.689			12.064 13.334	12.064 13.334		
INC255	DEFAULT	Atoka No1 Compressor Station		3627167.900	3665.9	16.601	1099.994	131.004	0.656			21.429	21.429		
INC257	DEFAULT	Atoka No1 Compressor Station		3627167.900	3665.9	50.000	1200.002	102.986	0.656			17.461	17.461		
INC258	DEFAULT	Atoka No1 Compressor Station	572460.800	3627167.900	3665.9	50.000	1200.002	102.986	0.656			17.461	17.461		

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

		ont Source increment input Data (Opuated 3-3-21)								Potenti	al to Emit (b/hr)		
	Stack			Base				Stack						
Source ID	Release Type	Source Description	Easting (X) Northing (Y) (m) (m)	Elevation (ft)	Stack Height (ft)	Temp (F)	Exit Velocity (ft/sec)	Diameter (ft)	PM10	PM25 ST PM25 LT	NO2 ST	NO2 LT	SO2_ST	SO2 LT
INC259	DEFAULT	Atoka No1 Compressor Station	572460.800 3627167.900		60.007	1025.006	81.004	0.984	1 141 10	1 M25_51 1 M25_E1	38.096	38.096	002_01	002_L1
INC259	DEFAULT	Atoka No1 Compressor Station	572460.800 3627167.900		50.007	1200.002	102.986	0.964			17.461	17.461		
INC261	DEFAULT	Illinois Camp Booster Station	574661.630 3627054.860		35.007	1340.006	57.415	0.656			39.683	39.683		
INC262	DEFAULT	Illinois Camp Booster Station	574634.650 3627054.880	3659.7	35.007	1340.006	57.415	0.656			39.683	39.683		
INC263	DEFAULT	Illinois Camp Booster Station	574643.640 3627054.830		35.007	1340.006	57.415	0.656			39.683	39.683		
INC264	DEFAULT	Illinois Camp Booster Station	574652.630 3627054.900		35.007	1340.006	57.415	0.656			39.683	39.683		
INC265 INC266	DEFAULT DEFAULT	Chalk Compressor Station Cimarex Enegy - Montana 1 Fee 3	569361.150 3621748.040 551935.760 3616514.870		22.014 10.007	465.008 887.000	49.803 358.301	1.115 0.492			12.540 11.349	12.540 11.349		
INC260	DEFAULT	Kristina Booster Station	572690.330 3624526.200		20.013	780.008	366.010	0.492			69.842	69.842		
INC268	DEFAULT	Mack - Mark Twain Federal Com Battery	575824.070 3636427.600		6.988	224.996	381.988	6.988			3.968	3.968		
INC269	DEFAULT	Dickens 29 Federal Battery	575704.960 3639831.920		6.988	224.996	381.988	6.988			3.968	3.968		
INC270	DEFAULT	Oxy USA IncSpurck 16 State Com No2	576460.460 3633013.760		22.966	854.330	91.864	0.984			7.143	7.143		
INC271	DEFAULT	Yates Petroleum - Pierre State No1 Facility	570982.950 3620931.670		22.966	854.330	91.864	0.984			4.457	4.457		
INC272 INC273	DEFAULT DEFAULT	Shakespeare 20 Federal No1 Artesia Gas Plant	575701.430 3640657.870 573990.740 3624597.900		10.991 40.289	564.998 1340.006	32.251 89.206	0.492 0.984			3.262 41.584	3.262 41.584		
INC273	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		40.289	1340.006	89.206	0.984			42.064	42.064		
INC275	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		44.685	750.002	21.194	2.986			57.144	57.144		
INC276	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		58.005	800.006	60.991	0.984			-324.532	-324.532		
INC277	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	58.005	800.006	60.991	0.984			-302.788	-302.788		
INC278	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		58.005	800.006	60.991	0.984			-241.179	-241.179		
INC279	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		58.990	800.006	54.987	0.984			-311.304	-311.304		
INC280 INC281	DEFAULT DEFAULT	Artesia Gas Plant Artesia Gas Plant	573990.740 3624597.900 573990.740 3624597.900		41.010 43.996	1000.004 986.000	49.016 58.005	0.984 0.984			-132.821 -140.613	-132.821 -140.613		
INC281	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		43.990	986.000	58.005	0.984			-164.658	-164.658		
INC283	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			-36.240	-36.240		
INC284	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			28.196	28.196		
INC285	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			84.128	84.128		
INC286	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			84.128	84.128		
INC287	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		75.000	1832.000	65.584	1.673			-17.690	-17.690		
INC288	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		42.290	750.002	21.194	3.609			57.144	57.144		
INC289 INC290	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		41.995 41.995	899.996	60.007	0.820 0.984			-5.056	-5.056		
INC290 INC291	DEFAULT DEFAULT	Artesia Gas Plant Artesia Gas Plant	573990.740 3624597.900 573999.690 3624382.850		70.604	854.996 1831.730	162.992 65.617	68.261			37.076 1.667	37.076 1.667		
INC291	DEFAULT	Artesia Gas Plant	574011.530 3624386.830		70.604	1831.730	65.617	68.261			0.714	0.714		
INC293	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		33.104	629.996	20.801	3.609			2.381	2.381		
INC294	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	45.997	1340.006	89.206	0.984			42.064	42.064		
INC295	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		41.995	854.996	162.992	0.984			35.772	35.772		
INC296	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		41.995	854.996	162.992	0.984			32.394	32.394		
INC297	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		41.995	854.996	162.992	0.984			39.637	39.637		
INC298 INC299	DEFAULT DEFAULT	Artesia Gas Plant Artesia Gas Plant	573990.740 3624597.900 573990.740 3624597.900		40.289 41.995	1340.006 854.996	89.206 162.992	0.984 0.984			41.584 34.604	41.584 34.604		
INC299	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1124.996	147.900	0.984			68.255	68.255		
INC301	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			42.064	42.064		
INC302	DEFAULT	Artesia Gas Plant	573990.740 3624597.900	3613.9	45.997	1340.006	89.206	0.984			42.064	42.064		
INC303	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			84.128	84.128		
INC304	DEFAULT	Artesia Gas Plant	573990.740 3624597.900		45.997	1340.006	89.206	0.984			84.128	84.128		
INC305	DEFAULT	Yates - Eastern Shores QW No1 Facility	565479.650 3615436.960		9.843	571.010	49.213	0.328			33.096	33.096		
INC306 INC307	DEFAULT DEFAULT	EOG - Secretariat 3 Fed Com No501H Frontier - Coyote Compressor Station	569284.850 3617086.880 578708.300 3628257.940		60.007 16.010	1831.730 1500.008	65.617 0.098	1.673 2.756			9.048 0.238	9.048 0.238		
INC307	DEFAULT	Frontier - Coyote Compressor Station Frontier - Coyote Compressor Station	578715.830 3628264.960		20.013	989.996	141.995	2.756 1.148			17.866	17.866		
INC309	DEFAULT	Frontier - Coyote Compressor Station	578701.450 3628266.420		22.014	600.008	18.012	0.820			0.079	0.079		
INC310	DEFAULT	Frontier - Coyote Compressor Station	578697.210 3628259.520		20.013	989.996	141.995	1.148			24.127	24.127		
INC311	DEFAULT	Frontier - Coyote Compressor Station	578698.860 3628251.370		22.999	872.996	127.986	0.919			46.906	46.906		
INC312	DEFAULT	Parallel - Hagerman Plant GCP4-3380	562777.140 3657403.570		22.966	854.330	91.864	0.984			0.556	0.556		
INC313	DEFAULT	Parallel - Hagerman Plant GCP4-3381	562784.680 3657410.590		22.966	854.330	91.864	0.984			1.429	1.429		
INC314 INC315	DEFAULT DEFAULT	Parallel - Hagerman Plant GCP4-3382 Parallel - Hagerman Plant GCP4-3383	562777.890 3657414.140 562770.300 3657412.050		22.999 22.999	854.006 854.006	162.008 162.008	0.984 0.984			35.153 35.153	35.153 35.153		
INC315	DEFAULT	COG - Man State 2H Battery	574496.980 3618616.590		16.010	1831.730	65.617	2.592			9.524	9.524		
INC310	DEFAULT	COG - Man State 2H Battery	574504.510 3618623.610		12.008	1043.006	189.993	0.328			3.968	3.968		
INC318	DEFAULT	Shelby 23 Tank Battery	551738.940 3611091.610		25.000	249.998	21.621	0.656			0.714	0.714		
INC319	DEFAULT	Shelby 23 Tank Battery	551746.480 3611098.630	3409.0	25.000	249.998	21.621	0.656			0.714	0.714		
INC320	DEFAULT	Shelby 23 Tank Battery	551739.690 3611102.180		25.000	249.998	21.621	0.656			0.714	0.714		
INC321	DEFAULT	Shelby 23 Tank Battery	551732.090 3611100.090		25.000	249.998	21.621	0.656			0.714	0.714		
INC322	DEFAULT	Spur - Shelby 23 Tank Battery	551729.500 3611085.030		35.007	1831.730	65.617	8.635			4.048	4.048		
INC323	DEFAULT	Spur - Shelby 23 Tank Battery	551736.450 3611080.070	3410.2	29.987	1831.730	65.617	8.635			4.048	4.048		I

HollyFrontier Off-Site Point Source Increment Input Data (Updated 5-5-21)

									Potential to Emit (lb/hr)						
	Stack				Base				Stack						
	Release		Easting (X)	Northing (Y)	Elevation	Stack		Exit Velocity							
Source ID	Type	Source Description	(m)	(m)	(ft)	Height (ft)	Temp (F)	(ft/sec)	(ft)	PM10	PM25_ST PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC324	DEFAULT	EOG- Falcata Battery	540689.170	3616360.840	3695.3	14.993	1131.008	29.987	0.689			1.270	1.270		
INC325	DEFAULT	EOG- Falcata Battery	586879.330	3576089.170	3002.3	14.993	930.992	192.946	0.689			6.032	6.032		
INC326	DEFAULT	EOG- Falcata Battery	540689.920	3616371.420	3696.4	14.993	831.992	349.934	0.689			12.064	12.064		
INC327	DEFAULT	EOG- Falcata Battery	540682.320	3616369.320	3695.0	14.993	600.008	161.877	0.689			13.334	13.334		
INC328	DEFAULT	EOG- Falcata Battery	540678.080	3616362.420	3693.9	39.993	1831.730	65.617	8.635			5.079	5.079		
INC329	DEFAULT	EOG- Falcata Battery	540679.740	3616354.270	3693.4	39.993	1831.730	65.617	68.261			0.794	0.794		
INC330	DEFAULT	EOG- Falcata Battery	540686.680	3616349.310	3694.0	14.993	600.008	17.848	0.689			0.873	0.873		
INC331	DEFAULT	Winchester Compressor Station	567991.310	3612198.320	3519.7	39.993	960.998	41.010	1.214			33.334	33.334		
INC332	DEFAULT	Winchester Compressor Station	567991.310	3612198.320	3519.7	39.993	960.998	41.010	1.214			33.334	33.334		
INC333	DEFAULT	Winchester Compressor Station	567991.310	3612198.320	3519.7	39.993	960.998	41.010	1.214			33.334	33.334		
INC334	DEFAULT	Spur Energy - Ross Ranch Battery	548845.660	3611195.950	3472.1	35.007	1831.730	65.617	29.754			89.208	89.208		

All sources within 25km and large (1,000lb/hr) emitters within 50km were included in the increment analysis.

HollyFrontier Off-Site Volume Source Increment Input Data (Updated 5-5-21)

,	m-Site Volume Source increment input Data (Opuater							Potential to Emit (lb/hr)						
		5	N . 41	Base	D.1									
Source ID	Source Description	Easting (X)	Northing (Y) (m)	(ft)		Sigma Y (ft)	Sigma 7 (ft)	PM10	PM25 ST	PM25 I T	NO2 ST	NO2_LT	SO2 ST	SO2 LT
INC335	Schlumberger - Artesia District Bulk Facility	556719.31	3635718.50	3362.8	3.28	1.54	3.05	2.38	FIMIZU_UI	FWIZ5_LT	NO2_31	NOZ_L1	302_31	302_L1
INC336	Schlumberger - Artesia District Bulk Facility	556726.85	3635725.52	3362.7	3.28	1.54	3.05	0.72						
INC337	Land O' Lakes Purina Feed - Artesia Feed Mill	556293.38	3637108.22	3373.8	20.01	1.54	3.05	0.72						
INC338	Holly Frontier Asphalt Company	556993.36	3637208.13	3360.0	32.81	32.81	30.51	6.51						
INC339	Holly Frontier Asphalt Company	556985.77	3637206.04	3360.1	32.81	32.81	30.51	6.50						
INC340	Holly Frontier Asphalt Company	556981.53	3637199.14	3360.1	32.81	32.81	30.51	6.35						
INC341	Par Five Energy LLC - Par Five Energy	564319.69	3632835.00	3342.9	3.28	1.54	3.05	2.38						
INC342	Par Five Energy LLC - Par Five Energy	564327.22	3632842.02	3343.0	32.81	32.81	30.51	5.56						
INC343	Helena Chemical Co - Artesia New Mexico	557950.20	3646037.75	3342.1	3.28	1.54	3.05	0.24						
INC344	Helena Chemical Co - Artesia New Mexico	557957.74	3646044.77	3341.9	3.28	1.54	3.05	0.56						
INC345	Helena Chemical Co - Artesia New Mexico	557950.95	3646048.32	3341.9	3.28	1.54	3.05	2.38						
INC346	Helena Chemical Co - Artesia New Mexico	557943.36	3646046.23	3342.0	3.28	1.54	3.05	0.24						
INC347	Helena Chemical Co - Artesia New Mexico	557939.12	3646039.33	3342.2	3.28	1.54	3.05	0.16						
INC348	Helena Chemical Co - Artesia New Mexico	557940.77	3646031.17	3342.2	3.28	1.54	3.05	0.48						
INC349	EOG - Rumble State No4	547030.03	3620827.16	3569.2	32.81	32.81	30.51	4.52						
INC350	EOG - Rumble State No5	547030.78	3620837.73	3569.0	14.99	1.54	3.05	80.0						
INC351	EOG - Rumble State No6	547023.19	3620835.64	3569.4	14.99	1.54	3.05	0.04						
INC352	EOG - Lacama 20 State Com 602H	545072.27	3621962.92	3614.3	32.81	32.81	30.51	4.92						
INC353	EOG - Lacama 20 State Com 602H	545062.83	3621956.35	3615.7	14.99	1.54	3.05	80.0						
INC354	Shelby 23 Tank Battery	551727.85	3611093.19	3409.7	25.00	1.54	3.05	0.08						
INC355	EOG- Falcata Battery	540689.17	3616360.84	3695.3	3.28	1.54	3.05	3.65						
INC356	Spur Energy - Ross Ranch Battery	548838.12	3611188.93	3472.3	25.00	1.54	3.05	0.04						
INC357	Spur Energy - Ross Ranch Battery	548845.66	3611195.95	3472.1	25.00	1.54	3.05	0.04						
INC358	Spur Energy - Ross Ranch Battery	548838.87	3611199.51	3472.7	25.00	1.54	3.05	0.04						
INC359	Spur Energy - Ross Ranch Battery	548831.28	3611197.41	3473.0	25.00	1.54	3.05	0.04						
INC360	Schlumberger - Artesia District Bulk Facility	556719.31	3635718.50	3362.8	3.28	1.54	3.05		2.381	2.381				
INC361	Schlumberger - Artesia District Bulk Facility	556726.85	3635725.52	3362.7	3.28	1.54	3.05		0.725	0.725				
INC362	EOG - Rumble State No4	547030.03	3620827.16	3569.2	32.81	32.81	30.51		0.476	0.476				
INC363	EOG - Rumble State No5	547030.78	3620837.73	3569.0	14.99	1.54	3.05		0.079	0.079				
INC364	EOG - Rumble State No6	547023.19	3620835.64	3569.4	14.99	1.54	3.05		0.037	0.037				
INC365	EOG - Lacama 20 State Com 602H	545072.27	3621962.92	3614.3	32.81	32.81	30.51		0.476	0.476				
INC366	EOG - Lacama 20 State Com 602H	545062.83	3621956.35	3615.7	14.99	1.54	3.05		0.079	0.079				
INC367	COG - Man State 2H Battery	574496.98	3618616.59	3549.2	3.28	1.54	3.05		1.812	1.812				
INC368	Shelby 23 Tank Battery	551727.85	3611093.19	3409.7	25.00	1.54	3.05		0.079	0.079				
INC369	EOG- Falcata Battery	540689.17	3616360.84	3695.3	3.28	1.54	3.05		0.317	0.317				
INC370	Spur Energy - Ross Ranch Battery	548838.12		3472.3	25.00	1.54	3.05		0.037	0.037				
INC371	Spur Energy - Ross Ranch Battery	548845.66	3611195.95	3472.1	25.00	1.54	3.05		0.037	0.037				
INC372 INC373	Spur Energy - Ross Ranch Battery Spur Energy - Ross Ranch Battery	548838.87 548831.28	3611199.51 3611197.41	3472.7 3473.0	25.00 25.00	1.54 1.54	3.05 3.05		0.037 0.037	0.037 0.037				
INC374	Lime Rock - Malco B Battery	563974.50	3627080.87	3442.5	22.01	1.54	3.05		0.037	0.037			26.191	26.191
INC375	Lime Rock - Condor 7 Battery	563709.45	3625436.95	3287.2	22.01	1.54	3.05						3.968	3.968
INC376	Lime Rock - Condor 7 Battery	563716.98	3625443.97	3287.6	22.01	1.54	3.05						3.968	3.968
INC377	Ramirez & Sons Inc - Crusher No2	552788.48	3623752.45	3448.6	32.81	1410.76	30.51						181.202	181.202
INC378	Lime Rock - Condor Stirling Battery	563708.44	3625403.35	3286.5	22.01	1.54	3.05						6.349	6.349
INC379	Lime Rock - Condor Stirling Battery	563715.98	3625410.37	3286.7	22.01	1.54	3.05						6.349	6.349
INC380	Lime Rock - Condor Stirling Battery	563709.19	3625413.92	3286.7	22.01	1.54	3.05						10.318	10.318
INC381	Lime Rock - Hawk 8 Battery	565549.93	3624873.88	3444.8	22.01	1.54	3.05						18.254	18.254
INC382	Lime Rock - Hawk 8 Battery	565543.14	3624877.43	3444.7	20.01	1.54	3.05						18.254	18.254
INC383	Lime Rock - Hondo Federal Battery	567436.20	3626826.66	3582.7	22.01	1.54	3.05						13.492	13.492
INC384	Lime Rock - Hondo Federal Battery	567429.41	3626830.21	3582.7	22.01	1.54	3.05						13.492	13.492
INC385	EOG - Rumble State No4	547037.57	3620834.18	3568.8	14.99	1.54	3.05						0.079	0.079
INC386	Cimarex Enegy - Montana 1	551943.30	3616521.89	3422.5	3.28	1.54	3.05						10.000	10.000
INC387	Total Malfunction Construction	573989.09	3624401.33	3608.9	3.28	1.54	3.05						685.124	685.124
INC388	Total Malfunction Construction	573990.74	3624393.17	3608.6	3.28	1.54	3.05						18.120	18.120
INC389	Frontier - Coyote Compressor Station	578698.86	3628251.37	3668.9	3.28	1.54	3.05						18.120	18.120
INC390	Southeast Readi-Mix - Artesia Plant	557117.00	3635667.03	3356.9	32.81	721.78	30.51				172.142	172.142		
INC391	Ramirez & Sons Inc - Crusher No2	552788.48	3623752.45	3448.6	32.81	1410.76	30.51				344.284	344.284		
INC392	EOG - Rumble State No4	547023.19	3620835.64	3569.4	14.99	1.54	3.05				0.873	0.873		

HollyFrontier Off-Site Volume Source Increment Input Data (Updated 5-5-21)

								Potential to Emit (lb/hr)						
Source ID	Source Description	Easting (X) (m)	Northing (Y) (m)	Base Elevation (ft)		Sigma Y (ft)	Sigma Z (ft)	PM10	PM25_ST	PM25_LT	NO2_ST	NO2_LT	SO2_ST	SO2_LT
INC393	EOG - Rumble State No5	547018.95	3620828.74	3569.5	14.99	1.54	3.05				0.476	0.476		
INC394	EOG - Lacama 20 State Com 602H	545069.78	3621951.39	3615.9	14.99	1.54	3.05				0.873	0.873		
INC395	Artesia Gas Plant	573981.91	3624410.31	3609.4	3.28	1.54	3.05				17.939	17.939		
INC396	Artesia Gas Plant	573979.32	3624394.96	3608.8	3.28	1.54	3.05				18.120	18.120		
INC397	Frontier - Coyote Compressor Station	578705.81	3628246.40	3669.1	3.28	1.54	3.05				18.120	18.120		
INC398	Spur - Shelby 23 Tank Battery	551727.85	3611093.19	3409.7	25.00	1.54	3.05				0.476	0.476		
INC399	Spur Energy - Ross Ranch Battery	548838.12	3611188.93	3472.3	25.00	1.54	3.05				0.476	0.476		
INC400	Spur Energy - Ross Ranch Battery	548838.87	3611199.51	3472.7	25.00	1.54	3.05				0.476	0.476		
INC401	Spur Energy - Ross Ranch Battery	548831.28	3611197.41	3473.0	25.00	1.54	3.05				0.476	0.476		
INC402	Spur Energy - Ross Ranch Battery	548827.04	3611190.51	3472.9	25.00	1.54	3.05				0.476	0.476		
INC403	WPX - DD and EE Federal Leases	543610.96	3613500.45	3619.1	3.28	1.54	3.05				0.397	0.397		

HollyFrontier Navajo Volume Source Parameter Calculation

Source Dimensions									Initial Dispers	sion Coefficients	
									Initial		
					Square	Structure		Tank	Horizontal		
					Root of	Height/Vertical	Release	Diameter	Dimension s _Y	Initial Vertical	
Source ID	Source Description	Length (ft)	Width (ft)	Area (ft2)	Area (ft)	Dimension (ft)	Height (ft)	(ft)	(ft)	Dimension sz (ft)	Note
TRLO_9	Molten Sulfur Railcar Loading	10.0	10.0	100.00	10.00	15.00	15.00	NA	2.33	6.98	Elevated source on or adjacent to building
T_0049	Slop Oil Tank	NA	NA	94.99	9.75	36.00	36.00	11.00	2.27	16.74	Elevated source on or adjacent to building
T_0081	Asphalt/Pitch Tank	NA	NA	9241.22	96.13	40.00	40.00	108.50	22.36	18.60	Elevated source on or adjacent to building
T_0082	Asphalt/Pitch Tank	NA	NA	15386.00	124.04	40.00	40.00	140.00	28.85	18.60	Elevated source on or adjacent to building
T_0110	Asphalt/Pitch Tank	NA	NA	9156.24	95.69	35.00	35.00	108.00	22.25	16.28	Elevated source on or adjacent to building
T_0410	Asphalt/Pitch Tank	NA	NA	4899.19	69.99	40.00	40.00	79.00	16.28	18.60	Elevated source on or adjacent to building
T_0420	Asphalt/Pitch Tank	NA	NA	1962.50	44.30	30.00	30.00	50.00	10.30	13.95	Elevated source on or adjacent to building
T_0814	Asphalt/Pitch Tank	NA	NA	1962.50	44.30	32.00	32.00	50.00	10.30	14.88	Elevated source on or adjacent to building
T_0914	Slop Oil Tank	NA	NA	4415.63	66.45	40.00	40.00	75.00	15.45	18.60	Elevated source on or adjacent to building
T_1227	Asphalt/Pitch Tank	NA	NA	4654.27	68.22	40.00	40.00	77.00	15.87	18.60	Elevated source on or adjacent to building
T_0106	T-0106 Sour Water Tank	NA	NA	3523.87	59.36	40.00	40.00	67.00	13.81	18.60	Elevated source on or adjacent to building
T_0435	T-0435 Sour Water Tank	NA	NA	706.50	26.58	40.00	40.00	30.00	6.18	18.60	Elevated source on or adjacent to building
T_0437	T-0437 Crude Oil Tank	NA	NA	11304.00	106.32	40.00	40.00	120.00	24.73	18.60	Elevated source on or adjacent to building
T_0439	T-0439 Sour Naphtha Tank	NA	NA	13266.50	115.18	46.00	46.00	130.00	26.79	21.40	Elevated source on or adjacent to building
T_0450	T-0450 Sour Naphtha Tank	NA	NA	11304.00	106.32	40.00	40.00	120.00	24.73	18.60	Elevated source on or adjacent to building
T_0737	T-0737 Sour Water Tank	NA	NA	3115.67	55.82	40.00	40.00	63.00	12.98	18.60	Elevated source on or adjacent to building
T_0802	T-0802 Sour Water Tank	NA	NA	1589.63	39.87	40.00	40.00	45.00	9.27	18.60	Elevated source on or adjacent to building
T_0830	T-0830 Slop Oil Tank	NA	NA	15386.00	124.04	40.00	40.00	140.00	28.85	18.60	Elevated source on or adjacent to building
T_1225	T-1225 Crude Oil Tank	NA	NA	17662.50	132.90	40.00	40.00	150.00	30.91	18.60	Elevated source on or adjacent to building

NA - Not applicable.

Sigma Y values calculated as the square root of the area, or average length of side, divided by 4.3 (Table 3-1 of AERMOD Manual for Single Volume Source). Area for tanks calculated from diameter.

Sigma Z values for surface based sources calculated as the initial vertical dimension of source divided by 2.15 (Table 3-1 of AERMOD Manual for Elevated Source Not on or Adjacent to Building).

Sigma Z values for elevated sources on or adjacent to a building calculated as the building height divided by 2.15 (Table 3-1 of AERMOD Manual for Elevated Source on or Adjacent to Building).

Sigma Z values for elevated sources not on or adjacent to a building calculated as the initial vertical dimension of source divided by 4.3 (Table 3-1 of AERMOD Manual for Elevated Source Not on or Adjacent to Building).

Release height for tanks and railcar loading equal to top of tank/railcar as this is where emissions occur.

HollyFrontier Flare Stack Parameter Calculation

Source ID	Source Description	Effective Stack Height (ft)	Temp. (°F)	Exit Velocity (ft/sec)	Effective Stack Diameter (ft)	MMBtu/hr	cal/sec	Actual Stack Height (ft)
FL0400	FL-0400, North Plant Flare	395.1	1832	65.6	16.11	8440	5.91E+08	162.0
FL0401	FL-0401, South Plant Flare	342.2	1832	65.6	9.60	3000	2.10E+08	200.0
FL0402	FL-0402, FCC Flare	304.6	1832	65.6	9.28	2800	1.96E+08	167.0
FL0403	FL-0403, Alky Flare	499.1	1832	65.6	19.45	12300	8.61E+08	220.0
FL0404	FL-0404, GOHT Flare	568.5	1832	65.6	26.01	22000	1.54E+09	200.0
TL4VCU	TL-4 VCU	81.8	1832	65.6	3.92	500	3.50E+07	21.4
FLHEP	HEP Portable Flare	51.1	1832	65.6	2.29	170	1.19E+07	15.0
TVCU	Tank VCU	18.5	1832	65.6	0.20	1.26	8.82E+04	15.0

Per AERSCREEN Manual

2.1.2 *Flares*

Flare sources are denoted by the term "** FLARE DATA" in the input file in the line above the source parameters. Flare source inputs are, with English and metric units:

- emission rate (lb/hr or g/s)
- stack height (feet or meters)
- total heat release rate (cal/sec)
- radiative heat loss fraction

The heat loss fraction can be user selected or the SCREEN3 default value of 0.55. For information about heat loss fractions, see Leahey and Davies (1984). AERSCREEN will process

the flare in AERMOD as a POINT source type. For the exit velocity and exit temperature, AERSCREEN defaults these values to 20 m/s and 1,273 K, respectively as done in SCREEN3 (U.S. EPA, 1995). The stack diameter and effective stack height used in AERMOD are calculated from the inputs as:

$$D = 9.88 \times 10^{-4} \times \sqrt{HR \times (1 - HL)} \tag{1}$$

$$h_{eff} = H_s + 4.56 \times 10^{-3} \times HR^{0.478} \tag{2}$$

Where D is effective stack diameter, HR is the heat release rate, HL is the heat loss fraction, H_{eff} is effective stack height and H_s is the stack height entered by the user.

1 MMBtu (IT)/hour [MMBtu/h] = 69998.8225308643 calorie (IT)/second [cal/s] HL is assumed to be 0.55 per AERSCREEN Manual

Holly Frontier - Artesia CALPUFF Input

	Model	LCC East	LCC North	Stack Height	Base Elevation	Stack Diameter	Exit Velocity		Sigma Y	Sigma Z	Momentum	SO ₂	SO2LT	SO ₄	SO₄LT	NOx	РМС	EC	SOA
Model Source Description	Source ID	(km)	(km)	(m)	(m)	(m)	•	Temp. (K)	•	(m)	Flux	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)
Unit 13 Naphtha Splitter Reboiler	H0009	-691.753	-762.453	23.63	1025.42	1.37	5.46	549.82	0	0	1	0.183	0.000	0.091	0.000	0.540	0.084	0.021	0.000
Unit 06 HDS Reboiler	H0018	-691.742	-762.355	22.87	1025.08	1.22	5.95	644.26	0	0	1	0.425	0.000	0.212	0.000	1.515	0.115	0.029	0.000
South Crude Charge Heater	H0019	-691.733	-763.054	47.46	1027.53	1.33	6.52	505.37	0	0	1	0.000	0.000	0.000	0.000	0.620	0.067	0.017	0.050
Unit 21 Heater	H0028	-691.531	-763.081	15.34	1027.71	0.81	5.73	727.59	0	0	1	0.100	0.000	0.050	0.000	1.718	0.031	0.008	0.000
Unit 06 Charge Heater	H0030	-691.741	-762.349	20.43	1025.05	1.22	6.86	574.82	0	0	1	0.188	0.000	0.094	0.000	1.002	0.000	0.000	0.000
Unit 13 Charge Heater	H0040	-691.740	-762.343	30.79	1025.02	1.22	6.95	583.15	0	0	1	0.000	0.000	0.000	0.000	0.720	0.000	0.000	0.000
Unit 10 FCC Feed Heater	H0312	-691.612	-762.409	29.41	1025.54	1.22	6.22	630.37	0	0	1	0.969	0.178	0.484	0.089	3.350	0.230	0.057	0.000
Unit 70 Stabilizer Reboiler Heater	H0355	-691.566	-762.385	41.21	1025.62	0.76	8.75	500.93	0	0	1	0.000	0.000	0.000	0.000	0.970	0.012	0.003	0.009
Unit 70 CCR Heaters	H0362_64	-691.579	-762.359	62.65	1025.63	2.13	5.15	443.15	0	0	1	1.338	0.000	0.669	0.000	2.506	0.310	0.077	0.000
Unit 44 Charge Heater	H0421	-691.550	-762.448	24.90	1025.61	0.99	7.23	616.48	0	0	1	0.238	0.000	0.119	0.000	0.630	0.074	0.018	0.000
SRU Hot Oil Heater	H0464	-691.786	-762.522	24.33	1025.71	0.84	2.93	505.37	0	0	1	0.000	0.000	0.000	0.000	0.053	0.009	0.002	0.007
Unit 33 Charge Heater	H0601	-691.522	-762.511	39.94	1025.71	1.98	3.54	422.04	0	0	1	0.798	0.000	0.399	0.000	1.304	0.235	0.059	0.000
Unit 45 Charge Heater	H2421	-691.542	-762.518	26.52	1025.69	1.07	7.56	749.82	0	0	1	0.000	0.000	0.000	0.000	0.023	0.024	0.006	0.018
Unit 25 ROSE® Unit No. 2 Hot Oil Heater	H2501	-691.369	-762.607	51.22	1025.76	2.39	5.79	649.82	0	0	1	4.352	1.641	2.176	0.821	3.600	0.993	0.248	0.000
SRU3 Hot Oil Heater	H3101	-691.759	-762.560	24.39	1025.75	0.84	2.93	505.37	0	0	1	0.411	0.162	0.205	0.081	0.330	0.092	0.023	0.000
Unit 34 Hydrocracker Reboiler 1	H3402	-691.370	-762.596	20.43	1025.72	1.22	8.51	574.82	0	0	1	1.886	0.711	0.943	0.356	1.560	0.430	0.108	0.000
Unit 34 Hydrocracker Reactor Charge Heat	H3403	-691.383	-762.589	26.24	1025.73	1.22	5.91	647.04	0	0	1	1.160	0.438	0.580	0.219	0.960	0.265	0.066	0.000
Unit 63 Hydrogen Plant Reformer Furnaces	H8801_02	-691.407	-762.518	39.63	1025.62	1.17	22.99	588.71	0	0	1	0.000	0.000	0.000	0.000	4.458	0.364	0.091	0.273
Unit 64 Hydrogen Plant Reformer	H9851	-691.407	-762.487	53.66	1025.62	3.05	7.26	449.82	0	0	1	0.000	0.000	0.000	0.000	11.222	2.594	0.648	1.945
SRU2 Tail Gas Incinerator	H0473	-691.792	-762.491	45.73	1025.63	1.22	13.48	894.26	0	0	1	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
SRU3 Tail Gas Incinerator	H3103	-691.764	-762.577	45.73	1025.82	1.22	15.21	922.04	0	0	1	50.000	18.740	25.000	9.370	6.500	13.320	3.330	0.000
FL-0404, GOHT Flare	FL0404	-691.387	-762.233	173.33	1024.95	7.93	20.00	1273.15	0	0	1	39.833	2.458	19.917	1.229	11.156	0.000	0.000	0.000
Notes:												101.88	24.33	50.94	12.16	54.74	19.25	4.81	2.30

Notes:
LCC Origin: 40.0N, 97.0W, Standard (Matching) Parallels: 33.0N, 45.0N. Datum: NWS-84.
PMCoarse (PMC) = PM between 2.5 and 10 um in diameter.
EC = elemental carbon

SOA = secondary organic aerosols

PM speciation based upon NPS guidance for NG Combustion Turbines.

Consensus Gas-fired Turbine

Example of Consensus Approach where H2SO4 emissions are not provided by applicant Applicant's estimates are in ${\it BoLD}$.

	Heat Input	Filterable PM	(25% Estimate)	Condensible P	M (75% Estimate)	Total PM (A	pplicant)	SO2 (Applicant)			
Turbine	(mmBtu/hr)	(lb/mmBtu)	(lb/hr)	(lb/mmBtu)	(lb/hr)	(lb/mmBtu)	(lb/hr)	(gr/100scf)		(lb/hr)	
			0.00		0.00		0.00	2.0		0.00	

SO4	
(lb/hr)	
	0.00

SO2 (Applicant-33%)	
(lb/hr)	
0	0.00

Organic Carbon
(lb/hr)
0.00

Impact of Consensus Combined Cycle Turbine Example on Extinction

Total

Relative hext

		Extinction			Emissions	bext	
Туре	Name	Coef.	f(RH)*	Efficiency	(lb/hr)	1/Mm	
Filterable	EC	10		10	0.00	0.00	
Inorganic CPM	SOIL	1		1		0.00	
Inorganic CPM	SO4	3	2	6	0.00	0.00	* f(RH) will vary
Organic CPM	SOA	4		4	0.00	0.00	
<u>.</u>					0.00	0.00	•



ATTACHMENT B

Model Summary Results

Model	File	Pollutant	Average	Group	Rank	Conc/Dep		North (Y)	Elev	Hill Flag	Tim
AERMOD 21112	Artesia SIL_2020_CO.SUM	CO	1-HR	ALL	1ST	41.21148	556397.63	3634797.91	1025.65	1025.65	0
AERMOD 21112	Artesia SIL_2019_CO.SUM	CO	1-HR	ALL	1ST	41.05966	556390.61	3634800.06	1025.67	1025.67	0
AERMOD 21112	Artesia SIL_2017_CO.SUM	CO	1-HR	ALL	1ST	40.16028	556379.06	3634896.87	1025.9	1025.9	0
AERMOD 21112	Artesia SIL_2018_CO.SUM	CO	1-HR	ALL	1ST	40.14757	556381.95	3634872.66	1025.85	1025.85	0
AERMOD 21112	Artesia SIL_2016_CO.SUM	CO	1-HR	ALL	1ST	39.89154	556381.95	3634872.66	1025.85	1025.85	0
AERMOD 21112	Artesia SIL 2016 CO.SUM	CO	8-HR	ALL	1ST	25.414	556381.95	3634872.66	1025.85	1025.85	0
ERMOD 21112	Artesia SIL 2020 CO.SUM	CO	8-HR	ALL	1ST	24.41507	556384.84	3634848.46	1025.81	1025.81	0
ERMOD 21112	Artesia SIL 2017 CO.SUM	CO	8-HR	ALL	1ST	23.04333	556384.84	3634848.46	1025.81	1025.81	0
ERMOD 21112	Artesia SIL 2018 CO.SUM	CO	8-HR	ALL	1ST	22.1883	556384.84	3634848.46	1025.81	1025.81	0
AERMOD 21112	Artesia SIL 2019 CO.SUM	CO	8-HR	ALL	1ST	22.05946	556384.84	3634848.46	1025.81	1025.81	0
ERMOD 21112	Artesia SIL 2016 H2S.SUM	H2S	1-HR	ALL	1ST	24.44764	556500	3634100	1027.15	1027.15	0
	Artesia SIL 2018 H2S.SUM	H2S	1-HR	ALL	1ST	23.62346		3634006.44	1027.45	1027.45	0
	Artesia SIL 2019 H2S.SUM	H2S	1-HR	ALL	1ST	22.44775		3634006.44	1027.45	1027.45	ō
	Artesia SIL 2017 H2S.SUM	H2S	1-HR	ALL	1ST	21.22834		3634007.39	1027.52	1027.52	ō
	Artesia SIL 2020 H2S.SUM	H2S	1-HR	ALL	1ST	21.15178		3634006.44	1027.45	1027.45	0
	Artesia SIL 2016-2020 NO2 ST.SUM	NO2	1ST-HIGHEST MAX DAIL		1ST	35.14309		3634040.29	1027.2	1027.2	0.5 Y
	Artesia SIL 2018 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.62696		3635002.7	1026.13	1026.13	0 1 Y
	Artesia SIL 2019 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.40098		3635002.7	1026.13	1026.13	0 1 Y
	Artesia SIL 2017 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.33655		3635002.7	1026.13	1026.13	0 1 Y
	Artesia SIL 2020 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.25856		3635002.7	1026.13	1026.13	0 1 Y
	Artesia SIL 2016 NO2 LT.SUM	NO2	ANNUAL	ALL	1ST	2.09455		3635002.7	1026.13	1026.13	0 1 Y
ERMOD 21112	Artesia SIL 2020 PM10.SUM	PM10	24-HR	ALL	1ST	2.12842		3635000	1026.57	1026.57	0
	Artesia SIL 2018 PM10.SUM	PM10	24-HR	ALL	1ST	2.09536		3634896.87	1025.9	1025.9	Ö
	Artesia SIL 2016 PM10.SUM	PM10	24-HR	ALL	1ST	1.98536		3634969.47	1026.16	1026.16	Ö
	Artesia SIL 2017 PM10.SUM	PM10	24-HR	ALL	1ST	1.91596		3635000	1026.10	1026.57	0
	Artesia SIL 2019 PM10.SUM	PM10	24-HR	ALL	1ST	1.91181		3634900	1026.41	1026.41	0
	Artesia SIL 2018 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.6628		3634896.87	1025.9	1025.9	0 1 Y
ERMOD 21112	Artesia SIL 2019 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.65634		3634896.87	1025.9	1025.9	0 1 Y
AERMOD 21112	Artesia SIL 2020 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.6208		3634921.07	1026.01	1026.01	0 1 Y
	Artesia SIL 2017 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.60552		3634896.87	1025.9	1025.9	0 1 Y
	Artesia SIL 2016 PM10.SUM	PM10	ANNUAL	ALL	1ST	0.57825		3634896.87	1025.9	1025.9	0 1 Y
	Artesia SIL 2016_PM10.50M Artesia SIL 2016-2020 PM25 ST.SUM	PM10 PM25	1ST-HIGHEST 24-HR	ALL	1ST	1.92291		3634921.07	1025.9	1026.01	0 5 Y
	Artesia SIL 2016-2020 PM25 ST.SUM Artesia SIL 2016-2020 PM25 LT.SUM	PM25	ANNUAL	ALL	1ST	0.30288		3635129.2		1025.74	0 5 Y
	Artesia SIL 2019 SO2 ST.SUM	SO2	1-HR	ALL	1ST	26.06468		3634500	1025.74	1025.74	0 5 1
	Artesia SIL 2019_SO2_ST.SUM Artesia SIL 2020 SO2 ST.SUM	SO2	1-HR	ALL	1ST	25.45004		3634400	1026.17	1026.17	0
	Artesia SIL 2020_SO2_ST.SUM Artesia SIL 2017 SO2 ST.SUM	SO2	1-HR	ALL	1ST	25.26063		3634400	1026.36	1026.36	0
		SO2 SO2									0
	Artesia SIL_2016_SO2_ST.SUM		1-HR	ALL	1ST	25.05872		3634255.43	1026.77	1026.77	
	Artesia SIL_2018_SO2_ST.SUM	SO2	1-HR	ALL	1ST	24.60504		3634300	1026.78	1026.78	0
	Artesia SIL_2020_SO2_ST.SUM	SO2	24-HR	ALL	1ST	7.93385		3635000	1026.57	1026.57	0
	Artesia SIL_2018_SO2_ST.SUM	SO2	24-HR	ALL	1ST	7.77685		3634896.87	1025.9	1025.9	0
	Artesia SIL_2016_SO2_ST.SUM	SO2	24-HR	ALL	1ST	7.28096		3634921.07	1026.01	1026.01	0
	Artesia SIL_2019_SO2_ST.SUM	SO2	24-HR	ALL	1ST	7.0093		3635002.7	1026.13	1026.13	0
	Artesia SIL_2017_SO2_ST.SUM	SO2	24-HR	ALL	1ST	6.91898		3635000	1026.57	1026.57	0
	Artesia SIL_2019_SO2_ST.SUM	SO2	3-HR	ALL	1ST	22.27776		3634800.06	1025.67	1025.67	0
ERMOD 21112		SO2	3-HR	ALL	1ST	22.24497		3634700	1026.14	1026.14	0
	Artesia SIL_2020_SO2_ST.SUM	SO2	3-HR	ALL	1ST	22.17742		3634200	1027.1	1027.1	0
	Artesia SIL_2018_SO2_ST.SUM	SO2	3-HR	ALL	1ST	21.39588		3634300	1026.78	1026.78	0
LERMOD 21112	Artesia SIL_2016_SO2_ST.SUM	SO2	3-HR	ALL	1ST	21.31755	556400	3634200	1027.1	1027.1	0

1ST

ALL

ALL

	012818 Arte	sia 2016-2020	(RTP P	23	1	8341
0 190	011518 Arte	sia 2016-2020	(RTP P	23	1	8341
0 170	012302 Arte	sia 2016-2020	(RTP P	23	1	8341
0 18	111006 Arte	sia 2016-2020	(RTP P	23	1	8341
0 16	101103 Arte	sia 2016-2020	(RTP P	23	1	8341
0 160	051516 Arte	sia 2016-2020	(RTP P	23	1	8341
0 200	031516 Arte	sia 2016-2020	(RTP P	23	1	8341
0 170	092816 Arte	sia 2016-2020	(RTP P	23	1	8341
0 180	070524 Arte	sia 2016-2020	(RTP P	23	1	8341
0 190	021816 Arte	sia 2016-2020	(RTP P	23	1	8341
0 16	121303 Arte	s	,	54	1	8341
0 180	090722 Arte	s		54	1	8341
	111903 Arte			54	1	8341
	113021 Arte			54	1	8341
	122506 Arte			54	i	8341
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				18	1	8341
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		sia 2016-2020		18	1	8341
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0 5 YEAR	S Arte	sia 2016-2020	(RTP P	18	1	8341
0 190	041611 Arte	sia 2016-2020	(RTP P	14	1	8341
0 20	103111 Arte	sia 2016-2020	(RTP P	14	1	8341
0 170	031812 Arte	sia 2016-2020	(RTP P	14	1	8341
0 160	061309 Arte	sia 2016-2020	(RTP P	14	1	8341
0 18	103010 Arte	sia 2016-2020	(RTP P	14	1	8341
0 200	060624 Arte	sia 2016-2020	(RTP P	14	1	8341
0 180	073124 Arte	sia 2016-2020	(RTP P	14	1	8341
0 160	092224 Arte	sia 2016-2020	(RTP P	14	1	8341
0 190	072624 Arte	sia 2016-2020	(RTP P	14	1	8341
		sia 2016-2020		14	1	8341
		sia 2016-2020		14	1	8341
		sia 2016-2020		14	1	8341
		sia 2016-2020		14	1	8341
		sia 2016-2020		14	1	8341
-		sia 2016-2020		14	i	8341
0 1 YEAR		sia 2016-2020 sia 2016-2020		7	1	8341
0 1 YEARS		sia 2016-2020		7	1	8341
0 1 YEARS		sia 2016-2020		7	1	8341
0 1 YEAR		sia 2016-2020		7	1	8341
0 1 YEAR	s Arte	sia 2016-2020	KIPP	7	1	8341

Groups

8341

Sources

Met File

20012818 Artesia 2016-2020 (RTP P

ANNUAL

ANNUAL

ANNUAL

ANNUAL

ANNUAL

SO2

AERMOD 21112 Artesia SIL 2016 SO2 ST.SUM AERMOD 21112 Artesia SIL 2019 SO2 LT.SUM

AERMOD 21112 Artesia SIL_2018_SO2_LT.SUM

AERMOD 21112 Artesia SIL 2020 SO2 LT.SUM

AERMOD 21112 Artesia SIL_2017_SO2_LT.SUM

AERMOD 21112 Artesia SIL_2016_SO2_LT.SUM

				Conc.	Secondary PM2.5	Total Conc.			
Pollutant	Average	Group	Rank	(ug/m3)	Conc. (ug/m3)	(ug/m3)	SIL (ug/m3)	%SIL	Max Distance to SIL (km
PM25	ANNUAL	ALL	1ST	0.30	0.008	0.31	0.2	155%	0.76
PM25	1ST-HIGHEST 24-HR	ALL	1ST	1.92	0.310	2.23	1.2	186%	1.48
PM10	ANNUAL	ALL	1ST	0.66	NA	0.66	1.0	66%	NA
PM10	24-HR	ALL	1ST	2.13	NA	2.13	5.0	43%	NA
SO2	1-HR	ALL	1ST	26.06	NA	26.06	7.8	334%	10.7
SO2	24-HR	ALL	1ST	7.93	NA	7.93	5.0	159%	1.73
SO2	3-HR	ALL	1ST	22.28	NA	22.28	25.0	89%	NA
SO2	ANNUAL	ALL	1ST	0.74	NA	0.74	1.0	74%	NA
NO2	1ST-HIGHEST MAX DAILY	1-FALL	1ST	35.14	NA	35.14	7.5	467%	1.82
NO2	ANNUAL	ALL	1ST	2.63	NA	2.63	1.0	263%	1.07
со	1-HR	ALL	1ST	41.21	NA	41.21	2000.0	2%	NA
co	8-HR	ALL	1ST	25.41	NA	25.41	500.0	5%	NA
H2S	1-HR	ALL	1ST	24.45	NA	24.45	5.0	489%	1.44

0.74039

0.73197

0.70143

0.66959

0.6453

556300

556300

556379.06

556379.06

556381.95

3634900

3634900

3634896.87

3634896.87

3634872.66

1025.9

1026.41

1025.9

1025.85

1026.41

1025.9

1026.41

1025.85

1025.9

NA - not applicable

Maximum 5-yr 1-hr SO2 impact conservatively used in lieu of 5-yr average of maxima.

NO2 modeling included the ARM2 method to account for NOx to NO2 conversion. The default minimum and maximum NO2/NOx ratios of 0.5 and 0.9 were employed.

7-7-22 Holly	Frontier Artesia	NAAQS Model, Significance Gri	

Model	l	File	Pollutant	Average	Group	Rank	Conc/Dep	East (X)	North (Y)	Elev	Hill	Flag	Tin	ne	Met File	Sources	Groups	Recep	otors
AERM	MOD 21112	Artesia NAAQS_2019_H2S.SUM	H2S	1-HR	ALL	1ST	28.9420	6 556415.7	3634620.21	1025	.46 1	025.46	0	191	23017 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2018_H2S.SUM	H2S	1-HR	ALL	1ST	27.6680	8 556854.85	3634006.44	1027	.45 1	027.45	0	180	90722 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2016_H2S.SUM	H2S	1-HR	ALL	1ST	27.6565	5 556664.07	3634229.22	1026	.56 1	026.56	0	161	01007 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2017_H2S.SUM	H2S	1-HR	ALL	1ST	27.3427	4 556413.44	3634642.42	1025	.43 1	025.43	0	170	20308 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2020_H2S.SUM	H2S	1-HR	ALL	1ST	26.336	2 556664.07	3634229.22	1026	.56 1	026.56	0	200	71106 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2019_H2S.SUM	H2S	1-HR	HOLLY	1ST	28.8711	7 556415.7	3634620.21	1025	.46 1	025.46	0	191	23017 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2018_H2S.SUM	H2S	1-HR	HOLLY	1ST	27.5932	5 556854.85	3634006.44	1027	.45 1	027.45	0	180	90722 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2016_H2S.SUM	H2S	1-HR	HOLLY	1ST	27.2864	1 556878.45	3634006.92	1027	.46 1	027.46	0	160	11205 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2017_H2S.SUM	H2S	1-HR	HOLLY	1ST	26.8926	1 556413.44	3634642.42	1025	.43 1	025.43	0	170	20308 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2020_H2S.SUM	H2S	1-HR	HOLLY	1ST	26.0360	5 556972.87	3634008.83	1027	.38 1	027.38	0	200	11207 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2018_H2S.SUM	H2S	1-HR	NEARBY	1ST	14.7847	4 557200	3633300	1026	.67 1	026.67	0	180	11705 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2020_H2S.SUM	H2S	1-HR	NEARBY	1ST	14.5806	8 556300	3633900	1028	.29 1	028.29	0	201	21320 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2016_H2S.SUM	H2S	1-HR	NEARBY	1ST	14.3889	7 556300	3633900	1028	.29 1	028.29	0	160	11724 Artes		84	3	397
AERM	MOD 21112	Artesia NAAQS_2019_H2S.SUM	H2S	1-HR	NEARBY	1ST	14.2802	6 555800	3634200	102	8.6	1028.6	0	190	10421 Artes		84	3	397
AERN	MOD 21112	Artesia NAAQS_2017_H2S.SUM	H2S	1-HR	NEARBY	1ST	13.9728	2 557600	3633700	1024	.37 1	024.37	0	170	22105 Artes		84	3	397
AERN	MOD 21112	Artesia NAAQS_2016-2020_NO2_ST.SUM	NO2	8TH-HIGHEST MAX DAILY 1	-l ALL	1ST	173.9995	7 556460.99	3635129.21	1025		025.95	051	/EARS	Artesia 2016-2020 (RTP P		48	2	618
AERN	MOD 21112	Artesia NAAQS_2016-2020_NO2_ST.SUM	NO2	8TH-HIGHEST MAX DAILY 1	-ł HOLLY	1ST	138.4380	8 556382.56	3635002.7	1026	.13 1	026.13	051	/EARS	Artesia 2016-2020 (RTP P		48	2	618
AERN	MOD 21112	Artesia NAAQS_2018_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	17.2972		3635129.21	1025		025.95	011	/EARS	Artesia 2016-2020 (RTP P		48	2	134
AERN	IOD 21112	Artesia NAAQS_2019_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	16.4375	1 556460.99	3635129.21	1025		025.95		/EARS			48	2	134
AERN	IOD 21112	Artesia NAAQS_2020_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	16.0442	9 556483.26	3635129.2	1025		025.85	011	/EARS	Artesia 2016-2020 (RTP P		48	2	134
AERN	1OD 21112	Artesia NAAQS_2017_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	15.1158	8 556460.99	3635129.21			025.95	011	/EARS	Artesia 2016-2020 (RTP P		48	2	134
	IOD 21112	Artesia NAAQS_2016_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	13.5668		3635129.2	1025		025.85		/EARS			48	2	134
AERN	IOD 21112	Artesia NAAQS_2018_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	17.2972	7 556460.99	3635129.21	1025	.95 1	025.95	011	/EARS	Artesia 2016-2020 (RTP P		48	2	134
AERN	IOD 21112	Artesia NAAQS_2019_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	16.4375	1 556460.99	3635129.21	1025	.95 1	025.95	011	/EARS	Artesia 2016-2020 (RTP P		48	2	134
	IOD 21112	Artesia NAAQS_2020_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	16.0442	9 556483.26	3635129.2	1025		025.85	011	/EARS	Artesia 2016-2020 (RTP P		48	2	134
AERN	IOD 21112	Artesia NAAQS_2017_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	15.1158	8 556460.99	3635129.21	1025	.95 1	025.95	011	/EARS	Artesia 2016-2020 (RTP P		48	2	134
	1OD 21112	Artesia NAAQS_2016_NO2_LT.SUM	NO2	ANNUAL	HOLLY	1ST	13.5668		3635129.2	1025		025.85		/EARS			48	2	134
	IOD 21112	Artesia NAAQS_2016-2020_PM25_ST.SUM	PM25	8TH-HIGHEST 24-HR	ALL	1ST	18.4273		3635129.2	1025		025.74		/EARS			74	3	218
	1OD 21112	Artesia NAAQS_2016-2020_PM25_ST.SUM	PM25	8TH-HIGHEST 24-HR	HOLLY	1ST	17.8861		3635129.2	1025		025.74		/EARS			74	3	218
	1OD 21112	Artesia NAAQS_2016-2020_PM25_ST.SUM	PM25	8TH-HIGHEST 24-HR	NEARBY	1ST	8.7123			1025		025.55		/EARS			74	3	218
AERN	IOD 21112	Artesia NAAQS_2016-2020_PM25_LT.SUM	PM25	ANNUAL	ALL	1ST	5.5649	9 556505.52	3635129.2	1025	.74 1	025.74	051	/EARS	Artesia 2016-2020 (RTP P		74	3	52
AERN	IOD 21112	Artesia NAAQS_2016-2020_PM25_LT.SUM	PM25	ANNUAL	HOLLY	1ST	4.379	5 556505.52	3635129.2	1025		025.74	051	/EARS	Artesia 2016-2020 (RTP P		74	3	52
			PM25	ANNUAL	NEARBY	1ST	1.8659		3635328.83			025.74		/EARS			74	3	52
AERN	1OD 21112	Artesia NAAQS_2016-2020_SO2_ST.SUM	SO2	4TH-HIGHEST MAX DAILY 1	-ł ALL	1ST	156.7962	6 556300	3634300	1026	.78 1	026.78	051	/EARS	Artesia 2016-2020 (RTP P		48	2	4364
AERN	MOD 21112	Artesia NAAQS_2016-2020_SO2_ST.SUM	SO2	4TH-HIGHEST MAX DAILY 1	-ł HOLLY	1ST	156.7962	6 556300	3634300	1026	.78 1	026.78	051	/EARS	Artesia 2016-2020 (RTP P		48	2	4364

7-7-22 HollyFrontier Artesia NAAQS Model, Significance Gri

	yi Tolitlei Altesia NAAQO iii	outi, eigiiiiteurie	0							
				Modeled		Secondary		NMAAQS/		
				Conc.	Background	PM2.5 Conc.	Total Conc.	NAAQS		
Pollutant	Average	Group	Rank	(ug/m3)	Conc. (ug/m3)	(ug/m3)	(ug/m3)	(ug/m3)	% NMAAQS/NAAQS	Comments
H2S	1-HR	ALL	1ST	28.94	NA	NA	28.9	41.8	69%	Includes off-site source inventory
H2S	1-HR	HOLLY	1ST	28.87	NA	NA	28.9	41.8	69%	
H2S	1-HR	NEARBY	1ST	14.8	NA	NA	14.8	41.8	35%	
NO2	ANNUAL	ALL	1ST	17.3	5.0	NA	22.3	94.02	24%	Oustide Carlsbad monito
NO2	8TH-HIGHEST MAX DAILY	1-ł ALL	1ST	174.0	NA	NA	174.0	188.03	93%	No offsite source inventory required.
PM25	ANNUAL	ALL	1ST	5.56	5.9	0.008	11.5	12.0	96%	Eastern NM monitor.
PM25	ANNUAL	HOLLY	1ST	4.38	5.9	0.008	10	12.0	86%	Includes off-site source inventory
PM25	ANNUAL	NEARBY	1ST	1.87	5.9	0.008	8	12.0	65%	
PM25	8TH-HIGHEST 24-HR	ALL	1ST	18.43	13.4	0.31	32.1	35.0	92%	
PM25	8TH-HIGHEST 24-HR	HOLLY	1ST	17.89	13.4	0.31	31.6	35.0	90%	
PM25	8TH-HIGHEST 24-HR	NEARBY	1ST	8.71	13.4	0.31	22.4	35.0	64%	
SO2	4TH-HIGHEST MAX DAILY	1-ł ALL	1ST	156.8	5.3	NA	162.1	196.4	83%	Bloomfield monitor. There are no offsite SO2 sources within 10km.

NA - Not applicable.
Background concentrations as recommended by the NMAQB.
1-hr NO2 background concentrations from the Carlsbad monitor added within model.
1-hr NO2 background concentrations from the Carlsbad monitor added within model.
1-HoLLY* source group includes only the Artsbar refinery sources.
NO2 modeling included the ARM2 method to account for NOx to NO2 conversion. The default minimum and maximum NO2/NOx ratios of 0.5 and 0.9 were employed.
SO2 24-hr NMAAQS modeling was not conducted as compliance is demonstrated using the 1-hr NAAQS (per NMED policy).

4-22-22 HollyFr	ontier Artesia Increment Model, PTE Assume	d for Holly, Si	gnificance Gri														
Model	File	Pollutant	Average	Group	Rank	Conc/Dep East	(X) N	lorth (Y)	Elev	Hill F	lag 1	ime	Met File	Sources	Groups	Recep	otors
AERMOD 21112	Artesia Increment_2018_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	24.67837	556505.52	3635129.2	1025.74	1025.74	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112		NO2	ANNUAL	ALL	1ST	24.16853	556505.52	3635129.2	1025.74	1025.74		YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment_2020_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	23.67046	556505.52	3635129.2	1025.74	1025.74		YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment_2017_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	23.2157	556505.52	3635129.2	1025.74	1025.74	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment_2016_NO2_LT.SUM	NO2	ANNUAL	ALL	1ST	22.19136	556527.78	3635129.2	1025.58	1025.58	0.1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2018 NO2 LT.SUM	NO2	ANNUAL	HOLLY	1ST	17.21266	556460.99	3635129.21	1025.95	1025.95	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2019 NO2 LT.SUM	NO2	ANNUAL	HOLLY	1ST	16.35653	556460.99	3635129.21	1025.95	1025.95	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2020 NO2 LT.SUM	NO2	ANNUAL	HOLLY	1ST	15.97009	556483.26	3635129.2	1025.85	1025.85	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2017 NO2 LT.SUM	NO2	ANNUAL	HOLLY	1ST	15.04591	556460.99	3635129.21	1025.95	1025.95	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2016 NO2 LT.SUM	NO2	ANNUAL	HOLLY	1ST	13.51191	556483.26	3635129.2	1025.85	1025.85	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2017 NO2 LT.SUM	NO2	ANNUAL	NEARBY	1ST	17.79712	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2016 NO2 LT.SUM	NO2	ANNUAL	NEARBY	1ST	16.83571	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2018 NO2 LT.SUM	NO2	ANNUAL	NEARBY	1ST	16.60564	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2019 NO2 LT.SUM	NO2	ANNUAL	NEARBY	1ST	16.57839	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment 2020 NO2 LT.SUM	NO2	ANNUAL	NEARBY	1ST	15.69278	556600.99	3635413.42	1025.64	1025.64	0 1	YEARS	Artesia 2016-2020 (RTP P		228	3	134
AERMOD 21112	Artesia Increment_2017_SO2_ST.SUM	SO2	24-HR	ALL	2ND	67.11136	556375.48	3635087.04	1026.35	1026.35	0	17040	624 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2019 SO2 ST.SUM	SO2	24-HR	ALL	2ND	65.72592	556527.78	3635129.2	1025.58	1025.58	0	19082	024 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2016 SO2 ST.SUM	SO2	24-HR	ALL	2ND	63.32752	556505.52	3635129.2	1025.74	1025.74	0	16100	824 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2018 SO2 ST.SUM	SO2	24-HR	ALL	2ND	60.36211	556416.47	3635129.21	1026.2	1026.2	0	18100	124 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2020 SO2 ST.SUM	SO2	24-HR	ALL	2ND	60.19588	556483.26	3635129.2	1025.85	1025.85	0	20061	624 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2019 SO2 ST.SUM	SO2	24-HR	HOLLY	2ND	63.5348	556527.78	3635129.2	1025.58	1025.58	0	19082	024 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2018 SO2 ST.SUM	SO2	24-HR	HOLLY	2ND	58.85538	556416.47	3635129.21	1026.2	1026.2	0	18091	724 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2017 SO2 ST.SUM	SO2	24-HR	HOLLY	2ND	57.47117	556375.48	3635087.04	1026.35	1026.35	0	17091	024 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2016 SO2 ST.SUM	SO2	24-HR	HOLLY	2ND	57.27247	556416.47	3635129.21	1026.2	1026.2	0	16072	024 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2020 SO2 ST.SUM	SO2	24-HR	HOLLY	2ND	54.91992	556483.26	3635129.2	1025.85	1025.85	0	20022	124 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2020 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	38.16688	557200	3634100	1025.78	1025.78	0	20022	224 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2019 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	31.71447	555900	3633100	1032.5	1032.5	0	19112	524 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2016 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	31.52081	555900	3635300	1031.49	1031.49	0	16122	324 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2017 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	29.08133	557537.74	3634690.06	1022.56	1022.56	0	17122	024 Artesia 2016-2020 (RTP P		127	3	248
AERMOD 21112	Artesia Increment 2018 SO2 ST.SUM	SO2	24-HR	NEARBY	2ND	25.97896	555800	3635200	1030.06	1030.06	0	18032	624 Artesia 2016-2020 (RTP P		127	3	248

4-22-22 HollyFrontier Artesia Increment Model, PTE Assumed for Holly, Significance Gri

Pollutant	Average	Group	Rank	Modeled Conc. (ug/m3)	Secondary PM2.5 Conc. (ug/m3)	Total Conc. (ug/m3)	Increment (ug/m3)	% Increment	Comments
NO2	ANNUAL	ALL	1ST	24.7	NA	24.7	25	99%	
NO2	ANNUAL	HOLLY	1ST	17.2	NA	17.2	25	69%	
NO2	ANNUAL	NEARBY	1ST	17.8	NA	17.8	25	71%	
SO2	24-HR	ALL	2ND	67.1	NA	67.1	91	74%	
SO2	24-HR	HOLLY	2ND	63.5	NA	63.5	91	70%	
SO2	24-HR	NEARBY	2ND	38.2	NA	38.2	91	42%	

NA - Not applicable.
PM2.5 increment not triggered due to project.

4-22-22 HollyFrontier Artesia TAP Mode

Model	File
AERMOD 21112	Artesia TAP_2017_H2SO4.SUM
AERMOD 21112	Artesia TAP 2020 H2SO4.SUM
AERMOD 21112	Artesia TAP 2016 H2SO4.SUM
AERMOD 21112	Artesia TAP 2018 H2SO4.SUM
AERMOD 21112	Artesia TAP 2019 H2SO4.SUM
AERMOD 21112	Artesia TAP 2020 NH3.SUM
AERMOD 21112	Artesia TAP 2018 NH3.SUM
AERMOD 21112	Artesia TAP 2017 NH3.SUM
AERMOD 21112	Artesia TAP 2019 NH3.SUM
AERMOD 21112	Artesia TAP 2016 NH3.SUM

Pollutant	Average	Group	Rank	Conc/Dep	East (X)	North (Y)	Elev H	Hill I	Flag	Time	e	Met File	Sources	Groups	Recep	ptors
H2SO4	8-HR	ALL	1ST	4.86031	556300	3634900	1026.41	1026.41		0	1702041	6 Artesia 2016-2020 (RTP P		3	1	8341
H2SO4	8-HR	ALL	1ST	4.59695	556575.62	3634197.94	1026.68	1026.68		0	2004031	6 Artesia 2016-2020 (RTP P		3	1	8341
H2SO4	8-HR	ALL	1ST	4.26709	556500	3634200	1026.85	1026.85		0	1601111	6 Artesia 2016-2020 (RTP P		3	1	8341
H2SO4	8-HR	ALL	1ST	4.25832	556300	3634900	1026.41	1026.41		0	1801061	6 Artesia 2016-2020 (RTP P		3	1	8341
H2SO4	8-HR	ALL	1ST	4.11581	556370.4	3634969.47	1026.16	1026.16		0	1911021	6 Artesia 2016-2020 (RTP P		3	1	8341
NH3	8-HR	ALL	1ST	32.28275	556380.79	3635023.79	1026.17	1026.17		0	2011230	8 Artesia 2016-2020 (RTP P		2	1	8341
NH3	8-HR	ALL	1ST	32.01996	556587.86	3634326.98	1026.22	1026.22		0	1811090	8 Artesia 2016-2020 (RTP P		2	1	8341
NH3	8-HR	ALL	1ST	29.49	556400	3634500	1025.86	1025.86		0	1708282	4 Artesia 2016-2020 (RTP P		2	1	8341
NH3	8-HR	ALL	1ST	28.23331	556416.92	3634389.47	1026.21	1026.21		0	1911112	4 Artesia 2016-2020 (RTP P		2	1	8341
NH3	8-HR	ALL	1ST	26.04177	556572.31	3635129.2	1025.36	1025.36		0	1608010	8 Artesia 2016-2020 (RTP P		2	1	8341

4-22-22 HollyFrontier Artesia TAP Mode

Pollutant		Average	Group	Rank	Modeled Conc. (ug/m3)	1/100 OEL(ug/m3)	% Standard
NH3	8-HR		ALL	1ST	32.3	180	18%
H2SO4	8-HR		ALL	1ST	4.9	10	49%

CALPUFF Results (9/6/21)

CALI OTT REsults (5) 0	•	Meteorological	Modeled				
Parameter	Averaging Time	Year Modeled	Value	Modeled Value Units	Standard	% Standard	Comments
AQRV - Visibility	24-hour	2013	2.78	Extinction (%)	5.0	56%	Only Carlsbad Caverns has Q/d > 10.
		2014	1.90	98% (8th high)	5.0	38%	8th high over all receptors, not by receptor, conservatively used.
		2015	2.24		5.0	45%	
SIL - PM10 (PMC)	24-hour	2013	6.66E-02	Concentration (ug/m3)	0.30	22%	Class I SIL
		2014	6.11E-02	(-8,)	0.30	20%	All Class I areas modeled.
		2015	5.78E-02		0.30	19%	
	Annual	2013	7.76E-03		0.20	4%	
	Alliludi	2013	7.76E-03 7.59E-03		0.20	4% 4%	
		2015	8.27E-03		0.20	4% 4%	
		2015	8.27E-U3		0.20	4%	
SIL - SO2	Annual	2013	3.52E-02	Concentration (ug/m3)	0.10	35%	Class I SIL
		2014	3.52E-02		0.10	35%	All Class I areas modeled.
		2015	3.79E-02		0.10	38%	
	24-hour	2013	3.01E-01		0.20	150%	SRU3 at 50 lb/hr.
		2013	1.93E-01		0.20	97%	SRU3 at 28 lb/hr.
		2014	2.70E-01		0.20	135%	SRU3 at 50 lb/hr.
		2014	1.78E-01		0.20	89%	SRU3 at 28 lb/hr.
		2015	2.41E-01		0.20	120%	SRU3 at 50 lb/hr.
		2015	1.56E-01		0.20	78%	SRU3 at 28 lb/hr.
	3-hour	2013	9.45E-01		1.00	95%	
	3 11001	2014	9.82E-01		1.00	98%	
		2015	8.76E-01		1.00	88%	
CII. NO.	Americal	2012	1 005 03	C	0.10	100/	Class I SIL
SIL - NOx	Annual	2013 2014	1.88E-02 1.89E-02	Concentration (ug/m3)	0.10	19% 19%	
					0.10		All Class I areas modeled.
		2015	2.00E-02		0.10	20%	
AQRV	Annual	2013	2.56E-03	Deposition (kg/ha/yr)	0.005	51%	All Class I areas conservatively modeled.
Nitrogen Deposition		2014	2.67E-03		0.005	53%	
		2015	2.87E-03		0.005	57%	
Sulfur Deposition	Annual	2013	3.14E-03		0.005	63%	Used annual SO2 and SO4 emissions.
		2014	3.32E-03		0.005	66%	
		2015	3.77E-03		0.005	75%	



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ATTACHMENT B

Model Summary Results



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